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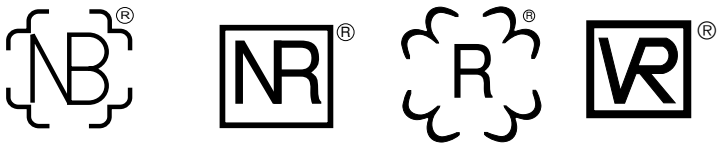
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INTRODUCTION

It is the purpose of the National Board Inspection Code (NBIC) to maintain the integrity of pressure-retaining items by providing rules for installation, and after the items have been placed into service, by providing rules for inspection and repair and alteration, thereby ensuring that these items may continue to be safely used.

The NBIC is intended to provide rules, information, and guidance to manufacturers, Jurisdictions, inspectors, owner-users, installers, contractors, and other individuals and organizations performing or involved in post-construction activities, thereby encouraging the uniform administration of rules pertaining to pressure-retaining items.

SCOPE

The NBIC recognizes three important areas of post-construction activities where information, understanding, and following specific requirements will promote public and personal safety. These areas include:

- Installation
- Inspection
- Repairs and Alterations

The NBIC provides rules, information, and guidance for post-construction activities, but does not provide details for all conditions involving pressure-retaining items. Where complete details are not provided in this code, the code user is advised to seek guidance from the Jurisdiction and from other technical sources.

The words shall, should, and may are used throughout the NBIC and have the following intent:

- Shall – action that is mandatory and required.
- Should – indicates a preferred but not mandatory means to accomplish the requirement unless specified by others such as the Jurisdiction.
- May – permissive, not required or a means to accomplish the specified task.

ORGANIZATION

The NBIC is organized into three parts to coincide with specific post-construction activities involving pressure-retaining items. Each part provides general and specific rules, information, and guidance within each applicable post-construction activity. Other NBIC parts or other published standards may contain additional information or requirements needed to meet the rules of the NBIC. Specific references are provided in each part to direct the user where to find this additional information. NBIC parts are identified as:

- Part 1, Installation – This part provides requirements and guidance to ensure all types of pressure-retaining items are installed and function properly. Installation includes meeting specific safety criteria for construction, materials, design, supports, safety devices, operation, testing, and maintenance.
- Part 2, Inspection – This part provides information and guidance needed to perform and document inspections for all types of pressure-retaining items. This part includes information on personnel safety, non-destructive examination, tests, failure mechanisms, types of pressure equipment, fitness for service, risk-based assessments, and performance-based standards.
- Part 3, Repairs and Alterations – This part provides information and guidance to perform, verify, and document acceptable repairs or alterations to pressure-retaining items regardless of code of construction. Alternative methods for examination, testing, heat treatment, etc., are provided when the original code of construction requirements cannot be met. Specific acceptable and proven repair methods are also provided.

Each NBIC part is divided into major sections as outlined in the Table of Contents.

Tables, charts, and figures provide relevant illustrations or supporting information for text passages, and are designated with numbers corresponding to the paragraph they illustrate or support within each section. Multiple tables, charts, or figures referenced by the same paragraph will have additional letters reflecting the order of reference. Tables, charts, and figures are located in or after each major section within each NBIC part.

TEXT IDENTIFICATION AND NUMBERING

Each page in the text will be designated in the top header with the publication's name, part number, and part title. The numbering sequence for each section begins with the section number followed by a dot to further designate major sections (e.g., 1.1, 1.2, 1.3). Major sections are further subdivided using dots to designate subsections within that major section (e.g., 1.1.1, 1.2.1, 1.3.1). Subsections can further be divided as necessary. Paragraphs under sections or subsections shall be designated with small letters in parenthesis (e.g., a), b), c)) and further subdivided using numbers in parenthesis (e.g., 1), 2), 3)).

Subdivisions of paragraphs beyond this point will be designated using a hierarchical sequence of letters and numbers followed by a dot.

Example: 2.1 Major Section
2.1.1 Section
2.1.2 Section
2.1.2. Subsection
a) paragraph
b) paragraph
1) subparagraph
2) subparagraph
a. subdivisions
1. subdivisions
2. subdivisions
b. subdivisions
1. subdivisions
2. subdivisions

Tables and figures will be designated with the referencing section or subsection identification. When more than one table or figure is referenced in the same section or subsection, letters or numbers in sequential order will be used following each section or subsection identification.

SUPPLEMENTS

Supplements are contained in each part of the NBIC to provide rules, information, and guidance only pertaining to a specific type of pressure-retaining item (e.g., Locomotive Boilers, Historical Boilers, Graphite Pressure Vessels.) Supplements follow the same numbering system used for the main text only preceded by the Letter "S." Each page of the supplement will be tabbed to identify the supplement number.

EDITIONS

Editions, which include revisions and additions to this code, are published every two years. Editions are permissive on the date issued and become mandatory six months after the date of issue.

INTERPRETATIONS

On request, the NBIC Committee will render an interpretation of any requirement of this code. Interpretations are provided for each part and are specific to the code edition and addenda referenced in the interpretation. Interpretations provide clarification of existing rules in the code only and are not part of this code.

JURISDICTIONAL PRECEDENCE

Reference is made throughout this code to the requirements of the "Jurisdiction." Where any provision herein presents a direct or implied conflict with any jurisdictional regulation, the Jurisdictional regulation shall govern.

UNITS OF MEASUREMENT

Both U.S. customary units and metric units are used in the NBIC. The value stated in U.S. customary units or metric units are to be regarded separately as the standard. Within the text, the metric units are shown in

parentheses. In Part 2, Supplement 6 and Part 3, Supplement 6 regarding DOT Transport Tanks, the metric units are shown first with the U.S. customary units shown in parentheses.

U.S. customary units or metric units may be used with this edition of the NBIC, but one system of units shall be used consistently throughout a repair or alteration of pressure-retaining items. It is the responsibility of National Board accredited repair organizations to ensure the appropriate units are used consistently throughout all phases of work. This includes materials, design, procedures, testing, documentation, and stamping. The NBIC policy for metrication is outlined in each part of the NBIC.

ACCREDITATION PROGRAMS

The National Board administers and accredits three specific repair programs[1] as shown below:

"**R**"…….Repairs and Alterations to Pressure-Retaining Items
"**VR**"……..Repairs to Pressure Relief Valves
"**NR**"……..Repair and Replacement Activities for Nuclear Items

Part 3, Repairs and Alterations, of the NBIC describes the administrative requirements for the accreditation of these repair organizations.

The National Board also administers and accredits four specific inspection agency programs as shown below:

New Construction
Criteria for Acceptance of Authorized Inspection Agencies for New Construction (NB-360)

Inservice
Qualifications and Duties for Authorized Inspection Agencies (AIAs) Performing Inservice Inspection Activities and Qualifications for Inspectors of Boilers and Pressure Vessels (NB-369)

Owner-User
Accreditation of Owner-User Inspection Organizations (OUIO) (NB-371) Owners or users may be accredited for both a repair and inspection program provided the requirements for each accreditation program are met.

Federal Government
Qualifications and Duties for Federal Inspection Agencies Performing Inservice Inspection Activities (FIAs) (NB-390)

These programs can be viewed on the National Board Website at www.nationalboard.org. For questions or further information regarding these programs contact the National Board by phone at (614) 888-8320 or by fax at (614) 847-1828

CERTIFICATES OF AUTHORIZATION FOR ACCREDITATION PROGRAMS

Any organization seeking an accredited program may apply to the National Board to obtain a Certificate of Authorization for the requested scope of activities. A confidential review shall be conducted to evaluate the organization's quality system. Upon completion of the evaluation, a recommendation will be made to the National Board regarding issuance of a Certificate of Authorization.

Certificate of Authorization scope, issuance, and revisions for National Board accreditation programs are specified in the applicable National Board procedures. When the quality system requirements of the appropriate accreditation program have been met, a Certificate of Authorization and appropriate National Board symbol stamp shall be issued.

1 Caution, some Jurisdictions may independently administer a program of authorization for organizations to perform repairs and alterations within that Jurisdiction.

FOREWORD

The National Board of Boiler and Pressure Vessel Inspectors is an organization comprised of Chief Inspectors for the states, cities, and territories of the United States and provinces and territories of Canada. It is organized for the purpose of promoting greater safety to life and property by securing concerted action and maintaining uniformity in post-construction activities of pressure-retaining items, thereby ensuring acceptance and interchangeability among Jurisdictional authorities responsible for the administration and enforcement of various codes and standards.

In keeping with the principles of promoting safety and maintaining uniformity, the National Board originally published the NBIC in 1946, establishing rules for inspection and repairs to boilers and pressure vessels. The National Board Inspection Code (NBIC) Committee is charged with the responsibility for maintaining and revising the NBIC. In the interest of public safety, the NBIC Committee decided, in 1995, to revise the scope of the NBIC to include rules for installation, inspection, and repair or alteration to boilers, pressure vessels, piping, and nonmetallic materials.

In 2007, the NBIC was restructured into three parts specifically identifying important post-construction activities involving safety of pressure-retaining items. This restructuring provides for future expansion, transparency, uniformity, and ultimately improving public safety.

The NBIC Committee's function is to establish rules of safety governing post-construction activities for the installation, inspection, and repair and alteration of pressure-retaining items, and to interpret these rules when questions arise regarding their intent. In formulating the rules, the NBIC Committee considers the needs and concerns of individuals and organizations involved in the safety of pressure-retaining items. The objective of the rules is to afford reasonably certain protection of life and property, so as to give a reasonably long, safe period of usefulness. Advancements in design and material and the evidence of experience are recognized.

The rules established by the NBIC Committee are not to be interpreted as approving, recommending, or endorsing any proprietary or specific design, or as limiting in any way an organization's freedom to choose any method that conforms to the NBIC rules.

The NBIC Committee meets regularly to consider revisions of existing rules, formulation of new rules, and respond to requests for interpretations. Requests for interpretation must be addressed to the NBIC Secretary in writing and must give full particulars in order to receive Committee consideration and a written reply. Proposed revisions to the code resulting from inquiries will be presented to the NBIC Committee for appropriate action.

Proposed revisions to the code approved by the NBIC Committee are submitted to the American National Standards Institute and published on the National Board web-site to invite comments from all interested persons. After the allotted time for public review and final approval, the new edition is published.

Organizations or users of pressure-retaining items are cautioned against making use of revisions that are less restrictive than former requirements without having assurance that they have been accepted by the Jurisdiction where the pressure-retaining item is installed.

The general philosophy underlying the NBIC is to parallel those provisions of the original code of construction, as they can be applied to post-construction activities.

The NBIC does not contain rules to cover all details of post-construction activities. Where complete details are not given, it is intended that individuals or organizations, subject to the acceptance of the Inspector and Jurisdiction when applicable, provide details for post-construction activities that will be as safe as otherwise provided by the rules in the original code of construction.

Activities not conforming to the rules of the original code of construction or the NBIC must receive specific approval from the Jurisdiction, who may establish requirements for design, construction, inspection, testing, and documentation.

There are instances where the NBIC serves to warn against pitfalls; but the code is not a handbook, and cannot substitute for education, experience, and sound engineering judgment.

It is intended that this edition of the NBIC not be retroactive. Unless the Jurisdiction imposes the use of an earlier edition, the latest effective edition is the governing document.

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PART 2, SECTION 1
INSPECTION — GENERAL REQUIREMENTS FOR INSERVICE INSPECTION OF PRESSURE-RETAINING ITEMS

1.1 SCOPE

This section provides general guidelines and requirements for conducting inservice inspection of pressure-retaining items. Appropriately, this section includes precautions for the safety of inspection personnel. The safety of the public and the Inspector is the most important aspect of any inspection activity.

1.2 ADMINISTRATION

Jurisdictional requirements describe the frequency, scope, type of inspection, whether internal, external, or both, and type of documentation required for the inspection. The Inspector shall have a thorough knowledge of jurisdictional regulations where the item is installed, as jurisdictional or regulatory inspection requirements do vary.

1.3 REFERENCE TO OTHER CODES AND STANDARDS

Other existing inspection codes, standards, and practices pertaining to the inservice inspection of pressure-retaining items can provide useful information and references relative to the inspection techniques listed in this part. Use of these codes, standards, and practices are subject to review and acceptance by the Inspector, and when required by the Jurisdiction. Any inconsistency or discrepancy between the requirements of the NBIC and these inspection codes, standards, and practices shall be resolved by giving precedence to requirements in the following order:

a) The requirements of the Jurisdiction having authority.

b) The requirements of the NBIC supersede general and specific requirements of other inspection codes, standards, and practices.

c) The general and specific requirements of the references to other codes and standards listed herein that are recognized and generally accepted good engineering practices.

Some examples are as follows:

a) National Board *Bulletin* - National Board Classic Articles Series

b) American Society of Mechanical Engineers - *ASME Boiler and Pressure Vessel Code Section V* (Nondestructive Examination)

c) American Society of Mechanical Engineers - *ASME Boiler and Pressure Vessel Code Section VI* (Recommended Rules for the Care and Operation of Heating Boilers) this section when performing inspections of heating boilers. There may be occasions where more detailed procedures will be required.

d) American Society of Mechanical Engineers- *ASME Boiler and Pressure Vessel Code Section VII* (Recommended Guidelines for the Care of Power Boilers)

e) American Society of Mechanical Engineers -*ASME B31G* (Manual for Determining the Remaining Strength of Corroded Pipelines)

f) American Society of Mechanical Engineers - *ASME PCC-1* (Guidelines for Pressure Boundary Bolted Joint Assembly)

g) American Society of Mechanical Engineers - *ASME PCC-2* (Repair of Pressure Equipment and Piping)

h) American Society of Mechanical Engineers - *ASME CRTD Volume 41,* Risk-Based Inspection for Equipment Life Management: An Application Handbook

i) American Petroleum Institute/American Society of Mechanical Engineers - *API 579-1/ASME FFS-I* (Fitness-For-Service)

j) American Petroleum Institute – *API-510* (Pressure Vessel Inspection Code: In-service Inspection, Rating, Repair and Alteration)

k) American Petroleum Institute - API 570 (Piping Inspection Code: In-Service Inspection, Rating, Repair and Alteration of Piping Systems)

l) American Petroleum Institute - *API 572* (Inspection of Pressure Vessels)

m) American Petroleum Institute - API 574 (Inspection Practices for Piping System Components)

n) American Petroleum Institute - *API 576* (Inspection of Pressure-Relieving Devices)

o) American Petroleum Institute - *Recommended Practice 580* (Risk Based Inspection)

p) American Petroleum Institute - *Recommended Practice* 581 (Base Resource Document on Risk-Based Inspection)

q) Institute of Petroleum - *Model Code of Safe Practice in the Petroleum Industry Part 12 ,* Pressure Vessel Examination

r) Institute of Petroleum - *Model Code of Safe Practice in the Petroleum Industry Part 13,* (Pressure Piping Systems Examination)

s) Australian Standard - *AS 1210* (Unfired Pressure Vessel Code)

t) Australian Standard - *AS* 4343 (Pressure equipment - Hazard levels)

u) Alberta Boilers Safety Association - *AB-506* (Pressure Equipment Inspection and Servicing Requirements)

1.4 PERSONNEL SAFETY

a) Personnel safety is the joint responsibility of the owner or user and the Inspector. All applicable safety regulations shall be followed. This includes federal, state, regional, and/or local rules and regulations. owner or user programs, safety programs of the Inspector's employer, or similar standards also apply. In the absence of such rules, prudent and generally accepted engineering safety procedures satisfactory to the Inspector shall be employed by the owner or user.

b) Inspectors are cautioned that the operation of safety devices involves the discharge of fluids, gases, or vapors. Extreme caution should be used when working around these devices due to hazards to personnel. Suitable hearing protection should be used during testing because extremely high noise levels can damage hearing.

c) Inspectors shall take all safety precautions when examining equipment. Proper personal protective equipment shall be worn, equipment shall be locked out, blanked off, decontaminated, and confined space entry permits obtained before internal inspections are conducted. In addition, Inspectors shall comply with plant safety rules associated with the equipment and area in which they are inspecting. Inspectors are also cautioned that a thorough decontamination of the interior of vessels is sometimes

very hard to obtain and proper safety precautions must be followed to prevent contact or inhalation injury with any extraneous substance that may remain in the tank or vessel.

1.4.1 PERSONAL SAFETY REQUIREMENTS FOR ENTERING CONFINED SPACES

a) No pressure-retaining item shall be entered until it has been properly prepared for inspection. The owner or user and Inspector shall jointly determine that pressure-retaining items may be entered safely. This shall include:

   1) Recognized hazards associated with entry into the object have been identified by the owner or user and are brought to the attention of the Inspector, along with acceptable means or methods for eliminating or minimizing each of the hazards;

   2) Coordination of entry into the object by the Inspector and owner or user representative(s) working in or near the object;

   3) Personal protective equipment required to enter an object shall be used. This may include, among other items, protective outer clothing, gloves, respiratory protection, eye protection, foot protection, and safety harnesses. The Inspector shall have the proper training governing the selection and use of any personal protective clothing and equipment necessary to safely perform each inspection. Particular attention shall be afforded respiratory protection if the testing of the atmosphere of the object reveals any hazards;

   4) Completing and posting of confined space entry permits, as applicable; and

   5) An effective energy isolation program (lock out and/or tag out) is in place and in effect that will prevent the unexpected energizing, start-up, or release of stored energy.

b) The Inspector shall determine that a safe atmosphere exists before entering the pressure-retaining item. The atmosphere shall be verified by the owner or user as directed by the Inspector.

   1) The oxygen content of the breathable atmosphere shall be between 19.5% and 23.5%.

   2) If any flammable or combustible materials are present in the atmosphere they shall not exceed 10% of their Lower Explosive Limit (LEL) or Lower Flammable Limit (LFL).

   3) The Inspector shall not enter an area if toxic, flammable or inert gases, vapors or dusts are present and above acceptable limits.

1.4.2 EQUIPMENT OPERATION

The Inspector shall not operate owner or user equipment. Operation shall be conducted only by competent owner or user employees familiar with the equipment and qualified to perform such tasks.

1.5 INSPECTION ACTIVITIES

A proper inspection of a pressure-retaining item requires many pre-inspection planning activities including: safety considerations, an inspection plan that considers the potential damage mechanisms, selection of appropriate inspection methods, and awareness of the jurisdictional requirements. This Section describes pre-inspection and post-inspection activities applicable to all pressure-retaining items. Specific inspection requirements for pressure-retaining items are identified in NBIC Part 2, 2.2 for boilers, 2.3 for pressure vessels, 2.4 for piping and piping systems, and 2.5 for pressure relief devices.

1.5.1 INSERVICE INSPECTION ACTIVITIES

Any defect or deficiency in the condition, operating, and maintenance practices of a boiler, pressure vessel, piping system, and pressure relief devices noted by the Inspector shall be discussed with the owner or user at the time of inspection and recommendations made for the correction of such defect or deficiency shall be documented. Use of a checklist to perform inservice inspections is recommended.

1.5.2 PRE-INSPECTION ACTIVITIES

a) Prior to conducting the inspection, a review of the known history of the pressure-retaining item and a general assessment of current conditions shall be performed. This shall include a review of information such as:

   1) Date of last inspection;

   2) Current jurisdictional inspection certificate;

   3) ASME Code Symbol Stamping or mark of code of construction;

   4) National Board and/or jurisdiction registration number;

   5) Operating conditions and normal contents of the vessel (discuss any unique hazards with the owner Previous inspection report, operating/maintenance logs and test records, and any outstanding recommendations from the previous inspection);

   6) Records of wall thickness checks, especially where corrosion or erosion is a consideration;

   7) Review of repairs or alterations and any associated records for compliance with applicable requirements; and

   8) Observation of the condition of the overall complete installation, including maintenance and operation records.

b) The following activities should be considered to support the inspection:

   1) Removal of pressure gages or other devices for testing and calibration; and

   2) Accessibility to inspect and test each pressure-retaining item and its appurtenances.

1.5.2.1 INSPECTION PLANNING

An inspection plan should be developed to better ensure continued safe operation of a pressure-retaining item (PRI).

A formal inspection plan is a document providing the scope of inspection activities necessary to determine if in-service damage has occurred. The plan identifies methods of examination, qualifications of examiners, and frequency of examination necessary to ensure PRI is suitable for continued service. It may provide a time interval for external and internal inspection as well as describe methods of repair and maintenance for a PRI.

A plan may include the following, as appropriate for a PRI:

a) The known or expected failure mechanisms that affect the specific equipment. See NBIC Part 2, 3.3 *Corrosion*, 3.4 *Failure Mechanisms*, and 4.4.6 *Identification of Damage Mechanisms* for examples;

b) The extent and locations of NDE methods and inspections required to detect and evaluate the failure mechanisms. See NBIC Part 2, Section 4 for examples;

c) The necessary corrosion and erosion monitoring activities such as NDE surveys and changes in process conditions;

d) The preparation required to accomplish the examination and inspection activities; and/or

e) The projected time interval for the inspection and evaluation activities. See NBIC Part 2, 4.4.7 *Determining Inspection Intervals* and 4.4.8 *Evaluating Inspection Intervals of Pressure Retaining Items Exposed to Inservice Failure Mechanisms*.

Recent operating history (e.g., process upsets or process changes or operating excursions) and management of change records should be reviewed during preparation of the inspection plan.

Industry standards may be used to prepare an inspection plan. A plan may be a simple single document or may be complex, having numerous documents. Risk-Based Assessment may be included in a plan. See 4.5 *Risk-Based Assessment Programs*.

Once a plan has been implemented, deferral of scheduled inspection or assessment activities specified in the plan is to be avoided. Any deviation from the planned intervals or inspection activities needs to be justified and documented. Additional monitoring of the PRI during a deferral period may be employed to better ensure safe PRI operation until the planned activity can be completed.

1.5.3 PREPARATION FOR INTERNAL INSPECTION

The owner or user has the responsibility to prepare a pressure-retaining item for internal inspection. Requirements of occupational safety and health regulations (i.e., federal, state, local, or other), as well as the owner-user's own program and the safety program of the Inspector's employer are applicable. The pressure-retaining item should be prepared in the following manner or as deemed necessary by the Inspector:

a) When a vessel is connected to a common header with other vessels or in a system where liquids or gases are present, the vessel shall be isolated by closing, locking, and/or tagging stop valves in accordance with the owner's or user's procedures. When toxic or flammable materials are involved, additional safety precautions may require removing pipe sections or blanking pipelines before entering the vessel. The means of isolating the vessel shall be in compliance with applicable occupational safety and health regulations and procedures. For boilers or fired pressure vessels, the fuel supply and ignition system shall be locked out and/or tagged out, in accordance with the owner's or user's procedures;

b) The vessel temperature shall be allowed to cool or warm at a rate to avoid damage to the vessel. When a boiler is being prepared for internal inspection, the water should not be withdrawn until it has been sufficiently cooled at a rate to avoid damage;

c) The vessel shall be drained of all liquid and shall be purged of any toxic or flammable gases or other contaminants that were contained in the vessel. The continuous use of mechanical ventilation using a fresh air blower or fan may be necessary to maintain the vessel's atmosphere within acceptable limits. During air purging and ventilation of vessels containing flammable gases, the concentration of vapor in air may pass through the flammable range before a safe atmosphere is obtained. All necessary precautions shall be taken to eliminate the possibility of explosion or fire;

d) Items requested by the Inspector, such as manhole and handhole plates, washout plugs, inspection plugs, and any other items shall be removed;

e) The Inspector shall not enter a vessel until all safety precautions have been taken. The temperature of the vessel shall be such that the inspecting personnel will not be exposed to excessive heat. Vessel surfaces should be cleaned as necessary so as to preclude entrant exposure to any toxic or hazardous materials;

f) If requested by the Inspector or required by regulation or procedure, a responsible attendant shall remain outside the vessel at the point of entry while the Inspector is inside and shall monitor activity inside and outside and communicate with the Inspector as necessary. The attendant shall have a means of summoning rescue assistance, if needed, and to facilitate rescue procedures for all entrants without personally entering the vessel.

Note: If a vessel has not been properly prepared for an internal inspection, the Inspector shall decline to make the inspection.

1.5.4 POST-INSPECTION ACTIVITIES

a) During any inspections or tests of pressure-retaining items, the actual operating and maintenance practices should be noted by the Inspector and a determination made as to their acceptability.

b) Any defects or deficiencies in the condition, operating, and maintenance practices of the pressure-retaining item shall be discussed with the owner or user at the time of inspection and recommendations made for correction. Follow-up inspections should be performed as needed to determine if deficiencies have been corrected satisfactorily.

c) Documentation of inspection shall contain pertinent data such as description of item, classification, identification numbers, inspection intervals, date inspected, type of inspection, and test performed, and any other information required by the inspection agency, jurisdiction, and/or owner or user. The Inspector shall sign, date, and note any deficiencies, comments, or recommendations on the inspection report. The Inspector should retain and distribute copies of the inspection report, as required.

d) The form and format of the inspection report shall be as required by the Jurisdiction. Where no Jurisdiction exists, forms NB-5, NB-6, or NB-7 (see NBIC Part 2, 5.3) or any other form(s) required by the inspection agency or owner or user may be used as appropriate.

1.6 CHANGE OF SERVICE (15)

Supplement 9 of this part provides requirements and guidelines to be followed when a change of service or service type is made to a pressure-retaining item.

Whenever there is a change of service, the Jurisdiction where the pressure-retaining item is to be operated, shall be notified for acceptance, when applicable. Any specific jurisdictional requirements shall be met.

PART 2, SECTION 2
INSPECTION — DETAILED REQUIREMENTS FOR INSERVICE INSPECTION OF PRESSURE-RETAINING ITEMS

2.1 SCOPE

a) This section describes general and detailed inspection requirements for pressure-retaining items to determine corrosion deterioration and possible prevention of failures for boilers, pressure vessels, piping, and pressure relief devices.

b) Materials to be inspected shall be suitably prepared so that surface irregularities will not be confused with or mask any defects. Material conditioning such as cleaning, buffing, wire brushing, or grinding may be required by procedure or, if requested, by the Inspector. The Inspector may require insulation or component parts to be removed.

2.2 BOILERS

2.2.1 SCOPE

This section provides guidelines for external and internal inspection of boilers used to contain pressure. This pressure may be obtained from an external source or by the application of heat from a direct or indirect source or a combination thereof.

2.2.2 SERVICE CONDITIONS

a) Boilers are designed for a variety of service conditions. The temperature and pressure at which they operate should be considered in establishing inspection criteria. This part is provided for guidance of a general nature. There may be occasions where more detailed procedures will be required.

b) The condition of the complete installation, including maintenance and operation, can often be used by the Inspector as a guide in forming an opinion of the care given to the boiler.

c) Usually the conditions to be observed by the Inspector are common to both power and heating boilers; however, where appropriate, the differences are noted.

2.2.3 PRE-INSPECTION ACTIVITIES

A review of the known history of the boiler shall be performed. This shall include a review of information contained in NBIC Part 2, 1.5.2, and other items listed in NBIC Part 2, 2.2.4.

2.2.4 CONDITION OF BOILER ROOM OR BOILER LOCATION

The general condition of the boiler room or boiler location should be assessed using appropriate jurisdictional requirements and overall engineering practice. Items that are usually considered are lighting, adequacy of ventilation for habitability, combustion air, housekeeping, personal safety, and general safety considerations.

2.2.5 EXTERNAL INSPECTION

The external inspection of a boiler is made to determine if it is in a condition to operate safely. Some items to consider are:

a) The boiler fittings, valves, and piping should be checked for compliance with ASME Code or other standards or equivalent requirements. Particular attention should be paid to pressure relief devices and other safety controls;

b) Firing equipment controls;

c) Adequacy of structure, boiler supports, and any associated support steel;

d) Boiler casing should be free from cracks, combustion gas or fluid leaks, excessive corrosion or other degradation that could interfere with proper operation;

e) Soot blowers, valves, and actuating mechanisms;

f) Gaskets on observation doors, access doors, drums, handhole and manhole covers and caps;

g) Valves and actuators, either chains, motors, and/or handwheels; and

h) Leakage of fluids or combustion gases.

2.2.6 INTERNAL INSPECTION

a) When a boiler is to be prepared for internal inspection, the water shall not be withdrawn until the setting has been sufficiently cooled at a rate to avoid damage to the boiler as well as additional preparations identified in NBIC Part 2, 1.4.1 and 1.5.3.

b) The owner or user shall prepare a boiler for internal inspection in the following manner:

   1) Before opening the manhole(s) and entering any part of the boiler that is connected to a common header with other boilers, the required steam or water system stop valves (including bypass) must be closed, locked out, and/or tagged in accordance with the owner or user's procedures, and drain valves or cocks between the two closed stop valves be opened. After draining the boiler, the blowoff valves shall be closed, locked out, and/or tagged out in accordance with the owner-user's procedures. Alternatively, lines may be blanked or sections of pipe removed. Blowoff lines, where practicable, shall be disconnected between pressure parts and valves. All drains and vent lines shall be open.

   2) The Inspector shall review all personnel safety requirements as outlined in NBIC Part 2, 1.4 prior to entry.

      Note: If a boiler has not been properly prepared for an internal inspection, the Inspector shall decline to make the inspection.

2.2.7 EVIDENCE OF LEAKAGE

a) It is not normally necessary to remove insulating material, masonry, or fixed parts of a boiler for inspection, unless defects or deterioration are suspected or are commonly found in the particular type of boiler being inspected. Where there is evidence of leakage showing on the covering, the Inspector shall have the covering removed in order that a thorough inspection of the area may be made. Such inspection may require removal of insulating material, masonry, or fixed parts of the boiler.

b) For additional information regarding a leak in a boiler or determining the extent of a possible defect, a pressure test may be performed per NBIC Part 2, 4.3.1.

2.2.8 BOILER CORROSION CONSIDERATIONS

a) Corrosion causes deterioration of the metal surfaces. It can affect large areas, or it can be localized in the form of pitting. Isolated, shallow pitting is not considered serious if not active.

b) The most common causes of corrosion in boilers are the presence of free oxygen and dissolved salts in the feedwater. Where active corrosion is found, the Inspector should advise the owner or user to obtain competent advice regarding proper feedwater treatment.

c) For the purpose of estimating the effect of severe corrosion over large areas on the safe working pressure, the thickness of the remaining sound metal should be determined by ultrasonic examination or by drilling.

d) Grooving is a form of metal deterioration caused by localized corrosion and may be accelerated by stress concentration. This is especially significant adjacent to riveted joints.

e) All flanged surfaces should be inspected, particularly the flanges of unstayed heads. Grooving in the knuckles of such heads is common since there is slight movement in heads of this design, which causes a stress concentration.

f) Some types of boilers have ogee or reversed-flanged, construction which is prone to grooving and may not be readily accessible for examination. The Inspector should insert a mirror through an inspection opening to examine as much area as possible. Other means of examination, such as the ultrasonic method, may be employed.

g) Grooving is usually progressive and when it is detected, its effect should be carefully evaluated and corrective action taken.

h) Pitting and corrosion on the waterside surfaces of the tubes should be examined. In vertical firetube boilers, excessive corrosion and pitting is often noted at and above the water level.

2.2.9 WATERSIDE DEPOSITS

a) All accessible surfaces of the exposed metal on the waterside of the boiler should be inspected for deposits caused by water treatment, scale, oil, or other substances. Oil or scale in the tubes of watertube boilers is particularly detrimental since this can cause an insulating effect resulting in overheating, weakening, possible metal fatigue, bulging, or rupture.

b) Excessive scale or other deposits should be removed by chemical or mechanical means.

2.2.10 INSPECTION OF BOILER PIPING, PARTS, AND APPURTENANCES

2.2.10.1 BOILER PIPING

Piping should be inspected in accordance with NBIC Part 2, 2.4.

2.2.10.2 FLANGED OR OTHER CONNECTIONS

a) The manhole and reinforcing plates, as well as nozzles or other connections flanged or bolted to the boiler, should be examined for evidence of defects both internally and externally. Whenever possible, observation should be made from both sides, internally and externally, to determine whether connections are properly made to the boiler.

b) All openings leading to external attachments, such as water column connections, low-water fuel cutoff devices, openings in dry pipes, and openings to safety valves, should be examined to ensure they are free from obstruction.

2.2.10.3 MISCELLANEOUS

a) The piping to the water column should be carefully inspected to ensure that water cannot accumulate in the steam connection. The position of the water column should be checked to determine that the column is placed in accordance with the original code of construction or jurisdictional requirements.

b) The gas side baffling should be inspected. Absence of proper baffling or defective baffling can cause high temperatures and overheat portions of the boiler. The location and condition of combustion arches should be checked for evidence of flame impingement, which could result in overheating.

c) Any localization of heat caused by improper or defective installation or improper operation of firing equipment shall be corrected before the boiler is returned to service.

d) The refractory supports and settings should be carefully examined, especially at points where the boiler structure comes near the setting walls or floor, to ensure that deposits of ash or soot will not bind the boiler and produce excessive strains on the structure due to the restriction of movement of the parts under operating conditions.

e) When tubes have been re-rolled or replaced, they should be inspected for proper workmanship. Where tubes are readily accessible, they may have been overrolled. Conversely, when it is difficult to reach the tube ends, they may have been underrolled.

f) Valves should be inspected on boiler feedwater, blowdown, drain, and steam systems for gland leakage, operability, tightness, handle or stem damage, body defects, and general corrosion.

2.2.10.4 GAGES

a) Ensure that the water level indicated is correct by having the gage tested as follows:

   1) Close the lower gage-glass valve, then open the drain cock and blow the glass clear;

   2) Close the drain cock and open the lower gage-glass valve. Water should return to the gage-glass immediately;

   3) Close the upper gage glass valve, then open the drain cock and allow the water to flow until it runs clean;

   4) Close the drain cock and open the upper gage-glass valve. Water should return to the gage-glass immediately; and

   5) If the water return is sluggish, the test should be discontinued. A sluggish response could indicate an obstruction in the pipe connections to the boiler. Any leakage at these fittings should be promptly corrected to avoid damage to the fittings or a false waterline indication.

b) Unless there is other information to assess their accuracy or reliability, all the pressure gages shall be removed, tested, and their readings compared to the readings of a calibrated standard test gage or a dead weight tester.

c) The location of a steam pressure gage should be noted to determine whether it is exposed to high temperature from an external source or to internal heat due to lack of protection by a proper siphon or trap. The Inspector should check that provisions are made for blowing out the pipe leading to the steam gage.

d) The Inspector should observe the pressure gage reading during tests; for example, the reduction in pressure when testing the low-water fuel cutoff control or safety valve on steam boilers. Defective gages shall be replaced.

2.2.10.5 PRESSURE RELIEF DEVICES

See NBIC Part 2, 2.5 for the inspection of safety devices (e.g., pressure relief valves) used to prevent over-pressure of boilers.

2.2.10.6 CONTROLS

Establishing proper operation and maintenance of controls and safety devices is essential to safe boiler operation. Owners or users are responsible for establishing and implementing management programs which will ensure such action is taken. In addition, any repairs to controls and safety devices must only be made by qualified individuals or organizations. Documentation of compliance with these management systems and repairs is an essential element of demonstrating the effectiveness of such systems.

When required by the Jurisdiction, the following guidelines are provided to aid in the evaluation of installed operating control devices:

a) Verify that the burner is labeled and listed by a recognized testing agency, that piping and wiring diagrams exist, that commissioning tests have been conducted and that a contractor/manufacturer's installation report has been completed and is available for review.

b) Verify that the owner or user has established function tests, inspection requirements, maintenance and testing of all controls and safety devices in accordance with manufacturer's recommendations. Verify that these activities are conducted at assigned intervals in accordance with a written procedure, that non-conformances which impact continued safe operation of the boiler are corrected, and that the results are properly documented. These activities shall be conducted at a frequency recommended by the manufacturer or the frequency required by the jurisdiction. Where no frequencies are recommended or prescribed, the activity should be conducted at least annually.

   Where allowed by the jurisdiction, Performance Evaluation may be used to increase or decrease the frequencies based on document review and approval by an appropriate engineer.

c) Verify that combustion air is supplied to the boiler room as required by the jurisdiction or if no jurisdictional requirements exist see NBIC, Part 1, 2.4.5 and 3.5.4 for additional guidance.

d) Verify that a manually operated remote boiler emergency stop button exists at each boiler room exit door, when required by the jurisdiction.

e) Verify operation of low water protection devices by observing the blowdown of these controls or the actual lowering of boiler water level under carefully controlled conditions with the burner operating. This test should shut off the heat source to the boiler. The return to normal condition such as the restart of the burner, the silencing of an alarm, or stopping of a feed pump should be noted. A sluggish response could indicate an obstruction in the connections to the boiler.

f) The operation of a submerged low-water fuel cutoff mounted directly in a steam boiler shell should be tested by lowering the boiler water level carefully. This should be done only after being assured that the water level gage glass is indicating correctly.

g) On a high-temperature water boiler, it is often not possible to test the control by cutoff indication, but where the control is of the float type, externally mounted, the float chamber should be drained to check for the accumulation of sediment.

(15) h) On forced circulation boilers, the flow sensing device shall be tested to verify that the burner will shut down the boiler on a loss of flow.

i) On electric boilers, it should be verified that the boiler is protected from a low water condition either by construction or a low water cutoff or a low flow sensing device.

j) In the event controls are inoperative or the correct water level is not indicated, the boiler shall be taken out of service until the unsafe condition has been corrected.

k) All automatic low-water fuel cutoff and water-feeding devices should be examined by the Inspector to ensure that they are properly installed. The Inspector should have the float chamber types of control devices disassembled and the float linkage and connections examined for wear. The float chamber should be examined to ensure that it is free of sludge or other accumulation. Any necessary corrective action shall be taken before the device is placed back into service. The Inspector should check that the operating instructions for the devices are readily available and

l) Check that the following controls/devices are provided:

1) Each automatically fired steam boiler is protected from overpressure by not less than two pressure operated controls, one of which may be an operating control.

When required by the code of construction or the jurisdiction, the high pressure limit control shall be of the manual reset type.

2) Each automatically fired hot-water boiler or hot-water boiler system is protected from over-temperature by not less than two temperature operating controls, one of which may be an operating control.

When required by the code of construction or the jurisdiction, the high temperature limit control shall be of the manual reset type.

3) Each hot-water boiler is fitted with a thermometer that will at all times, indicate the water temperature at or near the boiler outlet.

m) Verify that any repair, alteration, or replacement of a control or safety device complies with the following:

1) The requirements of the original installation code or jurisdiction, as appropriate.

2) The work is conducted by trained and qualified individuals, with any additional certification as required by the jurisdiction.

3) The work is documented.

2.2.11 RECORDS REVIEW

a) A review of the boiler log, records of maintenance, and feedwater treatment should be made by the Inspector to ensure that regular and adequate tests have been made on the boiler and controls.

b) The owner or user should be consulted regarding repairs or alterations, if any, which have been made since the last inspection. Such repairs or alterations should be reviewed for compliance with the jurisdictional requirements, if applicable.

2.2.12 DESCRIPTION AND CONCERNS OF SPECIFIC TYPES OF BOILERS

The following details are unique to specific type boilers and should be considered when performing inspections along with the general requirements as previously outlined.

2.2.12.1 CAST-IRON BOILERS

a) Cast-iron boilers are used in a variety of applications to produce low-or-high pressure steam and hot-water heat. Cast-iron boilers should only be used in applications that allow for nearly 100% return of condensate or water and are not typically used in process-type service. These boilers are designed

to operate with minimum scale, mud, or sludge, which could occur if makeup water is added to this system.

b) Due to the unique design and material considerations of cast-iron boilers, the following are common areas of inspection:

1) Scale and Sludge — Since combustion occurs at or near the bottom, accumulation of scale or sludge close to the intense heat can cause overheating and lead to cracking;

2) Feedwater — Makeup feedwater should not come in contact with hot surfaces. Supply should be connected to a return pipe for tempering;

3) Section Alignment — Misalignment of sections can cause leakage. Leakage or corrosion between sections will not allow normal expansion and contraction and that may cause cracking;

4) Tie Rods or Draw Rods — Used to assemble the boiler and pull the sections together. These rods must not carry any stress and need to be loose, allowing for section growth during heat up. Expansion washers may be used and nuts should be just snugged allowing for expansion;

5) Push Nipple or Seal Area — Corrosion or leakage is likely at the push-nipple opening, usually caused by the push nipple being pushed into the seat crooked, warping due to overheating, tie rods too tight, and push-nipple corrosion/erosion;

6) Corrosion — Firesides of sections can corrode due to ambient moisture coupled with acidic flue gas deposits; and

7) Soot — Inadequate oxygen supply or improperly adjusted burner can allow for soot buildup in fireside passages. A reduction in efficiency and hot spots may occur. Soot, when mixed with water, can form acidic solutions harmful to the metal.

2.2.12.2 FIRETUBE BOILERS

a) The distinguishing characteristic of a firetube boiler is that the products of combustion pass within tubes that are surrounded by the water that is being heated. Combustion of fuel takes place within the furnace area, with the resultant products of combustion traveling through one or more groups of tubes before exiting the boiler. Firetube boilers are classified by the arrangement of the furnace and tubes such as Horizontal Return Tubular (HRT) boiler, Firetube Fire Box (FTFB) boiler, or Vertical Tubular (VT) boiler. The number of passes that the products of combustion make through the tubes is also used in classifying the type of boiler, such as a two-pass or three-pass boiler.

b) Firetube boilers may be used in hot-water or steam applications. They may be either low-pressure or high-pressure construction, but typically are not designed for pressures greater than 250 psig (1,720 kPa). Steam capacities are generally less than 30,000 lb/hr (13,600 kg/hr). Firetube boilers are found in a wide variety of applications ranging from heating to process steam to small power generation.

c) Firetube boilers are subject to thermal stresses due to cycling, which may cause tube leakage and corrosion of joints. The following items are common areas of inspection:

1) Waterside — Scale buildup on and around the furnace tube. Scale on or around the firetubes in the first pass after the furnace (gas temperatures >1,800°F [980°C]). Scale and corrosion buildup on stay rods hiding the actual diameter. Corrosion pitting on all pressure boundaries;

2) Fireside — Tube-to-tube sheet joint leakage. Look for rust trails left by weeping joints. When in doubt where the leakage is coming from, perform a liquid penetrant exam. Take note of refractory locations protecting steel that is not water-cooled. Partial or complete removal of the refractory may be required for inspection purposes. Condensation of combustion gas dripping out of the fireside gaskets during a cold boiler start-up is expected. However, if it continues after the water

temperature in the boiler is at least 150°F (65°C), then further investigation to determine the source of water shall be conducted;

3) The fireside surfaces of tubes in horizontal firetube boilers usually deteriorate more rapidly at the ends nearest the fire. The Inspector should examine the tube ends to determine if there has been serious reduction in thickness. The tube surfaces in some vertical tube boilers are more susceptible to deterioration at the upper ends when exposed to the heat of combustion. These tube ends should be closely examined to determine if there has been a serious reduction in thickness. The upper tube sheet in a vertical “dry top” boiler should be inspected for evidence of overheating;

4) All stays, whether diagonal or through, should be inspected to determine whether or not they are in even tension. Staybolt ends and the stayed plates should be examined to determine whether cracks exist. In addition, stayed plates should be inspected for bulging in the general area of the stay. Each staybolt end should be checked for excessive cold working (heading) and seal welds as evidence of a possible leakage problem. Stays or staybolts that are not in tension or adjustment should be repaired. Broken stays or staybolts shall be replaced; and

5) The Inspector should test firebox staybolts by tapping one end of each bolt with a hammer and, where practicable, a hammer or other heavy tool should be held on the opposite end to make the test more effective. An unbroken bolt should give a ringing sound while a broken bolt will give a hollow or non-responsive sound. Staybolts with telltale holes should be examined for evidence of leakage, which will indicate a broken or cracked bolt. Broken staybolts shall be replaced.

d) Practical considerations lead to the use of basically cylindrical shells. Flat-end tubesheet surfaces are supported by various methods: diagonal stays, through-bolts, or the tubes themselves. Tubes may be rolled, welded, or rolled and seal-welded into the tubesheets. For steam applications, the water level is maintained several inches above the uppermost row of tubes, which allows for a steam space in the upper portion of the boiler shell. There are several different types of firetube boilers:

1) Firetube Scotch Marine (FTSM)

a. A Firetube Scotch Marine boiler consists of a horizontal cylindrical shell with an internal furnace. Fuel is burned in the furnace with the products of combustion making two, three, or four passes through the boiler tubes. The rear door may be either a dry refractory lined design (dry back) or a water-cooled (wet back) design. Two designs of the furnace are commonly used: one, the corrugated type, is known as a Morrison furnace; the other is the plain furnace.

b. The FTSM boiler design is one of the oldest firetube boiler designs with internal furnaces. Extensive use in early marine service added “marine” to the name of this type of boiler. Currently both the wet back design and the dry back design can be found in stationary applications. Firetube Scotch Marine boilers are used for both high-pressure and low-pressure steam applications and are also used for hot-water service.

2) Horizontal Return Tubular (HRT)

a. Horizontal Return Tubular boilers consist of a cylindrical shell with flat tube sheets on the ends. The tubes occupy the lower two-thirds of the shell with a steam space above the tubes. The lower portion of the shell is enclosed by refractory brick work forming the furnace of the boiler, which is normally quite large to accommodate solid fuel firing. The shell is supported by the brick work or by support beams that are connected by buckstays to suspension lugs mounted on the shell. This type of boiler is highly susceptible to overheating of the lower portion of the shell due to scale accumulation that prevents heat transfer from the shell to the water. Another area of concern is the bottom blowdown line, which passes through the rear of the furnace. It must be protected with a refractory baffle to prevent direct contact with the products of combustion. Another potential problem is deterioration of the furnace brickwork, allowing the products of combustion to escape and thus reducing efficiency.

b. HRT boilers were originally used for both high-pressure and low-pressure steam applications. HRT boilers were quite common in the early to-mid-1900s. These boilers are frequently of riveted construction. The design is quite inefficient due to the one pass design and the large amount of brickwork that is heated by the products of combustion. Units that are still in service are typically found in old industrial facilities and are generally only used for steam heating applications.

3) Firetube Fire Box (FTFB)

a. Firetube Fire Box boilers were popular in the mid-1900s, although many can still be found in service. An FTFB boiler consists of an external furnace that is enclosed by water legs on three or four sides. The water legs extend upward to the crownsheet to form the lower part of the boiler shell while the upper part of the shell is formed by the extension of the water leg outer shell. Flat heads are used on both ends of the boiler shell. The boilers may be two-, three-, or four-pass designs.

b. Since the water legs of FTFB boilers are the lowest point of the water side, loose scale and sludge tends to accumulate. Besides interfering with water flow, the accumulated sediment may accelerate corrosion of water leg stay bolts or the water legs themselves. The handholes in the water legs should be open during an internal inspection.

4) Locomotive

Locomotive boilers are similar in design to the boilers on old steam locomotives. This design saw limited stationary applications and few remain in service today. Most are of riveted construction. See Supplement 1 for detailed drawings.

5) Vertical Firetube

As the name implies, vertical firetube boilers are arranged with the shell and tubes in the vertical orientation. These boilers are generally small (<10,000 lb/hr [4,540 kg/hr] capacity) and are used where the rapid development of steam is necessary for operation. Vertical firetube boilers are found in many high- and low-pressure applications. The burner may be located on the top or bottom of the boiler. Due to their small size and frequent application where considerable makeup water is used, scale development is an important concern.

2.2.12.3 WATERTUBE BOILERS

a) Typically constructed of drums, headers, and tubes, watertube boilers are used to produce steam or hot water commonly in large quantities. They range in size and pressure from small package units to extremely large field-erected boilers with pressures in excess of 3,000 psig (21 MPa). These boilers may be fired by many types of fuels such as wood, coal, gas, oil, trash, and black liquor. Their size and type of construction poses mechanical and thermal cyclic stresses.

b) There are many locations, both internal and external, where moisture and oxygen combine, causing a primary concern for corrosion. The fuels burned in watertube boilers may contain ash, which can form an abrasive grit in the flue gas stream. The abrasive action of the ash in high-velocity flue gas can quickly erode boiler tubes.

c) Unique parts associated with this type of construction, such as casing, expansion supports, superheater, economizer, soot blowers, drums, headers, and tubes should be inspected carefully and thoroughly in accordance with NBIC Part 2, 2.2.

d) The surfaces of tubes should be carefully examined to detect corrosion, erosion, bulges, cracks, or evidence of defective welds. Tubes may become thinned by high velocity impingement of fuel and ash particles or by the improper installation or use of soot blowers. A leak from a tube frequently causes serious corrosion or erosion on adjacent tubes.

e) In restricted fireside spaces, such as where short tubes or nipples are used to join drums or headers, there is a tendency for fuel and ash to lodge at junction points. Such deposits are likely to cause corrosion if moisture is present, and the area should be thoroughly cleaned and examined.

f) Drums and headers should be inspected internally and externally for signs of leakage, corrosion, overheating, and erosion. Inspect blowdown piping and connections for expansion and flexibility. Check header seals for gasket leakage.

g) Soot blower mechanical gears, chains, pulleys, etc., should be checked for broken or worn parts. Inspect supply piping to the soot blowers for faulty supports, leakage, and expansion and contraction provisions. Check design for proper installation to allow for complete drainage of condensate, which may cause erosion.

h) Watertube boilers may contain dead air spaces between the boiler casing and the fireside cavity. These dead air spaces include the penthouse, upper arch dead air space and lower throat dead air spaces and frequently house the drums and headers. There is a tendency for unburned solid fuel and ash to collect in these dead air spaces which may limit the ability to inspect these spaces for corrosion, tube bulges, service-induced cracking, or defective welds. These dead air spaces should be thoroughly cleaned and examined.

2.2.12.4 ELECTRIC BOILERS

a) Electric boilers are heated by an electrical energy source, either by use of electric resistant coils or induction coils. These boilers may be used in either high-or low-pressure steam or hot water applications.

b) Due to the unique design and material considerations of electric boilers, the following are common areas of inspection:

1) Weight stress of the elements —Some electrodes and elements can be quite heavy, especially if covered with scale deposits. These elements will scale sooner and at a faster rate than internal surfaces. Excessive weight puts severe stress on the attachment fittings and welds at support points;

2) Thermal shock — Heaters are constantly cycling on and off, creating temperature gradients, but are less susceptible to thermal shock than a fired boiler, and

3) Leakage — Any leakage noted at the opening where electrodes or elements are inserted is extremely dangerous due to the possible exposure of electrical wires, contacts, and breakers.

2.2.12.5 FIRED COIL WATER HEATERS

a) Fired coil water heaters are used for rapid heating of potable water or hot water service. This design utilizes a coil through which the water being heated is passed. This type of heater has very little volume and may be used in conjunction with a hot-water storage vessel.

b) Due to the unique design and material considerations of fired coil water heaters, the following are common areas of inspection:

1) Erosion — Size and velocity of water flow through the coil combines to create wear and thinning of the coils. If a temperature differential is created within the coil, bubbles or steam may cause grooving or cavitation;

2) Corrosion — This type of system uses 100% makeup water that contains free oxygen, creating opportunities for extensive corrosion;

3) Vibration — Operation of the burner creates a certain amount of vibration. Creation of steam, hot spots, or lack of flow may create a water hammer, causing extensive vibration and mechanical stresses;

4) Scale — Due to the large volume of makeup, significant amounts of scale-forming particles will adhere to the hot surfaces.

2.2.12.6 FIRED STORAGE WATER HEATERS

a) Fired storage water heaters are vertical pressure vessels containing water to which heat is applied. Typically, gas burners are located directly beneath the storage vessel. These heaters should be insulated and fitted with an outer jacket and may be lined with porcelain, glass, galvanized metal, cement, or epoxy.

b) Due to the unique design and material considerations of fired storage water heaters, the following are common areas of inspection:

1) Corrosion — Moisture may be trapped between the insulation and outer jacket, which may cause corrosion of the pressure boundary;

2) Mud and sludge — There is 100% makeup of water, allowing for accumulation of mud and sludge in the bottom portions of the vessel. Any buildup can cause overheating and failure of the metal in this area;

3) Scale — Loose scale may accumulate in areas adjacent to the burner and lower portions of the vessel, interfering with heat transfer process and causing localized overheating. Scale and sludge can also shield temperature control probes, giving false readings and allowing the water to overheat;

4) Thermal cycling — Heated water is continually replaced with cold water causing thermal stress within the vessel;

5) Lining — Loss of lining or coating will allow for rapid deterioration of the pressure boundary;

6) Pressure — If water supply pressure exceeds 75% of set pressure of safety relief valve, a pressure-reducing valve may be required;

7) Expansion — If the water heater can be isolated by devices such as a check valve, it is recommended that an expansion tank be provided.

2.2.12.7 THERMAL FLUID HEATERS

a) Design and Operating Features

1) Many thermal fluid heaters are pressure vessels in which a synthetic or organic fluid is heated or vaporized. Some thermal fluid heaters operate at atmospheric pressure. The fluids are typically flammable, are heated above the liquid flash point, and may be heated above the liquid boiling point. The heaters are commonly direct-fired by combustion of a fuel or by electric resistance elements. Heater design may be similar to an electric resistance heated boiler, to a firetube boiler or, more commonly, to a watertube boiler. Depending on process heating requirements, the fluid may be vaporized with a natural circulation, but more often, the fluid is heated and circulated by pumping the liquid. Use of thermal fluid heating permits heating at a high temperature with a low system pressure (600°F to 700°F [316°C to 371°C] at pressures just above atmospheric). To heat water to those temperatures would require pressures of at least 1,530 psig (10.6 MPa).

2) Nearly all thermal heating fluids are flammable. Leaks within a fired heater can result in destruction of the heater. Leaks in external piping can result in fire and may result in an explosion. Water accumulation in a thermal heating system may cause upsets and possible fluid release from the system if the water contacts heated fluid (remember, flashing water expands approximately 1,600 times). It is essential for safe system operation to have installed and to maintain appropriate fluid

level, temperature and flow controls for liquid systems, and level, temperature, and pressure controls for vapor systems. Expansion tanks used in thermal heater systems, including vented systems, should be designed and constructed to a recognized standard such as ASME Section VIII, Div. 1, to withstand pressure surges that may occur during process upsets. This is due to the rapid expansion of water exceeding the venting capability.

3) Because heat transfer fluids contract and become more viscous when cooled, proper controls and expansion tank venting are required to prevent low fluid level and collapse of the tank. Some commonly used fluids will solidify at temperatures as high as 54°F (12°C). Others do not become solid until -40°F (-40°C) or even lower. The fluids that become viscous will also become difficult to pump when cooled. Increased viscosity could cause low flow rates through the heater. The heater manufacturer recommendations and the fluid manufacturer's Material Safety Data Sheets (MSDS) should be reviewed for heat tracing requirements.

b) Industrial Applications

Thermal fluid heaters, often called boilers, are used in a variety of industrial applications such as solid wood products manufacturing, resins, turpentines, and various types of chemicals, drugs, plastics, corrugating plants, and wherever high temperatures are required. They are also frequently found in asphalt plants for heating of oils, tars, asphalt pitches, and other viscous materials. Many chemical plants use this type of heater in jacketed reactors or other types of heat exchangers.

c) Inspection

1) Inspection of thermal fluid heaters typically is done in either the operating mode or the shutdown mode. Internal inspections, however, are rarely possible due to the characteristics of the fluids and the need to drain and store the fluid. Reliable and safe operation of a heater requires frequent analysis of the fluid to determine that its condition is satisfactory for continued operation. If the fluid begins to break down, carbon will form and collect on heat transfer surfaces within the heater. Overheating and pressure boundary failure may result. Review of fluid test results and control and safety device maintenance records are essential in determining satisfactory conditions for continued safe heater operation.

2) Due to the unique design and material considerations of thermal fluid heaters and vaporizers, common areas of inspection are:

a. Design — Specific requirements outlined in construction codes must be met. Some jurisdictions may require ASME Section I or Section VIII construction. Code requirements for the particular Jurisdiction should be reviewed for specific design criteria;

b. Materials — For some thermal fluids, the use of aluminum or zinc anywhere in the system is not advisable. Aluminum acts as a catalyst that will hasten decomposition of the fluid. In addition, some fluids when hot will cause aluminum to corrode rapidly or will dissolve zinc. The zinc will then form a precipitate that can cause localized corrosion or plug instrumentation, valves, or even piping in extreme cases. These fluids should not be used in systems containing aluminum or galvanized pipe. The fluid specifications will list such restrictions;

Note: Some manufacturers of these fluids recommend not using aluminum paint on valves or fittings in the heat transfer system.

c. Corrosion — When used in applications and installations recommended by fluid manufacturer, heat transfer fluids are typically noncorrosive. However, some fluids, if used at temperatures above 150°F (65°C) in systems containing aluminum or zinc, can cause rapid corrosion;

d. Leakage — Any sign of leakage could signify problems since the fluid or its vapors can be hazardous as well as flammable. Areas for potential leaks include cracks at weld attachment points

and tube thinning in areas where tubes are near soot blowers. The thermal fluid manufacturer specifications will list the potential hazards;

e. Solidification of the fluid — Determine that no conditions exist that would allow solidification of the thermal fluid. When heat tracing or insulation on piping is recommended by the heater manufacturer, the heat tracing and insulation should be checked for proper operation and installation;

f. Pressure relief devices — Pressure relief valves shall be a closed bonnet design with no manual lift lever. The pressure relief discharge should be connected to a closed, vented storage tank or blowdown tank with solid piping (no drip pan elbow or other air gap). When outdoor discharge is used, the following should be considered for discharge piping at the point of discharge:

1. Both thermal and chemical reactions (personnel hazard);

2. Combustible materials (fire hazard);

3. Surface drains (pollution and fire hazard);

4. Loop seal or rain cap on the discharge (keep both air and water out of the system);

5. Drip leg near device (prevent liquid collection); and

6. Heat tracing for systems using high freeze point fluids (prevent blockage).

2.2.12.8 WASTE HEAT BOILERS

a) Waste heat boilers are usually of firetube or watertube type and obtain their heat from an external source or process in which a portion of the thermal energy has been utilized. Generation of electrical energy is usually the primary application of waste heat boilers. The biggest disadvantage of this type of boiler is that it is not fired on the basis of load demand. Since the boiler does not have effective control over the amount of heat entering the boiler, there may be wide variations or fluctuations of metal temperatures. Waste process gases are usually in a temperature range of 400°F (205°C) to 800°F (427°C), where combustion gases of conventionally fired boilers are at about 2,000°F (1,010°C). Special design considerations are made to compensate for lower combustion gas temperatures such as the use of finned high-efficiency heat absorbing tubes, and by slowing the velocity of gases through the boiler.

b) Due to the unique design and material considerations of waste heat boilers, the following are common areas of inspection:

1) Corrosion — Chemicals in waste heat gases may create corrosive conditions and react adversely when combined with normal gasses of combustion. Water or steam leakage can create localized corrosion. Extreme thermal cycling can cause cracks and leakage at joints;

2) Erosion — Typically waste heat flow is very low and erosion is not a problem. However, when waste heat is supplied from an internal combustion engine, exhaust gasses can be high enough to cause erosion;

3) Vibration — In some process applications and all engine waste heat applications, the boiler may be subjected to high vibration stresses;

4) Acid attack — In sulfuric acid processes refractory supports and steel casings are subject to acid attack. Piping, filters, heat exchangers, valves, fittings, and appurtenances are subject to corrosive attacks because these parts are not normally made of corrosion resistant materials; and

5) Dry operation — in certain applications waste heat boilers are operated without water. Care must be taken not to expose carbon steel material to temperatures in excess of 800°F (427°C) for prolonged periods. Carbides in the steel may precipitate to graphite at elevated temperatures.

2.2.12.9 KRAFT OR SULFATE BLACK LIQUOR RECOVERY BOILERS

a) Kraft or Sulfate Black Liquor Recovery boilers are used in the pulp and paper industry. Black liquor is a by-product of pulp processing. It contains organic and inorganic constituents concentrated to at least 58% solids for firing in the recovery boilers. The organic material that is dissolved in the pulping process combusts, and the spent pulping chemicals form a molten pool in the furnace. The molten material, or "smelt," drains from the furnace wall through smelt spouts into a smelt-dissolving tank for recovery of the chemicals. Ultimately, the by-product of the recovery process is steam used for processing and power. Gas or oil auxiliary burners are used to start the self-sustaining black liquor combustion process and may be used to produce supplemental steam if sufficient liquor is not available.

b) The recovery combustion process requires a reducing atmosphere near the furnace floor and an oxidizing atmosphere in the upper furnace for completion of combustion. Pressure parts within the furnace require protection from the reducing atmosphere and from sulfidation. The rate of corrosion within the furnace is temperature dependent. Boilers operating up to 900 psi (6.21 MPa) typically have plain carbon steel steam generating tubes with pin studs applied to the lower furnace to retain a protective layer of refractory or "frozen" smelt. Above 900 psi (6.21 MPa) the lower furnace tubes will typically have a special corrosion protection outer layer. The most common is a stainless steel clad "composite tube." Other protection methods are corrosion-resistant overlay welding, thermal or plasma spray coating, and diffusion coating.

c) The unique hazard of these boilers is the potential for an explosion if water should be combined with the molten smelt. The primary source of water is from pressure part failure, permitting water to enter the furnace. The owner's inspection program is carefully developed and executed at appropriate intervals to avoid pressure part failure that could admit water to the furnace. A second source of water is the liquor fuel.

d) Permitting black liquor of 58% or lower solids content to enter the furnace can also result in an explosion. The black liquor firing controls include devices that monitor and automatically divert the liquor from the furnace if solids content is 58% or lower.

e) In addition to the general inspection requirements for all watertube-type boilers, particular awareness in the following areas is necessary:

1) Furnace — The type and scope of wall, roof, and water screen tube inspection is dependent on materials of construction, type of construction, and mode of boiler operation. In all cases, furnace wall opening tubes need inspection for thinning and cracking. The typical water-cooled smelt spout can admit water to the furnace if the spout fails. Common practice is to replace these spouts in an interval shorter than that in which failure is known to occur;

2) Water — Percentage of solids contained in the black liquor before entering the furnace shall be closely monitored. Verify that the black liquor firing system will automatically divert the liquor if solids drop to or below 58%;

3) Corrosion/erosion — The potential consequences of corrosion or erosion (smelt-water explosion due to pressure-retaining part failure) requires a well planned and executed inspection program by the owner. Maintenance of boiler water quality is crucial to minimizing tube failure originating from the water side;

4) Tubes — Depending on type of construction, inspect for damage such as loss of corrosion protection, thinning, erosion, overheating, warping, elongation, bulging, blistering, and misalignment. If floor tubes may have been mechanically damaged or overheated, clean the floor and perform the

appropriate type of inspection for suspected damage. Excursions in water treatment may result in scale and sludge on internal surfaces, creating conditions of poor heat transfer and ultimately causing tube cracks or rupture;

5) Welds — Leaks frequently originate at welds. The owner and repair agency should carefully plan and inspect all repair welds and seal welds that could admit water to the furnace. Tube butt welds that could admit water to the furnace should be examined by a volumetric NDE method acceptable to the inspector. Tube leaks at attachment welds may originate from the internal stress-assisted corrosion (SAC). Minor upsets in boiler water quality and improper chemical cleaning may initiate SAC;

6) Emergency response to water entering furnace — Operators of Kraft recovery boilers should have a plan to immediately terminate all fuel firing and drain water from the boiler if a tube is known or suspected to be leaking into the furnace. This system may be called Emergency Shutdown Procedure (ESP). The inspector should confirm the ESP is tested and maintained such that it will function as intended and that operators will activate the system when a leak into the furnace occurs or is suspected;

7) Overheating — Tube rupture due to overheating from low water level may admit water to the furnace. The inspector should verify a redundant low-water protection system is provided and maintained.

f) Recommended procedures for inspection of black liquor recovery boilers are identified below:

1) American Forest and Paper Association:

"Recovery Boiler Reference Manual for Owners and Operators of Kraft Recovery Boilers," sponsored by the Operations/Maintenance Subcommittee of the Recovery Boiler Committee, Volumes I, II, and III (current published editions);

2) The Black Liquor Recovery Boiler Advisory Committee (BLRBAC), Recommended Practices:

a. Emergency Shutdown Procedure (ESP) and Procedure for Testing ESP;

b. Safe Firing of Black Liquor Recovery Boilers;

c. System for Black Liquor Boilers;

d. Safe Firing of Black Liquor in Black Liquor Recovery Boilers;

e. Safe Firing of Auxiliary Fuel in Black Liquor Recovery Boilers;

f. Thermal Oxidation of Waste Streams in Black Liquor Recovery Boilers;

g. Instrumentation Checklist and Classification Guide for Instruments and Control Systems Used in the Operation of Black Liquor Recovery Boilers;

h. Recommended Guidelines for Personnel Safety;

3) Technical Association of the Pulp and Paper Industry (TAPPI), Technical Information Papers:

a. 0402-13, Guidelines for Specification and Inspection of Electric Resistance Welded (ERW) and Seamless Boiler Tube for Critical and Non-Critical Service;

b. 0402-15, Installation and Repair of Pin Studs in Black Liquor Recovery Boilers;

c. 0402-18, Ultrasonic Testing (UT) for Tube Thickness in Black Liquor Recovery Boilers:

1. Part I: Guidelines for Accurate Tube Thickness Testing

2. Part II: Default Layouts for Tube Thickness Surveys in Various Boiler Zones

d. 0402-21, Ultrasonic Technician Performance Test for Boiler Tube Inspection;

e. 0402-30, Inspection for Cracking of Composite Tubes in Black Liquor Recovery Boilers;

f. 0402-31, Guidelines for Evaluating the Quality of Boiler Tube Butt Welds with Ultrasonic Testing;

g. 0402-33, Guidelines for Obtaining High Quality Radiographic Testing (RT) of Butt Welds in Boiler Tubes.

2.3 PRESSURE VESSELS

2.3.1 SCOPE

This section provides guidelines for inservice inspection of pressure vessels used to contain pressure either internal or external. This pressure may be obtained from an external source, or by the application of heat from a direct or indirect source, or a combination thereof.

2.3.2 SERVICE CONDITIONS

a) Pressure vessels are designed for a variety of service conditions. The media that a pressure vessel contains and the temperature and pressure at which it operates should be considered in establishing inspection criteria. Usage, materials, and installation conditions should be considered in determining damage mechanisms that will affect the mechanical integrity of a pressure vessel as described in NBIC Part 2, Section 3. The general requirements for safety, pre-inspection, and post-inspection activities are specified in NBIC Part 2, Section 1 and should be followed in conjunction with the specific requirements outlined in this Section when performing inspections of pressure vessels. There may be occasions where more detailed procedures will be required.

b) The type of inspection given to pressure vessels should take into consideration the condition of the vessel and the environment in which it operates. This inspection may be either external or internal and use a variety of nondestructive examination methods as described in NBIC Part 2, Section 4. The inspection method may be performed when the vessel is operating on-stream or depressurized, but shall provide the necessary information to determine that the essential sections of the vessel are in satisfactory condition to operate for the expected time interval. On-stream inspection, including while under pressure, may be used to satisfy inspection requirements provided the accuracy of the method can be demonstrated.

c) New pressure vessels are placed in service to operate under their design conditions for a period of time determined by the service conditions and the corrosion rate. If the pressure vessel is to remain in operation, the allowable conditions of service and the length of time before the next inspection shall be based on the conditions of the vessel as determined by the inspection. See NBIC Part 2, 4.4.7 for determining remaining service life and inspection intervals.

2.3.3 EXTERNAL INSPECTION

The purpose of an external inspection is to provide information regarding the general condition of the pressure vessel. The following should be reviewed:

a) Insulation or other coverings:

If it is found that external coverings such as insulation and corrosion-resistant linings are in good condition and there is no reason to suspect any unsafe condition behind them, it is not necessary to remove them for inspection of the vessel. However, it may be advisable to remove small portions of the coverings in order to investigate attachments, nozzles, and material conditions;

Note: Precautions should be taken when removing insulation while vessel is under pressure.

b) Evidence of leakage:

Any leakage of gas, vapor, or liquid should be investigated. Leakage coming from behind insulation coverings, supports or settings, or evidence of past leakage should be thoroughly investigated by removing any covering necessary until the source of leakage is established;

For additional information regarding a leak in a pressure vessel or determining extent of a possible defect, a pressure test may be performed per NBIC Part 2, 4.3.1;

c) Structural attachments:

The pressure vessel mountings should be checked for adequate allowance for expansion and contraction, such as provided by slotted bolt holes or unobstructed saddle mountings. Attachments of legs, saddles, skirts, or other supports should be examined for distortion or cracks at welds;

d) Vessel connections:

Manholes, reinforcing plates, nozzles, or other connections should be examined for cracks, deformation, or other defects. Bolts and nuts should be checked for corrosion or defects. Weep holes in reinforcing plates should remain open to provide visual evidence of leakage as well as to prevent pressure buildup between the vessel and the reinforcing plate. Accessible flange faces should be examined for distortion and to determine the condition of gasket-seating surfaces; and

e) Miscellaneous conditions

1) Abrasives — The surfaces of the vessel should be checked for erosion.

2) Dents — Dents in a vessel are deformations caused by their coming in contact with a blunt object in such a way that the thickness of metal is not materially impaired. Dents can create stress risers that may lead to cracking.

3) Distortion — If any distortion is suspected or observed, the overall dimensions of the vessel shall be checked to determine the extent and seriousness of the distortion.

4) Cuts or gouges — Cuts or gouges can cause high stress concentrations and decrease the wall thickness. Depending upon the extent of the defect, repair may be necessary.

5) Surface inspection — The surfaces of shells and heads should be examined for possible cracks, blisters, bulges, corrosion, erosion, and other evidence of deterioration, giving particular attention to the skirt and to support attachment and knuckle regions of the heads.

6) Weld joints — Welded joints and the adjacent heat-affected zones should be examined for cracks or other defects. Magnetic particle or liquid penetrant examination is a useful means for doing this.

7) Riveted vessels — On riveted vessels, examine rivet head, butt strap, plate, and caulked edge conditions. If rivet shank corrosion is suspected, hammer testing for soundness or spot radiography at an angle to the shank axis may be useful.

2.3.4 INTERNAL INSPECTION

a) A general visual inspection is the first step in making an internal inspection of pressure vessels that are susceptible to corrosion. Vessels should be inspected for the conditions identified in NBIC Part 2, Section 3.

b) The following should be reviewed:

1) Vessel Connections:

   Threaded connections should be inspected to ensure that an adequate number of threads are engaged. All openings leading to any external fittings or controls should be examined as thoroughly as possible to ensure they are free from obstructions;

2) Vessel Closures:

   Any special closures including those on autoclaves, normally termed quick actuating (quick opening) closures, see NBIC Part 2, 2.3.6.5, which are used frequently in the operation of a pressure vessel, should be checked by the Inspector for integrity and wear. A check should also be made for cracks at areas of high stress concentration. Door safety interlock mechanisms, “man inside” alarm and associated audible and visual alarms should be verified. The “man inside” alarm is a safety cable running the length of the internal workspace that can be pulled by the operator, thereby shutting down all autoclave functions and initiating audible and visual alarms;

3) Vessel Internals:

   a. Where pressure vessels are equipped with removable internals, these internals need not be completely removed provided assurance exists that deterioration in regions rendered inaccessible by the internals is not occurring to an extent that might constitute a hazard, or to an extent beyond that found in more readily accessible parts of the vessel;

   b. If a preliminary inspection reveals unsafe conditions such as loose or corroded internals or badly corroded internal ladders or platforms, steps should be taken to remove or repair such parts so that a detailed inspection may be made;

4) Corrosion:

   The type of corrosion (local pitting or uniform), its location, and any obvious data should be established. Data collected for vessels in similar service will aid in locating and analyzing corrosion in the vessel being inspected. The liquid level lines, the bottom, and the shell area adjacent to and opposite inlet nozzles are often locations of most-severe corrosion. Welded seams, nozzles, and areas adjacent to welds are often subjected to accelerated corrosion.

2.3.5 INSPECTION OF PRESSURE VESSEL PARTS AND APPURTENANCES

Parts and appurtenances to be inspected depend upon the type of vessel and its operating conditions. The Inspector should be familiar with the operating conditions of the vessel and with the causes and characteristics of potential defects and deterioration.

2.3.5.1 GAGES

a) The pressure indicated by the required gage should be compared with other gages on the same system. If the pressure gage is not mounted on the vessel itself, it shall be installed in such a manner that it correctly indicates the actual pressure in the vessel. When required, the accuracy of pressure gages should be verified by comparing the readings with a calibrated test gage or a dead weight tester.

b) The location of a pressure gage should be observed to determine whether it is exposed to high temperature from an external source or to internal heat due to lack of protection by a proper siphon or trap. Provisions should be made for blowing out the pipe leading to the steam gage.

2.3.5.2 SAFETY DEVICES

See NBIC Part 2, 2.5 for the inspection of safety devices (pressure relief valves and non-closing devices such as rupture disks) used to prevent the overpressure of pressure vessels.

2.3.5.3 CONTROLS/DEVICES

a) Any control device attached to a vessel should be demonstrated by operation or the Inspector should review the procedures and records for verification of proper operation.

b) Temperature measuring devices shall be checked for accuracy and general condition.

2.3.5.4 RECORDS REVIEW

a) The Inspector shall review any pressure vessel log, record of maintenance, corrosion rate record, or any other examination results. The Inspector should consult with the owner or user regarding repairs or alterations made, if any, since the last internal inspection. The Inspector shall review the records of such repairs or alterations for compliance with applicable requirements.

b) A permanent record shall be maintained for each pressure vessel. This record should include the following:

   1) An ASME *Manufacturer's Data Report* or, if the vessel is not ASME Code stamped, other equivalent specifications or reports;

   2) Form NB-5, *Boiler or Pressure Vessel Data Report — First Internal Inspection*, may be used for this purpose. It shall show the following identification numbers as applicable:

      a. National Board No.

      b. Jurisdiction No.

      c. Manufacturer Serial No.

      d. Owner or User No.

   3) Complete pressure-relieving device information, including safety or safety relief valve spring data, or rupture disk data and date of latest inspection.

   4) Progressive record including, but not limited to, the following:

      a. Location and thickness of monitor samples and other critical inspection locations;

      b. Limiting metal temperature and location on the vessel when this is a factor in establishing the minimum allowable thickness;

      c. Computed required metal thicknesses and maximum allowable working pressure for the design temperature and pressure-relieving device opening pressure, static head, and other loadings;

      d. Test pressure, if tested at the time of inspection; and

      e. Required date of next inspection.

   5) Date of installation and date of any significant change in service conditions (pressure, temperature, character of contents, or rate of corrosion) and

6) Drawings showing sufficient details to permit calculation of the service rating of all components on pressure vessels used in process operations subject to corrosive conditions. Detailed data with sketches, where necessary, may serve this purpose when drawings are not available.

2.3.6 DESCRIPTION AND CONCERNS OF SPECIFIC TYPES OF PRESSURE VESSELS

Inspection and examination requirements identified below should also include any additional requirements mentioned above.

2.3.6.1 DEAERATORS

a) A deaerator is used to remove undesirable gases and is exposed to the following service conditions: harmful gases, fluctuation in temperature and pressure, erosion, and vibration. The air and water atmosphere in the deaerator has a corrosive effect and may contain high concentrations of hydrogen ions, which can cause hydrogen cracking, hydrogen embrittlement, or corrosion fatigue. The water entering the deaerator sometimes carries acids or oil that can cause acidic attacks on the metal.

b) Inspection shall consist of the following:

1) Welds — Inspect all longitudinal and circumferential welds, including the Heat Affected Zone (HAZ), visually along their entire length. Examine nozzle and attachment welds for erosion, corrosion, or cracking. Inspect with special attention all exposed internal welds at or below the normal water line;

2) Shell — Inspect exterior surfaces for corrosion or leaks. Inspect interior for pitting, corrosion, erosion, thinning, wastage of metal, cracks, etc;

3) Spray nozzles and trays — Inspect all nozzles and spray areas for erosion, wear, wastage, and broken parts or supports. Check to see that nozzles are not plugged and that all lines to nozzles are open. Inspect all trays for holes, erosion, wastage, broken or defective brackets, and broken support attachments;

4) Condenser and vents — Examine all vent lines to see that they are open to ensure proper exiting of the gases. Inspect the condenser unit to verify it is operable and not plugged with scale or sludge. Check for corrosion, pitting, erosion, and broken parts; and

5) Supports — Inspect all support structures for mechanical damage, cracks, loose bolting, and bent or warped components. Check all welds, especially attaching supports to the pressure boundary.

2.3.6.2 COMPRESSED AIR VESSELS

a) Compressed air vessels include receivers, separators, filters, and coolers. Considerations of concern include temperature variances, pressure limitations, vibration, and condensation. Drain connections should be verified to be free of any foreign material that may cause plugging.

b) Inspection shall consist of the following:

1) Welds — Inspect all welds for cracking or gouging, corrosion, and erosion. Particular attention should be given to the welds that attach brackets supporting the compressor. These welds may fail due to vibration;

2) Shells/heads — Externally, inspect the base material for environmental deterioration and impacts from objects. Hot spots and bulges are signs of overheating and should be noted and evaluated for acceptability. Particular attention should be paid to the lower half of the vessel for corrosion and leakage. For vessels with manways or inspection openings, an internal inspection should be performed for corrosion, erosion, pitting, excessive deposit buildup, and leakage around inspection

openings. UT thickness testing may be used where internal inspection access is limited or to determine actual thickness when corrosion is suspected;

3) Fittings and attachments — Inspect all fittings and attachments for alignment, support, deterioration, damage, and leakage around threaded joints. Any internal attachments such as supports, brackets, or rings shall be visually examined for wear, corrosion, erosion, and cracks;

4) Operation — Check the vessel nameplate to determine the maximum allowed working pressure and temperature of the vessel. Ensure the set pressure of the safety valve does not exceed that allowed on the vessel nameplate and determine that the capacity of the safety valve is greater than the capacity of the compressor. Ensure there is a functioning manual or automatic condensate drain; and

5) Quick-Closure Attachments — Filter-type vessels usually have one quick-type closure head for making filter changes, see NBIC Part 2, 2.3.6.5.

2.3.6.3 EXPANSION TANKS

a) The purpose of an expansion tank is to provide an air cushion to a system that will allow for expansion and contraction, thus minimizing fluctuations in pressure due to temperature variances. These vessels are susceptible to corrosion due to the air and water interface.

b) Inspection shall consist of the following:

1) Design/operation — Verify from the nameplate the code of construction, temperature, and pressure ratings to ensure jurisdictional and system compatibility. It is common to find expansion tanks water logged due to leakage of air out of the tank; therefore, it is important to verify the water level either by sight glass or sounding the tank. If the vessel is fitted with a water sight glass, inspect for visual cleanliness, water leakage, and gasket tightness;

2) Surface conditions — Check all surfaces external and internal, if possible, for any leaks, corrosion, erosion, cracks, and dents that may lead to failure. Thickness checks may be applicable to determine any reduction of base material thickness; and

3) Supports and attachments — These vessels are usually suspended from the ceiling by hangers or straps causing concentration of stresses in these areas. Specifically inspect for corrosion, wear, and cracks in these areas.

2.3.6.4 LIQUID AMMONIA VESSELS

Vessels in liquid ammonia service are susceptible to stress corrosion cracking (SCC) (see NBIC Part 2, 3.3.2 b)) in areas of high stress. High-strength and coarse-grained materials seem to be more at risk of SCC than are fine-grained or more moderate strength materials, although no commonly used steels appear to be immune to the problem. Postweld heat treatment of new or weld-repaired vessels or cold formed heads is beneficial in reducing the incidence of SCC. The presence of 0.2% minimum water in the liquid ammonia also inhibits SCC. Any leak should be thoroughly investigated and the necessary corrective action initiated.

a) Internal inspection

1) Where existing openings permit, perform a visual internal inspection of the vessel. Look for any obvious cracks (very advanced SCC) and note areas that are subject to high stress such as welds, welded repairs, head-to-shell transitions, sharp interior corners, and interior surfaces opposite external attachments or supports.

2) Fittings, such as liquid level gage floats and excess flow valves, should be removed or otherwise protected from power buffing or light sandblasting when preparing the interior surface of the vessels for inspection.

3) Vessels in services where liquid ammonia is used as a reactant or is being preheated/vaporized should be inspected for localized corrosion in the reaction or vaporizing zones.

b) Examination and detection of SCC

1) All interior welds and highly stressed areas should be examined by the Wet Fluorescent Magnetic Particle Testing method (WFMT) using an A/C yoke for magnetization. Note that weld cracks are often transverse in orientation. It is extremely important to ensure that the NDE method used will disclose cracks in any orientation.

2) If cracks are discovered, a calculation shall be made to determine what depth of grinding may be carried out for crack removal (without encroaching on the minimum thickness required by the original code of construction).

3) Where possible, crack removal by grinding is the preferred method of repair. Since the stresses at the crack tips are quite high, even very fine cracking shall be eliminated.

4) Where crack depth is such that removal requires welded repair, a weld procedure shall be employed that will minimize HAZ hardening and residual stresses. Welded repairs, regardless of the depth of the repair, shall be postweld heat treated. The use of alternative welding methods in lieu of PWHT is permitted. Any repairs required and associated postweld heat treatment shall be completed in accordance with NBIC Part 3.

5) Re-inspection by WFMT after welded repair shall be done to ensure complete crack removal.

6) It is not intended to inhibit or limit the use of other NDE evaluation methods. It is recognized that acoustic emission and fracture mechanics are acceptable techniques for assessing structural integrity of vessels. Analysis by fracture mechanics may be used to assess the structural integrity of vessels when complete removal of all ammonia stress cracks is not practical. If alternative methods are used, the above recommendation that all cracks be removed, even fine cracks, may not apply.

   In addition to NDE and repair of liquid ammonia vessels that are susceptible to SCC, it is acceptable to use fitness for service evaluation methods to determine acceptability of a pressure-retaining item to perform its intended function. These methods shall be consistent with NBIC Part 2, 4.4, *Methods To Assess Damage Mechanisms And Inspection Frequency For Pressure-Retaining Items*.

c) Inspection of parts and appurtenances

1) If valves or fittings are in place, check to ensure that these are complete and functional. Parts made of copper, zinc, silver, or alloys of these metals are unsuitable for ammonia service and shall be replaced with parts fabricated of steel or other suitable materials.

2) Check that globe valves are installed with the direction of flow away from the vessel.

3) Observe that excess flow valves are properly installed and in good repair.

4) Check that hydrostatic relief valves are installed in the system piping where required.

5) Piping shall be observed to be a minimum of Schedule 80 if threaded and Schedule 40 if welded. Seamless or ERW piping is acceptable. Type F piping shall not be used for ammonia service.

6) Fittings shall be forged or Class 300 malleable iron. Seal welding is permitted only with forged fittings.

7) The Inspector shall note the pressure indicated by the gage and compare it with other gages on the same system. If the pressure gage is not mounted on the vessel itself, it should be ascertained that the gage is installed on the system in such a manner that it correctly indicates actual pressure in the vessel.

8) The Inspector shall note the liquid level in the vessel by observing the liquid level gage or other liquid level indicating device.

d) Inspection of pressure relief devices

1) See NBIC Part 2, 2.5 for the inspection of pressure relief devices used to prevent the overpressure of liquid ammonia vessels. Pressure relief devices in ammonia service shall not be tested in place using system pressure. Bench testing or replacement is required, depending on the type of pressure relief device used.

2) The Inspector shall note the replacement date marked on vessel safety valves and piping system hydrostatic relief valves requiring replacement every five years.

e) External inspection of insulated vessels

1) Insulated pressure vessels can suffer from aggressive external corrosion that is often found beneath moist insulation. The Inspector should closely examine the external insulation scaling surfaces for cold spots, bulges, rust stains, or any unusual conditions in previous repair areas. Bulging or distorted insulation on refrigerated vessels may indicate the formation of ice patches between the vessel shell and insulation due to trapped moisture. Careful observation is also required where the temperatures of insulated vessels cycle continually through the freezing temperature range.

2) The lower half and the bottom portions of insulated vessels should receive special focus, as condensation or moisture may gravitate down the vessel shell and soak into the insulation, keeping it moist for long periods of time.

Penetration locations in the insulation or fireproofing, such as saddle supports, sphere support legs, nozzles, or fittings should be examined closely for potential moisture ingress paths. When moisture penetrates the insulation, the insulation may actually work in reverse, holding moisture in the insulation and/or near the vessel shell.

3) Insulated vessels that are run on an intermittent basis or that have been out of service require close scrutiny. In general, a visual inspection of the vessel's insulated surfaces should be conducted once per year.

4) The most common and superior method to inspect for suspected corrosion under insulation (CUI) damage is to completely or partially remove the insulation for visual inspection. The method most commonly utilized to inspect for CUI without insulation removal is by x-ray and isotope radiography (film or digital) or by real-time radiography, utilizing imaging scopes and surface profilers. The real time imaging tools will work well if the vessel geometry and insulation thickness allows. Other less common methods to detect CUI include specialized electromagnetic methods (pulsed eddy current and electromagnetic waves) and long range ultrasonic techniques (guided waves).

5) There are also several methods to detect moisture soaked insulation, which is often the beginning for potential CUI damage. Moisture probe detectors, neutron backscatter, and thermography are tools that can be used for CUI moisture screening.

6) Proper surface treatment (coating) of the vessel external shell and maintaining weather-tight external insulation are the keys to prevention of CUI damage.

f) Acceptance criteria

The following are the acceptance criteria for liquid ammonia vessels. Vessels showing indications or imperfections exceeding the conditions noted below are considered unacceptable.

1) Cracks

Cracks in the pressure vessel boundary (e.g., heads, shells, welds) are unacceptable. When a crack is identified, the vessel shall be removed from service until the crack is repaired by an "R" Stamp holder or the vessel permanently removed from service. (See NBIC Part 3, *Repairs and Alterations*.)

2) Dents

When dents are identified that exceed the limits set forth below, the vessel shall be removed from service until the dents are repaired by an "R" Stamp holder, a fitness for service analysis is performed, or the vessel permanently retired from service.

a. Dents in shells

The maximum mean dent diameter in shells shall not exceed 10% of the shell diameter, and the maximum depth of the dent shall not exceed 10% of the mean dent diameter. The mean dent diameter is defined as the average of the maximum dent diameter and the minimum dent diameter. If any portion of the dent is closer to a weld than 5% of the shell diameter, the dent shall be treated as a dent in a weld area, as shown in b. below.

b. Dents in welds

The maximum mean dent diameter on welds (i.e., part of the deformation includes a weld) shall not exceed 10% of the shell diameter. The maximum depth shall not exceed 5% of the mean dent diameter.

c. Dents in heads

The maximum mean dent diameter on heads shall not exceed 10% of the shell diameter. The maximum depth shall not exceed 5% of the mean dent diameter. The use of a template may be required to measure dents on heads.

3) Bulges

When bulges are identified that exceed the limits set forth below, the vessel shall be removed from service until the bulges are repaired by an "R" Stamp holder or a fitness for service analysis is performed, the vessel may also be permanently retired from service.

a. Bulges in shells

If a bulge is suspected, the circumference shall be measured at the suspect location and at several places remote from the suspect location. The variation between measurements shall not exceed 1%.

b. Dents in heads

If a bulge is suspected, the radius of the curvature shall be measured by the use of templates. At any point the radius of curvature shall not exceed 1.25% of the diameter for the specified shape of the head.

4) Cuts or gouges

When a cut or gouge exceeds 25% of the thickness of the vessel, the vessel shall be removed from service until it is repaired by an "R" Stamp Holder or a fitness-for-service analysis is performed. The vessel may also be permanently retired from service.

5) Corrosion

a. For line or crevice corrosion, the depth of the corrosion shall not exceed 25% of the original wall thickness.

b. Isolated pits may be disregarded provided that their depth is not more than 50% of the required thickness of the pressure vessel wall (exclusive of any corrosion allowance), provided the total area of the pits does not exceed 7 sq. in. (4,500 sq. mm) within any 8 in. (200 mm) diameter circle, and provided the sum of their dimensions along any straight line within that circle does not exceed 2 in. (50 mm).

c. For a corroded area of considerable size, the thickness along the most critical plane of such area may be averaged over a length not exceeding 10 in. (250 mm). The thickness at the thinnest point shall not be less than 75% of the required wall thickness. When general corrosion is identified that exceeds the limits set forth in this paragraph, the pressure vessel shall be removed from service until it is repaired by an “R” Stamp holder or a fitness-for-service analysis is performed, or the vessel may be permanently retired from service.

2.3.6.5 INSPECTION OF PRESSURE VESSELS WITH QUICK-ACTUATING CLOSURES

a) This section describes guidelines for inspection of pressure vessels equipped with quick-actuating closures. Due to the many different designs of quick-actuating closures, potential failures of components that are not specifically covered should be considered. The scope of inspection should include areas affected by abuse or lack of maintenance and a check for inoperable or bypassed safety and warning devices.

b) Temperatures above that for which the quick-actuating closure was designed can have an adverse effect on the safe operation of the device. If parts are found damaged and excessive temperatures are suspected as the cause, the operating temperatures may have exceeded those temperatures recommended by the manufacturer. Rapid fluctuations in temperatures due to rapid start-up and shutdown may lead to cracks or yielding caused by excessive warping and high thermal stress. A careful observation should be made of the condition of the complete installation, including maintenance and operation, as a guide in forming an opinion of the care the equipment receives. The history of the vessel should be established, including: year built, materials of construction, extent of postweld heat treatment, previous inspection results, and repairs or alterations performed. Any leak should be thoroughly investigated and the necessary corrective action initiated.

1) Inspection of parts and appurtenances

a. Seating surfaces of the closure device, including but not limited to the gaskets, O-rings, or any mechanical appurtenance to ensure proper alignment of the closure to the seating surface, should be inspected. This inspection can be made by using powdered chalk or any substance that will indicate that the closure is properly striking the seating surface of the vessel flange. If this method is used, a check should be made to ensure that:

1. Material used shall not contaminate the gasket or material with which it comes into contact; and

2. The substance used shall be completely removed after the examination.

b. The closure mechanism of the device should be inspected for freedom of movement and proper contact with the locking elements. This inspection should indicate that the movable portions of the locking mechanism are striking the locking element in such a manner that full stroke can be obtained. Inspection should be made to ensure that the seating surface of the locking mechanism is free of metal burrs and deep scars, which would indicate misalignment or improper operation. A check should be made for proper alignment of the door hinge mechanisms to ensure

that adjustment screws and locking nuts are properly secured. When deficiencies are noted, the following corrective actions should be initiated:

1. If any deterioration of the gasket, O-ring, etc., is found, the gasket, O-ring, etc., should be replaced immediately. Replacements should be in accordance with the vessel manufacturer's specifications;

2. If any cracking or excessive wear is discovered on the closing mechanism, the owner or user should contact the original manufacturer of the device for spare parts or repair information. If this cannot be accomplished, the owner or user should contact an organization competent in quick-actuating closure design and construction prior to implementing any repairs;

3. Defective safety or warning devices should be repaired or replaced prior to further operation of the vessel;

4. Deflections, wear, or warping of the sealing surfaces may cause out-of-roundness and misalignment. The manufacturer of the closure should be contacted for acceptable tolerances for out-of-roundness and deflection; and

5. The operation of the closure device through its normal operating cycle should be observed while under control of the operator. This should indicate if the operator is following posted procedures and if the operating procedures for the vessel are adequate.

2) Gages, safety devices, and controls

a. The required pressure gage should be installed so that it is visible from the operating area located in such a way that the operator can accurately determine the pressure in the vessel while it is in operation. The gage dial size should be of such a diameter that it can be easily read by the operator. This gage should have a pressure range of at least 1-1/2 times, but not more than four times, the operating pressure of the vessel. There should be no intervening valve between the vessel and gage.

b. The pressure gage should be of a type that will give accurate readings, especially when there is a rapid change in pressure. It should be of rugged construction and capable of withstanding severe service conditions. Where necessary, the gage should be protected by a siphon or trap.

c. Pressure gages intended to measure the operating pressure in the vessel are not usually sensitive or easily read at low pressures approaching atmospheric. It may be advisable to install an auxiliary gage that reads inches of water (mm of mercury) and is intended to measure pressure from atmospheric through low pressures. This ensures that there is zero pressure in the vessel before opening. It would be necessary to protect the auxiliary low pressure gage from the higher operating pressures.

d. Provisions should be made to calibrate pressure gages or to have them checked against a master gage as frequently as necessary.

e. A check should be made to ensure that the closure and its holding elements must be fully engaged in their intended operating position before pressure can be applied to the vessel. A safety interlock device should be provided that prevents the opening mechanism from operating unless the vessel is completely depressurized.

f. Quick-actuating closures held in position by manually operated locking devices or mechanisms, and which are subject to leakage of the vessel contents prior to disengagement of the locking elements and release of the closure, shall be provided with an audible and/or visible warning device to warn the operator if pressure is applied to the vessel before the closure and its holding elements are fully engaged, and to warn the operator if an attempt is made to operate the

locking device before the pressure within the vessel is released. Pressure tending to force the closure clear of the vessel must be released before the closure can be opened for access.

2.3.6.6 TRANSPORT TANKS

(15) For transport tanks, the Competent Authority (DOT) shall be consulted for any requirements which it has established since they take precedence.

a) Transport tanks manufactured prior to the adoption of ASME Section XII by the Competent Authority (DOT) were constructed in accordance with the ASME Section VIII Division 1. Certain transport tanks manufactured to this code were required to be stamped in accordance with Section VIII Division 1 if the design pressure of the transport tank was 241 kPa (35 psi) (depending on material being transported) and greater. If the design pressure was less than 241 kPa (35 psi) (depending on material being transported), the transport tank was manufactured in accordance with Section VIII, Division 1, but not required by the Competent Authority (DOT) to be stamped .

b) ASME stamped transport tanks are subject to the requirements of NBIC Part 2 for inservice inspection, unless exempted by the Competent Authority (DOT).

2.3.6.7 ANHYDROUS AMMONIA NURSE TANKS

a) Nurse tanks (considered as implements of husbandry) are anhydrous ammonia pressure vessels on farm wagons, not exceeding a capacity of 3,000 water gallons (11,355 liters), used for agricultural application of liquid anhydrous ammonia to farm fields as fertilizer. Nurse tanks come under United States Department of Transportation (DOT) requirements and may also be subject to various local jurisdictional requirements. Nurse tanks shall be inspected closely by the owner or operator at least once per seasonal use. Inspections of nurse tanks include the following items. These items are not meant to be all inclusive.

b) Inspection shall consist of the following:

1) Pressure vessel - Verify that the pressure vessel is constructed for anhydrous ammonia service and that it is ASME stamped and National Board registered, as required by the jurisdiction. Check that the data plate is legible and not painted over or sand blasted. If the data plate is missing or illegible, welding is prohibited, and the tank shall be tested and operated under the DOT Hazardous Material Regulation (HMR) as required in Title 49 Code of Federal Regulations (CFR) 173.315m or the tank shall be removed from service. Post-construction welding, if any, to the pressure vessel, nozzles or support legs shall be in accordance with NBIC procedures and stamping as required in NBIC, Part 3 (Also see ANSI K61.1 for the definition of repair). Cracks, dents, bulges, cuts, gouges and corrosion shall not exceed the acceptance criteria of NBIC Part 2, 2.3.6.4 f).

2) Valves and fittings - Verify that the pressure relief device is ASME constructed and National Board capacity certified, has correct capacity and set pressure, is date current, and is not leaking, corroded or painted. Check that a rain cap is installed. Ensure that the hydrostatic relief valve is set for 350-400 psi (2,415-2,760 kPa), is in place in or on the liquid withdrawal valve and that it is in good condition and date current. A liquid level float gage shall be installed and be operable. In addition, a fixed liquid level gage (85% gage) shall be operable and unobstructed by tape or paint. A pressure gage with a clear lens and with a 0-400 psi (0-2,760 kPa) dial range shall be installed and be observed to be operable. A liquid withdrawal valve shall be in place and observed to be in good condition. Liquid and vapor fill valves shall be in operable condition and their end fittings protected with valve covers. In addition, check that no galvanized, brass, or cast iron fittings are installed.

3) Nurse tank painting, decals, and marking – The paint shall be white or aluminum, the painted surface not damaged or faded, and the tank surface not rusted. A nurse tank unique owner identification number shall be observed to be in place. A DOT approved slow-moving vehicle (SMV) emblem

or sign shall be installed at the rear. Legible transfer and safety decals shall be in place near the fill valves. "INHALATION HAZARD" markings or decals shall be observed to be in place on each side. On each side and on each end, observe that "DOT 1005" markings or decals and "ANHYDROUS AMMONIA" markings or decals are in place (Note that these markings or decals are not required on the end of a tank with valves and fittings on that end). Liquid and vapor valves shall be observed to be color coded or labeled for liquid or vapor. Markings for tests and inspections required due to a missing or illegible data plates shall be in place as required by DOT Hazardous Material Regulations.

4) Safety specific and miscellaneous equipment - Roll-over protection for valves and appurtenances, to include the pressure relief device, shall be observed to be in place. This required protection must include any bottom liquid withdrawal valves. Observe that the transfer hose, if so equipped, is date current and in good condition (not cut to the cords or showing stretch damage, bulging, or kinking). Check that a fitting is in place to secure the transfer hose (if so equipped) during transport and storage. Protective gloves and Z87 rated goggles shall be observed to be in a safety kit on the nurse tank. A safety water container [5 gal (19 l) minimum capacity] with adequate withdrawal hose shall be on the nurse tank and be in usable condition.

5) Trailer and running gear – Ensure that the hitch and undercarriage are in good repair. Observe that welds are not cracked or the rails bent. The trailer tires shall be in serviceable condition with no cuts to the cords. Two safety chains and hooks shall be in place with one hitch pin and lock pin available. The tank to trailer anchorage shall be satisfactory and any bolting tightened. Spring leaves shall not be cracked or broken on inspection and the ends secured.

2.3.6.8 INSPECTION OF PRESSURE VESSELS FOR HUMAN OCCUPANCY (PVHO's)

A pressure vessel for human occupancy (PVHO), as defined by ASME PVHO-1 is a pressure vessel that encloses a human being or animal within its pressure boundary while it is subject to internal or external pressure that exceeds a 2 psi (14 kPa) differential pressure. PVHOs include, but are not limited to submersibles, diving bells, personal transfer capsules, decompression chambers, recompression chambers, hyperbaric chambers, high altitude chambers and medical hyperbaric oxygenation facilities.

This section provides guidelines for inspection of PVHOs. Due to the many different designs and applications of PVHOs, potential failures of components or safety concerns that are not specifically covered, such as rapid decompression or fire/sparking issues should be considered.

a) General/operational

1) PVHOs must be constructed in accordance with ASME PVHO-1 and PVHO-2. These codes adopt Section VIII and therefore the vessels should bear a "U" or "U2" ASME designator.

2) Cast and ductile iron fittings are not allowed.

3) Due to the human occupancy element, a person should be in attendance to monitor the PVHO when in operation, in the event there is an accident.

4) The installation should be such that there is adequate clearance to inspect it properly. In some applications, such as underground tunneling, it may be impossible to perform a complete external inspection.

b) Internal Inspection

1) Where existing openings permit, perform a visual internal inspection of the vessel. Look for any obvious cracks and note areas that are subject to high stress such as welds, welded repairs, head-to-shell transitions, sharp interior corners, and interior surfaces opposite external attachments or supports.

2) The vessel should be free of corrosion, damage, dents, gouges, or other damage.

3) All openings leading to external fittings or controls should be free from obstruction.

4) All exhaust inlets should be checked to prevent a chamber occupant from inadvertently blocking the opening.

c) External Inspection

1) The Inspector should closely examine the external condition of the pressure vessel for corrosion, damage, dents, gouges or other damage.

2) The lower half and the bottom portions of insulated vessels should receive special focus, as condensation or moisture may gravitate down the vessel shell and soak into the insulation, keeping it moist for long periods of time. Penetration locations in the insulation or fireproofing such as saddle supports, sphere support legs, nozzles, or fittings should be examined closely for potential moisture ingress paths. When moisture penetrates the insulation, the insulation may actually work in reverse, holding moisture in the insulation and/or near the vessel shell.

3) Insulated vessels that are run on an intermittent basis or that have been out of service require close scrutiny. In general, a visual inspection of the vessel's insulated surfaces should be conducted once per year.

4) The most common and superior method to inspect for suspected corrosion under insulation (CUI) damage is to completely or partially remove the insulation for visual inspection. The method most commonly utilized to inspect for CUI without insulation removal is by X-ray and isotope radiography (film or digital) or by real time radiography, utilizing imaging scopes and surface profilers. The real time imaging tools will work well if the vessel geometry and insulation thickness allows. Other less common methods to detect CUI include specialized electromagnetic methods (pulsed eddy current and electromagnetic waves) and long-range ultrasonic techniques (guided waves).

5) There are also several methods to detect moisture soaked insulation, which is often the beginning for potential CUI damage. Moisture probe detectors, neutron backscatter, and thermography are tools that can be used for CUI moisture screening.

6) Proper surface treatment (coating) of the vessel external shell and maintaining weather-tight external insulation are the keys to prevention of CUI damage.

d) Inspection of parts and appurtenances (e.g., piping systems, pressure gage, bottom drain)

1) As stated above, cast iron is not allowed on PVHOs and shall be replaced with parts fabricated with other suitable materials, in accordance with ASME Code Section II.

2) If valves or fittings are in place, check to ensure that these are complete and functional.

3) The Inspector shall note the pressure indicated by the gage and compare it with other gages on the same system. If the pressure gage is not mounted on the vessel itself, it should be ascertained that the gage is installed on the system in such a manner that it correctly indicates actual pressure in the vessel.

4) The Inspector shall verify that the vessel is provided with a drain opening.

5) The system should have a pressure gage designed for at least the most severe condition of coincident pressure in normal operation. This gage should be clearly visible to the person adjusting the setting of the pressure control valve. The graduation on the pressure gauge shall be graduated to not less than 1.5 times the MAWP of the vessel.

6) Provisions should be made to calibrate pressure gages or to have them checked against a standard test gage.

7) Any vents and exhausts should be piped at least 10 ft. (3.0 m) from any air intake.

8) Venting should be provided at all high points of the piping system.

e) Inspection of view ports / windows

1) Each window should be individually identified and be marked in accordance with PVHO-1.

2) If there are any penetrations through windows, they must be circular.

3) Windows must be free of crazing, cracks and scratches.

4) Windows and viewports have a maximum interval for seat/seal inspection and refurbishment. Documentation should be checked to ensure compliance with PVHO-2, Table 7.1.3.

f) Inspection of pressure relief devices

1) Pressure relief devices must have a quick opening manual shutoff valve installed between the chamber and the pressure relief device, with a frangible seal in place, within easy access to the operator.

2) The pressure relief device shall be constructed in accordance with ASME Code Section VIII.

3) The discharge from the pressure relief device must be piped outside to a safe point of discharge.

4) Rupture disks may be used only if they are in series with a pressure relief valve, or when there is less than 2 ft^3 (57 l) of water volume.

5) Verify that the safety valve is periodically tested either manually by raising the disk from the seat or by removing and testing the valve on a test stand.

g) Acceptance criteria

The following forms are required to be completed:

1) Form PVHO-1 Manufacturer's Data Report for Pressure Vessels for Human Occupancy

2) Form PVHO-2 Fabrication Certification for Acrylic Windows

h) All PVHOs under the jurisdiction of the U.S. Coast Guard must also comply with 46 CFR Part 197.

2.4 PIPING AND PIPING SYSTEMS

2.4.1 SCOPE

This section provides guidelines for internal and external inspection of piping and piping systems.

2.4.2 SERVICE CONDITIONS

a) Piping systems are designed for a variety of service conditions. The media that a piping system contains, the temperature at which it operates, and the piping corrosion history should be considered in establishing piping inspection criteria. Particular attention should be given to piping systems that are subject to corrosion, high temperatures, and hazardous fluid or gases. Piping operating beyond design temperature limits can cause sufficient deterioration of piping material properties due to graphitization, embrittlement, and creep to render the piping system unfit for continued service.

b) Any externally or internally corroded piping should be evaluated for integrity and repaired or replaced as necessary.

c) Requirements specified for inspection activities and safety are identified in NBIC Part 2, Section 1, and should be reviewed and followed as applicable.

2.4.3 ASSESSMENT OF PIPING DESIGN

a) All pipe material and fittings should be properly rated for the maximum service conditions to which they are subjected under normal operating conditions and shall be provided with suitable relief device protection. The design corrosion allowance of the piping system should be considered when reviewing the current piping thickness data.

b) If a piping system has a previous history of ultrasonic wall thickness measurements, the Inspector should review the data and request additional wall thickness measurements, if warranted.

2.4.4 EXTERNAL INSPECTION OF PIPING

Piping should be inspected externally for the following:

a) Evidence of leakage (See NBIC Part 2, 2.4.6);

b) Provision for expansion and adequate support (See NBIC Part 2, 2.4.7);

c) Proper alignment of piping joints and bolted connections. Check for missing bolts or studs, nuts, and improper or inadequate bolted connection thread engagement. Also check visible gasket and gasket alignment condition. Threaded connections should also be inspected for inadequate or excessive thread engagement;

d) Past or present evidence of excessive vibration or cyclic activity such as loose or missing piping supports or piping insulation. If such activity is present, piping and piping joints should be inspected for potential fatigue cracking;

e) Evidence of general corrosion, excessive external pitting, corrosion scale buildup, exfoliation, erosion, cuts, dents, distortion, or other detrimental conditions such as pipe sweating, water hammer damage, or hot spots. Ultrasonic thickness measurements should be taken in suspect areas to ensure adequate remaining piping wall thickness;

f) Evidence of corrosion under piping insulation or other weather related damage to piping coatings;

g) Evidence of freeze damage such as bulging, striations, or surface fissures; and

h) Dead leg or stagnant piping tends to have internal corrosion issues. Ultrasonic thickness measurements should be taken in suspect locations. Radiography is also useful to assess internal deposits and subsequent corrosion in no flow piping locations.

2.4.5 INTERNAL INSPECTION OF PIPING

a) Where the internal surfaces of piping, valves, and gasket surfaces are accessible to visual examination, internal inspection should include an examination of all available surfaces. Nondestructive examination for internal corrosion may be used to supplement the inspection. Boroscope or camera inspections are also useful to augment piping internal inspections.

b) Internal pipe surfaces should be cleaned before inspection, if necessary.

c) The internal surfaces of piping, piping welds, and connections, fittings, valves, and gasket surfaces should be inspected for localized corrosion, pitting, erosion, blistering, cracking, and impingement damage.

2.4.6 EVIDENCE OF LEAKAGE

a) A leak should be investigated thoroughly and corrective action initiated. Leaks beneath piping insulation should be approached with caution, especially when removing insulation from a pressurized piping system for inspection.

b) A pressure test may be required to obtain additional information regarding the extent of a defect or detrimental condition.

For additional information regarding a leak in piping or determining the extent of a possible defect, a pressure test may be performed per NBIC Part 2, 4.3.1.

2.4.7 PROVISIONS FOR EXPANSION AND SUPPORT

a) Visual inspection should include a check for evidence of improper provision for piping expansion and support. Piping supports shall indicate loads within their design range. Piping supports should keep piping in alignment and prevent piping from colliding with other piping or stationary objects. The alignment of connections between anchored equipment should be observed to determine if any change in position of the equipment due to settling, excessive cyclic activity, steady-state stresses beyond design allowances, or other causes has placed an undue strain on the piping or its connections. Inadequate support or the lack of provision for expansion may cause broken attachment welds, cracks, or leakage at fittings. Missing, damaged, or loose insulation materials may be an indication of vibration or pipe movements resulting from improper support.

b) Piping support locations should be inspected closely at the support points for external and crevice corrosion concerns.

2.4.8 INSPECTION OF GAGES, SAFETY DEVICES, AND CONTROLS

2.4.8.1 GAGES

Piping system pressure gages should be removed for testing unless there is other information to assess their accuracy. Faulty pressure gages should be recalibrated or replaced as necessary.

2.4.8.2 SAFETY DEVICES

See NBIC Part 2, 2.5 for information on the inspection of pressure-relieving devices used to prevent the overpressure of piping systems.

2.4.8.3 QUICK-DISCONNECT COUPLING

Piping connections utilizing a quick-disconnect coupling should be checked to ensure that the coupling and its holding elements are fully engaged in their intended operating position. Means should be provided that warn the operator against disengaging the coupling or prevent the opening mechanism from operating unless the piping is completely depressurized.

2.5 PRESSURE RELIEF DEVICES

2.5.1 SCOPE

a) The most important appurtenances on any pressurized system are the pressure relief devices (PRDs) provided for overpressure protection of that system. These are devices such as safety valves, safety

relief valves, pilot valves, and rupture disks or other non-reclosing devices that are called upon to operate and reduce an overpressure condition.

b) These devices are not designed or intended to control the pressure in the system during normal operation. Instead, they are intended to function when normal operating controls fail or abnormal system conditions are encountered.

c) Periodic inspection and maintenance of these important safety devices is critical to ensure their continued functioning and availability when called upon to operate. See NBIC Part 2, 2.5.8 for recommended testing frequency for PRDs.

d) Inspection areas of concern include:

1) correct set pressure;

2) safety considerations;

3) device data;

4) condition of the device;

5) condition of the installation; and

6) testing and operational inspection.

2.5.2 PRESSURE RELIEF DEVICE DATA

a) Nameplate marking or stamping of the device should be compared to stamping on the protected pressure-retaining item. For a single device, the set pressure shall be no higher than the maximum allowable working pressure (MAWP) marked on the protected pressure-retaining item or system.

b) If multiple devices are provided, the difference between set pressures shall not exceed that permitted by the original code of construction. The set pressure of additional devices may exceed the MAWP, as permitted by the original code of construction.

c) Verify nameplate capacity and, if possible, compare to system capacity requirements.

d) Check identification on seals and ensure they match nameplates or other identification (repair or reset nameplate) on the valve or device.

2.5.3 INSERVICE INSPECTION REQUIREMENTS FOR PRESSURE RELIEF DEVICE CONDITIONS

a) Check for evidence that the valve or device is leaking or not sealing properly. Evidence of leakage through pressure-relief valves may indicate that the system is being operated at a pressure that is too close to the valve's set pressure. See NBIC Part 2, Supplement 8.

b) Seals for adjustments should be intact and show no evidence of tampering.

c) Connecting bolting should be tight and all bolts intact.

d) The valve or device should be examined for deposits or material buildup.

e) Evidence of rust or corrosion should be checked.

f) Check for damaged or misapplied parts.

g) If a drain hole is visible, ensure it is not clogged with debris or deposits.

h) Check for test gages left in place after pressure testing of the unit.

i) Bellows valves shall be checked to ensure the bonnet vent is open or piped to a safe location. The vent shall not be plugged since this will cause the valve set pressure to be high if the bellows develops a leak. Leakage noted from the vent indicates the bellows is damaged and will no longer protect the valve from the effects of back pressure.

2.5.4 INSERVICE INSPECTION REQUIREMENTS FOR PRESSURE RELIEF DEVICE INSTALLATION CONDITION

a) Inspect inlet piping and ensure it meets the requirements of the original code of conctruction. For pressure relief valves, check that the inlet pipe size is not smaller than the device inlet size.

b) Inspect discharge piping and ensure it meets the original code of construction. Check that the discharge pipe size is not smaller than the device outlet size.

c) Check that the valve drain piping is open.

d) Check drainage of discharge piping.

e) Check that inlet and discharge piping are not binding or placing excessive stress on the valve body, which can lead to distortion of the valve body and leakage or malfunction.

f) Check the condition and adequacy of piping supports. Discharge piping should be supported independent of the device itself.

g) Check for possible hazards to personnel from the valve discharge or discharge pipe.

h) Check that there are no intervening isolation valves between the pressure source and the valve inlet or between the valve outlet and its point of discharge. Isolation valves may be permitted in some pressure vessel service. (See NBIC Part 1, 5.3.6 e) and jurisdictional requirements). Isolation valves are not permitted for power boilers, heating boilers, or water heaters.

i) A change-over valve, which is used to install two pressure relief devices on a single vessel location for the purpose of switching from one device to a spare device, is not considered a block valve if it is arranged such that there is no intermediate position that will isolate both pressure relief devices from the protected system. Change-over valves should be carefully evaluated to ensure they do not have excessive pressure drop that could affect the pressure relief device operation or capacity. These devices are commonly used in pressure vessel service. They may also be used in some boiler applications. It is recommended that the Jurisdiction be contacted to determine their acceptability on boiler applications.

2.5.5 ADDITIONAL INSPECTION REQUIREMENTS

Additional items should be considered for the specified services.

2.5.5.1 BOILERS

a) If boilers are piped together with maximum allowable working pressures differing by more than 6%, additional protective devices may be required on the lower-pressure units to protect them from overpressure from the higher pressure unit.

b) Hot-water heating boilers and water heaters.

1) These units generally do not use any water treatment and therefore may be more prone to problems with deposits forming that may impair a safety device's operation. Particular attention should be paid to signs of leakage through valves or buildups of deposits.

2) Hot-water boilers tend to have buildups of corrosion products since the system is closed with little makeup. These products can foul or block the valve inlet.

3) Water heaters will have cleaner water due to continuous makeup. However, these valves usually have a thermal element that will cause the valve to open slightly when the water is heated and not removed from the system. When this hot water evaporates in the discharge piping, calcium deposits may tend to form in the valve inlet and outlet.

2.5.5.2 PRESSURE VESSELS AND PIPING

Standard practice for overpressure protection devices is to not permit any type of isolation valve either before or after the device. However, some pressure vessel standards permit isolation valves under certain controlled conditions when shutting down the vessel to repair a damaged or leaking valve. If isolation block valves are employed, their use should be carefully controlled by written procedures. Block valves should have provisions to be either cap-sealed or locked in an open position when not being used. For ASME Section VIII, Div. 1 pressure vessels, see UG-135, Appendix M, and jurisdictional rules for more information.

2.5.5.3 RUPTURE DISKS

a) Rupture disks or other non-reclosing devices may be used as sole relieving devices or in combination with safety relief valves to protect pressure vessels.

b) The selection of the correct rupture disk device for the intended service is critical to obtaining acceptable disk performance. Different disk designs are intended for constant pressure, varying pressure, or pulsating pressure. Some designs include features that make them suitable for back pressure and/or internal vacuum in the pressure vessel.

c) The margin between the operating pressure and the burst pressure is an important factor in obtaining acceptable performance and service life of the disk. Flat and pre-bulged solid metal disks are typically used with an operating pressure that is no more than 60% to 70% of the burst pressure. Other designs are available that increase the operating pressure to as much as 90% of the burst pressure. Disks that have been exposed to pressures above the normal operating pressure for which they are designed are subject to fatigue or creep and may fail at unexpectedly low pressures. Disks used in cyclic service are also subject to fatigue and may require a greater operating margin or selection of a device suitable for such service.

d) The disk material is also critical to obtaining acceptable service life from the disk. Disks are available in a variety of materials and coatings, and materials that are unaffected by the process fluid should be used. Disks that experience corrosion may fail and open at an unexpectedly low pressure.

e) Disk designs must also be properly selected for the fluid state. Some disk types are not suitable for use in liquid service. Some disks may have a different flow resistance when used in liquid service, which may affect the sizing of the disk.

f) Information from the rupture disk manufacturer, including catalog data and installation instructions, should be consulted when selecting a disk for a particular service.

g) For rupture disks and other non-reclosing devices, the following additional items should be considered during inspections.

1) The rupture disk nameplate information, including stamped burst pressure and coincident temperature, should be checked to ensure it is compatible with the intended service. The coincident temperature on the rupture disk shall be the expected temperature of the disk when the disk is expected to burst and will usually be related to the process temperature, not the temperature on the pressure vessel nameplate.

2) Markings indicating direction of flow should be checked carefully to ensure they are correct. Some rupture disks when installed in the incorrect position may burst well above the stamped pressure.

3) The marked burst pressure for a rupture disk installed at the inlet of a safety relief valve shall be equal to or less than the safety relief valve set pressure. A marked burst pressure of 90% to 100% of the safety relief valve set pressure is recommended. A disk with a non-fragmenting design that cannot affect the safety relief valve shall be used.

   Note: If the safety relief valve set pressure is less than the vessel MAWP, the marked burst pressure may be higher than the valve set pressure, but no higher than the MAWP.

4) Check that the space between a rupture disk and a safety relief valve is supplied with a pressure gage, try cock, or telltale indicator to indicate signs of leakage through the rupture disk. The safety relief valve shall be inspected and the leaking disk shall be replaced if leakage through the disk is observed.

5) If a rupture disk is used on a valve outlet, the valve design must be of a type not influenced by back pressure due to leakage through the valve. Otherwise, for nontoxic and non-hazardous fluids, the space between the valve and the ruptured disk shall be vented or drained to prevent the accumulation of pressure.

6) For rupture disks installed on the valve inlet, the installation should be reviewed to ensure that the combination rules of the original code of construction have been applied. A reduction in the valve capacity up to 10% is expected when used in combination with a non-reclosing device.

7) The frequency of inspection for rupture disks and other non-reclosing devices is greatly dependent on the nature of the contents and operation of the system and only general recommendations can be given. Inspection frequency should be based on previous inspection history. If devices have been found to be leaking, defective, or damaged by system contents during inspection, intervals should be shortened until acceptable inspection results are obtained. With this in mind, the inspection frequency guidelines specified in NBIC Part 2, 2.5.8 are suggested for similar services.

8) Rupture disks are often used to isolate pressure relief valves from services where fouling or plugging of the valve inlet occurs. This tendency should be considered in establishing the inspection frequency.

9) Since these devices are for one-time use, a visual inspection is the only inspection that can be performed. Rupture disks that are installed using a specified bolting torque procedure cannot be reused after inspection and must be replaced.

10) It is recommended that all rupture disks be replaced periodically to prevent unintended failure while in service due to deterioration of the device.

    Rupture disks should be checked carefully for damage prior to installation and handled by the disk edges, if possible. Any damage to the surface of the ruptured disk can affect the burst pressure.

2.5.6 PACKAGING, SHIPPING, AND TRANSPORTATION

a) The improper packaging, shipment, and transport of pressure relief devices can have detrimental effects on device operation. Pressure relief devices should be treated with the same precautions as instrumentation, with care taken to avoid rough handling or contamination prior to installation.

b) The following practices are recommended:

   1) Valves should be securely fastened to pallets in the vertical position to avoid side loads on guiding surfaces, except threaded and socket-weld valves up to 2 in. (50 mm) may be securely packaged and cushioned during transport;

2) Valve inlet and outlet connection, drain connections, and bonnet vents should be protected during shipment and storage to avoid internal contamination of the valve. Ensure all covers and/or plugs are removed prior to installation;

3) The valve should not be picked up or carried using the lifting lever. Lifting levers should be wired or secured so they cannot be moved while the valve is being shipped or stored. These wires shall be removed before the valve is placed in service; and

4) Pilot valve tubing should be protected during shipment and storage to avoid damage and/or breakage.

2.5.7 TESTING AND OPERATIONAL INSPECTION OF PRESSURE RELIEF DEVICES

a) Pressure relief valves must be tested periodically to ensure that they are free to operate and will operate in accordance with the requirements of the original code of construction. Testing should include device set or opening pressure, reclosing pressure, where applicable, and seat leakage evaluation. Tolerances specified for these operating requirements in the original code of construction shall be used to determine the acceptability of test results.

b) Testing may be accomplished by the owner on the unit where the valve is installed or at a qualified test facility. In many cases, testing on the unit may be impractical, especially if the service fluid is hazardous or toxic. Testing on the unit may involve the bypassing of operating controls and should only be performed by qualified individuals under carefully controlled conditions. It is recommended that a written procedure be available to conduct this testing.

1) The Inspector should ensure that calibrated equipment has been used to perform this test and the results should be documented by the owner.

2) If the testing was performed at a test facility, the record of this test should be reviewed to ensure the valve meets the requirements of the original code of construction. Valves which have been in toxic, flammable, or other hazardous services shall be carefully decontaminated before being tested. In particular, the closed bonnet of valves in these services may contain fluids that are not easily removed or neutralized. If a test cannot be performed safely, the valve shall be disassembled, cleaned, and decontaminated, repaired, and reset.

3) If a valve has been removed for testing, the inlet and outlet connections should be checked for blockage by product buildup or corrosion.

c) Valves may be tested using lift assist devices when testing at full pressure may cause damage to the valve being tested, or it is impractical to test at full pressure due to system design considerations. Lift assist devices apply an auxiliary load to the valve spindle or stem, and using the measured inlet pressure, applied load and other valve data allow the set pressure to be calculated. If a lift assist device is used to determine valve set pressure, the conditions of NBIC Part 3, 4.5.3 shall be met. It should be noted that false set pressure readings may be obtained for valves which are leaking excessively or otherwise damaged.

d) If valves are not tested on the system using the system fluid, the following test mediums shall be used:

1) High-pressure boiler safety valves, high-temperature hot-water boiler safety relief valves, low-pressure steam heating boilers: steam;

2) Hot-water heating boiler safety relief valves: steam, air, or water;

3) Hot-water heater temperature and pressure relief valves: air or water;

4) Air and gas service process safety relief valves: air, nitrogen, or other suitable gas;

5) Liquid service process pressure relief valves: water or other suitable fluid;

6) Process steam service safety relief valves: steam or air with manufacturer's steam to air correction factor.

Note: Valves being tested after a repair must be tested on steam except as permitted by NBIC Part 3, 4.5.2.

e) As an alternative to a pressure test, the valve may be checked by the owner for freedom of operation by activating the test or "try" lever (manual check). For high pressure boiler and process valves, this test should be performed only at a pressure greater than 75% of the stamped set pressure of the valve or the lifting device may be damaged. This test will only indicate that the valve is free to operate and does not provide any information on the actual set pressure. All manual checks should be performed with some pressure under the valve in order to flush out debris from the seat that could cause leakage.

Note: The manual check at 75% or higher is based on lift lever design requirements for ASME Sections I and VIII valves. Code design requirements for lifting levers for ASME Section IV valves require that the valve be capable of being lifted without pressure.

f) If a valve is found to be stuck closed, the system should immediately be taken out of service until the condition can be corrected, unless special provisions have been made to operate on a temporary basis (such as additional relief capacity provided by another valve).

g) If a pressure test indicates the valve does not open within the requirements of the original code of construction, but otherwise is in acceptable condition, minor adjustments (defined as no more than twice the permitted set pressure tolerance) shall be made by an organization accredited by the National Board to reset the valve to the correct opening pressure. All adjustments shall be resealed with a seal identifying the responsible organization and a tag shall be installed identifying the organization and the date of the adjustment.

h) If a major adjustment is needed, this may indicate the valve is in need of repair or has damaged or mis-applied parts. Its condition should be investigated accordingly.

i) Systems with multiple valves will require the lower set valves to be held closed to permit the higher set valves to be tested. A test clamp or "gag" should be used for this purpose. The spring compression screw shall not be tightened. It is recommended that the test clamps be applied in accordance with the valve manufacturer's instructions when the valve is at or near the test temperature, and be applied hand tight only to avoid damage to the valve stem or spindle.

j) Upon completion of set pressure testing, all pressure relief valve gags shall be removed.

2.5.8 RECOMMENDED INSPECTION AND TEST FREQUENCIES FOR PRESSURE RELIEF DEVICES

a) Power Boilers

1) Pressure less than 400 psig (2.76 MPa): Manual check every 6 months; pressure test annually to verify nameplate set pressure or as determined by operating experience as verified by testing history.

2) Pressure greater than 400 psig (2.76 MPa): Pressure test to verify nameplate set pressure every three years or as determined by operating experience as verified by testing history.

3) Pressure tests should be performed prior to bringing the boiler down for planned internal inspection so needed repairs or adjustments can be made while the boiler is down.

b) High-temperature hot-water boilers

Pressure test annually to verify nameplate set pressure or as determined by operating experience as verified by testing history. For safety reasons, removal and testing on a steam test bench is recommended. Such testing will avoid damaging the safety valve by discharge of a steam-water mixture, which could occur if the valve is tested in place.

c) Low-pressure steam heating boilers

Manual check quarterly; pressure test annually prior to steam heating season to verify nameplate set pressure.

d) Hot-water heating boilers

Manual check quarterly; pressure test annually prior to heating season to verify nameplate set pressure.

Note: The frequencies specified for the testing of pressure relief valves on boilers is primarily based on differences between high pressure boilers that are continuously manned, and lower pressure automatically controlled boilers that are not monitored by a boiler operator at all times. When any boiler experiences an overpressure condition such that the safety or safety relief valves actuate, the valves should be inspected for seat leakage and other damage as soon as possible and any deficiencies corrected.

e) Water heaters

Manual check every two months. Due to the relatively low cost of safety valves for this service, it is recommended that a defective valve be replaced with a new valve if a repair or resetting is indicated.

f) Pressure vessels and piping

Frequency of test and inspection of pressure relief devices for pressure vessel and piping service is greatly dependent on the nature of the contents and operation of the system and only general recommendations can be given. Inspection frequency should be based on previous inspection history. If valves are found to be defective or damaged by system contents during inspection, intervals should be shortened until acceptable inspection results are obtained. Where test records and/or inspection history are not available, the inspection frequencies in Table 2.5.8 are suggested.

Service	Inspection Frequency
Steam	Annual
Air and clean dry gases	Every three years
Pressure relief valves in combination with rupture disks	Every five years
Propane, refrigerant	Every five years
All others	Per inspection history

g) Establishment of inspection and test intervals

Where a recommended test frequency is not listed, the valve user and Inspector must determine and agree on a suitable interval for inspection and test. Some items to be considered in making this determination are:

1) Jurisdictional requirements;

2) Records of test data and inspections from similar processes and similar devices in operation at that facility;

3) Recommendations from the device manufacturer. In particular, when the valve includes a non-metallic part such as a diaphragm, periodic replacement of those parts may be specified;

4) Operating history of the system. Systems with frequent upsets where a valve has actuated require more frequent inspection;

5) Results of visual inspection of the device and installation conditions. Signs of valve leakage, corrosion or damaged parts all indicate more-frequent operational inspections;

6) Installation of a valve in a system with a common discharge header. Valves discharging into a common collection pipe may be affected by the discharge of other valves by the corrosion of parts in the outlet portion of the valve or the buildup of products discharged from those valves;

7) Ability to coordinate with planned system shutdowns. The shutdown of a system for other maintenance or inspection activities is an ideal time for the operational inspection and test of a pressure relief valve;

8) Critical nature of the system. Systems that are critical to plant operation or where the effects of the discharge of fluids from the system are particularly detrimental due to fire hazard, environmental damage, or toxicity concerns all call for more frequent inspection intervals to ensure devices are operating properly; and

9) Where the effects of corrosion, blockage by system fluid, or ability of the valve to operate under given service conditions are unknown (such as in a new process or installation), a relatively short inspection interval, not to exceed one year or the first planned shutdown, whichever is shorter, shall be established. At that time the device shall be visually inspected and tested. If unacceptable test results are obtained, the inspection interval shall be reduced by 50% until suitable results are obtained.

h) Establishment of service intervals

1) The above intervals are guidelines for periodic inspection and testing. Typically if there are no adverse findings, a pressure relief valve would be placed back in service until the next inspection. Any unacceptable conditions that are found by the inspection shall be corrected immediately by repair or replacement of the device. Many users will maintain spare pressure relief devices so the process or system is not affected by excessive downtime.

2) Pressure relief valves are mechanical devices that require periodic preventive maintenance even though external inspection and test results indicate acceptable performance. There may be wear on internal parts, galling between sliding surfaces or internal corrosion, and fouling which will not be evident from an external inspection or test. Periodic re-establishment of seating surfaces and the replacement of soft goods such as o-rings and diaphragms are also well advised preventive maintenance activities that can prevent future problems. If the valve is serviced, a complete disassembly, internal inspection, and repair as necessary, such that the valve's condition and performance are restored to a like-new condition, should be done by an organization accredited by the National Board.

3) Service records with test results and findings should be maintained for all overpressure protection devices. A service interval of no more than three inspection intervals or ten years, whichever is less, is recommended to maintain device condition. Results of the internal inspection and maintenance findings can then be used to establish future service intervals.

PART 2, SECTION 3
INSPECTION — CORROSION AND FAILURE MECHANISMS

3.1 SCOPE

This section describes damage mechanisms applicable to pressure-retaining items. Further information concerning metallurgical properties of steels and nonferrous alloys are described in ASME Section II, Part D, of the Boiler and Pressure Vessel Code, Non Mandatory Appendix A, titled Metallurgical Phenomena.

A damage (or deterioration) mechanism is a process that induces deleterious micro and/or macro material changes over time that are harmful to the material condition or mechanical properties. Damage mechanisms are usually incremental, cumulative and, in some instances, unrecoverable. Common damage mechanisms include corrosion, chemical attack, creep, erosion, fatigue, fracture, and thermal aging.

3.2 GENERAL

Understanding the potential damage/deterioration mechanisms that can affect the mechanical integrity of a pressure-retaining item and knowledge of the inspection methods that can be used to find these damage mechanisms, are essential to an effective inspection. This section includes a general discussion of various damage mechanisms, and effective inspection methods are referenced in Section 4 of this part. In addition, some specific guidance is given on how to estimate the remaining life of a pressure-retaining item and determine the appropriate inspection frequencies as referenced in NBIC Part 2, Section 5.

3.3 CORROSION

All metals and alloys are susceptible to corrosion. Corrosion is deterioration that occurs when a metal reacts with its environment. Corrosion can be classified based on three factors:

a) Nature

   1) Wet — liquid or moisture present

   2) Dry — high-temperature gasses

b) Mechanism — electrochemical or direct chemical reactions

c) Appearance — either uniform or localized

3.3.1 MACROSCOPIC CORROSION ENVIRONMENTS

Macroscopic corrosion types are among the most-prevalent conditions found in pressure-retaining items causing deterioration. The following corrosion types are found.

a) Uniform corrosion (general)

   The most common form of corrosion is uniform attack over a large area of the metal surface. Safe working pressure is directly related to the remaining material thickness, and failures can be avoided by regular inspection.

b) Galvanic corrosion

   Two dissimilar metals in contact with each other and with an electrolyte (e.g., a film of water containing dissolved oxygen, nitrogen, and carbon dioxide) constitute an electrolytic cell, and the electric current flowing through the circuit may cause rapid corrosion of the less noble metal (the one having the

greater electrode potential). This corrosion mechanism is most active when there are large differences between the electrode potentials of the two metals, but galvanic corrosion may also exist with relatively minor changes of alloy composition (e.g., between a weld metal and the base metal). Natural (e.g., an oxide coating on aluminum) or protective coatings may inhibit galvanic corrosion, but in most instances the metals or alloys must be selected on the basis of intrinsic resistance to corrosion. In pressure vessels the effects of galvanic corrosion are most noticeable at rivets, welds, or at flanged and bolted connections.

c) Erosion corrosion

Movement of a corrosive over a metal surface increases the rate of attack due to mechanical wear and corrosion. This corrosion is generally characterized as having an appearance of smooth bottomed shallow pits and may also exhibit a directional pattern related to the path taken by the corrosive.

d) Crevice corrosion

Environmental conditions in a crevice can, with time, become different to those on a nearby clean surface. A more-aggressive environment may develop within the crevice and cause local corrosion. Crevices commonly exist at gasket surfaces, lap joints, bolts, rivets, etc. They are also created by dirt deposits, corrosion products, scratches in paint, etc. Crevice corrosion is usually attributed to one or more of the following:

1) Changes in acidity in the crevice;

2) Lack of oxygen in the crevice;

3) Buildup of detrimental ions in the crevice; and

4) Depletion of a corrosion inhibitor in the crevice.

e) Pitting corrosion

Pitting corrosion is the formation of holes in an otherwise relatively unattacked surface. Pitting is usually a slow process causing isolated, scattered pits over a small area that does not substantially weaken the vessel. It could, however, eventually cause leakage.

f) Line corrosion

This is a condition where pits are connected, or nearly connected, to each other in a narrow band or line. Line corrosion frequently occurs in the area of intersection of the support skirt and the bottom of the vessel or liquid-vapor interface.

g) Exfoliation

Exfoliation is a subsurface corrosion that begins on a clean surface but spreads below it. It differs from pitting in that the attack has a laminated appearance. These attacks are usually recognized by a flaky and sometimes blistered surface.

h) Selective leaching

Selective leaching is the removal of one element in an alloy. This corrosion mechanism is detrimental because it yields a porous metal with poor mechanical properties.

i) Grooving

Grooving is a form of metal deterioration caused by localized corrosion and may be accelerated by stress concentration. Grooving may be found adjacent to riveted lap joints or welds and on flanged surfaces, particularly the flanges of unstayed heads.

3.3.2 MICROSCOPIC CORROSION ENVIRONMENTS

Microscopic corrosion environments are not visible to the naked eye. The following corrosion types are among the most prevalent conditions found in pressure-retaining items causing deterioration.

a) Intergranular corrosion

Corrosion attack by a corrosive usually related to the segregation of specific elements or the formation of a compound in the grain boundary. It usually attacks the grain boundary that has lost an element necessary for adequate corrosion resistance. In severe cases entire grains are dislodged causing the surface to appear rough co the naked eye and feel sugary because of the loose grains. Susceptibility to intergranular corrosion is usually a by-product of heat treatment.

b) Stress corrosion cracking (SCC)

1) The action of tensile stress and a corrosive result in the cracking of metals. This is very serious because periods of time (often years) may pass before cracks become visible. The cracks then propagate quite rapidly and result in unexpected failures. Stresses that cause cracking arise from cold working, welding, thermal treatment, or may be externally applied during service. The cracks can follow intergranular or transgranular paths and often have a tendency for branching.

2) The principal variables affecting stress corrosion cracking are tensile stress, service temperature, solution chemistry, duration of exposure, and metal properties. Modifying any one of these parameters sufficiently can reduce or eliminate the possibility of stress corrosion cracking occurring in service. As an example, austenitic stainless steels used in water wetted service are susceptible to stress corrosion cracking.

c) Corrosion fatigue

This is a special form of stress corrosion cracking caused by repeated cyclic stressing. When fatigue occurs in the presence of a corrodent, the result is corrosion fatigue. Such damage is common to pressure-retaining items subjected to continuous vibration.

d) Microbiologically induced corrosion

Microbiologically induced corrosion (MIC) is caused by bacteria, algae or fungi and is often associated with the presence of tubercles or slimy organic substances. MIC is usually found in services where stagnant water is present.

3.3.3 CONTROL OF CORROSION

There are many ways to control and avoid corrosion, such as control of process variables, engineering design, protection, material selection, and coatings.

3.3.3.1 PROCESS VARIABLES

Some of the more common process variables that influence corrosion are listed below:

a) Concentration of major constituents;

b) Impurities;

c) Temperature;

d) pH;

e) Velocity;

f) Inhibitors; and

g) Start-up and downtime operations.

3.3.3.2 PROTECTION

Protective methods such as cathodic and anodic corrosion control can minimize attack and thereby reduce replacement costs or permit the use of less-expensive or thinner materials.

3.3.3.3 MATERIAL SELECTION

Chemical and physical properties of a material will enable selection of the best one for a specific application. The final choice will often be a compromise between the desired physical properties and economic factors. A checklist for material selection would include:

a) Evaluating requirements to be met (properties, design, appearance, mechanical, physical);

b) Material selection considerations;

c) Corrosive variables;

d) Application of equipment; and

e) Experience of materials.

3.3.3.4 COATINGS

Metallic and inorganic materials are typical coatings for controlling corrosion. Selection of materials depends on the corrosive, method of application, type of base material, and the nature of bonding between the base material and coating. The success or failure of a coating will often depend on the surface preparation.

a) Techniques for applying metallic coatings could include:

    1) Hot dipping;

    2) Metal spraying;

    3) Cladding;

    4) Cementation;

    5) Vapor deposition;

    6) Electroplating;

    7) Plating; and

    8) Welding.

b) Techniques for applying inorganic coatings would include:

1) Porcelain, ceramic;

2) Glass;

3) Cement;

4) Rubber;

5) Paint; and

6) Phosphates.

3.3.3.5 ENGINEERING DESIGN

Crevice, galvanic, erosion, and stress corrosion cracking are the types of corrosion most controllable by proper design of equipment. Procedures and situations such as welding, end-grain attack, and drainage are also controlled by proper design techniques.

3.3.3.6 CONCLUSION

a) By carefully selecting materials and protection methods, we can predict and control corrosive attack. However, there may be unexpected damage as a result of one or more of the following:

   1) Poor choice of materials;

   2) Operating conditions different from those anticipated;

   3) Defective fabrication;

   4) Improper design;

   5) Inadequate maintenance; and

   6) Defective material.

b) Corrective actions will depend on which factors caused the problems, making it important to diagnose the reason for damage. Early detection of corrosion problems is important to prevent further damage and can be achieved by performing regular inspections and encouraging employees to be observant and communicate their observations.

3.4 FAILURE MECHANISMS

The following failure mechanism information may assist inspectors in identifying service-induced deterioration and failure modes encountered in pressure-retaining items.

3.4.1 FATIGUE

Stress reversals (such as cyclic loading) in parts of equipment are common, particularly at points of high secondary stress. If stresses are high and reversals frequent, damage may occur because of fatigue. Fatigue damage in pressure vessels may also result from cyclic temperature and pressure changes. Locations where metals having different thermal coefficients of expansion are joined by welding may be susceptible to thermal fatigue.

3.4.2 CREEP

Creep damage may occur if equipment is subjected to temperatures above those for which the equipment is designed. Since metals become weaker at higher temperatures, such distortion may result in failure, particularly at points of stress concentration. If excessive temperatures are encountered, structural property and chemical changes in metals may also take place, which may permanently weaken equipment. Since creep is dependent on time, temperature and stress, the actual or estimated levels of these quantities should be used in any evaluations.

3.4.3 TEMPERATURE EFFECTS

At subfreezing temperatures, water and some chemicals handled in pressure vessels may freeze and cause damage. Carbon and low-alloy steels may be susceptible to brittle failure at ambient temperatures. A number of failures have been attributed to brittle fracture of steels that were exposed to temperatures below their transition temperature and that were exposed to pressures greater than 20% of the required hydrostatic test pressure. However, most brittle fractures have occurred on the first application of a particular stress level (that is, the first hydrostatic test or overload). Special attention should be given to low-alloy steels because they are prone to temper embrittlement. Temper embrittlement is defined as a loss of ductility and notch toughness due to postweld heat treatment or high-temperature service, above 700°F (371°C).

3.4.4 HYDROGEN EMBRITTLEMENT

a) The term hydrogen embrittlement (HE) refers to a loss of ductility and toughness in steels caused by atomic hydrogen dissolved in the steel. Hydrogen that is dissolved in carbon and low-alloy steels from steel making, welding, or from surface corrosion can cause either intergranular or transgranular cracking and “brittle” fracture behavior without warning.

b) Hydrogen embrittlement typically occurs below 200°F (93°C) because hydrogen remains dissolved within the steel at or below this temperature. One example of hydrogen embrittlement is underbead cracking. The underbead cracks are caused by the absorption of hydrogen during the welding process in the hard, high-strength weld heat affected zone (HAZ). Use of low-hydrogen welding practices to minimize dissolved hydrogen and/or the use of high preheat, and/or postweld heat treatment can reduce susceptibility to cracking from hydrogen embrittlement. The diffusivity of hydrogen is such that at temperatures above 450°F (232°C), the hydrogen can be effectively removed, eliminating susceptibility to cracking. Thus, hydrogen embrittlement may be reversible as long as no physical damage (e.g., cracking or fissures) has occurred in the steel.

c) Hydrogen embrittlement is a form of stress corrosion cracking (SCC). Three basic elements are needed to induce SCC: the first element is a susceptible material, the second element is environment, and the third element is stress (applied or residual). For hydrogen embrittlement to occur, the susceptible material is normally higher strength carbon or low alloy steels, the environment must contain atomic hydrogen, and the stress can be either service stress and/or residual stress from fabrication. If any of the three elements are eliminated, HE cracking is prevented.

d) In environments where processes are conducted at elevated temperature, the reaction of hydrogen with sulfur in carbon and low-alloy reactor vessel steels can produce hydrogen sulfide stress corrosion (SSC), which is a form of hydrogen embrittlement. Susceptibility to sulfide (H_2S) stress corrosion cracking depends on the strength of the steel. Higher-strength steels are more susceptible. The strength level at which susceptibility increases depends on the severity of the environment. Hydrogen sulfide, hydrogen cyanide, and arsenic in aqueous solutions, all increase the severity of the environment towards hydrogen embrittlement by increasing the amount of hydrogen that can be absorbed by the steel during the corrosion reaction. In hydrogen sulfide environments, susceptibility to cracking can be reduced by using steels with a strength level below that equivalent to a hardness of 22 on the Rockwell C scale.

e) Other forms of hydrogen embrittlement are wet hydrogen sulfide cracking, hydrogen stress cracking, hydrogen-induced cracking (HIC), and stress-oriented hydrogen-induced cracking (SOHIC). In each case, three basic elements are required for this damage mechanism — susceptible material, hydrogen generating environments, and stress (either residual or applied). Organic or inorganic coatings, alloy cladding or linings, are often used as a barrier to mitigate wet H_2S corrosion and subsequent cracking.

3.4.5 HIGH-TEMPERATURE HYDROGEN ATTACK

a) Hydrogen attack is a concern primarily in refinery and petrochemical plant equipment handling hydrogen and hydrogen-hydrocarbon streams at temperatures above 450°F (232°C) and pressure above 100 psi (700 kPa). A guideline for selection of steels to avoid hydrogen attack is given in API Publication 941, "Steels for Hydrogen Service at Elevated Temperatures and Pressures in Petrochemical Refineries and Petrochemical Plants." Also widely known as the "Nelson Curves," API 941 shows that the severity of hydrogen attack depends on temperature, hydrogen partial pressure, exposure time, and steel composition. Additions of chromium and molybdenum increase resistance to hydrogen attack. It is important to understand that hydrogen attack is different from hydrogen embrittlement, which is discussed in NBIC Part 2, 3.4.4.

b) Hydrogen attack occurs in a high-temperature, high-pressure hydrogen environment that can degrade the mechanical strength of carbon and low alloy steels. The damage is caused by hydrogen permeating into the steel and reacting with carbon to form methane. Since carbon is an element that strengthens steel, its removal by the high-temperature reaction with hydrogen causes the steel to lose strength. In addition, methane can become trapped within the steel at high pressures, eventually forming bubbles, fissures (cracks), and/or blisters.

c) Damage caused by hydrogen attack is preceded by an incubation period with no noticeable change in properties. After the incubation period, decarburization and/or blistering and fissuring will occur. The length of the incubation period varies with service temperature, the partial pressure of hydrogen, and alloy content of the steel. Damage is reversible during the incubation period, during which no loss of mechanical properties will have occurred. Once permanent degradation begins, the damage is irreversible.

3.4.6 HYDROGEN DAMAGE

a) Hydrogen damage has been encountered in steam boilers that operate in the high-pressure range (1,200 psi [8.27 MPa] or higher), with relatively high-purity boiler feedwater. In boilers, the mechanism of hydrogen damage is initiated by underdeposit corrosion on water-touched surfaces. During operation of the boiler, waterwall tubing exposed to high heat flux can result in a departure from nucleate boiling (DNB) condition on the ID (waterside) surface due to small flow disturbances. Because of the increased tube metal temperature, low levels of contaminants in the boiler feedwater precipitate (e.g., plate out) on the hot tube surface. The intermittent wetting from flow, over time, results in the accumulation of deposits.

b) As the deposit begins to thicken, the tube metal beneath the deposit locally increases in temperature, causing oxidation of the tube metal. The oxidation/reduction corrosion mechanism creates atomic hydrogen, which permeates into the tube wall at boiler pressures greater than 1,200 psig (8.27 MPa).

c) The atomic hydrogen reacts with the carbon in the steel, forming methane gas that results in microfissures at grain boundaries and decarburization. The combination of decarburization and microcracks increases the susceptibility to brittle fracture in service. The typical appearance of hydrogen damage in boiler tubes is a thick-lipped, "window-type" blow out of tube metal.

d) Hydrogen damage in copper and copper alloys has also been observed and is sometimes known as steam embrittlement. This type of damage commonly occurs when the copper contains oxygen. Hydrogen entering the metal reacts with the oxygen to form water. At certain combinations of pressures and

temperatures steam forms and the pressure generated is sufficient to produce micro-cavity formation and cracking.

3.4.7 BULGES AND BLISTERS

a) A bulge may be caused by overheating of the entire thickness of the metal, thereby lowering the strength of the metal which is then deformed by the pressure. Bulges may also be caused by creep or temperature gradients.

b) A blister may be caused by a defect in the metal, such as a lamination, where the side exposed to the fire overheats but the other side retains its strength due to cooling effect of water or other medium. Blisters may also be caused by a hydrogen environment (See NBIC Part 2, 3.4.5).

3.4.8 OVERHEATING

a) Overheating is one of the most serious causes of deterioration. Deformation and possible rupture of pressure parts may result.

b) Attention should be given to surfaces that have either been exposed to fire or to operating temperatures that exceed their design limit. It should be observed whether any part has become deformed due to bulging or blistering. If a bulge or blister reduces the integrity of the component or when evidence of leakage is noted coming from those defects, proper repairs must be made.

3.4.9 CRACKS

a) Cracks may result from flaws existing in material or excessive cyclic stresses. Cracking can be caused by fatigue of the metal due to continual flexing and may be accelerated by corrosion. Fire cracks are caused by the thermal differential when the cooling effect of the water is not adequate to transfer the heat from the metal surfaces exposed to the fire. Some cracks result from a combination of all these causes mentioned.

b) Cracks noted in shell plates and fire cracks that run from the edge of the plate into the rivet holes of girth seams should be repaired. Thermal fatigue cracks determined by engineering evaluation to be self arresting may be left in place.

c) Areas where cracks are most likely to appear should be examined. This includes the ligaments between tube holes, from and between rivet holes, any flange where there may be repeated flexing of the plate during operation, and around welded connections.

d) Lap joints are subject to cracking where the plates lap in the longitudinal seam. If there is any evidence of leakage or other distress at this point, the Inspector shall thoroughly examine the area and, if necessary, have the plate notched or slotted in order to determine whether cracks exist in the seam. Repairs of lap joint cracks on longitudinal seams are prohibited.

e) Where cracks are suspected, it may be necessary to subject the pressure-retaining item to a pressure test or a nondestructive examination to determine their presence and location.

For additional information regarding a crack or determining extent of a possible defect, a pressure test may be performed per NBIC Part 2, 4.3.1.

f) Cracks shall either be repaired or formally evaluated by crack propagation analysis to quantify their existing mechanical integrity.

PART 2, SECTION 4
INSPECTION — EXAMINATIONS, TEST METHODS, AND EVALUATIONS

4.1 SCOPE

This section describes acceptable examination and test methods that are available to the Inspector during inspection of pressure-retaining items. This section also describes evaluation of test results and assessment methodologies.

4.2 NONDESTRUCTIVE EXAMINATION METHODS (NDE)

a) Listed below is a variety of nondestructive examination methods that may be employed to assess the condition of pressure-retaining items. The skill, experience, and integrity of the personnel performing these examinations are essential to obtain meaningful results. The Inspector should review the methods and procedures to be employed to ensure compliance with jurisdictional requirements.

b) Generally, some form of surface preparation will be required prior to use of these examination methods. When there is doubt as to the extent of a defect or detrimental condition found in a pressure-retaining item, the Inspector is cautioned to seek competent technical advice and supplemental NDE.

c) Personnel performing examination and test methods shall have proper training and certification, as required by the owner and acceptable to the Inspector and Jurisdiction, if required.

4.2.1 VISUAL

a) Visual examination is the basic method used when conducting an inservice inspection of pressure-retaining items. Additional examination and test methods may be required at the discretion of the Inspector to provide additional information to assess the condition of the pressure-retaining item.

b) Visual examination is an inspection method to ascertain the surface condition of the pressure-retaining item. The Inspector should be aware of recognizing various surface features and comparing these features with damage mechanisms listed in NBIC Part 2, Section 3 that could indicate exposure of the pressure-retaining item to harmful corrosion or elevated temperature service.

c) In some cases the Inspector may have limited or no access while performing an inspection of the pressure-retaining item. Subject to approval of the Jurisdiction, remote camera or fiber optic devices may be considered acceptable methods to view and record the surface condition of the pressure-retaining item.

4.2.2 MAGNETIC PARTICLE

a) The magnetic particle examination method can be used only on ferromagnetic materials to reveal surface discontinuities and to a limited degree, those located below the surface. It uses the principle that magnetic lines of force will attract magnetizable material. The sensitivity of this method decreases rapidly with depth below the surface being examined and, therefore, it is used primarily to examine for surface discontinuities.

b) In order to use this method, a magnetic field has to be established within the material to be examined. This can be done directly by bringing a strong magnetic field into close proximity of the item being examined or by inducing a magnetic field in the object by passing electric current through the object.

c) If there is a discontinuity at or near the surface, it will deflect the magnetic lines of force out of the object, thus creating a north pole (magnetic lines leave the north pole of a magnet). The magnetic lines of force will re-enter the test object on the other side of the discontinuity, thereby creating a south pole (magnetic lines enter the south pole of a magnet). Since a north and a south pole have been created,

they will attract magnetizable objects. Iron powder placed on the discontinuity is held in place by the lines of force and will be visible on the surface of the test object

4.2.3 LIQUID PENETRANT

a) The liquid penetrant examination method is used to detect discontinuities that are open to the surface of the material being examined. This method may be used on both ferrous and nonferrous materials. Liquid penetrant examination may be used for the detection of surface discontinuities such as cracks, seams, laps, cold shuts, laminations, and porosity.

b) Liquid penetrant examination works by applying a colored liquid (penetrant) to the object to be examined. Time is allowed for the liquid to fill any voids that are open to the surface. Excess penetrant is then removed and a “developer” is applied in a uniform, thin coating. The developer acts as a blotter and draws the penetrant out of the discontinuity. The developer is usually of a contrasting color to the penetrant. The penetrant indications will appear as colored figures on a background of the developer.

c) Liquid penetrant examination is portable, fast, and requires minimal operator training.

4.2.4 ULTRASONIC

Ultrasonic testing is used for volumetric examination of welds and base materials (metallic and nonmetallic) for detection of flaws. This method depends on sound waves of very high frequency being transmitted through metal and reflected at any boundary, such as a metal to air boundary at the surface of the metal or metal crack boundary at a discontinuity. High-frequency sound waves can detect small irregularities but are easily absorbed, particularly by coarse-grained materials. Sound waves can be introduced into a part either normal to the surface or at predetermined angles. Factors such as material composition, surface condition, choice of equipment, and ability of the operator affect the results of ultrasonic inspection. Ultrasonic testing can also be used to measure material thickness.

4.2.5 RADIOGRAPHY

a) Radiography is a volumetric method that can detect discontinuities throughout a material. This method is commonly used to examine for surface and subsurface discontinuities. The use of this method may be restricted due to the configuration of the welded joint or the limitations of the radiographic equipment. Radiography will not give an indication of the depth of discontinuity unless special procedures are used.

b) The method uses a high-energy gamma ray or x-ray source to penetrate the material to be examined. The rays are absorbed, reflected, and refracted by the material, but some of the energy passes completely through. The energy of rays that pass completely through is determined by the thickness and other physical properties of the material.

c) Radiography uses film to detect the rays that penetrate the material. The higher the energy of the rays, the darker the film will become, similar to exposing photographic film to sunlight.

d) Most discontinuities (cracks, porosity, and inclusions) reduce the amount of base material available to absorb (attenuate) x-rays or gamma rays, thus allowing more energy to pass through the material. Most discontinuities will appear as dark shapes on the radiographic film.

e) The technique used for radiography depends largely on the equipment used and what experience has shown will produce the best results. It is not the function of the technician to indicate the procedure to be followed, provided the procedure and films satisfy all requirements of the applicable code of construction. The radiographic film provides a permanent record of the results of the examination.

4.2.6 EDDY CURRENT

Eddy current is an examination method that measures changes in a magnetic field caused by discontinuities. Eddy current can also detect a loss of material on inaccessible surfaces and be used to detect changes in hardness of a material. There are three general types of eddy current coils: the concentric coil, which surrounds the part to be tested (e.g., tubing); the probe coil, which is brought adjacent to the part to be tested; and the bobbin coil, which is inserted into the part to be tested (e.g., tubing).

4.2.7 METALLOGRAPHIC

Metallographic examination is a method of locally polishing, etching, and viewing the surface of a pressure-retaining item with either acetate tape (e.g., replication) or a field microscope to determine the condition of the metal microstructure.

4.2.8 ACOUSTIC EMISSION

Acoustic emission is a method of detecting and monitoring discontinuities in a pressure-retaining item or load-bearing structure. This method utilizes wave guides, transducers, cables, and a sophisticated data acquisition system to collect transient acoustic emissions generated by the rapid release of energy from localized sources within the material being tested. Signal amplitude, frequency, and location are collected for many hours of operation at various loads or pressures. Analysis of the data can determine if any part of the system requires additional nondestructive examination with a more sensitive test method.

4.3 TESTING METHODS

All testing methods should be performed by experienced personnel using written procedures acceptable to the Inspector.

4.3.1 PRESSURE TESTING

a) During an inspection, there may be certain instances where inservice conditions have adversely affected the leak tightness or the inspection discloses unusual, hard to evaluate forms of deterioration that may affect the pressure-retaining capability of the pressure retaining item. In these specific instances, a pressure test using an incompressible liquid, water, or other suitable test medium may be required at the discretion of the Inspector to assess pressure boundary integrity of the pressure-retaining item.

b) The Inspector is cautioned that a pressure test will not provide any indication of amount of remaining service life or the future reliability of a pressure-retaining item. The pressure test only serves to determine if the item contains defects that will not allow the item to retain pressure. In certain instances, pressure tests of inservice items may reduce remaining service life due to causing permanent deformation.

c) Use of pressure test methods written or otherwise, shall be in agreement between the owner or user and Inspector.

   All instrumentation, including pressure and temperature gages, used to monitor a test shall be properly calibrated.

   When contamination of vessel contents by water is prohibited or when a liquid pressure test is not practical due to weight or other considerations, alternate test media may be used provided precautionary requirements of the applicable section of the original construction code or other standards are followed. In such cases, there shall be agreement as to the testing procedure between the owner or user and the Inspector.

Pressure testing shall not be conducted using flammable or toxic fluids.

NOTE: The requirements of NBIC Part 3 shall be followed when performing a liquid pressure test following repair or alteration of a pressure-retaining item.

4.3.1.1 ALL PRESSURE TESTING

Careful design of test procedure can limit potential damage. For testing of pressure-retaining items, parameters that should be considered are the test media, test pressure, materials of construction and material temperature and temperature of test media. Some carbon steel and low-alloy steel materials that were manufactured prior to 1970 may not have sufficient notch toughness to prevent brittle fracture during pressure testing conducted at, or even above, the generally acceptable temperature of 60°F (16°C).

For thick-walled pressure-retaining items, it is recommended to seek technical guidance in establishing notch toughness characteristics of steel plate prior to pressure testing so that the material temperature may be warmed above 60˚F (16˚C) to avoid brittle fracture.

The organization making any pressure test shall determine pressure-retaining item material has adequate notch toughness at the minimum temperature of the material and test media during pressure test.

4.3.1.2 LIQUID PRESSURE TESTING

Test pressure should be selected or adjusted in agreement between the Inspector and owner or user.

The liquid test pressure shall not exceed the lesser of 150% of MAWP or test pressure established by the original code of construction.

When a pressure relief device is left in place, test pressure should not exceed 90% of set pressure of the lowest setting pressure relief device on the pressure-retaining item to avoid damage to pressure relief devices.

During a liquid pressure test where test pressure will exceed 90% of set pressure of a pressure relief device, the device shall be removed whenever possible. If removal of valve-type devices is not possible or practical, a spindle restraint such as a gag may be used provided that the valve manufacturer's instructions and recommendations are followed. Extreme caution should be employed to ensure only enough force is applied to contain pressure. Excessive mechanical force applied to the spindle restraint may result in damage to the seat and/or spindle and may interfere with proper operation of the valve. The spindle restraint shall be removed following the test.

The organization that performs the liquid pressure test and applies a spindle restraint shall attach a metal tag that identifies the organization with the date the work was performed to the pressure relieving device. If the seal was broken, the organization shall reseal the adjustment housing with a seal that identifies the responsible organization. The process shall be acceptable to the Jurisdiction where pressure-retaining items are installed.

Metal temperature shall not be more than 120°F (49°C) unless the owner or user specifies the requirement for a higher test temperature. If the owner or user specifies a test temperature higher than 120°F (49°C), then precautions shall be taken to afford the Inspector close examination without risk of injury.

Hold-time for liquid pressure tests shall be for a minimum of 10 minutes prior to examination by the Inspector. Test pressure shall be maintained for the time necessary for the Inspector to conduct inspection.

4.3.1.3 PNEUMATIC PRESSURE TESTING

A pressure test using a compressible gas should not be considered due to potential hazard unless a liquid pressure test cannot be performed without damaging the pressure-retaining item or causing contamination of internal surfaces of the pressure-retaining item.

Concurrence of the owner and Inspector shall be obtained and the Jurisdiction, where required, prior to conducting a pneumatic test. The test pressure shall be the minimum required to verify leak tightness integrity but shall not exceed maximum pneumatic test pressure of the original code of construction. Precautionary requirements of the original code of construction shall be followed.

WARNING: Adequate safety precautions shall be taken to ensure personnel safety when a compressible gas is used due to volumetric expansion potential upon release of pressure test gas. Consideration shall be given to possible asphyxiation hazards.

Properly calibrated instrumentation shall be used to detect leakage of testing medium. Instrumentation selected shall be appropriate for the test medium. Instrumentation may detect changes in pressure or chemical concentrations and shall be sensitive enough to detect leakage.

4.4 METHODS TO ASSESS DAMAGE MECHANISMS AND INSPECTION FREQUENCY FOR PRESSURE-RETAINING ITEMS

4.4.1 SCOPE

a) This section provides guidelines and alternative methods to assess materials and pressure-retaining items subject to degradation or containing flaws identified during inservice inspections or examinations. New pressure-retaining items are placed in service to operate within their intended design parameters for a period of time determined by service conditions, which can include exposure to corrosion, exposure to elevated temperature (creep), or other forms of damage. If the pressure-retaining item is to remain safe in operation, the service conditions and the length of time before the next inspection must be identified. There are various methods that can be used to assess the condition of a pressure-retaining item to establish remaining service life and to ultimately determine the inspection interval. In some cases, a visual inspection of the pressure-retaining item will suffice. However, more comprehensive condition assessment methods may be required, including an engineering evaluation performed by a competent technical source.

b) Various assessment methods (see NBIC Part 2, 1.3), including those mentioned in this section (an example of guidelines for performing fitness for service assessments are referenced in API recommended practice API-579 “Fitness-for-Service”), can be used to establish the next inspection interval of a pressure-retaining item and to ensure safe operation. Condition assessment methods shall be subject to review and acceptance by the Jurisdiction.

c) Safe and adequate implementation of Fitness for Service Assessment (FFSA) programs is the responsibility of the owner or user. Responsibility includes verifying and understanding jurisdictional rules/regulations and inservice inspection requirements. Application of these programs may result in decisions that will deviate from or conflict with jurisdictional requirements (e.g., frequency or types of inspections, repairs and alterations, etc.). The Inspector and Jurisdiction shall be contacted for acceptance, as appropriate, prior to implementing decisions that deviate from or conflict with established requirements.

d) If required by the Jurisdiction, FFSA shall be documented on a Report of FFSA Form NB-403, as shown in NBIC Part 2, 5.3.7. Preparation of the Report of FFSA shall be the responsibility of the owner or user. An Inspector shall indicate acceptance by signing the Report of FFSA. Legible copies of the FFSA report shall be distributed to the Jurisdiction, and the Authorized Inspection Agency responsible for the inservice inspection. The owner or user shall maintain a copy of the FFSA report in the relevant equipment inspection history file.

4.4.2 GENERAL REQUIREMENTS

a) Organizations or qualified individuals with experience in inspection, design, construction, repairs, or failure analysis of pressure-retaining items should be consulted to assist in identifying damage mechanisms, and to evaluate condition assessment results of pressure-retaining items. Documentation and

inspection data used for fitness for service assessment should be evaluated for compliance, with codes, industry standards/experience or good engineering practices, and shall be acceptable to the Jurisdiction. Understanding the operation of equipment or systems and interaction with their internal or external service environment is necessary to correctly identify damage mechanisms.

b) There are various condition assessment and fitness for service methods that can be used to determine inspection intervals, based on calculating the remaining service life of the pressure-retaining item. For items subject to corrosion or erosion, the method to determine or adjust inspection intervals is identified in NBIC Part 2, 4.4.7. Methods for assessing other types of inservice damage that affect remaining service life of pressure-retaining items are identified in NBIC Part 2, 4.4.8.

4.4.3 RESPONSIBILITIES

a) Owner or User

The owner or user of the pressure-retaining item is responsible for the selection and application of a suitable fitness for service or condition assessment methodology described in this section, subject to review and approval by the Jurisdiction, if required.

b) Inspector

The Inspector shall review the condition assessment methodology and ensure inspection data and documentation are in accordance with this section.

4.4.4 REMAINING SERVICE LIFE ASSESSMENT METHODOLOGY

a) An evaluation of inservice damage using one or more condition assessment methods is not intended to provide a precise determination of the actual time to failure for a pressure-retaining item. Instead, the extent of inservice damage should be estimated based on the quality of available information, established engineering assessment guidelines or methodology and appropriate assumptions used for safety, operation, and inspection.

b) If inspection and engineering assessment results indicate that a pressure-retaining item is safe for continued operation, future monitoring and inspection intervals should be determined and submitted to the Jurisdiction for review and approval. If an engineering assessment indicates that a pressure-retaining item is not suitable for service under current operating conditions, new operating conditions should be established (i.e., de-rate), or the item could be repaired subject to revised inspection intervals, or the item could be replaced.

c) Determination of the extent of inservice damage life requires the following:

1) Understanding applicable damage and failure mechanisms;

2) Developing inspection plans that can monitor the extent of inservice damage;

3) Performing an assessment of the damage including estimation of remaining life;

4) Considerations needed to minimize risk of failure;

5) Determination of root cause; and

6) Corrective measures.

4.4.5 DATA REQUIREMENTS FOR REMAINING SERVICE LIFE ASSESSMENTS

Evaluating the extent of inservice damage to a pressure-retaining item requires an understanding of known and potential damage mechanisms. Information that can be used to evaluate service life can be divided into

three categories: inspection history, operating and maintenance history, and equipment information. Examples of types of data are listed below:

a) Inspection history

1) Summary/records of repairs and alterations;

2) Test records including pressure tests;

3) Results of prior inservice examinations (NDE methods, thickness measurements, and corrosion rate); and

4) Physical measurements or inspections.

b) Operating history/conditions

1) Operating logs including pressure, temperature, startups/shutdowns, cycles;

2) Consultation with operating personnel to determine operating history;

3) Date of installation;

4) Identification of internal and external environmental conditions to include pressure, temperature, age, design, chemical and mechanical environment, loadings, processes, etc.;

5) List of damage mechanisms identified in the past and that may be present based on materials, contaminants, and operating conditions;

6) Identification of the damage mechanisms presently active or which may become active; and

7) Identification of the failure modes associated with the identified damage mechanisms, (e.g., leaks, cracks, bursts, etc.).

c) Equipment formation

1) Manufacturer's Data Reports;

2) Material Test Reports;

3) Drawings; and

4) Original design calculations/specifications.

4.4.6 IDENTIFICATION OF DAMAGE MECHANISMS

a) There are a variety of damage mechanisms that may affect the remaining service life of a pressure-retaining item. Damage mechanisms will cause either micro or macro changes to the material, affecting its conditions or properties. Damage mechanisms may be difficult to assess, therefore, detailed methods of evaluation for each damage mechanism should be performed in accordance with established industry practices or other acceptable standards should be followed (See NBIC Part 2, 1.3). These results should be evaluated and the inspection interval reviewed for possible adjustment. Various failure modes are described in NBIC Part 2, Section 3.

b) Common forms of damage and damage mechanisms that affect remaining service life evaluations are listed below:

1) Bulging;

2) Sagging;

3) Stress corrosion cracking;

4) Corrosion (local or general);

5) Creep;

6) Thermal or mechanical fatigue;

7) Hydrogen damage;

8) Metallurgical changes; and

9) Erosion.

c) Damage may also be caused by mechanical forces such as thermal shock, cyclic temperature changes, vibration, pressure surges, excessive temperature, external loading, and material and fabrication defects.

4.4.7 DETERMINING INSPECTION INTERVALS

a) The maximum period between internal inspections or a complete inservice evaluation of pressure-retaining items shall not exceed one-half of the estimated remaining service life of the vessel or ten years, whichever is less. The method for estimating inspection intervals of pressure-retaining items subject to internal erosion or corrosion is discussed in NBIC Part 2, 4.4.7.1 and 4.4.7.2.

b) Inspection intervals can be revised beyond the maximum period stated above, provided the owner or user has submitted technical justification for revising the inspection interval, subject to review and acceptance by the Jurisdiction, where required.

c) Data used in engineering assessment methods to develop revised inspection intervals for pressure-retaining items shall be re-evaluated every five years, when a change in operation occurs, or after discovery of new and/or altered damage mechanisms.

4.4.7.1 METHOD FOR ESTIMATING INSPECTION INTERVALS FOR PRESSURE-RETAINING ITEMS SUBJECT TO EROSION OR CORROSION

Assessment guidelines for pressure-retaining items subject to corrosion or erosion are provided in this Section. These guidelines are based on actual thickness measurements within the area of concern. Minimum required wall thickness shall be based on allowable stress of the material. Applicability and limitations of this guideline are as follows:

a) Original design criteria are known;

b) Item is not operating in the creep range;

c) Item does not contain crack-like indications;

d) Service stresses are known; and

e) Maintenance and operating history are known.

4.4.7.2 METHOD FOR ESTIMATING INSPECTION INTERVALS FOR EXPOSURE TO CORROSION

a) When the pressure-retaining item is exposed to service temperatures below the creep range, and the corrosion rate controls the remaining wall thickness of the pressure-retaining item, the inspection

interval shall be calculated by the formula below or by other industry methods as accepted by the Jurisdiction.

remaining life (years) = $(t_{(actual)} - t_{(required)})$ / corrosion rate

$t_{(actual)}$ = thickness in inches (mm) measured at the time of inspection for the limiting section used in the determination of $t_{(required)}$.

$t_{(required)}$ = minimum allowable thickness in inches (mm) for the limiting section of the pressure-retaining item or zone. It shall be the greater of the following:

1) The calculated thickness, exclusive of the corrosion allowance, required for the pressure relieving device set pressure, static head, or other loading and design temperature, or

2) The minimum thickness permitted by the provision of the applicable section of the original code of construction.

Corrosion Rate = inches (mm) per year of metal removal as a result of corrosion.

b) Any suitable nondestructive examination method may be used to obtain thickness measurements, provided the instruments employed are calibrated in accordance with the manufacturer's specification or an acceptable national standard.

1) If suitably located existing openings are available, measurements may be taken through the openings.

2) When it is impossible to determine thickness by nondestructive means, a hole may be drilled through the metal wall and thickness gage measurements taken.

c) For new pressure-retaining items or PRIs for which service conditions are being changed, one of the following methods shall be employed to determine the probable rate of corrosion from which the remaining wall thickness, at the time of the next inspection, can be estimated:

1) The corrosion rate as established by data for pressure-retaining items in the same or similar service;

2) If the probable corrosion rate cannot be determined by the above method, on-stream thickness determinations shall be made after approximately 1,000 hours of service. Subsequent sets of thickness measurements shall be taken after additional similar intervals until the corrosion rate is established.

d) Corrosion-resistant Lining

When part or all of the pressure-retaining items have a corrosion-resistant lining, the interval between inspections of those sections so protected may be based on recorded experience with the same type of lining in similar service, but shall not exceed ten years, unless sufficient data has been provided to establish an alternative inspection interval. If there is no experience on which to base the interval between inspections, performance of the liner shall be monitored by a suitable means, such as the use of removable corrosion probes of the same material as the lining, ultrasonic examination, or radiography. To check the effectiveness of an internal insulation liner, metal temperatures may be obtained by surveying the pressure-retaining item with temperature measuring or indicating devices.

e) Two or more zones

When a pressure-retaining item has two or more zones of pressure or temperature and the required thickness, corrosion allowance, or corrosion rate differ so much that the foregoing provisions give significant differences in maximum periods between inspections for the respective zones (e.g., the upper

and lower portions of some fractionating towers), the period between inspections may be established individually for each zone on the basis of the condition applicable thereto, instead of being established for the entire vessel on the basis of the zone requiring the more frequent inspection.

f) Above-Ground Pressure Vessels

All pressure vessels above ground shall be given an external examination after operating the lesser of five years, or one quarter of remaining life, preferably while in operation. Alternative intervals resulting in longer periods may be assigned provided the requirements of this section have been followed. Inspection shall include determining the condition of the exterior insulation, the supports, and the general alignment of the vessel on its supports. Pressure vessels that are known to have a remaining life of over ten years or that are prevented from being exposed to external corrosion (such as being installed in a cold box in which the atmosphere is purged with an inert gas, or by the temperature being maintained sufficiently low or sufficiently high to preclude the presence of water), need not have the insulation removed for the external inspection. However, the condition of the insulating system and/or the outer jacketing, such as the cold box shell, shall be observed periodically and repaired if necessary.

g) Interrupted service

1) The periods for inspection referred to above assume that the pressure-retaining item is in continuous operation, interrupted only by normal shutdown intervals. If a pressure-retaining item is out of service for an extended interval, the effect of the environmental conditions during such an interval shall be considered.

2) If the pressure-retaining item was improperly stored, exposed to a detrimental environment or the condition is suspect, it shall be given an inspection before being placed into service.

3) The date of next inspection, which was established at the previous inspection, shall be revised if damage occurred during the period of interrupted service.

h) Circumferential stresses

For an area affected by a general corrosion in which the circumferential stresses govern the MAWP, the least thicknesses along the most critical plane of such area may be averaged over a length not exceeding:

1) The lesser of one-half the pressure vessel diameter, or 20 in. (500 mm) for vessels with inside diameters of 60 in. (1.5 m) or less, or

2) The lesser of one-third the pressure vessel diameter, or 40 in. (1 m), for vessels with inside diameters greater than 60 in. (1.5 m), except that if the area contains an opening, the distance within which thicknesses may be averaged on either side of such opening shall not extend beyond the limits of reinforcement as defined in the applicable section of the ASME Code for ASME Stamped vessels and for other vessels in their applicable codes of construction.

i) Longitudinal stresses

If because of wind loads or other factors the longitudinal stresses would be of importance, the least thicknesses in a length of arc in the most critical plane perpendicular to the axis of the pressure vessel may be averaged for computation of the longitudinal stresses. The thicknesses used for determining corrosion rates at the respective locations shall be the most critical value of average thickness. The potential for buckling shall also be considered.

j) Local metal loss

Corrosion pitting shall be evaluated in accordance with NBIC Part 2, 4.4.8.7. Widely scattered corrosion pits may be left in the pressure-retaining item in accordance with the following requirements:

1) Their depth is not more than one-half the required thickness of the pressure-retaining item wall (exclusive of corrosion allowance);

2) The total area of the pits does not exceed 7 sq. in. (4,500 sq mm) within any 50 sq. inches (32,000 sq. mm); and

3) The sum of their dimensions (depth and width) along any straight line within this area does not exceed 2 in. (50 mm).

k) Weld joint efficiency factor

When the surface at a weld having a joint efficiency factor of other than one is corroded as well as surfaces remote from the weld, an independent calculation using the appropriate weld joint efficiency factor shall be made to determine if the thickness at the weld or remote from the weld governs the maximum allowable working pressure. For the purpose of this calculation, the surface at a weld includes 1 in. (25 mm) on either side of the weld, or two times the minimum thickness on either side of the weld, whichever is greater.

l) Formed heads

1) When evaluating the remaining service life for ellipsoidal, hemispherical, torispherical or toriconical shaped heads, the minimum thickness may be calculated by:

a) Formulas used in original construction, or

b) Where the head contains more than one radii of curvature, the appropriate strength formula for a given radius.

2) When either integral or non-integral attachments exist in the area of a knuckle radius, the fatigue and strain effects that these attachments create shall also be considered.

m) Adjustments in corrosion rate

If, upon measuring the wall thickness at any inspection, it is found that an inaccurate rate of corrosion has been assumed, the corrosion rate to be used for determining the inspection frequency shall be adjusted to conform with the actual rate found.

n) Riveted construction

For a pressure-retaining item with riveted joints, in which the strength of one or more of the joints is a governing factor in establishing the maximum allowable working pressure, consideration shall be given as to whether, and to what extent, corrosion will change the possible modes of failure through such joints. Also, even though no additional thickness may have originally been provided for corrosion allowance at such joints, credit may be taken for the corrosion allowance inherent in the joint design.

4.4.7.3 ESTIMATING INSPECTION INTERVALS FOR PRESSURE-RETAINING ITEMS WHERE CORROSION IS NOT A FACTOR

When the corrosion rate of a pressure-retaining item is not measurable, the item need not be inspected internally provided all of the following conditions are met and complete external inspections, including thickness measurements, are made periodically on the vessel.

a) The non-corrosive character of the content, including the effect of trace elements, has been established by at least five years comparable service experience with the fluid being handled.

b) No questionable condition is disclosed by external inspection.

c) The operating temperature of the pressure-retaining item does not exceed the lower limits for the creep range of the vessel metal. Refer to NBIC Part 2, Table 4.4.8.1.

d) The pressure-retaining item is protected against inadvertent contamination.

4.4.8 EVALUATING INSPECTION INTERVALS OF PRESSURE-RETAINING ITEMS EXPOSED TO INSERVICE FAILURE MECHANISMS

Pressure-retaining items are subject to a variety of inservice failure mechanisms that are not associated with corrosion. The following provides a summary of evaluation processes that may require a technical evaluation to assess resultant inspection intervals.

4.4.8.1 EXPOSURE TO ELEVATED TEMPERATURE (CREEP)

a) The owner or user of the pressure-retaining item and the Inspector are cautioned to seek competent technical advice to determine which of the condition assessment methods can be used to ensure safe operation and determination of the next inspection interval for the pressure-retaining item when elevated service temperature is a consideration.

b) When creep damage is suspected in a pressure-retaining item, an assessment of remaining service life should be determined either by the owner or user of the pressure-retaining item or a competent engineer. This assessment may include, but is not limited to, the following methods:

1) Dimensional measurements of the item to check for creep;

2) Measurement of oxide scale and wall thickness for use in engineering analysis to determine remaining service life. Creep life can be predicted through an empirical approach that uses available data for the pressure-retaining component; total number of operating hours to the present is needed. Oxide scale thickness (steam side) can be measured directly from material samples or be measured in situ using ultrasonic techniques;

3) Metallographic examination to determine the extent of exposure to creep damage; and

4) After removal of a material sample for creep rupture testing, a test matrix is selected to yield the most meaningful results from the sample. Test specimens are machined from the sample and tested under representative loads and temperatures (as selected in the test matrix). Creep strain vs. time and temperature vs. time to rupture data are recorded.

TABLE 4.4.8.1
TEMPERATURES ABOVE WHICH CREEP BECOMES A CONSIDERATION

Carbon steel and C-1/2 Mo and ferritic stainless steels	750°F (400°C)
Low alloy steels (Cr-Mo)	850°F (455°C)
Austenitic stainless Steel	950°F (510°C)
Aluminum alloys	200°F (93°C)

4.4.8.2 EXPOSURE TO BRITTLE FRACTURE

a) Determining susceptibility to brittle fracture should be required as part of the overall assessment for evaluating remaining service life or to avoid failure of the pressure-retaining item during a pressure test. In order to carry out brittle fracture assessment, mechanical design information, materials of construction and materials properties are to be determined. This information is required for pressure-retaining components in order to identify the most limiting component material that governs brittle fracture.

Design information, maintenance/operating history, and information relating to environmental exposure shall be evaluated to determine if there is a risk of brittle fracture.

b) When brittle fracture is a concern, methods to prevent this failure shall be taken. These methods could include changes to operating conditions and further engineering evaluations to be performed by a qualified engineer (metallurgical/corrosion/mechanical). Engineering evaluation methods to prevent brittle fracture shall be reviewed and accepted by the owner or user, Inspector, and Jurisdiction, as required.

4.4.8.3 EVALUATING CONDITIONS THAT CAUSE BULGES/BLISTERS/LAMINATIONS

a) Blistering in pressure-retaining items can result from laminations, inclusions in the metal, or damage mechanisms that occur in service. Procedures for evaluating bulges/blisters/laminations are referenced in applicable standards (see NBIC Part 2, 1.3).

b) An engineering evaluation shall be performed to ensure continued safe operation when bulges/blisters/laminations are identified. If a bulge/blister/lamination is within the specified corrosion allowance, further assessment shall be performed to evaluate any crack-like indications in surrounding base material.

Note: Proximity of crack-like indications in welds and HAZ is important. Cracks and blisters should be evaluated separately.

4.4.8.4 EVALUATING CRACK-LIKE INDICATIONS IN PRESSURE-RETAINING ITEMS

a) Crack-like indications in pressure-retaining items are planar flaws characterized by length and depth with a sharp root radius. Cracks may occur within material or on the surface and may be individual or multiple in nature. In some cases, a conservative approach is to treat aligned porosity, inclusions, undercuts, and overlaps as crack-like indications. It is important that the cause of cracking be identified prior to any further determination of inspection intervals.

b) If crack-like indications are on the surface and within the specified corrosion allowance, removal by blend grinding or air arc gouging can be performed. Measurements shall be taken to ensure minimum thickness is met, and effective monitoring techniques should be established. If a crack-like flaw is not completely removed and repaired, then an engineering fracture mechanics or other evaluation must be performed to verify continued safe operation.

c) There are various methods or approaches for evaluating crack-like indications, some of which are referenced in applicable standards (see NBIC Part 2, 1.3).

4.4.8.5 EVALUATING EXPOSURE OF A PRESSURE-RETAINING ITEM TO FIRE DAMAGE

a) The extreme heat of a fire can produce visual structural damage and less apparent degradation of mechanical properties (decrease in yield strength or fracture toughness). Potential damage includes changes in mechanical properties, decrease in corrosion resistance, distortion, and cracking of pressure boundary components. Distortion of equipment extremities such as ladders and platforms does not necessarily mean that the pressure equipment is no longer suitable for continued service. Process fluid inside the vessel may serve as a cooling medium, thus preserving mechanical properties of the equipment. Instrumentation and wiring are commonly damaged during a fire. Data requirements and history information should be obtained as identified in NBIC Part 2, 4.4.5.

b) Recommended measurements and collection of data for evaluation of fire damage shall include but are not limited to:

1) Concentrated areas of fire damage versus overall fire damage as it relates to normal operation;

2) Determination of cause and origin of fire;

3) Temperature extremes;

4) Nature of the fuel;

5) Source of ignition;

6) Time at temperature;

7) Cooling rate;

8) Photographs taken;

9) Plant personnel interviewed; and

10) Actual strength and toughness properties of the material.

Note: It is important that evidence be maintained in order to perform a proper evaluation.

c) Components subjected to fire damage can exhibit altered mechanical properties, and should be evaluated to determine if the material has retained necessary strength and toughness as specified in the original code of construction. Heating above the lower critical temperature results in a phase transformation that, upon rapid cooling, can dramatically affect material properties. Evaluation methods may consist of:

1) Portable hardness testing;

2) Field metallography or replication;

3) Liquid pressure testing;

4) Magnetic particle testing;

5) Liquid penetrant testing;

6) Visual examination; or

7) Dimensional verification checks.

d) If visual distortion or changes in the microstructure or mechanical properties are noted, consider replacing the component, or a detailed engineering analysis shall be performed to verify continued safe operation.

e) Techniques for evaluating fire damage are referenced in applicable standards. See NBIC Part 2, 1.3.

4.4.8.6 EVALUATING EXPOSURE OF PRESSURE-RETAINING ITEMS TO CYCLIC FATIGUE

a) A fatigue evaluation should be performed if a component is subject to cyclic operation. The allowable number of cycles (mechanical or thermal) at a given level of stress should be adequate for the specified duration of service to determine suitability for continued operation.

b) Data requirements and history information should be obtained as identified in NBIC Part 2, 4.4.5.

c) Techniques for evaluating fatigue are referenced in applicable standards. See NBIC Part 2, 1.3.

4.4.8.7 EVALUATING PRESSURE-RETAINING ITEMS CONTAINING LOCAL THIN AREAS

a) Local thin areas can result from corrosion/erosion, mechanical damage, or blend/grind techniques during fabrication or repair, and may occur internally or externally. Types of local thin areas are grooves,

gouges, and pitting. When evaluating these types of flaws, the following should be considered:

1) Original design and current operating conditions;

2) Component is not operating in the creep range;

3) Material has sufficient toughness;

4) Not operating in cyclic service;

5) Does not contain crack-like indications;

6) Flaws are not located in knuckle regions of heads or conical transitions;

7) Applied loads; and

8) The range of temperature or pressure fluctuation.

b) Where appropriate, crack-like indications should be removed by blend/grinding, and evaluated as a local thin area.

c) Data requirements and history information should be obtained as identified in NBIC Part 2, 4.4.5.

d) Required measurements for evaluation of local thin areas shall include:

1) Thickness profiles within the local region;

2) Flaw dimensions;

3) Flaw to major structural discontinuity spacing;

4) Vessel geometry; and

5) Material properties.

e) Required measurements for evaluation of pitting corrosion shall include:

1) Depth of the pit;

2) Diameter of the pit;

3) Shape of the pit; and

4) Uniformity.

(15) f) Widely scattered corrosion pits may be left in the pressure-retainig item in accordance with the following requirements:

1) Their depth is not more than one-half the required thickness of the pressure-retaining item wall (exclusive of corrosion allowance);

2) The total area of the pits does not exceed 7 in.^{2} (4,500 mm^2) within any 50 in.^{2} (32,000 mm^2); and

3) The sum of their dimensions (depth and width) along any straight line within this 50 in.^{2} (32,000 mm^2) area does not exceed 2 in. (50 mm).

g) If metal loss is less than specified, corrosion/erosion allowance and adequate thickness is available for future corrosion, then monitoring techniques should be established. If metal loss is greater than specified corrosion/erosion allowance and repairs are not performed, and a detailed engineering evaluation shall be performed to ensure continued safe operation.

h) Techniques for evaluating local thin areas and pitting are referenced in applicable standards. See NBIC Part 2, 1.3.

4.5 RISK-BASED INSPECTION ASSESSMENT PROGRAMS

4.5.1 SCOPE

a) This section describes the basic elements, principles, and guidelines of a risk-based inspection (RBI) program. This section does not address any one method but is intended to clarify the elements associated with a RBI program. Risk assessment is a process to evaluate continued safe operation of a pressure-containing component. This process is based on sound engineering practices, proven risk assessment experience, and management principles. There are numerous risk-based assessment methods being applied throughout many industries. Details for developing and implementing risk-based inspection programs are defined in other referenced standards.

b) Implementation of a (RBI) assessment program allows an owner or user to plan inspection frequencies based on assessing probability of failure (POF) and consequence of failure (COF) (risk = POF x COF). Risk assessment programs involve a team concept based on knowledge, training, and experience between engineers, inspectors, operators, analysts, financial, maintenance, and management personnel. Appropriate and responsible decisions must be made from input by all team members to ensure safe operation of systems and their components. Organizational commitment and cooperation is required to successfully implement and maintain a RBI program.

4.5.2 DEFINITIONS

COF — Consequence of failure. Outcome from a failure. There may be one or more outcomes from a single failure.

POF — Probability of failure. Extent to which a failure is likely to occur within a specific time frame.

Risk — A combination of probability of an event occurring and the consequences associated with the event. Risk = (POF x COF).

Risk Assessment — A process of risk analysis and evaluation.

Risk Analysis — Identification and use of information such as historical data, opinions, and concerns to evaluate, treat, and accept risk.

Risk-Based Inspection — Inspection managed through risk assessment.

Risk Criteria — Terms used whereby the significance of risk is assessed, such as personnel safety, cost benefits, legal/statutory requirements, economic/environmental aspects, stakeholders concerns, priorities, etc.

Risk Evaluation — Process to compare risk with given criteria to determine the significance of risk to assist in accepting or mitigating the risk.

Uncertainty — A measure of confidence in the expected value.

4.5.3 GENERAL

Risk-based inspection assessment programs can provide the following benefits for organizations:

a) An overall reduction in risk of equipment failure;

b) Identification of items not requiring inspection or mitigation;

c) An acceptable understanding of the current risk for specific items under consideration;

d) Process safety improvements; by concentrating inspections, maintenance and associated expenditures on items of high risk and reducing efforts on low-risk items;

e) Improved record retention for items by retaining both historical and latest essential data and information needed for assessment;

f) Provides a management tool to continually:

1) Maintain an effective inspection and maintenance program;

2) Improve reliability and safety for operation;

3) Define staffing needs;

4) Evaluate and define funds required;

5) Adjust risk assessment program based on desired results; and

6) Manage uncertainty.

4.5.4 CONSIDERATIONS

Effective risk-based inspection programs should consider the following:

a) Significance of failure to personnel safety;

b) Identifying and obtaining accurate and appropriate information on system or component;

c) Using appropriate inspection methods and types (internal, external, inservice, etc.) frequencies, and understanding limitations;

d) Design requirements;

e) Installation requirements;

f) Operational requirements and limitations;

g) Proper execution of plans;

h) Qualifications and training requirements for personnel;

i) Use and development of procedures;

j) Sound engineering and operating judgment;

k) Effective communication among all affected areas of management and personnel;

l) Jurisdictional and Inspector involvement as required;

m) Human error;

n) Consequential and secondary effects; and

o) Impact of failure on personnel or operations.

4.5.5 KEY ELEMENTS OF AN RBI ASSESSMENT PROGRAM

The following key elements should be included when establishing an RBI program:

a) Establish objectives and goals;

b) Understand risk of operation by identifying effects of inspection, maintenance, operating parameters, and mitigating actions;

c) Defining roles, responsibilities, training, and qualifications;

d) Define risk criteria;

e) Managed actions for acceptable levels of risk;

f) Understanding and meeting safety and environmental requirements;

g) Optimizing expenditures;

h) Assessing mitigation alternatives;

i) Data and information collection;

j) Identifying deterioration mechanisms (see NBIC Part 2, Section 3);

k) Assessing POF and COF;

l) Determining an acceptable risk matrix;

m) Reassessing and updating RBI assessments; and

n) Required documentation and retention.

4.5.6 RBI ASSESSMENT

Assessments provide a systematic approach to screen risk, identify areas of concern, and develop a list for needed inspections or analysis. (POF) and (COF) must first be evaluated separately. Risk is then determined as (POF x COF) to develop a risk ranking measure or estimate.

4.5.6.1 PROBABILITY OF FAILURE

Probability of failure can be expressed in terms of number of events occurring during a specific time frame. There are three main considerations when analyzing POF.

a) Evaluate deterioration mechanisms based on materials and the item's operating environment.

b) Evaluate the impact of deterioration mechanisms on the integrity of the PRI(s).

c) Determine the effectiveness of the inspection program to quantify and monitor deterioration mechanisms either on-or off-line, so that mitigation can be effective prior to failure.

4.5.6.2 CONSEQUENCE OF FAILURE

Consequence analysis involves logic modeling to depict combinations of events to represent effects of failure. These models usually contain one or more failure scenarios. Consequence categories for consideration include the following:

a) Personnel safety;

b) Business/production effects, including cost related to downtime or collateral damage to surrounding equipment;

c) Affected area;

d) Environmental damage;

e) Volume of fluid or gas released;

f) Toxic or flammable events; and

g) Maintenance/repairs/replacement.

4.5.6.3 RISK EVALUATION

Once POF and COF are assessed and assigned, categories of risk can be calculated and evaluated. A risk matrix or plot is helpful to display or present risk without using numerical values with categories such as low, medium, and high typically assigned to identify POF and COF. POF and COF categories can be presented easily to understand and manage risk. Using the risk evaluation, an inspection plan, including proposed inspection frequencies and appropriate inspection methods, is developed and implemented.

4.5.6.4 RISK MANAGEMENT

Based on risk ranking and identifying acceptable thresholds, risk management or mitigation can proceed. When risk is considered unacceptable, the following action should be taken to minimize POF or COF. These may include, but are not limited to, the following:

a) Decommissioning;

b) Increased monitoring/inspection;

c) Repair/replace/maintain;

d) De-rate equipment — needs/limits/cycles;

e) Modifications/redesign;

f) Training; and

g) Enhance process control.

4.5.7 JURISDICTIONAL RELATIONSHIPS

Jurisdictions mandate specific codes/standards with rules or laws that may differ between jurisdictions. Frequency and types of inspections are examples of requirements that may vary. Owners and users implementing RBI assessment plans should understand jurisdictional requirements, so deviations from the mandated types of inspection and frequency of inspection can be requested. Methods used to develop and implement RBI assessment methods and the RBI program developed from those methods shall be acceptable to the Jurisdiction and the Inspector as required.

PART 2, SECTION 5
INSPECTION — STAMPING, DOCUMENTATION, AND FORMS

5.1 SCOPE

This section provides guidelines and requirements for stamping and documentation (forms) for inservice inspections of PRIs. This section also describes evaluation of inspection results and assessment methodologies.

5.2 REPLACEMENT OF STAMPING OR NAMEPLATE

5.2.1 AUTHORIZATION (15)

a) When the stamping on a pressure-retaining item becomes indistinct or the nameplate is lost, illegible, or detached, but traceability to the original pressure-retaining item is still possible, the Inspector shall instruct the owner or user to have the nameplate or stamped data replaced. All re-stamping shall be done in accordance with the original code of construction, except as modified herein. Requests for permission to re-stamp or replace nameplates shall be made to the Jurisdiction in which the nameplate or stamping is reapplied. Application must be made on the *Replacement of Stamped Data Form*, NB-136 (see NBIC Part 2, 5.3.2). Proof of traceability to the original nameplate or stamping and other such data, as is available, shall be furnished with the request. Permission from the Jurisdiction is not required for the reattachment of nameplates that are partially attached. When traceability cannot be established, the Jurisdiction shall be contacted. The completed Form NB-136 (see 5.3.2) shall be submitted to the National Board.

b) When there is no Jurisdiction, the traceability shall be accepted and the replacement of the nameplate or stamped data shall be authorized and witnessed by a National Board Commissioned Inspector. The completed Form NB-136 shall be submitted to the National Board.

5.2.2 REPLACEMENT OF NAMEPLATE OR STAMPED DATA (15)

a) The re-stamping or replacement of data shall be witnessed by a National Board Commissioned Inspector.

b) The re-stamping or replacement of a code symbol stamp shall be performed only as permitted by the governing code of construction.

c) Replacement nameplates shall be clearly marked “replacement.”

5.2.3 REPORTING (15)

Form NB-136 shall be filed with the Jurisdiction by the owner or user (if required) and the National Board by the “R” Stamp Holder bearing a facsimile of the replacement stamping or nameplate, as applied, and shall also bear the signature of the “R” Stamp holder that performed the replacement and the National Board Commissioned Inspector who authorized and witnessed the replacement.

5.3 NATIONAL BOARD INSPECTION FORMS

(15) ### 5.3.1 SCOPE

The following forms 5.3.2 may be used for documenting specific requirements as indicated on the top of each form.

Note: Jurisdictions may have adopted other forms for the same purpose and may not accept these forms.

5.3.2 FORMS

1) **REPLACEMENT OF STAMPED DATA FORM (NB-136)**, see Pg. 77
2) **FORM NB-4 NEW BUSINESS OR DISCONTINUANCE OF BUSINESS**, see Pg. 79
3) **FORM NB-5 BOILER OR PRESSURE VESSEL DATA REPORT**, see Pg. 80
4) **FORM NB-6 BOILER-FIRED PRESSURE VESSELS REPORT OF INSPECTION**, see Pg. 82
5) **FORM NB-7 PRESSURE VESSELS REPORT OF INSPECTION**, see Pg. 83
6) **FORM NB-403 REPORT OF FITNESS FOR SERVICE ASSESSMENT**, see Pg. 85

5.3.3 GUIDE FOR COMPLETING FITNESS FOR SERVICE ASSESSMENT REPORTS

1) For tracking and reference purposes, indicate the sequential Fitness for Service Assessment number.
2) Name and address of the owner of the equipment that is being assessed for Fitness for Service.
3) Name and address of the organization or individual performing the Fitness for Service Assessment.
4) Name and address of the facility where the equipment being assessed for Fitness for Service is located.
5) Name of the Jurisdiction where the assessed equipment is located.
6) Identification of equipment, including manufacturer, manufacturer's serial number, National Board number, Jurisdiction-assigned registration number, and year built. Also include equipment/component material specification/grade, design and operating pressures, design and operating temperatures, if applicable.
7) Indicate the name, section, division, edition, and addenda of the original code of construction.
8) Name of the standard used to perform the Fitness for Service Assessment.
9) Description of the equipment / component damage mechanism or flaw types considered in the Fitness for Service Assessment.
10) Description of the Fitness for Service Assessment level and technique. Attach all relevant Fitness for Service Assessment procedures and detailed documentation.
11) Description of the Inspection and NDE results as prescribed in the Fitness for Service Assessment analysis.
12) Description of the failure, damage and/or deterioration modes identified in the Fitness for Service Assessment.
13) Indicate the results of the Fitness for Service Assessment, including remediation recommendations.

14) Indicate if the equipment can continue current operation.

15) Indicate if repairs are required.

16) Indicate if equipment replacement is required.

17) Indicate if continued operation has a finite date.

18) Indicate finite date of continued operation (if applicable).

19) Indicate the required Inspection intervals as determined by the Fitness for Service Assessment.

20) Indicate the required inservice monitoring methods and intervals for the equipment as defined by the Fitness for Service Assessment.

21) Describe any operating or inservice limitations for the equipment. This would include any reductions / changes in operating pressures or temperatures.

22) Type or print the name of the representative of the Organization or individual performing the Fitness for Service Assessment.

23) Name of the owner of the equipment.

24) Signature of owner.

25) Indicate the month, day, and year of the owner review and acceptance of Fitness for Service Assessment.

26) Indicate the name of the organization performing the Fitness for Service Assessment (this may be the same name as in line 22)

27) Signature of the responsible engineer performing the Fitness for Service Assessment.

28) Indicate the month, day, and year of the completion of the Fitness for Service Assessment by the Organization responsible.

29) Type or print the name of the Inspector.

30) Name of the Accredited Inspection Agency employing the Inspector.

31) Signature of the Inspector.

32) Indicate the month, day, and year of the review and acceptance by the Inspector of the Fitness for Service Assessment.

33) National Board commission number of Inspector, Jurisdiction, and Certificate of Competency Numbers.

REPLACEMENT OF STAMPED DATA FORM, NB-136

in accordance with provisions of the *National Board Inspection Code*

Submitted to:

(name of jurisdiction)

(address)

(telephone no.)

Submitted by:

(name of owner, user, or certificate holder)

(address)

(telephone no.)

1. Manufactured by _____ (name and address)
2. Manufactured for _____ (name and address)
3. Location of installation _____ (address)
4. Date installed _____
5. Previously installed at _____
6. Manufacturer's Data Report attached ☐ No ☐ Yes
7. Item registered with National Board ☐ No ☐ Yes, NB Number _____
8. Item identification Year built _____

   Type _____ Dimensions _____

   Mfg. serial no. _____ Jurisdiction no. _____

   MAWP _____ psi Safety relief valve set at _____ psi
9. Complete the reverse side of this report with a true facsimile of the legible portion of the nameplate.
10. If nameplate is lost or illegible, traceability documentation, verified by the Inspector shall be attached to this report.

11. I request authorization to replace the stamped data and/or nameplate on the above described pressure-retaining item in accordance with the rules of the *National Board Inspection Code* (NBIC).

    "R" Certificate Holder's Name: _____ Number _____

    Signature _____ Date _____

    Verification of Traceability _____ (Name of inspector) NB Commission _____

12. Authorization is granted to replace the stamped data or to replace the nameplate of the above described pressure-retaining item.

    Signature _____ (chief inspector or authorized representative) Date _____

    Jurisdiction (if available) or NB Commission no. _____

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-136 Rev.7

The following is a true facsimile of the legible portion of the item's original nameplate (if available). Please print. Where possible, also attach a rubbing or picture of the nameplate.

The following is a true facsimile of the item's replacement stamping or nameplate.

I certify that to the best of my knowledge and belief, the statements in this report are correct, and that the replacement information, data, and identification numbers are correct and in accordance with provisions of the *National Board Inspection Code*.

"R" Certificate Holder _____ Number _____

Signature _____ Date _____
(authorized representative)

Witnessed by _____ Employer _____
(name of inspector)

Signature _____ Date _____ NB Commission _____
(inspector)

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-136 Rev.7(Back)

FORM NB-4
NEW BUSINESS OR DISCONTINUANCE
USED BY AUTHORIZED INSPECTION AGENCIES

To: _____ _____
JURISDICTION 1. DATE OF SERVICE

2. Notice of: ☐ New insurance business ☐ Discontinuance or cancellation ☐ Refusal to insure 3. Effective date _____ 4. Type of object: ☐ High-pressure boiler ☐ Low-pressure boiler ☐ Pressure vessel

5. OBJECT	6. OWNER'S NO.	7. JURISDICTION NO.	8. NATIONAL BOARD NO.	9. NAME OF MANUFACTURER

10. NAME OF OWNER

11. NAME OF OWNER INCLUDING COUNTY

12. LOCATION OF OBJECT INCLUDING COUNTY

13. USER OF OBJECT (IF SAME AS OWNER SHOW "SAME")

14. DATE OF LAST CERTIFICATE INSPECT., IF ANY	15. CERTIFICATE ISSUED ☐ Yes ☐ No	16. REASON FOR DISCONTINUANCE OR CANCELLATION ☐ Phys. condition ☐ Out of use ☐ Other

17. REMARKS (USE REVERSE SIDE)

18. By: _____
CHIEF INSPECTOR BRANCH OFFICE

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-4 Rev. 2

FORM NB-5 BOILER OR PRESSURE VESSEL DATA REPORT

FIRST INTERNAL INSPECTION

Standard Form for Jurisdictions Operating Under the ASME Code

Complete When Not Registered National Board

1	DATE INSPECTED MO | DAY | YEAR	CERT EXP DATE MO | YEAR	CERTIFICATE POSTED ☐ Yes ☐ No	OWNER NO.	JURISDICTION NUMBER	NAT'L BD NO. ☐ OTHER NO. ☐
2	OWNER				NATURE OF BUSINESS	KIND OF INSPECTION ☐ Int ☐ Ext / CERTIFICATE INSPECTION ☐ Yes ☐ No
	OWNER'S STREET ADDRESS NUMBER				OWNER'S CITY	STATE / ZIP
3	USER'S NAME - OBJECT LOCATION				SPECIFIC LOCATION IN PLANT	OBJECT LOCATION - COUNTY
	USER'S STREET ADDRESS NUMBER				USER'S CITY	STATE / ZIP
4	CERTIFICATE COMPANY NAME				CERTIFICATE COMPANY CONTACT NAME	EMAIL
	CERTIFICATE COMPANY ADDRESS				CERTIFICATE COMPANY CITY	STATE / ZIP
5	TYPE ☐ FT ☐ WT ☐ CI ☐ AIR TANK ☐ WATER TANK Other			YEAR BUILT	MANUFACTURER	YEAR INST ☐ New ☐ Secondhand
6	USE ☐ Power ☐ Process ☐ Steam Htg ☐ HWH ☐ HWS ☐ Storage ☐ Heat Exchange ☐ Other				FUEL (BOILER)	METHOD OF FIRING (BOILER) / PRESSURE GAGE TESTED ☐ Yes ☐ No
7	PRESSURE This Inspection Prev. Inspection			SAFETY-RELIEF VALVES Set at	EXPLAIN IF PRESSURE CHANGED	
8	IS CONDITION OF OBJECT SUCH THAT A CERTIFICATE MAY BE ISSUED? ☐ Yes ☐ No (If no, explain fully on back of form - listing code violation)				PRESSURE TEST ☐ Yes psi Date ☐ No	
9	SHELL No.	DIAMETER ☐ ID ☐ OD in.	OVERALL LENGTH ft. in.	THICKNESS in.	TOTAL HTG SURFACE (BOILER) Sq. Ft.	MATERIAL ASME Spec Nos
10	ALLOWABLE STRESS psi	BUTT STRAP Thks in ☐ Single ☐ Double	HEADERS - WT BOILERS Thickness in.	TYPE ☐ Box ☐ Sinuous ☐ Wtr Wall ☐ Other		
11	TYPE LONGITUDINAL SEAM ☐ Lap ☐ Butt ☐ Welded ☐ Brazed ☐ Riveted	RIVETED Dia Hole in.	PITCH in. X in. X in.	SEAM EFF %		
12	HEAD THICKNESS in.	HEAD TYPE ☐ Fixed ☐ Movable ☐ Plus ☐ Minus ☐ Flat ☐ Quick Opening	RADIUS DISH in.	ELLIP RATIO	BOLTING No. Dia. in. Material	
13	TUBE SHEET THICKNESS in.	TUBES No. Dia. in. Length ft. in.	PITCH (WT BLRS) in. X in.	LIGAMENT EFF %		
14	**FIRE TUBE BOILERS**	DISTANCE UPPER TUBES TO SHELL Front in. Rear in.	STAYED AREA FRONT HEAD { Above Tubes / Below Tubes	REAR HEAD { Above Tubes / Below Tubes		
	STAYS ABOVE TUBES Front No. Rear No.	TYPE ☐ Head to Head ☐ Diagonal ☐ Welded ☐ Weldless	AREA OF STAYS Front Rear			
	STAYS BELOW TUBES Front No. Rear No.	TYPE ☐ Head to Head ☐ Diagonal ☐ Welded ☐ Weldless	AREA OF STAYS Front Rear			
15	FURNACE - TYPE Adamson (No. Sect) ☐ Corrugated ☐ Plain ☐ Other		THICKNESS in.	TOTAL LENGTH ft. in.	TYPE LONG. SEAM ☐ Welded ☐ Riveted ☐ Seamless	
16	STAYBOLTS - TYPE Threaded Welded Hollow Drilled (Size Hole in.)		DIAMETER in.	PITCH in. X in.	NET AREA sq. in.	
17	SAFETY-RELIEF VALVES No. Size	TOTAL CAPACITY Cfm Lb/Hr Btu/Hr	OUTLETS No. Size	PROPERLY DRAINED ☐ Yes ☐ No (*If no, explain on back of form*)		
18	**STOP VALVES** ON STEAM LINE ☐ Yes ☐ No	ON RETURN LINES ☐ Yes ☐ No	OTHER CONNECTIONS ☐ Yes ☐ No	STEAM LINES PROPERLY DRAINED ☐ Yes ☐ No (*If no, explain on back of form*)		
19	FEED PIPE Size in.	FEED APPLIANCES No.	TYPE DRIVE ☐ Steam ☐ Motor	**CHECK VALVES** FEED LINE ☐ Yes ☐ No	RETURN LINE ☐ Yes ☐ No	
20	WATER GAGE GLASS No.	TRY COCKS No.	BLOWOFF PIPE Size in. Location	INSPECTION OPENINGS COMPLY WTH CODE ☐ Yes ☐ No (*If no, explain on back of form*)		
21	CAST-IRON BOILERS Length in. Width in. Height in.	SECTIONS No.	DOES WELDING ON STEAM, FEED BLOWOFF AND OTHER PIPING COMPLY WITH CODE? ☐ Yes ☐ No (*If no, explain on back of form*)			
22	SHOW ALL CODE STAMPING ON BACK OF FORM. Give details (use sketch) for special objects NOT covered above - such as double wall vessels, etc.		DOES ALL MATERIAL OTHER THAN AS INDICATED ABOVE COMPLY WITH CODE? ☐ Yes ☐ No (*If no, explain on back of form*)			
23	NAME AND TITLE OF PERSON TO WHOM REQUIREMENTS WERE EXPLAINED:					
24	I HEREBY CERTIFY THIS IS A TRUE REPORT OF MY INSPECTION Signature of Inspector	IDENT NO.	EMPLOYED BY	IDENT NO.		

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229

NB-5 Rev. 1

OTHER CONDITIONS AND REQUIREMENTS

CODE STAMPING

(BACK)

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-5 Rev. 1(Back)

FORM NB-6 BOILER-FIRED PRESSURE VESSEL
REPORT OF INSPECTION
Standard Form for Jurisdictions Operating Under the ASME Code

1	DATE INSPECTED MO | DAY | YEAR	CERT EXP DATE MO | YEAR	CERTIFICATE POSTED ☐ YES ☐ NO	OWNER NO.	JURISDICTION NUMBER	☐ NAT'L BD NO. ☐ OTHER NO.	
2	OWNER				NATURE OF BUSINESS	KIND OF INSPECTION ☐ INT ☐ EXT	CERTIFICATE INSPECTION ☐ YES ☐ NO
	OWNER'S STREET ADDRESS NUMBER				OWNER'S CITY	STATE	ZIP
3	USER'S NAME – OBJECT LOCATION				SPECIFIC LOCATION IN PLANT	OBJECT LOCATION - COUNTY	
	USER'S STREET ADDRESS NUMBER				OWNER'S CITY	STATE	ZIP
4	CERTIFICATE COMPANY NAME				CERTIFICATE COMPANY CONTACT NAME	EMAIL	
	CERTIFICATE COMPANY ADDRESS				CERTIFICATE COMPANY CITY	STATE	ZIP
5	TYPE ☐ FT ☐ WT ☐ CI ☐ OTHER _____			YEAR BUILT	MANUFACTURER		
6	USE ☐ POWER ☐ PROCESS ☐ STEAM HTG ☐ HWH ☐ HWS ☐ OTHER _____				FUEL	METHOD OF FIRING	PRESSURE GAGE TESTED ☐ YES ☐ NO
7	PRESSURE ALLOWED MAWP _____ THIS INSPECTION _____ PREV. INSPECTION _____				SAFETY-RELIEF VALVES SET AT _____ TOTAL CAPACITY _____		HEATING SURFACE OR BTU (INPUT/OUTPUT)
8	IS CONDITION OF OBJECT SUCH THAT A CERTIFICATE MAY BE ISSUED? ☐ YES ☐ NO (IF NO, EXPLAIN FULLY UNDER CONDITIONS)					HYDRO TEST ☐ YES _____ PSI DATE _____ ☐ NO	
9	CONDITIONS: With respect to the internal surface, describe and state location of any scale, oil or other deposits. Give location and extent of any corrosion and state whether active or inactive. State location and extent of any erosion, grooving, bulging, warping, cracking or similar condition. Report on any defective rivets, bowed, loose or broken stays. State condition of all tubes, tube ends, coils, nipples, etc. Describe any adverse conditions with respect to pressure gage, water column, gage glass, gage cocks, safety valves, etc. Report condition of setting, linings, baffles, supports, etc. Describe any major changes or repairs made since last inspection.						
10	REQUIREMENTS: (LIST CODE VIOLATIONS)						
11	NAME AND TITLE OF PERSON TO WHOM REQUIREMENTS WERE EXPLAINED:						
	I HEREBY CERTIFY THIS IS A TRUE REPORT OF MY INSPECTION SIGNATURE OF INSPECTOR		IDENT NO.		EMPLOYED BY		IDENT NO.

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-6 Rev. 6

FORM NB-7 PRESSURE VESSELS
REPORT OF INSPECTION
Standard Form for Jurisdictions Operating Under the ASME Code

1	DATE INSPECTED MO | DAY | YEAR	CERT EXP DATE MO | YEAR	CERTIFICATE POSTED ☐YES ☐NO	OWNER NO.	JURISDICTION NUMBER	☐ NAT'L BD NO. ☐OTHER NO.	
2	OWNER				NATURE OF BUSINESS	KIND OF INSPECTION ☐INT ☐EXT	CERTIFICATE INSPECTION ☐YES ☐NO
	OWNER'S STREET ADDRESS				OWNER'S CITY	STATE	ZIP
3	USER'S NAME - OBJECT LOCATION				SPECIFIC LOCATION IN PLANT	OBJECT LOCATION - COUNTY	
	USER'S STREET ADDRESS				USER'S CITY	STATE	ZIP
4	CERTIFICATE COMPANY NAME				CERTIFICATE COMPANY CONTACT NAME	EMAIL	
	CERTIFICATE COMPANY ADDRESS				CERTIFICATE COMPANY CITY	STATE	ZIP
5	TYPE ☐ AIR TANK ☐ WATER TANK ☐OTHER _____			YEAR BUILT	MANUFACTURER		
6	USE ☐ STORAGE ☐ PROCESS ☐ HEAT EXCHANGE ☐OTHER _____				SIZE	PRESSURE GAGE TESTED ☐YES ☐NO	
7	PRESSURE ALLOWED THIS INSPECTION _____ PREVIOUS INSPECTION _____			SAFETY RELIEF VALVES SET AT _____ TOTAL CAPACITY _____		EXPLAIN IF PRESSURE CHANGED	
8	IS CONDITION OF OBJECT SUCH THAT A CERTIFICATE MAY BE ISSUED? ☐ YES ☐ NO (IF NO EXPLAIN FULLY UNDER CONDITIONS)				HYDRO TEST ☐ YES _____ PSI DATE _____ ☐ NO		
9	CONDITIONS: With respect to the internal surface, describe and state location of any scale, oil or other deposits. Give location and extent of any corrosion and state whether active or inactive. State location and extent of any erosion, grooving, bulging, warping, cracking or similar condition. Report on any defective rivets, bowed, loose or broken stays. State condition of all tubes, tube ends, coils, nipples, etc. Describe any adverse conditions with respect to pressure gage, water column, gage glass, gage cocks, safety valves, etc. Report condition of setting, linings, baffles, supports, etc. Describe any major changes or repairs made since last inspection.						
10	REQUIREMENTS: (LIST CODE VIOLATIONS)						
11	NAME AND TITLE OF PERSON TO WHOM REQUIREMENTS WERE EXPLAINED:						
	I HEREBY CERTIFY THIS IS A TRUE REPORT OF MY INSPECTION _____ SIGNATURE OF INSPECTOR			IDENT NO.	EMPLOYED BY		IDENT NO.

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-7 Rev. 4

PRESSURE VESSEL — REPORT OF INSPECTION — (EXTENSION SHEET)

DATE INSPECTED		OWNER-USER						LOCATION			
OWNER'S NO.	JURISDICTION NO.	NB ASME OR STD. NO.	INT	EXT	*CERT – NO. OF YEARS	TYPE OF OBJECT	YEAR BUILT	MADE BY	ALLOW. PRESS.	TEMP. OF	R.V.S.V. SETTING

** In this column show the number of years for which the inspector authorizes the issuance of the certificate.*

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-7 Rev. 4(Back)

FORM NB-403 REPORT OF FITNESS FOR SERVICE ASSESSMENT

F.F.S. Assessment No. _____ (1)

1. Equipment Owner Information: (2) _____
(Name)
_____
(Address)

2. FFS Assessment Performed By: (3) _____
(Name of Organization or Individual)
_____
(Address)

3. Location of Equipment Installation: (4) _____
(Name of Company)
_____ (5)
(Address) (Jurisdiction)

4. Equipment or Component Information: (6) _____
(MFG SR#, NB#, Jurisdiction# , Year Built, Other)
_____
(Equipment Material Specification, Grade)
_____
(Design & Operating Pressures, Design & Operating Temperatures)

5. Original Code of Construction: (7) _____
(Name) (Section) (Division) (Edition) (Addendum)

FITNESS FOR SERVICE STANDARD USED FOR ASSESSMENT (8) _____

6. Flaw Type(s) and / or Damage Mechanisms considered in FFS Assessment: (9)
_____
_____
_____
_____

7. FFS Assessment Procedures (attach FFS Assessment reference documents with details if applicable): (10)
_____
_____

Inspection Results: (11) _____
(Type of NDE Performed, Pressure Tests, Thickness Measurements, etc.)
_____
_____

Failure Modes Identified: (12) _____
(Crack-Like Flaws, Pitting, Bulges/Blisters, General or Localized Corrosion, etc.)

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-403 Rev. 1

8. FFS Assessments Results / Recommendations (Check boxes that apply and provide details): (13)
(14) ❑ Continued Operation (15) ❑ Repair (16) ❑ Replace (17) ❑ Continue Operation Until: _____ (18)

Details (if applicable) _____

9. Owners Inspection Intervals (Based on Assessment): (19) _____
(Months/Years)

10. In Service Monitoring Methods and Intervals: (20) _____
(Methods, Months/Years)

11. Operating Limitations (if applicable): (21) _____

I, (22) _____ certify that to the best of my knowledge and belief the statements in this report are correct and that the information, data, and identification numbers are correct and in accordance with provisions of the *National Board Inspection Code*, Part 2, 4.4. Applicable documentation is attached to support this assessment

Owner Name (23) _____
(Printed)

Signature (24) _____ Date (25) _____
(Owner)

Organization Performing Assessment (26) _____
(Name)

Signature (27) _____ Date (28) _____
Responsible Engineer

Verified By (29) _____ Employer (30) _____
(Inspector, Printed) (Accredited Inspection Agency)

Signature (31) _____ Date (32) _____
(Inspector)

NB Commission # (33) _____
National Board & Jurisdiction Number

This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-403 Rev. 1

PART 2, SECTION 6
INSPECTION — SUPPLEMENTS

6.1 SCOPE

a) This section contains detailed inspection requirements for specific pressure-retaining items identified as supplements.

b) Inspection of items described in these supplements may include application of additional inspection requirements contained in other sections of NBIC Part 2.

c) Each supplement is numbered in sequential order and follows the same numbering system used for the main text preceded by the letter “S.” Each page of the supplement will identify the supplement name and number in the top heading.

SUPPLEMENT 1
STEAM LOCOMOTIVE FIRETUBE BOILER INSPECTION AND STORAGE

S1.1 SCOPE

This supplement is provided as a guide for inspection and storage of steam locomotive firetube boilers operating on tracks gaged 24 in (610 mm) or greater or for steam locomotives under the requirements of the Federal Railroad Administration (FRA). These rules shall be used in conjunction with the applicable rules of the NBIC. See NBIC Part 2, Figures S1.1-a and S1.1-b.

FIGURE S1.1-a

LOCOMOTIVE BOILER GENERAL ARRANGEMENT

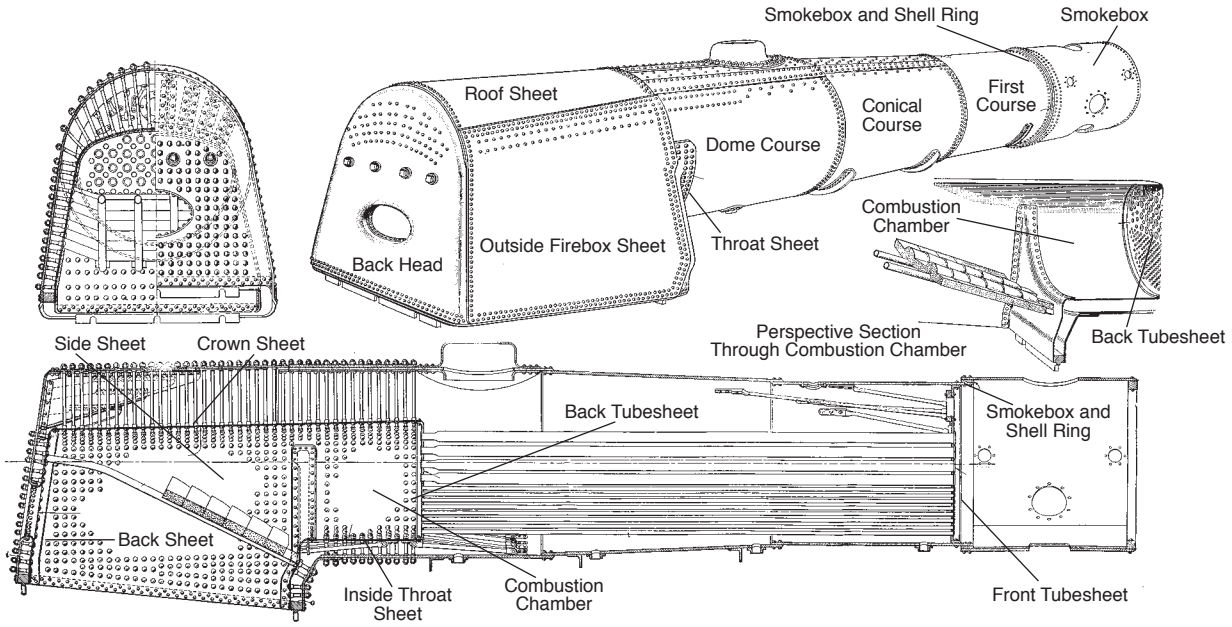
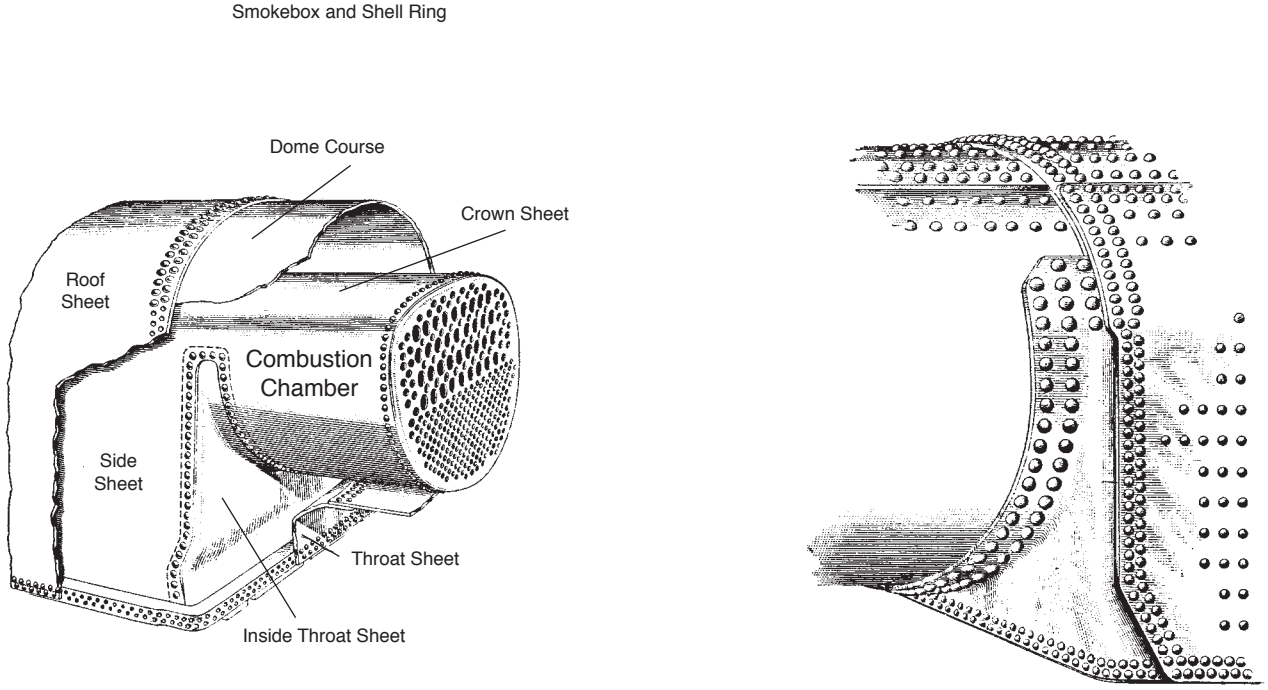


FIGURE S1.1-b
ARRANGEMENT OF FIREBOX SHEETS (STAYBOLTS DELETED FOR CLARITY)



S1.2 SPECIAL JURISDICTIONAL REQUIREMENTS

Many Jurisdictions have special requirements for locomotive boilers. Such requirements shall be considered in addition to those in this supplement.

S1.3 FEDERAL RAILROAD ADMINISTRATION (FRA)

The FRA rules for steam locomotive boilers are published in the *Code of Federal Regulations* (CFR) 49CFR Part 230, dated November 17,1999.[2] All locomotives under FRA Jurisdiction are documented on FRA Form 4 as defined in 49CFR Part 230. This document is the formal documentation of the steam locomotive boiler and is required to be completed prior to the boiler being placed in service. This document shall be used as the data report for the boiler, applicable to all repairs and alterations performed. National Board "R" Certificate Holders shall document their repairs and/or alterations on National Board Forms R-1 or R-2. These reports shall be distributed to the owner or user of the boiler, who is required to incorporate them into the FRA Form 19, which becomes an attachment to the FRA Form 4. The design margin for all such repairs or alterations shall not be less than four, based on ultimate tensile strength of the material.

S1.4 LOCOMOTIVE FIRETUBE BOILER INSPECTION

S1.4.1 INSPECTION METHODS

a) Plate thickness and depth of corrosion may be determined by use of the ultrasonic thickness testing process.

2 Steam locomotive inspection and maintenance standards, which are now codified at 49CFR Part 230, may be obtained at the FRA Website.

b) Where access is possible, the depth of pitting may be determined by use of a depth micrometer or a pit gage.

c) On stayed sections, the plate thickness readings should be taken on a grid not exceeding the maximum staybolt pitch at the center of each section of four staybolts. Additional readings may be taken close to each staybolt to determine if localized thinning has occurred. Particular attention should be given to the joint between the staybolt and the plate.

d) On unstayed sections, the plate thickness readings should be taken on a grid not exceeding 12 inch (305 mm) centers. Additional readings should be taken if conditions warrant.

e) Cracks in plates may be located by the use of appropriate Nondestructive Examination (NDE) methods.

f) Separation of plates at riveted seams may be detected by use of a feeler gage and magnifying glass or other applicable method.

g) Varying the intensity of inspection lights may facilitate discovery of defects. Placement of the light to shine parallel to the surface is one method of detecting pits and surface irregularities.

h) When inspecting internal stayed surfaces, placement of a light source within the stayed zone will aid the inspection.

i) Broken staybolts may be detected by leakage through telltale holes and by hammer testing. Both methods are most effective when the boiler is under hydrostatic pressure of at least 95% MAWP. If a hydrostatic test cannot be applied, the hammer test may be performed alone with the boiler drained.

j) Visual inspection shall be performed as a supplement to all of the above.

S1.4.2 INSPECTION ZONES

S1.4.2.1 RIVETED SEAMS AND RIVET HEADS

Riveted seams and rivet heads shall be inspected for:

a) Grooving;

b) Corrosion;

c) Cracks;

d) Pitting;

e) Leakage;

f) Separation of the plates;

g) Excessive or deep caulking of the plate edges and rivet head;

h) Seal welding of the plate edges and rivet heads;

i) Rivet heads that have been built up by, or covered over completely by, welding;

j) Rivets replaced by patch bolts;

k) Defective components of the seam; and

Notes: Broken rivet heads or cracked plates may result from sodium hydroxide cracking (caustic embitterment).

Riveted longitudinal lap seams should be given careful examination, using NDE if necessary, because this type of construction is prone to cracking.

When determining the extent of corrosion to rivet heads, it is important to know the rivet size and the type of rivet head used for the original construction. Corrosion can alter the appearance of these items and disguise the full extent of the damage.

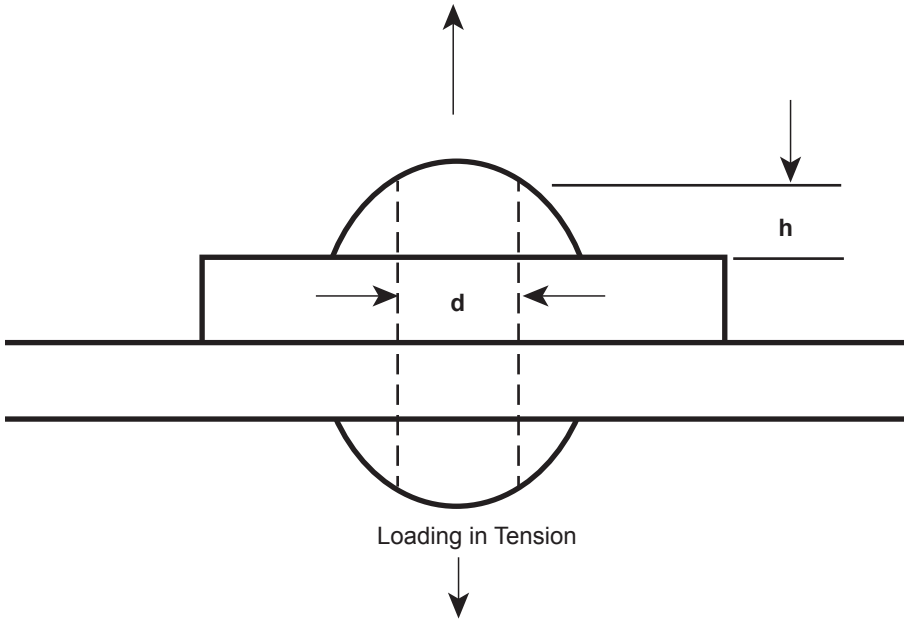
Fire cracks extending to the rivet holes in riveted lap seams of firebox sheets may be acceptable under NBIC Part 2, 3.4.9.

l) Rivet head wastage for rivet joint in tension;
Rivet head wastage for riveted joints in tension shall not exceed 0.250d. In NBIC Part 2, Figure S1.4.2.1, h shall be equal to or greater than 0.250d where:

h= average height of rivet head on circumference of diameter d
d= shank diameter of driven rivet

Note: This calculation is independent of the type and style of the rivet head.

FIGURE S1.4.2.1



S1.4.2.2 WELDED AND RIVETED REPAIRS

Welded and riveted repairs shall be inspected for:

a) Correct application of welded patches or weld application;

b) Correct application of riveting;

c) Cracks;

d) Separation of the plates;

e) Dents or other mechanical damage; and

f) Leakage.

S1.4.2.3 BOILER SHELL COURSE

The boiler shell course shall be inspected for:

a) Grooving or cuts;

b) Corrosion;

c) Cracks;

d) Pitting;

e) Separation of the plates;

f) Dents or other mechanical damage; and

g) Leakage.

Note: An accurate inspection often cannot be performed until the interior has been cleaned, since mud and scale make it difficult to detect defects.

S1.4.2.4 DOME AND DOME LID

The dome and dome lid shall be inspected for:

a) Grooving;

b) Corrosion, especially at the interior section attached to the boiler course;

c) Cracks;

d) Pitting;

e) Separation of plates;

f) Dents or other mechanical damage;

g) Leakage;

h) Stretched, bent, or corroded dome studs; and

i) Damage to the steam dome cover sealing surfaces.

Notes: Close inspection should be made to the interior section at the joint attached to the boiler course. If the dome studs are bent, a careful evaluation should be made of the lid for leakage and mechanical damage.

S1.4.2.5 MUDRING

The mudring and mudring rivets shall be inspected for:

a) Mud and scale on the waterside;

b) Debris on the waterside;

c) Corrosion;

d) Grooving;

e) Cracks;

f) Separation of the firebox plates from the mudring;

g) Dents or other mechanical damage; and

h) Leakage.

S1.4.2.6 FLUE SHEETS

Flue sheets shall be inspected for:

a) Grooving around flue holes, rivet seams and braces;

b) Pitting;

c) Fireside and waterside corrosion;

d) Fire cracks at riveted lap seams;

e) Cracks;

f) Bulges;

g) Leakage; and

h) Excessive or deep caulking of the plate edges.

Note: Corrosion is common at the bottom section of the front flue sheet. Close inspection of the joint between the front flue sheet and shell shall be made.

S1.4.2.7 FLANGED SHEETS

The flanged section of all flanged sheets shall be inspected for:

a) Pitting;

b) Corrosion;

c) Cracks;

d) Grooving;

e) Scale and mud deposits; and

f) Correct fit up and alignment of the flanged sheet to the adjacent sheets.

Notes: Corrosion is common at the bottom section of the front flue sheet. The flanges should have a smooth, uniform curvature and should make a smooth transition to the flat sheets.

S1.4.2.8 STAYED SHEETS

Stayed sheet shall be examined for:

a) Scale and mud deposits;

b) Grooving around staybolt holes;

c) Deterioration of the joint between the staybolt and the sheet;

d) Grooving on the waterside section;

e) Pitting;

f) Fireside and waterside corrosion;

g) Overheating;

h) Fire cracks at riveted lap seams;

i) Cracks; and

j) Bulges.

Notes: Close inspection for fireside corrosion should be given to sections located behind refractory or grate bars.

Close inspection should be made for grooving on waterside surfaces of the stayed sheets just above the mudring.

Fire cracks extending to the rivet holes in riveted lap seam firebox sheets may be acceptable under NBIC Part 2, 3.4.9.

(15) S1.4.2.8.1 BULGED STAYED SHEETS

a) The maximum depth of the bulged section of the firebox sheet shall not exceed the firebox sheet thickness. The bulged section depth is defined as the protrusion of the firebox sheet beyond its original position. Where sheets are bulged more than one quarter inch within one staybolt pitch, the thickness of the plate shall be verified. If the thickness is less than required the sheet shall be replaced. If the thickness of the sheet is adequate for the pressure, it shall be ensured that there is complete thread engagement between the staybolts and the sheet in the bulged area. If any deficiency is found in the thread engagement that impedes the holding power of the staybolt to a level below what is required for the operating pressure, the defective area shall be repaired or replaced.

b) If the maximum depth of the bulge exceeds the firebox sheet thickness, the bulged section of the firebox sheet shall be replaced. All staybolts within and/or contacting the bulged firebox sheet section shall be replaced. The adjacent sections of the firebox sheet shall be inspected to determine the cause of the bulge such as scale or mud accumulation prior to completing the repair.

c) If the bulged firebox sheet will remain in service, the conditions that caused the bulge shall be identified and corrected prior to placing the boiler back into operation.

d) If the bulged firebox sheet will remain in service the bulged sheet section and the sheet sections adjacent to the bulge shall be inspected for cracking and thinning (wastage) by use of NDE in order to confirm their suitability for service prior to placing the boiler back into operation.

S1.4.2.9 STAYBOLTS

Staybolts shall be inspected for:

a) Cracks in or breakage of the body;

b) Erosion of the driven head from corrosion or combustion gases;

c) Staybolt head flush with or below the surface of the sheet;

d) Plugging of telltale holes except as permitted by 49 CFR Part 230.41;

e) Waterside corrosion;

f) Staybolt heads that have been covered over by welding; and

g) Correct application of seal welding to staybolt heads.

Notes: An indicator of waterside corrosion on threaded staybolts is the lack of threads on the section of the staybolt body just above the sheet.

Broken staybolts may be detected by leakage through telltale holes and by hammer testing. Both methods are most effective when the boiler is under hydrostatic pressure of at least 95% MAWP. If a hydrostatic test cannot be applied, the hammer test may be performed alone with the boiler drained.

When a broken stay is found, the stays adjacent to it should be examined closely because these may have become overstressed by addition of the load from the broken stay.

A telltale hole plugged by installation of a nail or pin may indicate the staybolt is broken and requires replacement.

The plugging of telltale holes by refractory to prevent buildup of foreign matter in the telltale hole is permitted for locomotives operating under FRA Jurisdiction per 49 CFR Section 230.41.

One indication that a threaded staybolt leaks during service is when the head of it is found to have been re-driven repeatedly.

S1.4.2.10 FLEXIBLE STAYBOLTS AND SLEEVES

Flexible staybolt sleeves and caps shall be inspected for:

a) Corrosion;

b) Cracks;

c) Dents or other mechanical damage;

d) Leakage;

e) Damaged threads or welds;

f) Scale and mud accumulations inside the sleeve that could restrict bolt movement;

g) Correct application of welding to welded sleeves and welded caps; and

h) Seal welding of threaded sleeves or threaded caps.

Notes: An indicator of waterside corrosion on threaded staybolts is the lack of threads on the section of the staybolt body just above the sheet.

Broken staybolts may be detected by leakage through telltale holes and by hammer testing. Both methods are most effective when the boiler is under hydrostatic pressure of at least 95% MAWP. If a hydrostatic test cannot be applied, the hammer test may be performed alone with the boiler drained.

On ball head flexible staybolts, one method of testing the stay for cracks or breakage is to strike the ball head using a pneumatic hammer or hand hammer. Another method is to twist the ball head using a long- handled wrench. Access to the ball head is gained by removing the cap from the sleeve.

When a broken stay is found, the stays adjacent to it should be examined closely because these may have become overstressed by addition of the load from the broken stay.

A telltale hole plugged by installation of a nail or pin may indicate the staybolt is broken and requires replacement.

The plugging of telltale holes by refractory to prevent buildup of foreign matter in the telltale hole is permitted for locomotives operating under FRA Jurisdiction per 49 CFR Section 230.41.

One indication that a threaded staybolt leaks during service is when the head of it is found to have been re-driven repeatedly.

S1.4.2.11 GIRDER STAY AND CROWN BARS

Girder stays, crown bars, and their associated fasteners including stays, rivets, pins, washers, nuts, thimbles, spacers, and the adjacent sections of the firebox plates shall be inspected for:

a) Corrosion;

b) Cracks;

c) Mud and scale;

d) Correct fit and alignment of the girder stay or crown bar to the firebox plate surface, including flanged sections;

e) Correct fit and alignment of the thimbles, spacers, and pins to the girder stay or crown bar, and the firebox plates;

f) Dents or other mechanical damage;

g) Stays or rivets built up by or covered over completely by welding;

h) Leakage from the stay heads;

i) Seal welding of rivet heads;

j) Correct application of retainers to all nuts and fasteners; and

k) Missing fasteners, nuts or retainers.

Notes: An accurate inspection often cannot be performed until the girder stay or crown bar has been cleaned, since mud and scale will make it difficult to detect defects.

When a broken stay is found, the stays adjacent to it should be examined closely because these may have become overstressed by addition of the load from the broken stay.

S1.4.2.12 SLING STAYS

Sling stays and their associated fasteners including the pins, retainers, washers, nuts, and their associated attachment at eyes, girder stays, or crown stays shall be inspected for:

a) Corrosion;

b) Cracks;

c) Dents, wear or other mechanical damage;

d) Mud and scale;

e) Wear to the pinhole or expansion slot of the sling stay and mating component;

f) Correct application of retainers to the pins;

g) Missing fasteners, nuts, or retainers; and

h) Any of the above that would restrict movement of the sling stays.

Notes: An accurate inspection often cannot be performed until the sling stay has been cleaned, since mud and scale will make it difficult to detect defects.

When a broken or loose stay is found, the stays adjacent to it should be examined closely because these may have become overstressed by addition of the load from defective stays.

Special attention should be given to the row of sling stays adjacent to the flue sheet to ensure that these stays are not loose.

S1.4.2.13 CROWN STAYS AND EXPANSION STAYS

Crown stays and expansion stays shall be inspected for:

a) Cracks in or breakage of the body;

b) Dents, wear, or other mechanical damage;

c) Erosion of the driven head from corrosion or combustion gases;

d) Stay head flush with or below the surface of the sheet;

e) Plugging of telltale holes, except as permitted by 49 CFR Part 230.41;

f) Waterside corrosion;

g) Stay heads that have been covered over by welding;

h) Correct application of seal welding to stay heads;

i) Correct application of retainers to the pins;

j) Missing fasteners, nuts, or retainers;

k) Correct fit and alignment of the stay assembly; and

l) Any of the above that would restrict movement of the stay.

Notes: An indicator of waterside corrosion on threaded stays is the lack of threads on the section of the stay body just above the sheet.

Broken stays may be detected by leakage through telltale holes and by hammer testing. Both methods are most effective when the boiler is under hydrostatic pressure of at least 95% MAWP. If a hydrostatic test cannot be applied, the hammer test may be performed alone with the boiler drained.

When a broken stay is found, the stays adjacent to it should be examined closely because these may have become overstressed by addition of the load from broken stays.

A telltale hole plugged by installation of a nail or pin may indicate the stay is broken and requires replacement.

The plugging of telltale holes by refractory to prevent buildup of foreign matter in the telltale hole is permitted for locomotives operating under FRA Jurisdiction per 49 CFR Part 230.41.

One indication that a threaded stay leaks during service is when the head of it is found to have been re-driven repeatedly.

Special attention should be given to the row of stays adjacent to the flue sheet to ensure that these stays are not loose.

S1.4.2.14 DIAGONAL AND GUSSET BRACES

Diagonal and gusset braces, and their attachments, shall be inspected for:

a) Looseness;

b) Corrosion;

c) Cracks;

d) Welded repairs;

e) Missing pins or pin retainers;

f) Defective rivets; and

g) Scale and mud deposits.

Notes: Diagonal and gusset braces should be under tension.

The brace pins should fit the brace clevis and eye securely and be retained from coming out by some type of fixed or keyed retainer.

Diagonal braces having loop-type ends should be given close inspection for cracks and corrosion. The loop-type end is formed by the brace body being split, looped around, and forged to the body. Some versions of it have a low margin of material to provide the required strength.

S1.4.2.15 FLUES

All boiler and super heater flues shall be inspected for:

a) Fire cracks;

b) Pitting;

c) Corrosion;

d) Erosion;

e) Obstructions in the flue interior;

f) Mud or scale buildup on the waterside;

g) Erosion or cracking of the flue ends, flue beads and/or seal welds;

h) Leakage;

i) Number of circumferential welded joints on flues repaired by re-ending; and

j) Correct application including expanding/rolling and belling, beading, or seal welding of the flue end.

Notes: Erosion (cinder cutting) generally occurs to the firebox end of the flue.

Galvanic corrosion of the flue in the flue sheet may occur if flues are installed with copper ferrules.

S1.4.2.16 SUPERHEATER UNITS AND HEADER

Superheater units and the superheater header shall be inspected for:

a) Pitting;

b) Cracks;

c) Erosion;

d) Corrosion;

e) Bulges;

f) Leakage;

g) Missing shields;

h) Missing or broken bands or supports on the superheater units;

i) Missing, damaged, or welded attachment bolts, nuts, clamps, studs, and washers; and

j) Adequate structural bracing and support of the superheater header.

S1.4.2.17 ARCH TUBES, WATER BAR TUBES, AND CIRCULATORS

Arch tubes, water bar tubes, and circulators shall be inspected for:

a) Erosion;

b) Corrosion;

c) Fire cracks;

d) Pitting;

e) Cracking of tube ends;

f) Overheating and blistering;

g) Bulges;

h) Mud and scale buildup in the waterside;

i) Welded repairs; and

j) Correct application including expanding/rolling and belling, beading, or seal welding of the tube end.

Note: Weld buildup or welded patches are not permitted on arch tubes and water bar tubes of locomotives operating under FRA Jurisdiction per 49 CFR Section 230.61. The defective tubes must be replaced.

S1.4.2.18 THERMIC SYPHONS

Thermic syphons shall be inspected for:

a) Erosion;

b) Corrosion;

c) Fire cracks;

d) Pitting;

e) Cracking of the siphon neck;

f) Overheating and blistering;

g) Bulges;

h) Mud and scale blockage in the waterside; and

i) Broken or damaged staybolts.

Note: Refer to inspection zones — Staybolts, Stayed Sheets, and Flanged Sheets - for additional inspection procedures.

S1.4.2.19 FIREBOX REFRACTORY

Firebox refractory shall be inspected to ensure it is properly applied and maintained to prevent undesired flame impingement on the firebox sheets.

S1.4.2.20 DRY PIPE

The dry pipe of boilers having dome mounted (internal) throttle valves shall be inspected for:

a) Erosion;

b) Corrosion;

c) Cracks;

d) Adequate structural bracing, support, and attachment to the boiler and dome; and

e) Loose, bent, or damaged rivets, nuts, bolts, and studs.

Note: A steam leak into the dry pipe of a dome mounted (internal) throttle valve will send an unregulated flow of steam to the cylinders.

S1.4.2.21 THROTTLE AND THROTTLE VALVE

The throttle handle and its mechanism shall be inspected for:

a) Proper operation;

b) Lost motion or looseness;

c) Adequate structural bracing, support and attachment to the boiler, dome, and firebox; and

d) Loose, bent, or damaged nuts, bolts, and studs.

Note: The throttle handle shall be equipped with some type of locking mechanism to prevent the throttle from being opened by the steam pressure.

S1.4.2.22 SCREW-TYPE WASHOUT PLUGS, HOLES, AND SLEEVES

Screw-type washout plugs, holes, and sleeves, especially those having square or Acme thread, shall be inspected for:

a) Damaged or cracked threads on the plug, hole, or sleeve;

b) Corrosion;

c) Cracks;

d) Distortion;

e) Looseness;

f) Leakage;

g) Steam cuts to threads and sealing surfaces; and

h) Twisting of the plug head or body.

Note: When washout plugs are threaded with USF or NPT thread, the minimum number of threads in good condition in the threaded hole shall be adequate for the service.

S1.4.2.23 HANDHOLE WASHOUT DOORS

Handhole washout doors and their mating surfaces shall be inspected for:

a) Damaged or cracked threads on the door studs;

b) Corrosion of door sealing surfaces and studs;

c) Cracks;

d) Stretching or bending of the door stud or handhole door;

e) Looseness;

f) Leakage and steam cuts;

g) Damage to the clamp;

h) Damage to the clamp seating surface on the sheet;

i) Confirmation that the handhole door makes unbroken line contact along the entire circumference of the sheet at the opening;

j) Handhole doors and assembly components shall have proper fit assembly;

k) Distortion of any components at assembly is prohibited; and

l) Material of the handhole door gaskets shall be suitable for the pressure and temperature of service.

Notes: Confirmation that the handhole door has unbroken line contact against the sheet can be determined by performing a "blue check." This requires applying a light coating of "contact blue" or "Prussian Blue" to the handhole door sealing surfaces. The door then is held against the sheet and removed. The transfer of the bluing will show the areas that contact the sheet surfaces.

The material of the handhole door gaskets should be reviewed with the operator to confirm that it meets the pressure and temperature requirements of the boiler.

S1.4.2.24 THREADED AND WELDED ATTACHMENT STUDS

Threaded and welded attachment studs shall be inspected for:

a) Corrosion, especially at the sheet;

b) Cracks;

c) Damaged threads;

d) Stretching or bending;

e) Looseness; and

f) Leakage.

S1.4.2.25 FUSIBLE PLUGS

Fusible plugs shall be inspected for:

a) Corrosion;

b) Scale buildup on the waterside;

c) Damage;

d) Tampering;

e) Leakage from the threads;

f) Height of the plug above waterside of crown sheet;

g) Evidence of melting or overheating; and

h) Proper marking.

S1.4.2.26 WATER GLASS, WATER COLUMN, AND GAGE COCKS

The water glass, water column, and gage cock boiler connections and piping shall be inspected for:

a) Mud and scale blockage;

b) Kinks or sharp, restricted, or flattened bends in the piping;

c) Sags in the piping horizontal runs;

d) Condition of tubular or reflex water glass;

e) Correct type and material of piping and fittings;

f) Correct location, size, and installation of the connections to the sheets;

g) Correct installation of the safety shield (if used);

h) Correct installation of the viewing light (if used);

i) Correct installation of the test and drain valves;

j) Proper installation;

k) Proper bracing to prevent vibration; and

l) Loose, bent, or damaged nuts, bolts, and studs.

S1.4.2.27 STEAM PRESSURE GAGE

The steam pressure gage, gage cock boiler connections, and piping shall be inspected for:

a) Kinks or sharp, restricted, or flattened bends in the piping;

b) Correct installation of the shutoff valve and siphon;

c) Proper size, type, and material of piping and fittings;

d) Proper installation;

e) Proper lighting for viewing;

f) Proper bracing to prevent vibration; and

g) Calibration.

S1.4.2.28 BOILER FITTINGS AND PIPING

The boiler fittings and associated piping shall be inspected for:

a) Cracks;

b) Corrosion;

c) Pitting;

d) Leakage;

e) Looseness;

f) Loose, bent,or damaged nuts, bolts, and studs;

g) Adequate structural bracing, support, attachment, and provision for expansion; and

h) Proper size, type, and material.

S1.4.2.29 BOILER ATTACHMENT BRACKETS

The boiler attachment brackets and associated components and fasteners used to secure the boiler to the frame shall be inspected for:

a) Correct installation;

b) Damaged or missing components;

c) Looseness;

d) Leakage;

e) Loose, bent, or damaged rivets, nuts, bolts and studs;

f) Defective rivets; and

g) Provision for expansion.

S1.4.2.30 FIRE DOOR

The fire door, the locking mechanism, and the operating mechanism shall be inspected for:

a) Safe and suitable operation;

b) Cracked, damaged, or burned parts; and

c) Loose, damaged, or bent rivets, nuts, bolts, and studs.

Note: The locking mechanism should be inspected for correct operation to confirm it will not allow the door to open in the event the firebox becomes pressurized.

S1.4.2.31 GRATES AND GRATE OPERATING MECHANISM

The grates shall be inspected for:

a) Cracked, damaged, burned, or missing segments; and

b) The grate operating mechanism of rocking grates shall be checked for:

1) Uniform operation of all segments;

2) Corrosion;

3) Worn or cracked linkage;

4) Correct fit of the shaker bar on the linkage;

5) Missing pins or pin retainers; and

6) Loose, bent, or damaged nuts, bolts, and studs.

S1.4.2.32 SMOKEBOX

The smokebox shall be inspected for:

a) Erosion;

b) Corrosion;

c) Leakage;

d) Holes;

e) Looseness; and

f) Loose, bent, or damaged nuts, bolts, and studs.

S1.4.2.33 SMOKEBOX STEAM PIPES

The smokebox steam pipes shall be inspected for:

a) Erosion;

b) Corrosion;

c) Pitting;

d) Leakage;

e) Looseness; and

f) Loose, bent, or damaged nuts, bolts, and studs.

Note: Pitting from the casting process may be evident on cast thick wall steam pipes, but may not constitute a defect.

S1.4.2.34 ASH PAN AND FIRE PAN

The ash pan or fire pan shall be inspected for:

a) Corrosion;

b) Holes;

c) Looseness;

d) Loose or damaged rivets, nuts, bolts, and studs;

e) Secure attachment to the frame or firebox;

f) Proper operation of the slides, clean out doors, dumping mechanism, and dampers; and

g) Proper sealing of the slides, clean out doors, and dampers.

S1.4.3 METHOD OF CHECKING HEIGHT OF WATER GAGE GLASS

The height of the bottom gage cock and water glass or water column above the highest section of the crown sheet should be checked to confirm it meets the height requirements for the service intended and those of the regulatory agency. It is especially important this be checked if the water glass location or piping was changed, or if a new crown sheet or complete firebox is installed.

S1.4.3.1 WATER HEIGHT MEASUREMENT METHOD

The following method is intended for use where it is possible to enter the boiler shell interior to measure the water level at the highest section of the crown sheet. (See NBIC Part 2, Figure S1.4.3.1)

1) Level the locomotive in the longitudinal and transverse planes so that it is in the position used for normal operation.

2) Place a measurement gage or ruler on the longitudinal centerline of the highest section of the crown sheet. The measurement gage or ruler must be placed vertical and tangent to the highest section of the crown sheet.

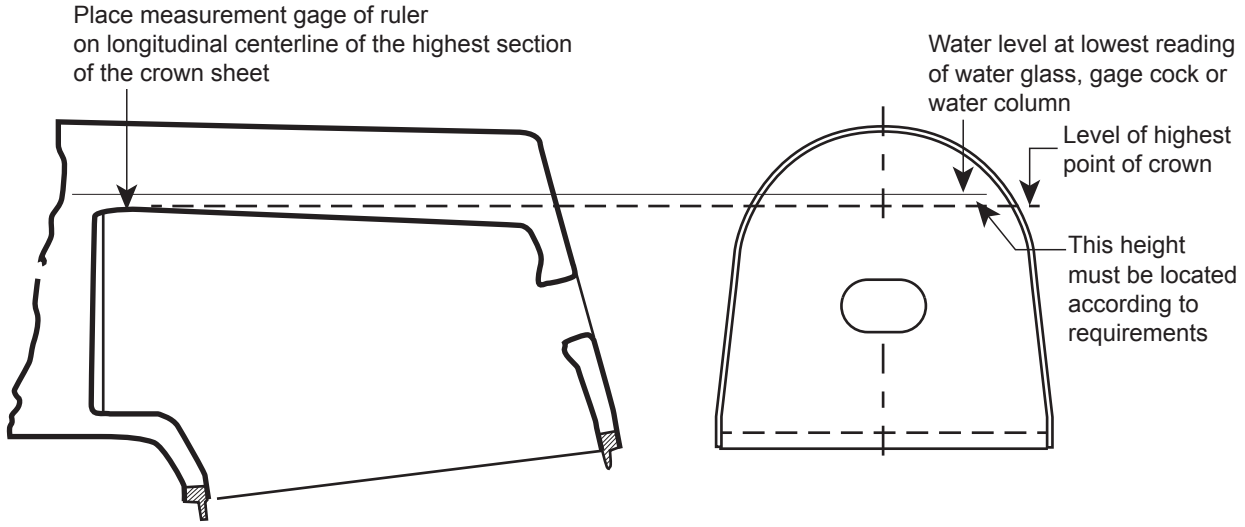
3) Fill the boiler with water until water exits the lowest gage cock and/or is just visible at the bottom of the water glass or water column.

4) Measure the height of water over the crown sheet using the ruler or gage.

5) Record the height reading and compare it to the required height. Repeat Steps 3 to 5 and compare the readings of the first and second tests.

FIGURE S1.4.3.1

Water Height Measurement Method



S1.4.3.2 FLEXIBLE SPIRIT LEVEL METHOD

The following method is intended for use where it is difficult to enter the boiler shell interior to measure the water level. The method is based on use of a flexible spirit level made from flexible rubber hose and clear plastic tubing. The measurements are taken from the fireside of the crown sheet.

a) The flexible spirit hose is made from a suitable length of flexible rubber tubing, such as garden hose, with a minimum internal diameter of 5/8 in. (16 mm). The tubing must be long enough to extend from the front of the firebox to the back head without kinks or sharp bends. At each end of the hose fasten an 8 in. (200 mm) long piece of clear plastic tube using hose clamps. The upper end of each piece of tubing must have four 1/8 in. (3.2 mm) deep x 1/8 in. (3.2 mm) wide air openings (slots) cut into it in order to allow the air to be vented out when held against the crown sheet. (See NBIC Part 2, Figure S1.4.3.2)

b) Fill the hose with water and bring the clear plastic tubes side by side vertically to observe the water level. If the level is not the same, there is an air bubble or other obstruction in the hose. Repair it and retest the water level before proceeding.

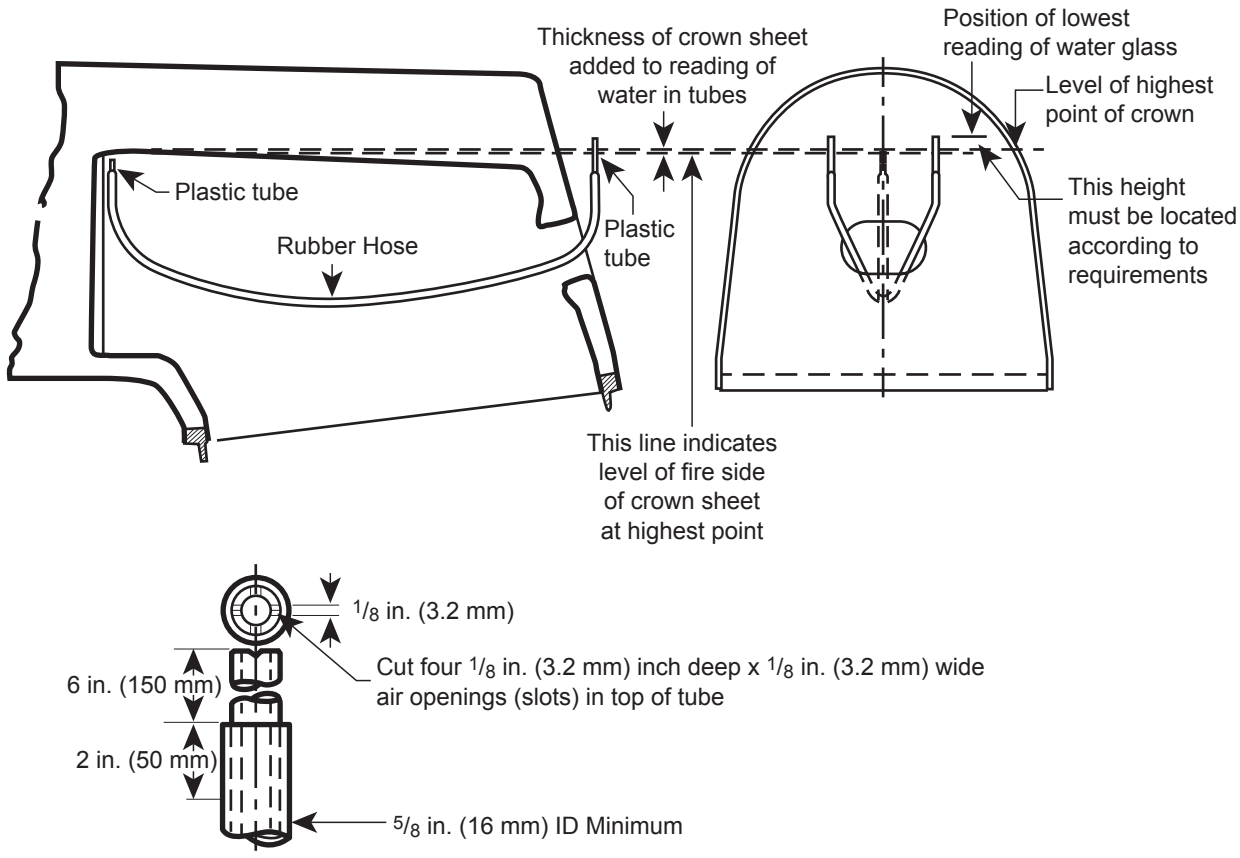
c) Level the locomotive in the longitudinal and transverse planes so that it is in the position used for normal operation.

d) Locate the approximate longitudinal centerline of the fireside of the crown sheet and the highest section of the crown sheet using a ruler and chalk.

e) Place one end of the hose against the approximate center of crown sheet at the highest point with the plastic tube held vertically.

FIGURE S1.4.3.2

Flexible Spirit Level Method



f) Place the other end of the hose and tube against the back head exterior vertical centerline and hold vertically in a position slightly lower than the crown sheet.

g) Slowly raise the end of the hose held against the back head until water is discharged from the tube held against the crown sheet. Hold both tubes in position until the water stops flowing. At this point the level of water in the tube held at the back head will show the height of the bottom side of the crown sheet. Mark this water level position on the back head.

h) Repeat the measuring procedure several times, each time moving the tube held against the crown sheet laterally to another position to confirm the highest location of the crown sheet has been located. Mark the level position of each measurement on the back head.

i) Above the line on the back head obtained by the spirit level measurement make a second line of the same curvature but higher by a height equal to the crown sheet thickness plus the 1/8” deep slots cut into the tubing. This second line represents the top (waterside) of the crown sheet at the highest point.

j) Use the second line as the reference point for measurements to determine whether the water glasses and/or water column are located at the required height above the crown sheet. To simplify taking the measurements the second line can be extended across the back head by use of a long ruler and precision spirit level.

S1.5 GUIDELINES FOR STEAM LOCOMOTIVE STORAGE

The steam locomotive guidelines published herein list the general recommendations for storage of locomotive boilers and locomotives. The exact procedures used by the owner/operator must be reviewed by the railroad mechanical officers/engineers and be based on the conditions and facilities at the railroad shop or storage facility.

S1.5.1 STORAGE METHODS

a) The methods for preparing a steam locomotive for storage depend upon several factors, including:

   1) The anticipated length of time the locomotive will be stored;

   2) Whether storage will be indoors or outdoors;

   3) Anticipated weather conditions during the storage period;

   4) The availability of climate-controlled storage;

   5) Type of fuel used; and

   6) Equipment available at the storage site.

b) Indoor storage can be categorized into two types: indoor with climate control, and indoor without climate control.

c) Outdoor storage can also be categorized into two types: outdoors during a warm time of year or in a geographic location where it can reasonably be expected to be above freezing during storage, and outdoors during a time period or in a geographic location where it can be expected that freezing temperatures will occur during storage.

d) Locomotive boilers may be stored using the “wet method” or the “dry method.”

e) Before any method of storage, the boiler must be thoroughly washed out, with mud and scale removed from the mudring, crownsheet, bottom of the barrel, and the top of the firing door.

S1.5.2 WET STORAGE METHOD

a) When utilizing the “wet storage method” the boiler is completely filled with treated water to exclude air.

   Note: This method cannot be used if the locomotive is exposed to freezing weather during storage.

b) Chemicals may be added to the storage water to further inhibit corrosion. However, depending on the chemical used, the treated water may have to be disposed of as a hazardous waste to prevent chemical contamination of the surrounding property.

c) The procedure applies only to the sections of the boiler that contain water. The firebox interior, cylinders, piping, and auxiliary equipment of the locomotive still require draining, preservation, and dry storage.

S1.5.3 DRY STORAGE METHOD

a) When utilizing the “dry storage method” the boiler is completely emptied of water, dried out, and allowed to stand empty. Several variations of the “dry method” may be used. These include but are not limited to:

   1) Airtight storage with a moisture absorbent placed in trays in the boiler;

2) Airtight storage with the boiler filled with inert gas to exclude oxygen; and

3) Open-air storage with the mudring washout plugs removed to enable air circulation for evaporation of formed moisture.

b) Each variation has positive and negative points that must be taken into account before use. If the boiler is filled with inert gas such as nitrogen, care must be taken because this method can result in asphyxiation of personnel if the gas escapes the boiler through a leaking valve or washout plug and enters a pit, sump, or enclosed room. In addition, the boiler must be completely vented to remove gas, then tested and declared gas-free before personnel may enter.

c) Although the use of dry storage with several washout plugs removed for air circulation is the most common method, there are some potential drawbacks. The boiler interior may be subject to moisture forming from condensation created from humidity changes in the ambient air. Small animals may take up residence inside if screens are not used to cover handholes and washouts.

d) Before storage, the boiler must be thoroughly washed out with mud and scale removed from the mudring, crownsheet, bottom of the barrel, and top of the firing door. Any mud or loose scale left in the boiler will retain moisture, leading to corrosion. After washing, water must be removed and the boiler dried before storage. A portable gas or electric heater placed in the firebox to aid evaporation and drying, along with a vacuum used to siphon water out via the lower washout plugs, is recommended.

Note: Use of the common railroad drying-out procedure of building a small wood fire in the firebox is not recommended because of the danger of overheating the firebox sheets.

e) The typical railroad dry storage method required blow down of the boiler until empty while steam pressure registered on the gage and removal of the washout plugs while the shell plates were hot and there was no steam pressure. This allowed the heat remaining in the boiler plates to evaporate remaining water in the boiler. However, this method may result in staybolt damage from temperature change and requires extreme care, if used.

f) Oil should not be applied to the interior surfaces of the boiler because it is difficult to remove. Further, the oil must be removed before steaming or it will form scale and contribute to foaming.

S1.5.4 RECOMMENDED GENERAL PRESERVATION PROCEDURES

a) When the locomotive is under steam, inspect piping, fittings, and appliances for steam and water leaks that may introduce moisture into the lagging. Repair leaks as necessary and remove wet lagging. Wet lagging can accelerate corrosion of the boiler external surfaces, especially staybolt sleeves and caps.

b) Thoroughly wash the boiler and firebox and remove mud and scale from the mudring, crownsheet, bottom of the barrel, and top of the firing door. Any mud or loose scale left in the boiler will retain moisture, leading to corrosion. Wash out thermic siphons, arch tubes, and circulators.

c) To protect the boiler interior during storage, dry the boiler by using compressed air to blow out as much water as possible. A portable heater placed in the firebox to warm the boiler to 200°F (93°C), along with a vacuum used to siphon water out via the lower washout plugs, can aid evaporation and drying of any moisture that collects in low or impossible-to-drain locations without harming the sheets.

Caution: To prevent a buildup of steam pressure during the drying process, the steam dome cover or top washout plugs should be removed to enable the moisture to escape. In addition, the driving wheels should be blocked and the throttle and cylinder cocks should be opened to permit any steam that forms in the superheater units to escape.

d) Superheater units, by nature of design, can be difficult to drain and dry out. Typical methods include:

1) Pressurize the boiler with compressed air with the locomotive stationary and blocked in place. Using the throttle to regulate the airflow, allow the air to blow through the entire bank of superheater units and dry pipe and discharge into the cylinders. The cylinder cocks must be open.

2) Pressurize the boiler with compressed air and then operate the locomotive under air pressure over a short distance of track. The cylinder cocks should be opened during the initial operation to prevent damaging the cylinders by hydraulic lock.

3) If the air pressure draining procedure is not practical or cannot be accomplished correctly, the superheater units can be protected against trapped moisture by filling the entire superheater bundle with a standard antifreeze/water mixture or with diesel fuel.

Notes: The air pressure dry-out methods "1" or "2" may have to be performed several times to discharge all of the moisture. Refer to NBIC Part 2, S1.5.5, *Use of Compressed Air to Drain Locomotive Components*, for additional information on compressed-air drying.

If the locomotive is operated under air pressure, the air brake system should be made operational to provide safe stopping or other steps taken to control and stop the locomotive.

e) After drying, it will be necessary to either vent the boiler or place containers of desiccant inside the boiler through the dome cap to absorb any condensation that may occur during storage. Venting the boiler to allow air circulation is accomplished by leaving two or more of the lower washout plugs out and opening the vent valve on the top of the boiler. A vent line consisting of two 90° elbows and pipe nipples should be installed in the vent valve to locate the opening to the downward direction in order to keep rain or snow from entering the open valve.

f) If the locomotive will be stored outdoors, the following should be completed:

1) Inspect the boiler jacket and confirm it is tight with no gaps leading into the lagging or shell. Pay close attention to areas at shell openings such as for studs, safety valves, etc. Repair all gaps or damaged jacket sections as necessary. Consideration should be given to covering the entire locomotive and tender with a tarp. Otherwise, all jacket openings should be covered to prevent the entrance of rain or snow. Where necessary, apply a waterproof covering over the exposed or open sections;

2) The smokestack should be sealed by applying a wood and sheet rubber cover held in place by clamps or a through bolt;

3) The safety valves should either be covered or removed, with plugs or caps installed in the holes if the valves are removed;

4) The dynamo, air pump, and feedwater heater exhausts should also be covered;

5) Empty and clean the smokebox, front tubesheet, superheater units, steam pipes, and front end plates of all coal, ash, or burnt oil. This work is especially critical at the bottom section of the smokebox and front tubesheet rivet flange. The smokebox door should be sealed by applying a gasket or sealant and any other air openings in the smokebox sealed. The exhaust nozzle should be sealed by applying a wood and sheet rubber cover held in place by clamps;

6) The potential for corrosion of the smokebox interior can be further minimized by applying a coating of outdoor paint or primer. All inspection of the smokebox and front tubesheet must be accomplished before painting since it will cover up many types of defects. The coating will burn off quickly when the locomotive is returned to service;

7) Thoroughly clean the firebox sheets, flues, and superheater return bends of all ash and clinker;

8) On coal burners, empty and clean the grates and ash pan of all coal and ash completely. This work is especially critical at the sections between the grate bearers, the mudring rivets, and firebox

sheets; and from the grate segment air openings. On oil burners, care should be taken to remove ash from between the flash wall refractory and the firebox sheets;

9) If the locomotive will be out of service for longer than 12 months, removal of the brick arch or flash wall refractory that extends above the mudring should be considered to prevent condensation and corrosion from occurring between the brick and the steel. Temporary removal of the brick arch or flash wall to permit application of a preservative to firebox sides, arch tubes, or siphons should be considered for shorter storage periods;

10) All appliances and piping that might contain water or condensation should be drained and blown dry using dry compressed air. This includes the air and equalizing reservoirs, dirt collectors, injectors, cylinders, stoker engine cylinders, dynamos, the steam and water sides of feedwater heaters and pumps, the steam side of air pumps, the steam side of lubricators, atomizers, oil tank heaters, gage siphons, tank hoses, and cab heater piping. A small quantity of valve oil should be sprayed into the valve chambers, cylinders and the steam side of all appliances to protect against corrosion. Refer to S1.5.5, *Use of Compressed Air To Drain Locomotive Components*, for details;

11) The cylinder castings, exhaust cavities, and steam lines must be drained of all moisture and blown dry. Typical methods include:

    a. Pressurizing the boiler with compressed air, with the locomotive stationary and blocked in place. Using the throttle to regulate the airflow, allow the air to blow through the dry pipe and discharge into the cylinders. The cylinder cocks must be open;

    b. Pressurizing the boiler with compressed air, then operate the locomotive under air pressure over a short distance of track. The cylinder cocks should be opened during the initial operation to prevent damaging the cylinders by hydraulic lock;

    Note: Methods “1” or “2” may have to be performed several times to discharge all of the moisture from the cylinders, and steam pipes. If the locomotive is operated under air pressure, the air brake system should be made operational to provide safe stopping or other steps taken to control and stop the locomotive.

    Refer to NBIC Part 2, S1.5.5, *Use of Compressed Air to Drain Locomotive Components*, for additional information;

g) Drain and wash tender water spaces. The tank should be inspected afterward and any remaining water removed by siphon or vacuum. When dry, spray the water space with outdoor paint or a commercial rust preventative. Drain and dry tender tank hoses and clean screens;

h) On coal or wood burners, spray any exposed surfaces of the tender fuel space with outdoor paint or a commercial rust preventative. If the locomotive is to be stored outdoors for a long term, remove all coal and spray the surfaces as above or cover the coal space with a tarp or a roof;

i) On oil burners, drain and blow out all fuel lines, tank heater and blowback lines, and the burner itself. Drain sludge and water from the bottom of the fuel tank. Ensure that tank hatches are secure and the tank is vented to prevent condensation. Draining the oil tank is recommended if the fuel oil is known to lose its volatile content during storage;

j) After cleaning thoroughly, coat all side and main rods, cross heads, valve gear, guides, piston rods, brake pistons, feedwater pump pistons, and air pump pistons with water-resistant grease or a rust preventative. Grease should be applied to the junction of each axle and driving box and journal box to prevent water entering. Grease should be applied to junction of rod and pin in valve gear and rods to prevent water entering;

k) If the locomotive is moved after grease is applied, it will be necessary to reapply the coating to piston rods and guides;

Note: Heavy oil or unrefined oil such as any of the Bunker types (e.g., Bunker 6, etc.) should not be used for preservation of any components because the sulfur contained in it can accelerate corrosion. Standard motor oil or journal oil will not stick to and preserve wetted surfaces. All surfaces, to be so coated, must be dry. If moisture is a problem, steam cylinder oil should be applied.

l) Plain journal bearings should be inspected for water and repacked. Roller bearing boxes should have all moisture drained and the boxes filled with lubricant. Grease plugs should be screwed down so that the threads are not exposed;

m) If the locomotive is to be stored outdoors with questionable or no security, remove and store all cab gages, water glasses, lubricators, brass handles, seatboxes, and any other items that thieves or vandals might attack. Remove the whistle, bell, headlight and marker, and/or classification lights. Remove tools, radios, and spare parts. Secure wood or metal covers over all windows and doors, and board up the back of the cab. Secure all manholes on the top of the tender; and

n) Inspect stored locomotives regularly for signs of rust, corrosion, damage, deterioration, or vandalism and immediately take any corrective measures necessary.

S1.5.5 USE OF COMPRESSED AIR TO DRAIN LOCOMOTIVE COMPONENTS

a) The process of using air pressure to drain and empty auxiliary components such as the cylinders, superheater units, and piping completely of water offers several advantages over other methods.

b) The air compressor must be equipped with a suitable filter to enable it to supply oil-free air because the introduction of air that contains oil into the water/steam parts of the boiler and superheater will promote the formation of scale and water foaming when the locomotive is returned to service.

c) The air compressor must be large enough to provide the volume and pressure of air required.

d) If the boiler is pressurized with compressed air, the air pressure must be raised slowly to prevent distorting or overstressing the firebox sheets or staybolts because the normal expansion of the boiler that occurs under steam pressure is not present when air pressure is used.

e) Auxiliary components such as the stokers, air compressors, turbo generators, and power reverse are drained by pressurizing the boiler to between one-half and three-quarters of the rated boiler pressure with compressed air from the stationary air compressor, then operating each component individually until the exhaust from it contains no moisture.

f) When necessary, specific pipe lines can be drained by breaking the line at each end, attaching the air line to it directly then blowing the line out.

S1.5.6 RETURN TO SERVICE

a) When returning a locomotive to service, the boiler, firebox, and tender tank shall be ventilated to remove a potentially hazardous atmosphere from the boiler interior before personnel enter it. In addition, the atmosphere in the boiler shall be verified to be safe for human occupancy before personnel enter it. For the boiler this can be accomplished by removing the washout plugs and placing a fan or air blower on top of the steam dome opening to force air into the boiler. For the firebox this can be accomplished by opening the smokebox door and firebox door and placing a fan or air blower at either location to force air through. Failure to do this could result in asphyxiation of the personnel entering the boiler or firebox.

b) If possible, the locomotive should be moved into a heated engine house and the boiler allowed to warm up in the air for several days until it is the same temperature as the air.

c) The initial fire-up should be done slowly to allow even heating of the boiler.

d) Before movement, the cylinders should be warmed up by allowing a small quantity of steam to blow through them and out the cylinder cocks and exhaust passages. This is necessary to reduce the stress in the casting from thermal expansion of the metal.

e) Steam should be discharged through the cylinder cocks for several minutes to aid removal of any solvent, debris, or rust that may have formed in the superheater units, steam pipes, and dry pipe.

f) All appliances should be tested under steam pressure before the locomotive is moved.

S1.6 SAFETY VALVES

The minimum safety valve capacity in pounds per hour (kilograms per hour) shall be calculated by multiplying the boiler heating surface area by the factor from the appropriate chart in NBIC Part 2, Table S1.6 (1 pound steam/hr/sq. ft = 4.88 kg steam/hr/sq meter).

TABLE S1.6

MINIMUM POUNDS OF STEAM/HR./SQ. FT. OF STEAM HEATING SURFACE

Firebox Heating Surface	
Type	Factor
Hand-Fired	8 (39)
Stoker-Fired	10 (49)
Oil-Fired	14 (68)
Flue Heating Surface	
Type	Factor
Hand-Fired	5 (24)
Stoker-Fired	7 (34)
Oil-Fired	8 (39)
Superheater Heating Surface	
Type	Factor
Hand-Fired	5 (24)
Stoker-Fired	7 (34)
Oil-Fired	8 (39)

S1.7 TABLES AND FIGURES

a) FIGURE S1.1-a Locomotive Boiler General Arrangement

b) FIGURE S1.1-b Arrangement of Firebox Sheets

c) FIGURE S1.4.2.1 Loading in Tension

d) FIGURE S1.4.3-a Water Height Measurement Method

e) FIGURE S1.4.3-b Flexible Spirit Level Method

f) FIGURE S1.6 Minimum Pounds of Steam/hr./sq. ft. of Steam Heating Surface

SUPPLEMENT 2
HISTORICAL BOILERS

S2.1 SCOPE

a) This supplement is provided as a guide to inspection of historical steam boilers of riveted and/or welded construction not falling under the scope of NBIC Part 2, Supplement 1. These historical steam boilers would include: steam tractors, traction engines, hobby steam boilers, portable steam boilers, certain steam locomotive boilers, and other such boilers that are being preserved, restored, and maintained for demonstration, viewing, or educational purposes. (See Note below)

Note: This supplement is not to be used for steam locomotive boilers operating on tracks gaged 24 in. (610 mm) or greater or for steam locomotive boilers falling under the requirements of the Federal Railroad Administration (FRA). FRA rules for steam locomotive boilers are published in 49 CFR 230. Specific rules and special requirements for inspection, repairs, alterations, and storage of steam locomotive boilers are identified in NBIC Part 2, Supplement 1.

b) The rules specified in this supplement shall be used in conjunction with the applicable rules in this code. References specified or contained in this supplement may provide additional information to assist the user when applying the requirements of this supplement.

S2.2 INTRODUCTION

a) The following inspection rules are minimum requirements for safe and satisfactory operation of historical boilers. Users of this supplement are cautioned that where complete details are not provided, the user is advised to seek technical guidance to provide sound engineering evaluations and practices.

b) Where adopted by a Jurisdiction, these requirements are mandatory. Where a Jurisdiction establishes different requirements for historical boilers or where a conflict exists, the rules of the Jurisdiction prevail.

S2.3 RESPONSIBILITIES

The owner or user and/or operator are responsible for ensuring that the boiler meets the requirements of the Jurisdiction where the boiler is operated, including inspections, repairs, licensing, operating certificates, permits, and operator training.

Note: It should be recognized that safety of these boilers is dependent upon the knowledge and training of the operator in proper use, repair, maintenance, and safe operation of each specific boiler proposed to be operated. (See NBIC Part 2, S2.4.3.)

S2.4 GENERAL INSPECTION REQUIREMENTS

The owner or user and Inspector should refer to NBIC Part 2, 1.4 *Personnel Safety*; NBIC Part 3, Section 3, *Corrosion and Failure Mechanisms*; and NBIC Part 2, Section 4, *Examinations, Test Methods, and Evaluations*, for additional information when performing inspections.

S2.4.1 PRE-INSPECTION REQUIREMENTS

a) The owner or user has the responsibility to prepare the boiler for any required inspections needed to ensure safety as deemed necessary by the Inspector. Prior to performing any type of inspection, the owner and Inspector shall ensure safety precautions are taken to prevent personal injury.

b) Prior to conducting an inspection, the following shall be reviewed by the Inspector to the extent possible to aid in determining safe operation:

1) Operating and maintenance history and/or other information contained in the operator log book;

2) Inspection history;

3) Construction code/design;

4) Materials — types and thickness;

5) Certifications;

6) Operator knowledge and training as required by the Jurisdiction;

7) Repairs/Alterations performed;

8) Cleanliness of the boiler; and

9) Potential hazards to personnel.

Note: If a boiler has not been properly prepared for an inspection, the Inspector may decline to make the inspection.

S2.4.2 POST-INSPECTION ACTIVITIES

a) Upon completion of inspection activities, the results of examinations and tests shall be documented by an Inspector, in a manner acceptable to the Jurisdiction.

b) Any defects or deficiencies in the condition, operation, and/or maintenance practice of the boiler and appurtenances shall be discussed and documented with the owner or user. Recommendations for correction and/or repair requirements (if required) shall be discussed and documented.

S2.4.3 BOILER OPERATORS

a) The following guidelines should be understood by each historical boiler operator and demonstrated safely during jurisdictional inspection and testing for each boiler proposed to be operated:

1) Jurisdictional rules for construction, maintenance, repairs, operation, and certification;

2) Boiler functions and purpose of controls, appurtenances, and safety devices;

3) Proper operation, maintenance, types, use and testing of valves, including safety valves;

4) Fusible plugs including installation, maintenance, design, and purpose;

5) Performance of normal and emergency system operating procedures associated with blowdown of the boiler, feed, or water delivery system, steam system, water level control, and combustion of fuel;

6) Importance of maintenance, cleaning, and inspection of components and safety devices such as pressure gages, sight glass, governor, water column, firebox, etc; and

7) Preparation and actions to be taken on emergency situations for fire, low water, foaming, overpressure, and excessive leakage.

b) Organizations/associations involved with historical boilers should verify operator knowledge by examination or practical testing or a combination of both. Some Jurisdictions may require specific operator qualifications or certifications. (See additional safety procedures in NBIC Part 2, S2.14)

S2.4.4 EXAMINATIONS AND TESTS

The examinations and tests shall be as required by the Jurisdiction and verified by an Inspector. The Inspector shall accept and verify procedures and personnel qualifications when examinations and tests are performed.

S2.4.4.1 NONDESTRUCTIVE EXAMINATION METHODS

There are a variety of nondestructive examination methods that may be employed to assess the condition of historical boilers. Skill, experience, and integrity of personnel performing examinations are essential to obtaining meaningful results. Generally, some form of surface preparation will be required prior to the use of examination methods.

S2.4.4.2 TESTING METHODS

Testing should be performed by experienced personnel using procedures acceptable to the Inspector. Typical test methods available to the Inspector during the inspection of historical boilers are listed below:

a) Hydrostatic testing/pressure testing;

b) Leak testing; and

c) Ultrasonic thickness testing.

S2.5 SPECIFIC EXAMINATION AND TEST METHODS

S2.5.1 SPECIFIC EXAMINATION METHODS

a) This part describes nondestructive examination and test methods that are typically available to the Inspector during inspection of historical boilers.

    1) Visual (VT)

    2) Ultrasonic (UT)

    3) Liquid Penetrant (PT)

    4) Magnetic Particle (MT)

    5) Radiographic (RT)

b) Additional examination or test methods may be performed if a deficiency is detected during initial or reoccurring inspection. Use of additional examination and testing methods shall be acceptable to the Inspector and the Jurisdiction, if required.

S2.5.2 VISUAL EXAMINATION

Visual examination is the most widely used method to ascertain surface condition and recognize surface features typical of various damage mechanisms associated with historical boilers. Damage mechanisms such as corrosion or cracking may be due to operation, age of material, or improper maintenance.

S2.5.2.1 PREPARATION FOR VISUAL INSPECTION

The owner or user shall ensure the following areas, as a minimum, are prepared for visual examination, and are acceptable to the Inspector at the time of the examination.

a) Fireside open and grates removed;

b) Fireside tubesheets and tubes thoroughly cleaned of soot and ash;

c) Waterside drained and handholes, plugs, and inspection openings removed;

d) Sediment, scale, and mud flushed; and

e) Insulation or jackets removed, as appropriate.

Note: Where there is limited or no access for visual inspection, remote camera or fiber optic devices may be used.

S2.5.2.2 VISUAL EXAMINATION REQUIREMENTS

To the extent possible, the following areas and items shall be visually examined by the Inspector and results documented on the Boiler Inspection Guideline (NBIC Part 2, S2.11) provided in this supplement, or as required by the Jurisdiction. The Boiler Inspection Guideline should be used as a reference when performing visual inspections.

a) The fusible plugs shall be removed, inspected, and confirmed to meet requirements of NBIC Part 2, S2.8.4.

b) Threaded openings or connections in the boiler shall be inspected for wear or deterioration when there is evidence of leakage. ANSI standard plug and ring gages may be used to verify thread integrity.

c) Inspect the condition of boiler sheets, shell, tubesheets, fittings, staybolts, and other materials for thinning, pitting, cracks, or corrosion.

d) Verify that requirements of NBIC Part 2, S2.8 and S2.9, are in compliance, as applicable.

S2.5.3 ULTRASONIC EXAMINATION

Ultrasonic examination is used as a volumetric examination of welds and base materials for detection of flaws. Factors such as material composition, surface condition, choice of equipment, and ability of the operator affect the results of ultrasonic examination.

S2.5.4 LIQUID PENETRANT EXAMINATION

Liquid penetrant examination is used to detect discontinuities open to the surface, such as cracks, seams, laps, cold shuts, laminations, and porosity.

S2.5.5 MAGNETIC PARTICLE EXAMINATION

Magnetic particle examination can be used to reveal surface discontinuities and, to a limited degree, discontinuities slightly below the surface. The sensitivity of this method decreases rapidly with depth below the surface and therefore is used primarily to examine surface discontinuities.

S2.6 SPECIFIC TESTING METHODS

During inspection of historical boilers there may be instances where conditions have adversely affected the tightness of the boiler or the inspection discloses hard to evaluate forms of deterioration that may affect the safety of the vessel. In these specific instances, a pressure test using water or other suitable liquid test medium may be required at the discretion of the Inspector to assess leak tightness of the pressure-retaining item. For safety, pneumatic pressure tests shall not be performed.

S2.6.1 HYDROSTATIC PRESSURE TESTING

When performing hydrostatic pressure testing for verification of leak tightness or when required by the Jurisdiction, the following requirements shall be met:

a) Hydrostatic pressure test shall be between the calculated maximum allowable working pressure and 1.25 times the calculated maximum allowable working pressure, and held for a minimum of 10 minutes or as required to perform a complete visual examination;

b) The metal and water temperature of the boiler shall be between 60°F to 120°F (16°C to 49°C) anytime a hydrostatic test is being performed;

c) A calibrated gage, acceptable to the Inspector, shall be used when hydrostatically pressure testing a boiler; and

d) During hydrostatic testing, safety valve(s) shall be removed.

S2.6.2 ULTRASONIC THICKNESS TESTING

Ultrasonic thickness (UT) testing shall be performed to determine boiler plate thickness. UT testing shall be performed by personnel acceptable to the Jurisdiction and the Inspector. The following requirements shall be met, to the extent possible. Performance and results shall be acceptable to the Inspector and, if required, the Jurisdiction.

a) Equipment, operator, and calibration standards used shall be documented.

b) To calculate MAWP, ultrasonic thickness testing results in areas of generalized thinning (3 in. [76 mm] in diameter or greater) or where grooved thinning is noted (2 in. [50 mm] in length or greater) are to be used in determining minimum thickness in accordance with S2.10. The MAWP calculation in S2.10 shall be completed based on the thickness data gathered.

c) On initial UT of stayed sections, the plate thickness readings should be taken on a grid not exceeding the maximum staybolt pitch. Additional readings may be taken close to each staybolt to determine if localized thinning has occurred. Particular attention should be given to the joint between the staybolt and the plate.

d) On initial UT of unstayed sections, the plate thickness readings should be taken on a grid not exceeding 12 inch (300mm) centers. Additional readings should be taken if conditions warrant.

e) UT test results shall be documented so location of test results can be checked at subsequent UT tests to determine if material loss has occurred.

f) Recurring UT testing shall be performed by randomly checking 10% of original UT checks. Areas of thinning identified during previous inspections shall be given particular attention. If material loss is determined, additional testing may be requested by the Inspector.

g) Particular attention should be placed upon areas that typically exhibit thinning. These areas include the ogee curve, the mudlegs, the fusible plug, around feedwater inlets, and around the firebox door ring.

h) The owner/operator shall maintain the initial and recurring grid mapped UT readings in conjunction with the calculations in permanent boiler records. Documentation shall be available to the Inspector for review and acceptance.

S.2.6.3 EVALUATION OF CORROSION

S2.6.3.1 LINE AND CREVICE CORROSION (15)

Line and crevice corrosion may be disregarded for MAWP calculations when:

a) The thickness of the remaining material is at least 75% of the required thickness per the MAWP calculations.

b) The total length does not exceed 2 inches (50 mm).

S2.6.3.2 RANDOMLY SCATTERED PITS (15)

Randomly scattered corrosion pits may be disregarded for MAWP calculations when:

a) The depths of the pits are such that the remaining material shall not be less than 50% of the required thickness per the MAWP calculations.

b) The total area of pits, below the required thickness per the MAWP calculations, does not exceed 7 sq. in. (4,500 sq. mm) within any 50 sq. in. (32,000 sq. mm) area.

c) Total length of pits in an 8 inch (200 mm) straight line cannot exceed 2 inches (50 mm).

S2.6.3.3 LOCALLY THINNED AREAS (15)

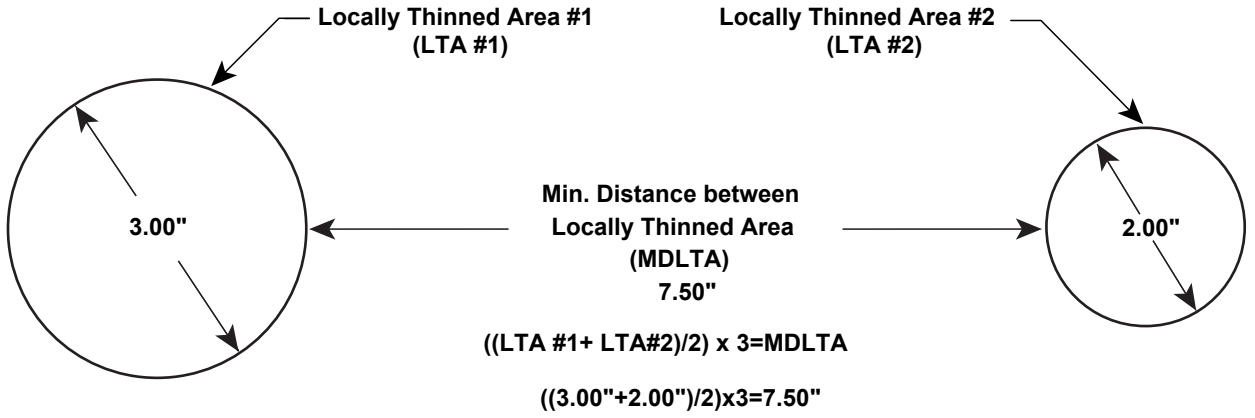
Locally thinned areas (LTA), 3 inch (75 mm) in diameter or less, may be disregarded for MAWP calculations when:

a) The average depth of the corrosion is such that remaining material shall not be less than 75% of the required thickness per the MAWP calculations.

b) The remaining thickness at the thinnest point shall not be less than 50% of the required thickness per the MAWP calculations.

c) The minimum distance between the boundaries of two locally thinned areas (MDLTA) must be greater than the average diameters of the two locally thinned areas (LTA) multiplied by 3.0. See Figure S2.6.3.3.

FIGURE S2.6.3.3
LOCALLY THINNED AREA



(15) **S2.6.3.4 GENERALIZED THINNED AREAS**

a) For corroded areas exceeding the specifications in S2.6.3.1, S2.6.3.2, and S2.6.3.3, the remaining thickness may be averaged over an area not exceeding the UT-grid size specified in S2.6.2 c) or S2.6.2 d).

1) The least measured remaining thickness within the grid indicated in S2.6.2 c) or S2.6.2 d) as applicable shall not be less than 50% of the required thickness per the calculation for MAWP.

2) The average remaining thickness recognized from the grid indicated in S2.6.2 c) or S2.6.2 d) as applicable shall not be less than 75% of the required thickness per the calculation for MAWP.

b) When general corrosion exceeds the limits of S2.6.3.4 a), the conditions shall be presented and reviewed with the Inspector, and when required, the Jurisdiction for resolution.

Note: The guidance presented at S2.6.3.1, S2.6.3.2, S2.6.3.3, and S2.6.3.4 is to be used to evaluate areas of thinning due to corrosion. Areas where plates have been formed to make corners whereby the radiuses may have thinned due to the forming process shall not be considered in calculating MAWP.

S2.7 INSPECTIONS

The requirements of this section shall be used in conjunction with the general requirements identified in NBIC Part 2, S2.4.

S2.7.1 INSERVICE INSPECTIONS

The following examinations and tests shall be performed while the boiler is in operation:

a) Two independent means of boiler feedwater delivery systems shall be demonstrated to the Inspector. Observance to be performed at an operating pressure no less than 90% of the safety valve set point of the boiler. If the boiler is equipped with more than one feedwater tank, each feedwater device must be

able to take water out of either feedwater tank. Pumped feedwater shall be preheated prior to entering the boiler;

b) Demonstration of operable try-cocks that show a level of water that correlates with that shown in the gage glass;

c) Demonstration of operating gage glass upper and lower shutoff valves;

d) Demonstration of an operating gage glass blowdown valve;

e) Check that the gage glass is visually clear and fully operational;

f) Visual inspection for leaks; and

g) Safety valves shall be tested by having the operator raise boiler pressure to the safety valve popping point. Popping point pressure and blowdown will be observed to ensure they are within tolerances (see NBIC Part 2, S2.8). Alternatively, a certification acceptable to the Jurisdiction may be used for verification of set pressures.

S2.7.2 INSERVICE INSPECTION DOCUMENTATION

Inservice inspection shall be documented as required by the Jurisdiction where the boiler is operated, or Form NB-5 or similar form may be used.

S2.7.3 INSPECTION INTERVALS

S2.7.3.1 INITIAL INSPECTION

a) Initial inspections shall be performed to determine baseline criteria needed for the operating life of the boiler. The owner or user shall maintain documentation and inspection results, as required by this section. In addition to the required Jurisdiction inservice inspection report identified in NBIC Part 2, S2.7.2, Form C-1 (See NBIC Part 2, S2.12) may be used for the documentation of initial examinations and inspections.

b) Boilers initially evaluated in accordance with this inspection code shall be subject to the following examinations and tests:

   1) A visual internal examination per NBIC Part 2, S2.5.2;

   2) A visual inservice examination per NBIC Part 2, S2.7.1;

   3) Initial UT test requirements per NBIC Part 2, S2.6.2;

   4) MAWP calculation per NBIC Part 2, S2.10;

   5) Hydrostatic Pressure Testing per NBIC Part 2, S2.6.1; and

   6) Other examinations (UT, PT, MT) as required by the Jurisdiction or Inspector to determine boiler integrity.

c) For new boilers constructed to a design code acceptable to the Jurisdiction, the initial inspection shall be a visual inservice exam per NBIC Part 2, S2. 7. 1. Subject to jurisdictional acceptance, the other initial inspection items above may be omitted. These new boilers may be mounted on existing running gear or settings and may include the original appurtenances.

S2.7.3.2 SUBSEQUENT INSPECTIONS

a) Boilers that have completed the initial inspection requirements begin the subsequent inspection intervals. The following inspection intervals should be used unless other requirements are mandated by the Jurisdiction.

1) Interval #1 — One year following initial inspection. Inservice inspection per NBIC Part 2, S2.7.1.

2) Interval #2 — Two years following initial inspection. Visual inspection per NBIC Part 2, S2.5.2.2.

3) Interval #3 — Three years following initial inspection. A pressure test per NBIC Part 2, S2.6.1.

4) Interval #4 — Same as interval #1.

5) Interval #5 — Visual inspection per NBIC Part 2, S2.5.2.2 and UT thickness testing per NBIC Part 2 S2.6.2.

6) Interval #6 — Same as interval #3.

b) After interval #6 is completed, the subsequent inspection cycle continues with interval #1.

S2.8 SAFETY DEVICES — GENERAL REQUIREMENTS

Each boiler shall be equipped with the following safety devices: safety valve(s), gage glass(es), try-cock(s), fusible plug(s), and pressure gage(s). These safety devices shall be verified by the owner and Inspector and documented on the Boiler Inspection Guideline, NBIC Part 2, S2.11, for proper installation and purpose during each inspection.

S2.8.1 SAFETY VALVES

a) The following requirements shall be verified acceptable when performing inspections of safety valves:

1) Set pressures of safety valves installed shall be verified by operation or certification acceptable to the Jurisdiction.

2) Safety valve(s) shall be National Board capacity certified.

3) Safety valve(s) shall be sealed by an ASME “V” Stamp holder or National Board “VR” repair firm.

4) The required safety valve capacity in pounds per hour (kg per hour) shall be calculated by multiplying boiler heating surface area by the type of fuel factor used (see NBIC Part 2, Table S2.8.1, for fuel factors). Excessive safety valve capacity should be avoided. (Only heating surface area above the grates shall be used when calculating heating surface for safety valve required capacity.)

Note: An additional pressure relief valve may be used in conjunction with the above required ASME safety valve if set at a lower pressure, although no credit for relieving capacity may be used.

5) Safety valve(s) shall have a test lever.

6) No isolation valve of any description shall be placed between the required safety valve(s) and the boiler, or on the discharge pipe between the valve and the atmosphere.

7) The piping connection between the boiler and the safety valve shall not be less than the inlet size of the safety valve, and the discharge pipe, if used, shall not be reduced between the safety valve and the point of discharge.

(15) 8) The safety valve(s) shall be connected so as to stand in an upright position with the spindle vertical.

9) The discharge from the safety valve(s) shall be arranged that there is no danger of scalding either the operator(s) or individuals who may be in the vicinity of the boiler. If the valve(s) is a top discharge design, no discharge piping is required. If a side discharge design valve(s) is used, an elbow should be attached to the outlet to assure a vertical discharge. The elbow must be located as close to the valve(s) as possible to minimize reaction moment stress.

10) Provision for ample gravity drain shall be made in the discharge pipe at or near each safety valve, and where water can collect.

11) If the boiler is equipped with a canopy, the elbow may be other than 90 degrees to direct the discharge out from under the canopy, while still directing the discharge to a safe location. The elbow must be located as close to the valve(s) as possible to minimize reaction moment stress.

12) If the boiler is equipped with a canopy, the discharge may be piped through the canopy. When the discharge piping is piped through a canopy, the elbow must be located as close to the valve as possible to minimize reaction moment stress. The discharge piping may be a larger pipe but in no case be smaller than the discharge size of the valve. Discharge piping shall be completely supported separate from the valve and elbow so no extra loading is transmitted to the safety valve(s).

b) To reduce cycling stress on the boiler, it is recommended that a safety valve with a blowdown between 2% and 4% be used. The blowdown, however, should never exceed 6%.

TABLE S2.8.1

MINIMUM POUNDS OF STEAM PER HOUR PER SQUARE FOOT OF HEATING SURFACE
(1 LB. STEAM/HR./SQ. FT. [4.88 KG/HR./SQ. M])

Boiler Heating Surface	Firetube Boilers	Watertube Boilers
Hand-Fired	5 (24)	6 (29)
Stoker-Fired	7 (34)	8 (39)
Power Burner	8 (68)	10 (78)
Hand-Fired Waterwall	8 (39)	8 (39)
Stoker Waterwall	10 (49)	12 (59)
Power Burner Waterwall	14 (68)	16 (78)

S2.8.2 GAGE GLASS

Historical boilers shall be equipped with at least one gage glass meeting the following requirements:

a) The gage glass shall be fitted with a guard to protect the glass;

b) The gage glass shall indicate the minimum safe operating water level;

c) The gage glass shall be provided with a drain valve or petcock, piped to a safe location;

d) The gage glass shall be visually clear and fully operational; and

e) The distance from the highest point on the crown sheet to the top of the lowest packing nut of the gage glass should be checked and documented.

S2.8.3 TRY-COCKS

Historical boilers shall be equipped with try-cocks meeting the following requirements:

a) Try-cocks shall be correctly located in reference to the minimum required water level;

b) Try-cocks shall be open (unplugged) and fully operational; and

c) If the boiler was not originally fitted with try-cocks, a newly installed try-cock shall be located 3 in. (76 mm) above the crownsheet.

S2.8.4 FUSIBLE PLUG

Historical boilers equipped with fusible plugs shall meet the following requirements:

a) The fusible plug shall be inspected to determine the condition of the threads in the crown sheet and on the fusible plug;

b) Boilers shall have a fusible plug unless equipped and operated with automatic controls;

c) Fusible plugs shall be constructed to meet the requirements of the ASME Code, and indicated as such by the ASME marking on the filler material;

d) Fireside fusible plugs must protrude a minimum of 3/4 inch (19 mm) into the water;

e) Fusible plugs may not protrude into the fire area more than 1 inch (25 mm);

f) Fusible plugs shall not be refilled;

g) Fusible plugs shall be replaced on initial jurisdictional inspection and after 500 hours of service, if hours of service can be proven. If hours of service cannot be proven they shall be replaced every three calendar years. Fusible plug life shall not exceed ten calendar years; and

h) Leaking fusible plugs shall be replaced.

S2.8.5 PRESSURE GAGE

Historical boilers shall be equipped with at least one pressure gage meeting the following requirements:

a) Tested and proven accurate within plus or minus 5 psi (35 kPa) of the safety valve set point at the time of the inservice inspection pressure test. If the gage is found to be out of this specified range it shall be calibrated to a national standard using a master gage or dead weight tester traceable to a national standard;

b) Siphon, or water seal, shall be installed between pressure gage and boiler;

c) If a valve is installed between the gage and the boiler, the valve shall indicate the open position or be sealed open; and

d) The range of pressure gage shall be 1.5 to 3.5 times the set point of the safety valve.

S2.9 APPURTENANCES — PIPING, FITTINGS, AND VALVES

Boiler piping and fittings shall meet the following requirements:

a) Threaded openings shall follow accepted standard piping practices and ANSI general pipe thread requirements;

b) Schedule 80, black pipe (SA-53 GR. A or B types ERW or Seamless; SA-106 GR A,B,C) shall be used for boiler pressure piping. Galvanized pipe and fittings and A-53 Type F and API-5L Grade A 25 pipe are prohibited on boiler pressure piping;

c) Steam piping components shall be used in the manner for which they were designed and shall not exceed manufacturer's pressure rating. Malleable iron Class 300 threaded fittings per ASME B16.3 are

acceptable for use. The use of malleable iron class 150 is not recommended. Forged threaded fittings per ASME B16.11 classes 2,000-6,000 are acceptable for use;

d) The blowdown line shall be piped to a safe point of discharge during the time the boiler is operating;

e) Piping shall be properly supported;

f) Valves shall be used in the manner for which they were designed, and shall be used within the specified pressure-temperature ratings. Valves shall be rated at or above the pressure setting of the boiler safety valve, denoted by the general or primary pressure class identification on the valve body and/or by the initials “WSP” or “S” to indicate working steam pressure or steam rating. Valves in cold-water service may be designated by the initials “WOG” to indicate water, oil, or gas rating and/or by the pressure class identification on the valve body; and

g) The boiler shall be equipped with two means of supplying feedwater while the boiler is under pressure.

S2.9.1 PIPING, FITTINGS, AND VALVE REPLACEMENTS

The installation date should be stamped or stenciled on the replaced boiler piping. Alternatively, the installation date may be documented in permanent boiler records, such as the operator log book.

S2.10 MAXIMUM ALLOWABLE WORKING PRESSURE (MAWP)

The MAWP of a boiler shall be determined by computing the strength of each boiler component. The computed strength of the weakest component using the factor of safety allowed by these rules shall determine the MAWP.

Note: The rules of ASME Section I 1971 Edition, Part “PR” and “PFT” may be used for determining specific requirements of design and construction of boilers and parts fabricated by riveting.[3]

S2.10.1 STRENGTH

a) In calculating the MAWP, when the tensile strength of the steel or wrought iron is known, that value shall be used. When the tensile strength of the steel or wrought iron is not known, the values to be used are 55,000 psi (379 MPa) for steel and 45,000 psi (310 MPa) for wrought iron. Original steel stamp marks, original material certifications, or current laboratory tests are acceptable sources for verification of tensile strength. Catalogs and advertising literature are not acceptable sources for tensile strength values.

b) In computing the ultimate strength of rivets in shear, the following values shall be used:

1)	Iron rivets in single shear	38,000 psi (262 MPa)
2)	Iron rivets in double shear	76,000 psi (524 MPa)
3)	Steel rivets in single shear	44,000 psi (303 MPa)
4)	Steel rivets in double shear	88,000 psi (607 MPa)

c) The resistance to crushing of mild steel shall be taken as 95,000 psi (655 MPa) unless otherwise known.

d) S = TS/FS. See definitions of nomenclature in NBIC Part 2,S2.10.6.

3 Copies of ASME Section I 1971 Edition Part “PR” and “PFT” referenced section may be obtained by contacting the National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229.

S2.10.2 RIVETS AND RIVET HEADS

When the diameter of the rivet holes in the longitudinal joints of a boiler is not known, the diameter of rivets, after driving, shall be ascertained from the NBIC Part 2, Table S2.10.2.

TABLE S2.10.2
SIZES FOR RIVETS BASED ON PLATE THICKNESS

Thickness of Plate, in. (mm)	Diameter of Rivet after Driving, in. (mm)
1/4 (6)	11/16 (17)
9/32 (7)	11/16 (17)
5/16 (8)	3/4 (19)
11/32 (9)	3/4 (19)
3/8 (10)	13/16 (21)
13/32 (10)	13/16 (21)
7/16 (11)	15/16 (24)
15/32 (12)	15/16 (24)
1/2 (13)	15/16 (24)
9/16 (14)	1-1/16 (27)
5/8 (16)	1-1/16 (27)

S2.10.2.1 RIVET HEAD TYPES

Finished rivet heads are shown in NBIC Part 3, Figure S2.13.13.4. Note that a riveted seam may have more than one type of rivet to, for example, provide necessary clearance during operation, or for provision for equipment assembly and maintenance.

S2.10.2.2 INSPECTION OF CORRODED RIVETS

A riveted seam or joint is very redundant by design. Therefore, the following guidelines apply when generalized corrosion is present and consistent on a group of adjacent rivets (typically four or more), and not to individual rivets. The Inspector must consider the frequency and consistency of corroded rivet heads, and condition, location, and type of riveted joint (and how it may fail) in determining allowable corrosion.

a) Visually identify all connections containing rivets which show signs of significant corrosion.

b) Categorize each connection as the type which loads the rivets in one of three possible modes (pure shear, pure tension, or combined shear and tension). Refer to Figure S2.10.2.2.

c) A leak around a rivet head may be indicative of a rivet which is loose, broken, or otherwise failing to provide adequate clamping force and shall require further inspection.

    1) A rivet shall be deemed loose if it can be felt to move after being struck on the side of the head in a direction approximately perpendicular to its shank with a 40 oz. engineer's hammer.

    2) NBIC Part 3, S2.13.13 defines procedures to address a leak around a rivet head.

d) Allowable corrosion:

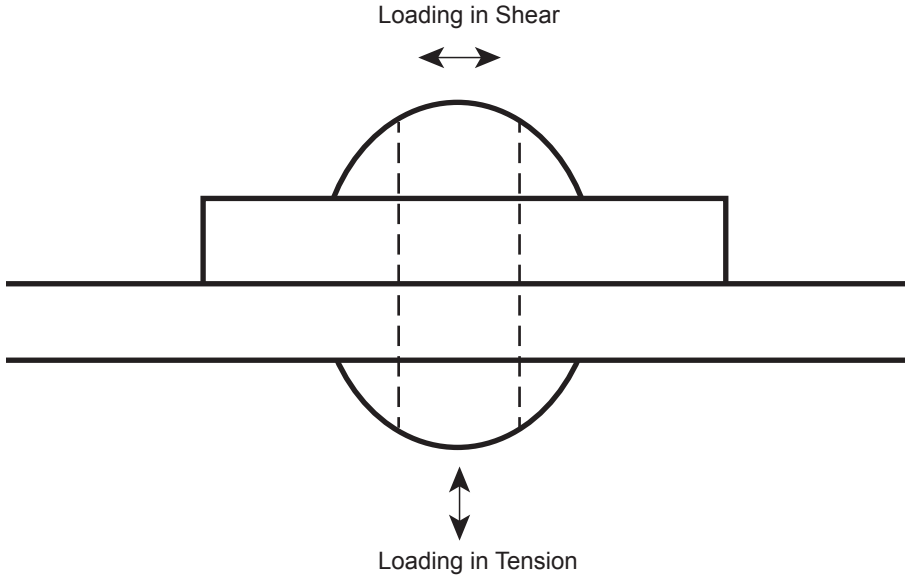
1) For rivets in pure shear load, the amount of measured head deterioration shall not exceed 80% of their total head volume. Where rivets have countersunk heads, the head diameter must be equal to or greater than 65% of the original head diameter. Severe head corrosion shall require further evaluation of the condition and thickness of the plate at the joint.

2) For rivets in pure tension, the amount of measured head deterioration shall not exceed 35% of their total head volume. Where rivets have countersunk heads, the head diameter must be equal or greater than 85% of original head diameter. Application of this value shall take into consideration the consistency and frequency of adjacent rivets showing excessive corrosion.

3) For connections subjected to combined shear and tension loads, the amount of measured head deterioration shall not exceed 60% of their total head volume. Where rivets have countersunk heads, the head diameter must be equal or greater than 75% of original head diameter. Application of this value shall take into consideration the consistency and frequency of adjacent rivets showing excessive corrosion.

Note: The condition of the plate surrounding the rivets including general wastage, pitting, and the condition of the caulking edge, must be considered.

FIGURE S2.10.2.2



S2.10.3 CYLINDRICAL COMPONENTS

The MAWP of cylindrical components under internal pressure shall be determined by the strength of weakest course computed from the minimum thickness of the plate, the tensile strength of the plate, the efficiency of the longitudinal joint, the inside diameter of weakest course, and the design margin allowed by these rules using the following formula or NBIC Part 2, Tables S2.10.3.1 through S2.10.3.6:

$$\mathrm{MAWP} = \frac{\mathrm{TS} \times \mathrm{t} \times \mathrm{E}}{(\mathrm{R} \times \mathrm{FS})}$$

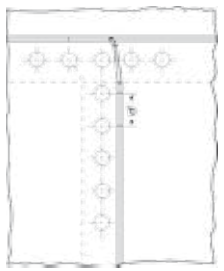
See definitions of nomenclature in NBIC Part 2, S2.10.6.

TABLE S2.10.3.1

MAXIMUM ALLOWABLE WORKING PRESSURE FOR CYLINDRICAL COMPONENTS (BARREL)

For Single-Riveted Lap Joint

Shell ID	Minimum Thickness of Shell Plate																																
	0.19	0.2	0.21	0.22	0.23	0.24	0.25	0.26	0.27	0.28	0.29	0.3	0.31	0.32	0.33	0.34	0.35	0.36	0.37	0.38	0.39	0.4	0.41	0.42	0.43	0.44	0.45	0.46	0.47	0.48	0.49	0.5
12	168	177	186	195	204	213	222	230	239	248	257	266	275	284	292	301	310	319	328	337	346	354	363	372	381	390	399	408	416	425	434	443
13	155	164	172	180	188	196	204	213	221	229	237	245	254	262	270	278	286	294	303	311	319	327	335	344	352	360	368	376	384	393	401	409
14	144	152	160	167	175	182	190	197	205	213	220	228	235	243	251	258	266	273	281	286	296	304	311	319	327	334	342	349	357	365	372	380
15	135	142	149	156	163	170	177	184	191	198	206	213	220	227	234	241	248	255	262	269	276	284	291	298	305	312	319	326	333	340	347	354
16	126	133	140	146	153	160	166	173	179	186	193	199	206	213	219	226	233	239	246	253	259	266	272	279	286	292	299	306	312	319	326	332
17	119	125	131	138	144	150	156	163	169	175	181	188	194	200	206	213	219	225	231	238	244	250	256	263	269	275	281	288	294	300	306	313
18	112	118	124	130	136	142	148	154	160	165	171	177	183	189	195	201	207	213	219	224	230	236	242	248	254	260	266	272	278	284	289	295
19	106	112	118	123	129	134	140	146	151	157	162	168	173	179	185	190	196	201	207	213	218	224	229	235	241	246	252	257	263	269	274	280
20	101	106	112	117	122	128	133	138	144	149	154	160	165	170	175	181	186	191	197	202	207	213	218	223	229	234	239	245	250	255	261	266
21	96	101	106	111	116	122	127	132	137	142	147	152	157	162	167	172	177	182	187	192	197	203	208	213	218	223	228	233	238	243	248	253
22	92	97	102	106	111	116	121	126	131	135	140	145	150	155	160	164	169	174	179	184	189	193	198	203	208	213	218	222	227	232	237	242
23	88	92	97	102	106	111	116	120	125	129	134	139	143	148	153	157	162	166	171	176	180	185	190	194	199	203	208	213	217	222	227	231
24	84	89	93	97	102	106	111	115	120	124	128	133	137	142	146	151	155	160	164	168	173	177	182	186	191	195	199	204	208	213	217	222
25	81	85	89	94	98	102	106	111	115	119	123	128	132	136	140	145	149	153	157	162	166	170	174	179	183	187	191	196	200	204	208	213
26	78	82	86	90	94	98	102	106	110	115	119	123	127	131	135	139	143	147	151	155	160	164	168	172	176	180	184	188	192	196	200	204
27	75	79	83	87	91	95	98	102	106	110	114	118	122	126	130	134	138	142	146	150	154	158	161	165	169	173	177	181	185	189	193	197
28	72	76	80	84	87	91	95	99	103	106	110	114	118	122	125	129	133	137	141	144	148	152	156	160	163	167	171	175	178	182	186	190
29	70	73	77	81	84	88	92	95	99	103	106	110	114	117	121	125	128	132	136	139	143	147	150	154	158	161	165	169	172	176	180	183
30	67	71	74	78	82	85	89	92	96	99	103	106	110	113	117	121	124	128	131	135	138	142	145	149	152	156	160	163	167	170	174	177
31	65	69	72	75	79	82	86	89	93	96	99	103	106	110	113	117	120	123	127	130	134	137	141	144	147	151	154	158	161	165	168	172
32	63	66	70	73	76	80	83	86	90	93	96	100	103	106	110	113	116	120	123	126	130	133	136	140	143	146	150	153	156	160	163	166
33	61	64	68	71	74	77	81	84	87	90	93	97	100	103	106	110	113	116	119	122	126	129	132	135	139	142	145	148	151	155	158	161
34	59	63	66	69	72	75	78	81	84	88	91	94	97	100	103	106	109	113	116	119	122	125	128	131	134	138	141	144	147	150	153	156
35	58	61	64	67	70	73	76	79	82	85	88	91	94	97	100	103	106	109	112	115	118	122	125	128	131	134	137	140	143	146	149	152
36	56	59	62	65	68	71	74	77	80	83	86	89	92	95	97	100	103	106	109	112	115	118	121	124	127	130	133	136	139	142	145	148
37	55	57	60	63	66	69	72	75	78	80	83	86	89	92	95	98	101	103	106	109	112	115	118	121	124	126	129	132	135	138	141	144
38	53	56	59	62	64	67	70	73	76	78	81	84	87	90	92	95	98	101	104	106	109	112	115	118	120	123	126	129	132	134	137	140
39	52	55	57	60	63	65	68	71	74	76	79	82	85	87	90	93	95	98	101	104	106	109	112	115	117	120	123	125	128	131	134	136
40	51	53	56	58	61	64	66	69	72	74	77	80	82	85	88	90	93	96	98	101	104	106	109	112	114	117	120	122	125	128	130	133
41	49	52	54	57	60	62	65	67	70	73	75	78	80	83	86	88	91	93	96	99	101	104	106	109	112	114	117	119	122	124	127	130
42	48	51	53	56	58	61	63	66	68	71	73	76	78	81	84	86	89	91	94	96	99	101	104	106	109	111	114	116	119	122	124	127
43	47	49	52	54	57	59	62	64	67	69	72	74	77	79	82	84	87	89	91	94	96	99	101	104	106	109	111	114	116	119	121	124
44	46	48	51	53	56	58	60	63	65	68	70	73	75	77	80	82	85	87	89	92	94	97	99	102	104	106	109	111	114	116	118	121
45	45	47	50	52	54	57	59	61	64	66	69	71	73	76	78	80	83	85	87	90	92	95	97	99	102	104	106	109	111	113	116	118



TS = Tensile Strength (55,000)

t = Thickness of Cylindrical Component

TS x t x E/R x FS

R = Radius of Shell (inside diameter/2)

E = Joint Efficiency (58%)

FS = Factor of Safety (6)

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	4.75	5	5.25	5.5	5.75	6	6.25	6.5	6.75	7	7.25	7.5	7.75	8	8.25	8.5
300	1163.	1224	1286	1347	1408	1469	1531	1592	1653	1714	1775	1837	1898	1959	2020	2082
325	1074	1130	1187	1243	1300	1356	1413	1469	1526	1582	1639	1695	1752	1808	1865	1921
350	997	1050	1102	1154	1207	1259	1312.	1364	1417	1469	1522	1574	1627	1679	1732	1784
375	931	980	1029	1078	1126	1175	1224	1273	1322	1371	1420	1469	1518	1567	1616	1665
400	872	918	964	1010	1056	1102	1148	1194	1240	1286	1332	1378	1423	1469	1515	1561
425	821	864	908	951	994	1037	1080	1124	1167	1210	1253	1296	1340	1383	1426	1469
450	775	816	857	898	939	980	1020	1061	1102	1143	1184	1224	1265	1306	1347	1388
475	735	773	812	851	889	928	967	1005	1044	1083	1121	1160	1199	1237	1276	1315
500	698	735	771	808	845	882	918	955	992	1029	1065	1102	1139	1175	1212	1249
525	665	700	735	770	805	840	875	910	945	980	1015	1050	1085	1119	1154	1189
550	634	668	701	735	768	801	835	868	902	935	968	1002	1035	1069	1102	1135
575	607	639	671	703	735	767	799	830	862	894	926	958	990	1022	1054	1086
600	582	612	643	673	704	735	765	796	827	857	888	918	949	980	1010	1041
625	558.	588	617	647	676	705	735	764	793	823	852	882	911	940	970	999
650	537	565	593	622	650	678	706	735	763	791	819	848	876	904	932	961
675	517	544	571	599	626	653	680	707	735	762	789	816	844	871	898	925
700	499.	525	551	577	603	630	656	682	708	735	761	787	813	840	866	892
725	481	507	532	557	583	608	633	659	684	709	735	760	785	811	836	861
750	465	490	514	539	563	588	612	637	661	686	710	735	759	784	808	833
775	450	474	498	521	545	569	592	616	640	664	687	711	735	758	782	806
800	436	459	482	505	528	551	574	597	620	643	666	689	712	735	758	781
825	423	445	468	490	512	534	557	579	601	623	646	668	690	712	735	757
850	411	432	454	475	497	519	540	562	583	605	627	648	670	691	713	735
875	399	420	441	462	483	504	525	546	567	588	609	630	651	672	693	714
900	388	408	429	449	469	490	510	531	551	571	592	612	633	653	673	694
925	377	397	417	437	457	477	496	516	536	556	576	596	616	635	655	675
950	367	387	406	425	445	464	483	503	522	541	561	580	599	619	638	657
975	358	377	396.	414	433	452	471	490	509	527	546	556	584	603	622	640
1000	349	367	386	404	422	441	459	478	496	514	533	551	569	588	606	624
1025	340	358	376	394	412	430	448	466	484	502	520	538	555	573	591	609
1050	332	350	367	385	402	420	437	455	472	490	507	525	542	560	577	595
1075	325.	342	359	376	393	410	427	444	461	478	495	513	530	547	564	581
1100	317	334	351	367	384	401	417	434	451	468	484	501	518	534	551	568
1125	310	327	343	359	375	392	408	424	441	457	473	490	506	522	539	555
1150	303	319	335	351	367	383	399	415	431	447	463	479	495	511	527	543

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 58 %

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 6
P = MAWP, kPa

Table S2.10.3.1 Metric (Page 1 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Single-Riveted Lap Joint

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	8.75	9	9.25	9.5	9.75	10	10.25	10.5	10.75	11	11.25	11.5	11.75	12	12.25	12.5
300	2143	2204	2265	2326	2395	2449	2510	2571	2633	2694	2755	2816	2877	2939	3000	3061
325	1978	2034	2091	2147	2211	2261	2317	2374	2430	2487	2543	2600	2656	2713	2769	2826
350	1837	1889	1942	1994	2053	2099	2152	2204	2256	2309	2361	2414	2466	2519	2571	2624
375	1714	1763	1812	1861	1916	1959	2008	2057	2106	2155	2204	2253	2302	2351	2400	2449
400	1607	1653	1699	1745	1796	1837	1883	1929	1974	2020	2066	2112	2158	2204	2250	2296
425	1513	1556	1599	1642	1691	1729	1772	1815	1858	1901	1945	1988	2031	2074	2118	2161
450	1429	1469	1510	1551	1597	1633	1673	1714	1755	1796	1837	1877	1918	1959	2000	2041
475	1353	1392	1431	1469	1513	1547	1585	1624	1663	1701	1740	1779	1817	1856	1895	1933
500	1286	1322	1359	1396	1437	1469	1506	1543	1580	1616	1653	1690	1726	1763	1800	1837
525	1224	1259	1294	1329	1369	1399	1434	1469	1504	1539	1574	1609	1644	1679	1714	1749
550	1169	1202	1236	1269	1306	1336	1369	1403	1436	1469	1503	1536	1570	1603	1636	1670
575	1118	1150	1182	1214	1250	1278	1310	1342	1374	1405	1437	1469	1501	1533	1565	1597
600	1071	1102	1133	1163	1198	1224	1255	1286	1316	1347	1378	1408	1439	1469	1500	1531
625	1029	1058	1087	1117	1150	1175	1205	1234	1264	1293	1322	1352	1381	1411	1440	1469
650	989	1017	1045	1074	1105	1130	1159	1187	1215	1243	1272	1300	1328	1356	1385	1413
675	952	980	1007	1034	1064	1088	1116	1143	1170	1197	1224	1252	1279	1306	1333	1360
700	918	945	971	997	1026	1050	1076	1102	1128	1154	1181	1207	1233	1259	1286	1312
725	887	912	937	963	991	1013	1039	1064	1089	1115	1140	1165	1191	1216	1241	1267
750	857	882	906	931	958	980	1004	1029	1053	1078	1102	1126	1151	1175	1200	1224
775	829	853	877	901	927	948	972	995	1019	1043	1066	1090	1114	1138	1161	1185
800	804	827	849	872	898	918	941	964	987	1010	1033	1056	1079	1102	1125	1148
825	779	801	824	846	871	891	913	935	957	980	1002	1024	1046	1069	1091	1113
850	756	778	799	821	845	864	886	908	929	951	972	994	1016	1037	1059	1080
875	735	756	777	798	821	840	861	882	903	924	945	966	987	1008	1029	1050
900	714	735	755	775	798	816	837	857	878	898	918	939	959	980	1000	1020
925	695	715	735	755	777	794	814	834	854	874	894	913	933	953	973	993
950	677	696	715	735	756	773	793	812	831	851	870	889	909	928	947	967
975	659	678	697	716	737	754	772	791	810	829	848	867	885	904	923	942
1000	643	661	680	698	719	735	753	771	790	808	827	845	863	882	900	918
1025	627	645	663	681	701	717	735	753	771	788	806	824	842	860	878	896
1050	612	630	647	665	684	700	717	735	752	770	787	805	822	840	857	875
1075	598	615	632	649	668	683	700	718	735	752	769	786	803	820	837	854
1100	584	601	618	634	653	668	685	701	718	735	751	768	785	801	818	835
1125	571	588	604	620	639	653	669	686	702	718	735	751	767	784	800	816
1150	559	575	591	607	625	639	655	671	687	703	719	735	751	767	783	799

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 58 %

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 6
P = MAWP, kPa

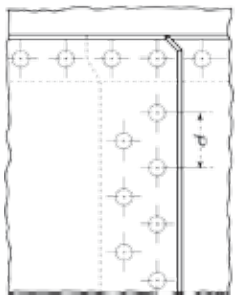
Table S2.10.3.1 Metric (Page 2 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Single-Riveted Lap Joint

TABLE S2.10.3.2

MAXIMUM ALLOWABLE WORKING PRESSURE FOR CYLINDRICAL COMPONENTS (BARREL)

For Double-Riveted Lap Joint

Shell ID	Minimum Thickness of Shell Plate																																	
	0.19	0.2	0.21	0.22	0.23	0.24	0.25	0.26	0.27	0.28	0.29	0.3	0.31	0.32	0.33	0.34	0.35	0.36	0.37	0.38	0.39	0.4	0.41	0.42	0.43	0.44	0.45	0.46	0.47	0.48	0.49	0.5
12	215	226	237	249	260	271	283	294	305	317	328	339	350	362	373	384	396	407	418	430	441	452	464	475	486	497	509	520	531	543	554	565
13	198	209	219	230	240	250	261	271	282	292	303	313	324	334	344	355	365	376	386	397	407	417	428	438	449	459	470	480	490	501	511	522
14	184	194	204	213	223	233	242	252	262	271	281	291	300	310	320	329	339	349	359	368	378	388	397	407	417	426	436	446	455	465	475	485
15	172	181	190	199	208	217	226	235	244	253	262	271	280	289	298	308	317	326	335	344	353	362	371	380	389	398	407	416	425	434	443	452
16	161	170	178	187	195	204	212	220	229	237	246	254	263	271	280	288	297	305	314	322	331	339	348	356	365	373	382	390	399	407	415	424
17	152	160	168	176	184	192	200	207	215	223	231	239	247	255	263	271	279	287	295	303	311	319	327	335	343	351	359	367	375	383	391	399
18	143	151	158	166	173	181	188	196	204	211	219	226	234	241	249	256	264	271	279	286	294	301	309	317	324	332	339	347	354	362	369	377
19	136	143	150	157	164	171	179	186	193	200	207	214	221	228	236	243	250	257	264	271	278	286	293	300	307	314	321	328	336	343	350	357
20	129	136	142	149	156	163	170	176	183	190	197	204	210	217	224	231	237	244	251	258	265	271	278	285	292	298	305	312	319	326	332	339
21	123	129	136	142	149	155	162	168	174	181	187	194	200	207	213	220	226	233	239	245	252	258	265	271	278	284	291	297	304	310	317	323
22	117	123	130	136	142	148	154	160	167	173	179	185	191	197	204	210	216	222	228	234	241	247	253	259	265	271	278	284	209	296	302	308
23	112	118	124	130	136	142	147	153	159	165	171	177	183	189	195	201	206	212	218	224	230	236	242	248	254	260	265	271	277	283	289	295
24	107	113	119	124	130	136	141	147	153	158	164	170	175	181	187	192	198	204	209	215	220	226	232	237	243	249	254	260	266	271	277	283
25	103	109	114	119	125	130	136	141	147	152	157	163	168	174	179	185	190	195	201	206	212	217	222	228	233	239	244	250	255	260	266	271
26	99	104	110	115	120	125	130	136	141	146	151	157	162	167	172	177	183	188	193	198	204	209	214	219	224	230	235	240	245	250	256	261
27	95	100	106	111	116	121	126	131	136	141	146	151	156	161	166	171	176	181	186	191	196	201	206	211	216	221	226	231	236	241	246	251
28	92	97	102	107	111	116	121	126	131	136	141	145	150	155	160	165	170	174	179	184	189	194	199	204	208	213	218	223	228	233	237	242
29	89	94	98	103	108	112	117	122	126	131	136	140	145	150	154	159	164	168	173	178	182	187	192	196	201	206	211	215	220	225	229	234
30	86	90	95	99	104	109	113	118	122	127	131	136	140	145	149	154	158	163	167	172	176	181	185	190	194	199	204	208	213	217	222	226
31	83	88	92	96	101	105	109	114	118	123	127	131	136	140	144	149	153	158	162	166	171	175	179	184	188	193	197	201	206	210	214	219
32	81	85	89	93	98	102	106	110	114	119	123	127	131	136	140	144	148	153	157	161	165	170	174	178	182	187	191	195	199	204	208	212
33	78	82	86	90	95	99	103	107	111	115	119	123	127	132	136	140	144	148	152	156	160	164	169	173	177	181	185	189	193	197	201	206
34	76	80	84	88	92	96	100	104	108	112	116	120	124	128	132	136	140	144	148	152	156	160	164	168	172	176	180	184	188	192	196	200
35	74	78	81	85	89	93	97	101	105	109	112	116	120	124	128	132	136	140	143	147	151	155	159	163	167	171	174	178	182	186	190	194
36	72	75	79	83	87	90	94	98	102	106	109	113	117	121	124	128	132	136	139	143	147	151	155	158	162	166	170	173	177	181	185	188
37	70	73	77	81	84	88	92	95	99	103	106	110	114	117	121	125	128	132	136	139	143	147	150	154	158	161	165	169	172	176	180	183
38	68	71	75	79	82	86	89	93	96	100	104	107	111	114	118	121	125	129	132	136	139	143	146	150	154	157	161	164	168	171	175	179
39	66	70	73	77	80	83	87	90	94	97	101	104	108	111	115	118	122	125	129	132	136	139	143	146	150	153	157	160	163	167	170	174
40	64	68	71	75	78	81	85	88	92	95	98	102	105	109	112	115	119	122	125	129	132	136	139	142	146	149	153	156	159	163	166	170
41	63	66	69	73	76	79	83	86	89	93	96	99	103	106	109	113	116	119	122	126	129	132	136	139	142	146	149	152	156	159	162	165
42	61	65	68	71	74	78	81	84	87	90	94	97	100	103	107	110	113	116	120	123	126	129	132	136	139	142	145	149	152	155	158	162
43	60	63	66	69	73	76	79	82	85	88	91	95	98	101	104	107	110	114	117	120	123	126	129	133	136	139	142	145	148	151	155	158
44	59	62	65	68	71	74	77	80	83	86	89	93	96	99	102	105	108	111	114	117	120	123	126	130	133	136	139	142	145	148	151	154
45	57	60	63	66	69	72	75	78	81	84	87	90	93	96	99	103	106	109	112	115	118	121	124	127	130	133	136	139	142	145	148	151



TS = Tensile Strength (55,000)

t = Thickness of Cylindrical Component

E = Joint Efficiency (74%)

TS x t x E/R x FS

R = Radius of Shell (inside diameter/2)

FS = Factor of Safety (6)

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	4.75	5	5.25	5.5	5.75	6	6.25	6.5	6.75	7	7.25	7.5	7.75	8	8.25	8.5
300	1484	1562	1640	1718	1797	1875	1953	2031	2109	2187	2265	2343	2421	2500	2578	2656
325	1370	1442	1514	1586	1658	1730	1803	1875	1947	2019	2091	2163	2235	2307	2379	2451
350	1272	1339	1406	1473	1540	1607	1674	1741	1808	1875	1942	2009	2076	2142	2209	2276
375	1187	1250	1312	1375	1437	1500	1562	1625	1687	1750	1812	1875	1937	2000	2062	2125
400	1113	1172	1230	1289	1347	1406	1465	1523	1582	1640	1699	1758	1816	1875	1933	1992
425	1048	1103	1158	1213	1268	1323	1378	1434	1489	1544	1599	1654	1709	1764	1820	1875
450	989	1041	1094	1146	1198	1250	1302	1354	1406	1458	1510	1562	1614	1666	1718	1771
475	937	987	1036	1085	1135	1184	1233	1283	1332	1381	1431	1480	1529	1579	1628	1677
500	890	937	984	1031	1078	1125	1172	1219	1265	1312	1359	1406	1453	1500	1547	1593
525	848	893	937	982	1027	1071	1116	1161	1205	1250	1294	1339	1384	1428	1473	1518
550	810	852	895	937	980	1023	1065	1108	1150	1193	1236	1278	1321	1363	1406	1449
575	774	815	856	897	937	978	1019	1060	1100	1141	1182	1223	1263	1304	1345	1386
600	742	781	820	859	898	937	976	1015	1055	1094	1133	1172	1211	1250	1289	1328
625	712	750	787	825	862	900	937	975	1012	1050	1087	1125	1162	1200	1237	1275
650	685	721	757	793	829	865	901	937	973	1009	1045	1082	1118	1154	1190	1226
675	660	694	729	764	798	833	868	903	937	972	1007	1041	1076	1111	1146	1180
700	636	670	703	736	770	803	837	870	904	937	971	1004	1038	1071	1105	1138
725	614	646	679	711	743	776	808	840	873	905	937	970	1002	1034	1067	1099
750	594	625	656	687	719	750	781	812	844	875	906	937	969	1000	1031	1062
775	574	605	635	665	695	726	756	786	816	847	877	907	937	968	998	1028
800	557	586	615	644	674	703	732	762	791	820	849	879	908	937	967	996
825	540	568	596	625	653	682	710	739	767	795	824	852	881	909	937	966
850	524	551	579	607	634	662	689	717	744	772	799	827	855	882	910	937
875	509	536	562	589	616	643	670	696	723	750	777	803	830	857	884	911
900	495	521	547	573	599	625	651	677	703	729	755	781	807	833	859	885
925	481	507	532	557	583	608	633	659	684	709	735	760	785	811	836	861
950	469	493	518	543	567	592	617	641	666	691	715	740	765	789	814	839
975	457	481	505	529	553	577	601	625	649	673	697	721	745	769	793	817
1000	445	469	492	516	539	562	586	609	633	656	680	703	726	750	773	797
1025	434	457	480	503	526	549	572	594	617	640	663	686	709	732	754	777
1050	424	446	469	491	513	536	558	580	603	625	647	670	692	714	736	759
1075	414	436	458	480	501	523	545	567	589	610	632	654	676	698	719	741
1100	405	426	447	469	490	511	533	554	575	596	618	639	660	682	703	724
1125	396	417	437	458	479	500	521	542	562	583	604	625	646	667	687	708
1150	387	408	428	448	469	489	509	530	550	571	591	611	632	652	672	693

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 6
P = MAWP, kPa

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 74 %

Table S2.10.3.2 Metric (Page 1 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Double-Riveted Lap Joint

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	8.75	9	9.25	9.5	9.75	10	10.25	10.5	10.75	11	11.25	11.5	11.75	12	12.25	12.5
300	2734	2812	2890	2968	3056	3124	3203	3281	3359	3437	3515	3593	3671	3749	3827	3906
325	2524	2596	2668	2740	2821	2884	2956	3028	3100	3173	3245	3317	3389	3461	3533	3605
350	2343	2410	2477	2544	2619	2678	2745	2812	2879	2946	3013	3080	3147	3214	3281	3348
375	2187	2250	2312	2375	2445	2500	2562	2625	2687	2750	2812	2874	2937	2999	3062	3124
400	2050	2109	2168	2226	2292	2343	2402	2461	2519	2578	2636	2695	2753	2812	2871	2929
425	1930	1985	2040	2095	2157	2205	2261	2316	2371	2426	2481	2536	2591	2647	2702	2757
450	1823	1875	1927	1979	2037	2083	2135	2187	2239	2291	2343	2395	2447	2500	2552	2604
475	1727	1776	1825	1875	1930	1973	2023	2072	2121	2171	2220	2269	2319	2368	2417	2467
500	1640	1687	1734	1781	1833	1875	1922	1968	2015	2062	2109	2156	2203	2250	2296	2343
525	1562	1607	1651	1696	1746	1785	1830	1875	1919	1964	2009	2053	2098	2142	2187	2232
550	1491	1534	1576	1619	1667	1704	1747	1789	1832	1875	1917	1960	2002	2045	2088	2130
575	1426	1467	1508	1549	1594	1630	1671	1712	1752	1793	1834	1875	1915	1956	1997	2038
600	1367	1406	1445	1484	1528	1562	1601	1640	1679	1718	1758	1797	1836	1875	1914	1953
625	1312	1350	1387	1425	1467	1500	1537	1575	1612	1650	1687	1725	1762	1800	1837	1875
650	1262	1298	1334	1370	1410	1442	1478	1514	1550	1586	1622	1658	1694	1730	1767	1803
675	1215	1250	1284	1319	1358	1389	1423	1458	1493	1528	1562	1597	1632	1666	1701	1736
700	1172	1205	1239	1272	1310	1339	1373	1406	1439	1473	1506	1540	1573	1607	1640	1674
725	1131	1164	1196	1228	1264	1293	1325	1358	1390	1422	1454	1487	1519	1551	1584	1616
750	1094	1125	1156	1187	1222	1250	1281	1312	1344	1375	1406	1437	1468	1500	1531	1562
775	1058	1089	1119	1149	1183	1209	1240	1270	1300	1330	1361	1391	1421	1451	1482	1512
800	1025	1055	1084	1113	1146	1172	1201	1230	1260	1289	1318	1347	1377	1406	1435	1465
825	994	1023	1051	1079	1111	1136	1165	1193	1221	1250	1278	1307	1335	1363	1392	1420
850	965	992	1020	1048	1078	1103	1130	1158	1185	1213	1241	1268	1296	1323	1351	1378
875	937	964	991	1018	1048	1071	1098	1125	1152	1178	1205	1232	1259	1285	1312	1339
900	911	937	963	989	1019	1041	1068	1094	1120	1146	1172	1198	1224	1250	1276	1302
925	887	912	937	963	991	1013	1039	1064	1089	1115	1140	1165	1191	1216	1241	1267
950	863	888	913	937	965	987	1011	1036	1061	1085	1110	1135	1159	1184	1209	1233
975	841	865	889	913	940	961	985	1009	1033	1058	1082	1106	1130	1154	1178	1202
1000	820	844	867	890	917	937	961	984	1008	1031	1055	1078	1101	1125	1148	1172
1025	800	823	846	869	894	914	937	960	983	1006	1029	1052	1075	1097	1120	1143
1050	781	803	826	848	873	893	915	937	960	982	1004	1027	1049	1071	1094	1116
1075	763	785	807	828	853	872	894	916	937	959	981	1003	1025	1046	1068	1090
1100	746	767	788	810	833	852	873	895	916	937	959	980	1001	1023	1044	1065
1125	729	750	771	792	815	833	854	875	896	917	937	958	979	1000	1021	1041
1150	713	734	754	774	797	815	835	856	876	897	917	937	958	978	998	1019

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 74 %

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 6
P = MAWP, kPa

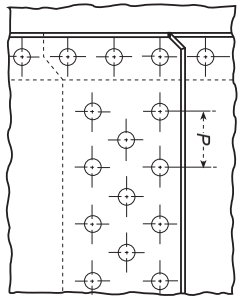
Table S2.10.3.2 Metric (Page 2 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Double-Riveted Lap Joint

TABLE S2.10.3.3

MAXIMUM ALLOWABLE WORKING PRESSURE FOR CYLINDRICAL COMPONENTS (BARREL)

For Triple-Riveted Lap Joint

Shell ID	Minimum Thickness of Shell Plate																																
	0.19	0.2	0.21	0.22	0.23	0.24	0.25	0.26	0.27	0.28	0.29	0.3	0.31	0.32	0.33	0.34	0.35	0.36	0.37	0.38	0.39	0.4	0.41	0.42	0.43	0.44	0.45	0.46	0.47	0.48	0.49	0.5
12	226	238	250	262	274	286	298	310	322	334	346	358	369	381	393	405	417	429	441	453	465	477	489	501	512	524	536	548	560	572	584	596
13	209	220	231	242	253	264	275	286	297	308	319	330	341	352	363	374	385	396	407	418	429	440	451	462	473	484	495	506	517	528	539	550
14	194	204	215	225	235	245	255	266	276	286	296	306	317	327	337	347	358	368	378	388	398	409	419	429	439	449	460	470	480	490	501	511
15	181	191	200	210	219	229	238	248	257	267	276	286	296	305	315	324	334	343	353	362	372	381	391	400	410	419	429	439	448	458	467	477
16	170	179	188	197	206	215	223	232	241	250	259	268	277	286	295	304	313	322	331	340	349	358	366	375	384	393	402	411	420	429	438	447
17	160	168	177	185	193	202	210	219	227	236	244	252	261	269	278	286	294	303	311	320	328	336	345	353	362	370	379	387	395	404	412	421
18	151	159	167	175	183	191	199	207	215	222	230	238	246	254	262	270	278	286	294	302	310	318	326	334	342	350	358	365	373	381	389	397
19	143	151	158	166	173	181	188	196	203	211	218	226	233	241	248	256	263	271	278	286	294	301	309	316	324	331	339	346	354	361	369	376
20	136	143	150	157	164	172	179	186	193	200	207	215	222	229	236	243	250	257	265	272	279	286	293	300	307	315	322	329	336	343	350	358
21	129	136	143	150	157	163	170	177	184	191	197	204	211	218	225	232	238	245	252	259	266	272	279	286	293	300	306	313	320	327	334	340
22	124	130	137	143	150	156	163	169	176	182	189	195	202	208	215	221	228	234	241	247	254	260	267	273	280	286	293	299	306	312	319	325
23	118	124	131	137	143	149	155	162	168	174	180	187	193	199	205	211	218	224	230	236	242	249	255	261	267	274	280	286	292	298	305	311
24	113	119	125	131	137	143	149	155	161	167	173	179	185	191	197	203	209	215	220	226	232	238	244	250	256	262	268	274	280	286	292	298
25	109	114	120	126	132	137	143	149	154	160	166	172	177	183	189	194	200	206	212	217	223	229	235	240	246	252	257	263	269	275	280	286
26	105	110	116	121	127	132	138	143	149	154	160	165	171	176	182	187	193	198	204	209	215	220	226	231	237	242	248	253	259	264	270	275
27	101	106	111	117	122	127	132	138	143	148	154	159	164	169	175	180	185	191	196	201	207	212	217	222	228	233	238	244	249	254	260	265
28	97	102	107	112	117	123	128	133	138	143	148	153	158	163	169	174	179	184	189	194	199	204	209	215	220	225	230	235	240	245	250	255
29	94	99	104	108	113	118	123	128	133	138	143	148	153	158	163	168	173	178	182	187	192	197	202	207	212	217	222	227	232	237	242	247
30	91	95	100	105	110	114	119	124	129	133	138	143	148	153	157	162	167	172	176	181	186	191	195	200	205	210	215	219	224	229	234	238
31	88	92	97	101	106	111	115	120	125	129	134	138	143	148	152	157	161	166	171	175	180	185	189	194	198	203	208	212	217	221	226	231
32	85	89	94	98	103	107	112	116	121	125	130	134	139	143	147	152	156	161	165	170	174	179	183	188	192	197	201	206	210	215	219	223
33	82	87	91	95	100	104	108	113	117	121	126	130	134	139	143	147	152	156	160	165	169	173	178	182	186	191	195	199	204	208	212	217
34	80	84	88	93	97	101	105	109	114	118	122	126	130	135	139	143	147	151	156	160	164	168	172	177	181	185	189	193	198	202	206	210
35	78	82	86	90	94	98	102	106	110	114	118	123	127	131	135	139	143	147	151	155	159	163	168	172	176	180	184	188	192	196	200	204
36	75	79	83	87	91	95	99	103	107	111	115	119	123	127	131	135	139	143	147	151	155	159	163	167	171	175	179	183	187	191	195	199
37	73	77	81	85	89	93	97	100	104	108	112	116	120	124	128	131	135	139	143	147	151	155	158	162	166	170	174	178	182	186	189	193
38	72	75	79	83	87	90	94	98	102	105	109	113	117	120	124	128	132	135	139	143	147	151	154	158	162	166	169	173	177	181	184	188
39	70	73	77	81	84	88	92	95	99	103	106	110	114	117	121	125	128	132	136	139	143	147	150	154	158	161	165	169	172	176	180	183
40	68	72	75	79	82	86	89	93	97	100	104	107	111	114	118	122	125	129	132	136	139	143	147	150	154	157	161	164	168	172	175	179
41	66	70	73	77	80	84	87	91	94	98	101	105	108	112	115	119	122	126	129	133	136	140	143	146	150	153	157	160	164	167	171	174
42	65	68	72	75	78	82	85	89	92	95	99	102	106	109	112	116	119	123	126	129	133	136	140	143	146	150	153	157	160	163	167	170
43	63	67	70	73	76	80	83	86	90	93	96	100	103	106	110	113	116	120	123	126	130	133	136	140	143	146	150	153	156	160	163	166
44	62	65	68	72	75	78	81	85	88	91	94	98	101	104	107	111	114	117	120	124	127	130	133	137	140	143	146	150	153	156	159	163
45	60	64	67	70	73	76	79	83	86	89	92	95	99	102	105	108	111	114	118	121	124	127	130	133	137	140	143	146	149	153	156	159



TS = Tensile Strength (55,000)

t = Thickness of Cylindrical Component

TS x t x E/R x FS

R = Radius of Shell (inside diameter/2)

E = Joint Efficiency (78%)

FS = Factor of Safety (6)

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	4.75	5	5.25	5.5	5.75	6	6.25	6.5	6.75	7	7.25	7.5	7.75	8	8.25	8.5
300	1564	1647	1729	1811	1894	1976	2058	2141	2223	2305	2388	2470	2552	2635	2717	2799
325	1444	1520	1596	1672	1748	1824	1900	1976	2052	2128	2204	2280	2356	2432	2508	2584
350	1341	1411	1482	1553	1623	1694	1764	1835	1905	1976	2047	2117	2188	2258	2329	2399
375	1251	1317	1383	1449	1515	1581	1647	1713	1778	1844	1910	1976	2042	2108	2174	2239
400	1173	1235	1297	1359	1420	1482	1544	1606	1667	1729	1791	1853	1914	1976	2038	2100
425	1104	1162	1220	1279	1337	1395	1453	1511	1569	1627	1685	1744	1802	1860	1918	1976
450	1043	1098	1153	1208	1262	1317	1372	1427	1482	1537	1592	1647	1702	1756	1811	1866
475	988	1040	1092	1144	1196	1248	1300	1352	1404	1456	1508	1560	1612	1664	1716	1768
500	939	988	1037	1087	1136	1186	1235	1284	1334	1383	1433	1482	1531	1581	1630	1680
525	894	941	988	1035	1082	1129	1176	1223	1270	1317	1364	1411	1458	1506	1553	1600
550	853	898	943	988	1033	1078	1123	1168	1213	1257	1302	1347	1392	1437	1482	1527
575	816	859	902	945	988	1031	1074	1117	1160	1203	1246	1289	1332	1375	1418	1461
600	782	823	865	906	947	988	1029	1070	1112	1153	1194	1235	1276	1317	1359	1400
625	751	790	830	869	909	948	988	1028	1067	1107	1146	1186	1225	1265	1304	1344
650	722	760	798	836	874	912	950	988	1026	1064	1102	1140	1178	1216	1254	1292
675	695	732	768	805	842	878	915	951	988	1025	1061	1098	1134	1171	1208	1244
700	670	706	741	776	812	847	882	917	953	988	1023	1059	1094	1129	1164	1200
725	647	681	715	750	784	818	852	886	920	954	988	1022	1056	1090	1124	1158
750	626	659	692	725	757	790	823	856	889	922	955	988	1021	1054	1087	1120
775	606	637	669	701	733	765	797	829	861	892	924	956	988	1020	1052	1084
800	587	618	648	679	710	741	772	803	834	865	895	926	957	988	1019	1050
825	569	599	629	659	689	719	748	778	808	838	868	898	928	958	988	1018
850	552	581	610	639	668	697	726	756	785	814	843	872	901	930	959	988
875	536	565	593	621	649	677	706	734	762	790	819	847	875	903	932	960
900	521	549	576	604	631	659	686	714	741	768	796	823	851	878	906	933
925	507	534	561	587	614	641	668	694	721	748	774	801	828	854	881	908
950	494	520	546	572	598	624	650	676	702	728	754	780	806	832	858	884
975	481	507	532	557	583	608	633	659	684	709	735	760	785	811	836	861
1000	469	494	519	543	568	593	618	642	667	692	716	741	766	790	815	840
1025	458	482	506	530	554	578	602	627	651	675	699	723	747	771	795	819
1050	447	470	494	518	541	565	588	612	635	659	682	706	729	753	776	800
1075	437	460	483	505	528	551	574	597	620	643	666	689	712	735	758	781
1100	427	449	472	494	516	539	561	584	606	629	651	674	696	719	741	763
1125	417	439	461	483	505	527	549	571	593	615	637	659	681	703	725	746
1150	408	430	451	473	494	515	537	558	580	601	623	644	666	687	709	730

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 78%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 6
P = MAWP, kPa

Table S2.10.3.3 Metric (Page 1 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Triple-Riveted Lap Joint

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	8.75	9	9.25	9.5	9.75	10	10.25	10.5	10.75	11	11.25	11.5	11.75	12	12.25	12.5
300	2882	2964	3046	3129	3221	3293	3376	3458	3540	3623	3705	3787	3870	3952	4034	4117
325	2660	2736	2812	2888	2973	3040	3116	3192	3268	3344	3420	3496	3572	3648	3724	3800
350	2470	2541	2611	2682	2761	2823	2893	2964	3035	3105	3176	3246	3317	3387	3458	3529
375	2305	2371	2437	2503	2577	2635	2701	2766	2832	2898	2964	3030	3096	3162	3227	3293
400	2161	2223	2285	2347	2416	2470	2532	2594	2655	2717	2779	2841	2902	2964	3026	3088
425	2034	2092	2150	2208	2274	2325	2383	2441	2499	2557	2615	2673	2732	2790	2848	2906
450	1921	1976	2031	2086	2147	2196	2250	2305	2360	2415	2470	2525	2580	2635	2690	2744
475	1820	1872	1924	1976	2034	2080	2132	2184	2236	2288	2340	2392	2444	2496	2548	2600
500	1729	1778	1828	1877	1933	1976	2025	2075	2124	2174	2223	2272	2322	2371	2421	2470
525	1647	1694	1741	1788	1841	1882	1929	1976	2023	2070	2117	2164	2211	2258	2305	2352
550	1572	1617	1662	1707	1757	1796	1841	1886	1931	1976	2021	2066	2111	2156	2201	2245
575	1503	1546	1589	1632	1680	1718	1761	1804	1847	1890	1933	1976	2019	2062	2105	2148
600	1441	1482	1523	1564	1610	1647	1688	1729	1770	1811	1853	1894	1935	1976	2017	2058
625	1383	1423	1462	1502	1546	1581	1620	1660	1699	1739	1778	1818	1857	1897	1936	2976
650	1330	1368	1406	1444	1487	1520	1558	1596	1634	1672	1710	1748	1786	1824	1862	1900
675	1281	1317	1354	1391	1432	1464	1500	1537	1573	1610	1647	1683	1720	1756	1793	1830
700	1235	1270	1306	1341	1380	1411	1447	1482	1517	1553	1588	1623	1658	1694	1729	1764
725	1192	1226	1261	1295	1333	1363	1397	1431	1465	1499	1533	1567	1601	1635	1669	1703
750	1153	1186	1219	1251	1288	1317	1350	1383	1416	1449	1482	1515	1548	1581	1614	1647
775	1115	1147	1179	1211	1247	1275	1307	1339	1370	1402	1434	1466	1498	1530	1562	1594
800	1081	1112	1142	1173	1208	1235	1266	1297	1328	1359	1389	1420	1451	1482	1513	1544
825	1048	1078	1108	1138	1171	1198	1228	1257	1287	1317	1347	1377	1407	1437	1467	1497
850	1017	1046	1075	1104	1137	1162	1191	1220	1250	1279	1308	1337	1366	1395	1424	1453
875	988	1016	1044	1073	1104	1129	1157	1186	1214	1242	1270	1299	1327	1355	1383	1411
900	961	988	1015	1043	1074	1098	1125	1153	1180	1208	1235	1262	1290	1317	1345	1372
925	935	961	988	1015	1045	1068	1095	1122	1148	1175	1202	1228	1255	1282	1308	1335
950	910	936	962	988	1017	1040	1066	1092	1118	1144	1170	1196	1222	1248	1274	1300
975	887	912	937	963	991	1013	1039	1064	1089	1115	1140	1165	1191	1216	1241	1267
1000	865	889	914	939	966	988	1013	1037	1062	1087	1112	1136	1161	1186	1210	1235
1025	843	868	892	916	943	964	988	1012	1036	1060	1084	1108	1133	1157	1181	1205
1050	823	847	870	894	920	941	964	988	1012	1035	1059	1082	1106	1129	1153	1176
1075	804	827	850	873	899	919	942	965	988	1011	1034	1057	1080	1103	1126	1149
1100	786	808	831	853	878	898	921	943	966	988	1010	1033	1055	1078	1100	1123
1125	768	790	812	834	859	878	900	922	944	966	988	1010	1032	1054	1076	1098
1150	752	773	795	816	840	859	881	902	924	945	967	988	1009	1031	1052	1074

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 78%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 6
P = MAWP, kPa

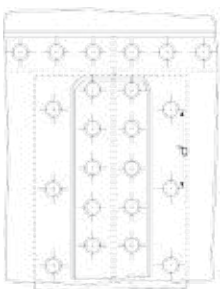
Table S2.10.3.3 Metric (Page 2 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Triple-Riveted Lap Joint

TABLE S2.10.3.4

MAXIMUM ALLOWABLE WORKING PRESSURE FOR CYLINDRICAL COMPONENTS (BARREL)

For Buttstrap Double-Riveted Joint

Shell ID	Minimum Thickness of Shell Plate																																
	0.19	0.2	0.21	0.22	0.23	0.24	0.25	0.26	0.27	0.28	0.29	0.3	0.31	0.32	0.33	0.34	0.35	0.36	0.37	0.38	0.39	0.4	0.41	0.42	0.43	0.44	0.45	0.46	0.47	0.48	0.49	0.5
12	286	301	316	331	346	361	376	391	406	421	436	451	466	481	496	511	526	541	556	571	586	601	616	631	646	661	677	692	707	722	737	752
13	264	278	291	305	319	333	347	361	375	389	402	416	430	444	458	472	486	500	513	527	541	555	569	583	597	611	624	638	652	666	680	694
14	245	258	271	283	296	309	322	335	348	361	374	387	399	412	425	438	451	464	477	490	503	515	528	541	554	567	580	593	606	619	631	644
15	229	241	253	265	277	289	301	313	325	337	349	361	373	385	397	409	421	433	445	457	469	481	493	505	517	529	541	553	565	577	589	601
16	214	226	237	248	259	271	282	293	304	316	327	338	350	361	372	383	395	406	417	428	440	451	462	474	485	496	507	519	530	541	552	564
17	202	212	223	233	244	255	265	276	287	297	308	318	329	340	350	361	371	382	393	403	414	424	435	446	456	467	478	488	499	509	520	531
18	190	200	210	220	231	241	251	261	271	281	291	301	311	321	331	341	351	361	371	381	391	401	411	421	431	441	451	461	471	481	491	501
19	180	190	199	209	218	228	237	247	256	266	275	285	294	304	313	323	332	342	351	361	370	380	389	399	408	418	427	437	446	456	465	475
20	171	180	189	198	207	216	226	235	244	253	262	271	280	289	298	307	316	325	334	343	352	361	370	379	388	397	406	415	424	433	442	451
21	163	172	180	189	198	206	215	223	232	241	249	258	266	275	283	292	301	309	318	326	335	344	352	361	369	378	387	395	404	412	421	430
22	156	164	172	180	189	197	205	213	221	230	238	246	254	262	271	279	287	295	303	312	320	328	336	344	353	361	369	377	385	394	402	410
23	149	157	165	173	180	188	196	204	212	220	227	235	243	251	259	267	275	282	290	298	306	314	322	329	337	345	353	361	369	376	384	392
24	143	150	158	165	173	180	188	195	203	210	218	226	233	241	248	256	263	271	278	286	293	301	308	316	323	331	338	346	353	361	368	376
25	137	144	152	159	166	173	180	188	195	202	209	216	224	231	238	245	253	260	267	274	281	289	296	303	310	318	325	332	339	346	354	361
26	132	139	146	153	160	167	173	180	187	194	201	208	215	222	229	236	243	250	257	264	271	278	284	291	298	305	312	319	326	333	340	347
27	127	134	140	147	154	160	167	174	180	187	194	200	207	214	220	227	234	241	247	254	261	267	274	281	287	294	301	307	314	321	327	334
28	122	129	135	142	148	155	161	168	174	180	187	193	200	206	213	219	226	232	238	245	251	258	264	271	277	283	290	296	303	309	316	322
29	118	124	131	137	143	149	156	162	168	174	180	187	193	199	205	212	218	224	230	236	243	249	255	261	267	274	280	286	292	299	305	311
30	114	120	126	132	138	144	150	156	162	168	174	180	186	192	198	204	210	216	222	229	235	241	247	253	259	265	271	277	283	289	295	301
31	111	116	122	128	134	140	145	151	157	163	169	175	180	186	192	198	204	209	215	221	227	233	239	244	250	256	262	268	274	279	285	291
32	107	113	118	124	130	135	141	147	152	158	163	169	175	180	186	192	197	203	209	214	220	226	231	237	242	248	254	259	265	271	276	282
33	104	109	115	120	126	131	137	142	148	153	159	164	169	175	180	186	191	197	202	208	213	219	224	230	235	241	246	251	257	262	268	273
34	101	106	111	117	122	127	133	138	143	149	154	159	164	170	175	180	186	191	196	202	207	212	218	223	228	233	239	244	249	255	260	265
35	98	103	108	113	119	124	129	134	139	144	149	155	160	165	170	175	180	186	191	196	201	206	211	216	222	227	232	237	242	247	253	258
36	95	100	105	110	115	120	125	130	135	140	145	150	155	160	165	170	175	180	185	190	195	200	205	210	215	220	226	231	236	241	246	251
37	93	98	102	107	112	117	122	127	132	137	141	146	151	156	161	166	171	176	180	185	190	195	200	205	210	215	219	224	229	234	239	244
38	90	95	100	104	109	114	119	123	128	133	138	142	147	152	157	161	166	171	176	180	185	190	195	199	204	209	214	218	223	228	233	237
39	88	93	97	102	106	111	116	120	125	130	134	139	143	148	153	157	162	167	171	176	180	185	190	194	199	204	208	213	217	222	227	231
40	86	90	95	99	104	108	113	117	122	126	131	135	140	144	149	153	158	162	167	171	176	180	185	189	194	198	203	207	212	216	221	226
41	84	88	92	97	101	106	110	114	119	123	128	132	136	141	145	150	154	158	163	167	172	176	180	185	189	194	198	202	207	211	216	220
42	82	86	90	94	99	103	107	112	116	120	125	129	133	137	142	146	150	155	159	163	168	172	176	180	185	189	193	198	202	206	210	215
43	80	84	88	92	96	101	105	109	113	117	122	126	130	134	138	143	147	151	155	159	164	168	172	176	180	185	189	193	197	201	206	210
44	78	82	86	90	94	98	103	107	111	115	119	123	127	131	135	139	144	148	152	156	160	164	168	172	176	180	185	189	193	197	201	205
45	76	80	84	88	92	96	100	104	108	112	116	120	124	128	132	136	140	144	148	152	156	160	164	168	172	176	180	184	188	192	196	200



TS = Tensile Strength (55,000)

t = Thickness of Cylindrical Component

TS x t x E/R x FS

R = Radius of Shell (inside diameter/2)

E = Joint Efficiency (82%)

FS = Factor of Safety (5)

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	4.75	5	5.25	5.5	5.75	6	6.25	6.5	6.75	7	7.25	7.5	7.75	8	8.25	8.5
300	1973	2077	2181	2285	2389	2493	2597	2701	2804	2908	3012	3116	3220	3324	3428	3531
325	1822	1918	2013	2109	2205	2301	2397	2493	2589	2685	2780	2876	2972	3068	3164	3260
350	1692	1781	1870	1959	2048	2137	2226	2315	2404	2493	2582	2671	2760	2849	2938	3027
375	1579	1662	1745	1828	1911	1994	2077	2160	2244	2327	2410	2493	2576	2659	2742	2825
400	1480	1558	1636	1714	1792	1870	1948	2025	2103	2181	2259	2337	2415	2493	2571	2649
425	1393	1466	1540	1613	1686	1760	1833	1906	1980	2053	2126	2200	2273	2346	2419	2493
450	1316	1385	1454	1523	1593	1662	1731	1800	1870	1939	2008	2077	2147	2216	2285	2354
475	1246	1312	1378	1443	1509	1574	1640	1706	1771	1837	1902	1968	2034	2099	2165	2230
500	1184	1246	1309	1371	1433	1496	1558	1620	1683	1745	1807	1870	1932	1994	2057	2119
525	1128	1187	1246	1306	1365	1424	1484	1543	1603	1662	1721	1781	1840	1899	1959	2018
550	1076	1133	1190	1246	1303	1360	1416	1473	1530	1586	1643	1700	1756	1813	1870	1926
575	1030	1084	1138	1192	1246	1301	1355	1409	1463	1517	1572	1626	1680	1734	1788	1843
600	987	1039	1091	1143	1194	1246	1298	1350	1402	1454	1506	1558	1610	1662	1714	1766
625	947	997	1047	1097	1147	1197	1246	1296	1346	1396	1446	1496	1546	1595	1645	1695
650	911	959	1007	1055	1103	1151	1198	1246	1294	1342	1390	1438	1486	1534	1582	1630
675	877	923	969	1016	1062	1108	1154	1200	1246	1293	1339	1385	1431	1477	1523	1570
700	846	890	935	979	1024	1068	1113	1157	1202	1246	1291	1335	1380	1424	1469	1513
725	817	860	903	946	989	1032	1074	1117	1160	1203	1246	1289	1332	1375	1418	1461
750	789	831	872	914	956	997	1039	1080	1122	1163	1205	1246	1288	1329	1371	1413
775	764	804	844	885	925	965	1005	1045	1086	1126	1166	1206	1246	1287	1327	1367
800	740	779	818	857	896	935	974	1013	1052	1091	1130	1169	1207	1246	1285	1324
825	718	755	793	831	869	906	944	982	1020	1058	1095	1133	1171	1209	1246	1284
850	697	733	770	806	843	880	916	953	990	1026	1063	1100	1136	1173	1210	1246
875	677	712	748	783	819	855	890	926	962	997	1033	1068	1104	1140	1175	1211
900	658	692	727	762	796	831	866	900	935	969	1004	1039	1073	1108	1143	1177
925	640	674	707	741	775	808	842	876	910	943	977	1011	1044	1078	1112	1145
950	623	656	689	722	754	787	820	853	886	918	951	984	1017	1050	1082	1115
975	607	639	671	703	735	767	799	831	863	895	927	959	991	1023	1055	1087
1000	592	623	654	686	717	748	779	810	841	872	904	935	966	997	1028	1059
1025	578	608	638	669	699	730	760	790	821	851	882	912	942	973	1003	1034
1050	564	594	623	653	683	712	742	772	801	831	861	890	920	950	979	1009
1075	551	580	609	638	667	696	725	754	783	812	841	870	899	928	957	986
1100	538	567	595	623	652	680	708	737	765	793	821	850	878	906	935	963
1125	526	554	582	609	637	665	692	720	748	776	803	831	859	886	914	942
1150	515	542	569	596	623	650	677	704	732	759	786	813	840	867	894	921

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 82%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 5
P = MAWP, kPa

Table S2.10.3.4 Metric (Page 1 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Buttstrap Double-Riveted Joint

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	8.75	9	9.25	9.5	9.75	10	10.25	10.5	10.75	11	11.25	11.5	11.75	12	12.25	12.5
300	3635	3739	3843	3947	4051	4155	4259	4362	4466	4570	4674	4778	4882	4986	5089	5193
325	3356	3452	3547	3643	3739	3835	3931	4027	4123	4219	4314	4410	4506	4602	4698	4794
350	3116	3205	3294	3383	3472	3561	3650	3739	3828	3917	4006	4095	4184	4273	4362	4451
375	2908	2991	3074	3158	3241	3324	3407	3490	3573	3656	3739	3822	3905	3988	4072	4155
400	2727	2804	2882	2960	3038	3116	3194	3272	3350	3428	3506	3583	3661	3739	3817	3895
425	2566	2639	2713	2786	2859	2933	3006	3079	3153	3226	3299	3373	3446	3519	3593	3666
450	2424	2493	2562	2631	2701	2770	2839	2908	2978	3047	3116	3185	3254	3324	3393	3462
475	2296	2362	2427	2493	2558	2624	2690	2755	2821	2886	2952	3018	3083	3149	3214	3280
500	2181	2244	2306	2368	2430	2493	2555	2617	2680	2742	2804	2867	2929	2991	3054	3116
525	2077	2137	2196	2255	2315	2374	2433	2493	2552	2612	2671	2730	2790	2849	2908	2968
550	1983	2040	2096	2153	2210	2266	2323	2379	2436	2493	2549	2606	2663	2719	2776	2833
575	1897	1951	2005	2059	2113	2168	2222	2276	2330	2384	2439	2493	2547	2601	2655	2710
600	1818	1870	1922	1973	2025	2077	2129	2181	2233	2285	2337	2389	2441	2493	2545	2597
625	1745	1795	1845	1895	1944	1994	2044	2094	2144	2194	2244	2293	2343	2393	2443	2493
650	1678	1726	1774	1822	1870	1918	1965	2013	2061	2109	2157	2205	2253	2301	2349	2397
675	1616	1662	1708	1754	1800	1847	1893	1939	1985	2031	2077	2123	2170	2216	2262	2308
700	1558	1603	1647	1692	1736	1781	1825	1870	1914	1959	2003	2048	2092	2137	2181	2226
725	1504	1547	1590	1633	1676	1719	1762	1805	1848	1891	1934	1977	2020	2063	2106	2149
750	1454	1496	1537	1579	1620	1662	1703	1745	1787	1828	1870	1911	1953	1994	2036	2077
775	1407	1447	1488	1528	1568	1608	1648	1689	1729	1769	1809	1849	1890	1930	1970	2010
800	1363	1402	1441	1480	1519	1558	1597	1636	1675	1714	1753	1792	1831	1870	1909	1948
825	1322	1360	1397	1435	1473	1511	1549	1586	1624	1662	1700	1737	1775	1813	1851	1888
850	1283	1320	1356	1393	1430	1466	1503	1540	1576	1613	1650	1686	1723	1760	1796	1833
875	1246	1282	1318	1353	1389	1424	1460	1496	1531	1567	1603	1638	1674	1709	1745	1781
900	1212	1246	1281	1316	1350	1385	1420	1454	1489	1523	1558	1593	1627	1662	1696	1731
925	1179	1213	1246	1280	1314	1347	1381	1415	1449	1482	1516	1550	1583	1617	1651	1684
950	1148	1181	1214	1246	1279	1312	1345	1378	1410	1443	1476	1509	1542	1574	1607	1640
975	1119	1151	1182	1214	1246	1278	1310	1342	1374	1406	1438	1470	1502	1534	1566	1598
1000	1091	1122	1153	1184	1215	1246	1278	1309	1340	1371	1402	1433	1465	1496	1527	1558
1025	1064	1094	1125	1155	1186	1216	1246	1277	1307	1338	1368	1398	1429	1459	1490	1520
1050	1039	1068	1098	1128	1157	1187	1217	1246	1276	1306	1335	1365	1395	1424	1454	1484
1075	1015	1043	1072	1101	1130	1159	1188	1217	1246	1275	1304	1333	1362	1391	1420	1449
1100	991	1020	1048	1076	1105	1133	1161	1190	1218	1246	1275	1303	1331	1360	1388	1416
1125	969	997	1025	1053	1080	1108	1136	1163	1191	1219	1246	1274	1302	1329	1357	1385
1150	948	975	1003	1030	1057	1084	1111	1138	1165	1192	1219	1246	1273	1301	1328	1355

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 82%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 5
P = MAWP, kPa

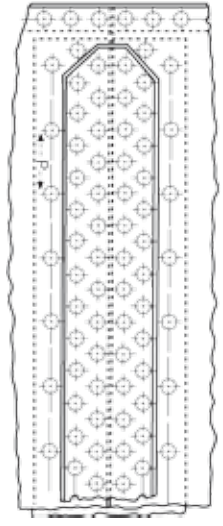
Table S2.10.3.4 Metric (Page 2 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Buttstrap Double-Riveted Joint

TABLE S2.10.3.5

MAXIMUM ALLOWABLE WORKING PRESSURE FOR CYLINDRICAL COMPONENTS (BARREL)

For Buttstrap Triple-Riveted Joint

Shell ID	Minimum Thickness of Shell Plate																																
	0.19	0.2	0.21	0.22	0.23	0.24	0.25	0.26	0.27	0.28	0.29	0.3	0.31	0.32	0.33	0.34	0.35	0.36	0.37	0.38	0.39	0.4	0.41	0.42	0.43	0.44	0.45	0.46	0.47	0.48	0.49	0.5
12	307	323	339	355	371	387	403	419	436	452	468	484	500	516	532	549	565	581	597	613	629	645	661	678	694	710	726	742	758	774	791	807
13	283	298	313	328	343	357	372	387	402	417	432	447	462	477	491	506	521	536	551	566	581	596	611	625	640	655	670	685	700	715	730	745
14	263	277	290	304	318	332	346	360	373	387	401	415	429	443	456	470	484	498	512	525	539	553	567	581	595	608	622	636	650	664	678	691
15	245	258	271	284	297	310	323	336	348	361	374	387	400	413	426	439	452	465	478	490	503	516	529	542	555	568	581	594	607	620	632	645
16	230	242	254	266	278	290	303	315	327	339	351	363	375	387	399	411	424	436	448	460	472	484	496	508	520	532	545	557	569	581	593	605
17	216	228	239	251	262	273	285	296	307	319	330	342	353	364	376	387	399	410	421	433	444	456	467	478	490	501	512	524	535	547	558	569
18	204	215	226	237	247	258	269	280	290	301	312	323	333	344	355	366	376	387	398	409	419	430	441	452	462	473	484	495	506	516	527	538
19	194	204	214	224	234	245	255	265	275	285	295	306	316	326	336	346	357	367	377	387	397	408	418	428	438	448	459	469	479	489	499	509
20	184	194	203	213	223	232	242	252	261	271	281	290	300	310	319	329	339	348	358	368	378	387	397	407	416	426	436	445	455	465	474	484
21	175	184	194	203	212	221	230	240	249	258	267	277	286	295	304	313	323	332	341	350	360	369	378	387	396	406	415	424	433	443	452	461
22	167	176	185	194	202	211	220	229	238	246	255	264	273	282	290	299	308	317	326	334	343	352	361	370	378	387	396	405	414	422	431	440
23	160	168	177	185	194	202	210	219	227	236	244	253	261	269	278	286	295	303	311	320	328	337	345	354	362	370	379	387	396	404	412	421
24	153	161	169	177	186	194	202	210	218	226	234	242	250	258	266	274	282	290	298	307	315	323	331	339	347	355	363	371	379	387	395	403
25	147	155	163	170	178	186	194	201	209	217	225	232	240	248	256	263	271	279	287	294	302	310	318	325	333	341	348	356	364	372	379	387
26	141	149	156	164	171	179	186	194	201	208	216	223	231	238	246	253	261	268	276	283	290	298	305	313	320	328	335	343	350	357	365	372
27	136	143	151	158	165	172	179	186	194	201	208	215	222	229	237	244	251	258	265	272	280	287	294	301	308	315	323	330	337	344	351	359
28	131	138	145	152	159	166	173	180	187	194	201	207	214	221	228	235	242	249	256	263	270	277	283	290	297	304	311	318	325	332	339	346
29	127	134	140	147	154	160	167	174	180	187	194	200	207	214	220	227	234	240	247	254	260	267	274	280	287	294	300	307	314	320	327	334
30	123	129	136	142	148	155	161	168	174	181	187	194	200	207	213	219	226	232	239	245	252	258	265	271	277	284	290	297	303	310	316	323
31	119	125	131	137	144	150	156	162	169	175	181	187	194	200	206	212	219	225	231	237	244	250	256	262	269	275	281	287	294	300	306	312
32	115	121	127	133	139	145	151	157	163	169	175	182	188	194	200	206	212	218	224	230	236	242	248	254	260	266	272	278	284	290	296	303
33	111	117	123	129	135	141	147	153	158	164	170	176	182	188	194	199	205	211	217	223	229	235	241	246	252	258	264	270	276	282	287	293
34	108	114	120	125	131	137	142	148	154	159	165	171	177	182	188	194	199	205	211	216	222	228	233	239	245	251	256	262	268	273	279	285
35	105	111	116	122	127	133	138	144	149	155	160	166	171	177	183	188	194	199	205	210	216	221	227	232	238	243	249	254	260	266	271	277
36	102	108	113	118	124	129	134	140	145	151	156	161	167	172	177	183	188	194	199	204	210	215	220	226	231	237	242	247	253	258	264	269
37	99	105	110	115	120	126	131	136	141	147	152	157	162	167	173	178	183	188	194	199	204	209	215	220	225	230	235	241	246	251	256	262
38	97	102	107	112	117	122	127	132	138	143	148	153	158	163	168	173	178	183	189	194	199	204	209	214	219	224	229	234	239	245	250	255
39	94	99	104	109	114	119	124	129	134	139	144	149	154	159	164	169	174	179	184	189	194	199	204	208	213	218	223	228	233	238	243	248
40	92	97	102	106	111	116	121	126	131	136	140	145	150	155	160	165	169	174	179	184	189	194	198	203	208	213	218	223	227	232	237	242
41	90	94	99	104	109	113	118	123	127	132	137	142	146	151	156	161	165	170	175	179	184	189	194	198	203	208	212	217	222	227	231	236
42	88	92	97	101	106	111	115	120	124	129	134	138	143	148	152	157	161	166	171	175	180	184	189	194	198	203	207	212	217	221	226	230
43	86	90	95	99	104	108	113	117	122	126	131	135	140	144	149	153	158	162	167	171	176	180	185	189	194	198	203	207	212	216	221	225
44	84	88	92	97	101	106	110	114	119	123	128	132	136	141	145	150	154	158	163	167	172	176	180	185	189	194	198	202	207	211	216	220
45	82	86	90	95	99	103	108	112	116	120	125	129	133	138	142	146	151	155	159	163	168	172	176	181	185	189	194	198	202	207	211	215



TS = Tensile Strength (55,000)

t = Thickness of Cylindrical Component

TS x t x E/R x FS

R = Radius of Shell (inside diameter/2)

E = Joint Efficiency (88%)

FS = Factor of Safety (5)

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	4.75	5	5.25	5.5	5.75	6	6.25	6.5	6.75	7	7.25	7.5	7.75	8	8.25	8.5
300	2118	2229	2341	2452	2564	2675	2787	2898	3010	3121	3233	3344	3455	3567	3678	3790
325	1955	2058	2161	2264	2367	2469	2572	2675	2778	2881	2984	3087	3190	3293	3395	3498
350	1815	1911	2006	2102	2197	2293	2389	2484	2580	2675	2771	2866	2962	3057	3153	3248
375	1694	1783	1873	1962	2051	2140	2229	2319	2408	2497	2586	2675	2764	2854	2943	3032
400	1588	1672	1756	1839	1923	2006	2090	2174	2257	2341	2424	2508	2592	2675	2759	2842
425	1495	1574	1652	1731	1810	1888	1967	2046	2124	2203	2282	2360	2439	2518	2597	2675
450	1412	1486	1561	1635	1709	1783	1858	1932	2006	2081	2155	2229	2304	2378	2452	2527
475	1338	1408	1478	1549	1619	1690	1760	1830	1901	1971	2042	2112	2182	2253	2323	2394
500	1271	1338	1404	1471	1538	1605	1672	1739	1806	1873	1940	2006	2073	2140	2207	2274
525	1210	1274	1338	1401	1465	1529	1592	1656	1720	1783	1847	1911	1975	2038	2102	2166
550	1155	1216	1277	1338	1398	1459	1520	1581	1642	1702	1763	1824	1885	1946	2006	2067
575	1105	1163	1221	1279	1338	1396	1454	1512	1570	1628	1687	1745	1803	1861	1919	1977
600	1059	1115	1170	1226	1282	1338	1393	1449	1505	1561	1616	1672	1728	1783	1839	1895
625	1017	1070	1124	1177	1231	1284	1338	1391	1445	1498	1552	1605	1659	1712	1766	1819
650	977	1029	1080	1132	1183	1235	1286	1338	1389	1440	1492	1543	1595	1646	1698	1749
675	941	991	1040	1090	1139	1189	1239	1288	1338	1387	1437	1486	1536	1585	1635	1684
700	908	955	1003	1051	1099	1147	1194	1242	1290	1338	1385	1433	1481	1529	1576	1624
725	876	922	969	1015	1061	1107	1153	1199	1245	1291	1338	1384	1430	1476	1522	1568
750	847	892	936	981	1025	1070	1115	1159	1204	1248	1293	1338	1382	1427	1471	1516
775	820	863	906	949	992	1036	1079	1122	1165	1208	1251	1294	1338	1381	1424	1467
800	794	836	878	920	961	1003	1045	1087	1129	1170	1212	1254	1296	1338	1379	1421
825	770	811	851	892	932	973	1013	1054	1094	1135	1175	1216	1257	1297	1338	1378
850	747	787	826	866	905	944	984	1023	1062	1102	1141	1180	1220	1259	1298	1338
875	726	764	803	841	879	917	955	994	1032	1070	1108	1147	1185	1223	1261	1299
900	706	743	780	817	855	892	929	966	1003	1040	1078	1115	1152	1189	1226	1263
925	687	723	759	795	831	868	904	940	976	1012	1048	1085	1121	1157	1193	1229
950	669	704	739	774	810	845	880	915	950	986	1021	1056	1091	1126	1162	1197
975	652	686	720	755	789	823	857	892	926	960	995	1029	1063	1098	1132	1166
1000	635	669	702	736	769	803	836	869	903	936	970	1003	1037	1070	1104	1137
1025	620	652	685	718	750	783	816	848	881	913	946	979	1011	1044	1077	1109
1050	605	637	669	701	732	764	796	828	860	892	924	955	987	1019	1051	1083
1075	591	622	653	684	715	747	778	809	840	871	902	933	964	995	1027	1058
1100	578	608	638	669	699	730	760	790	821	851	882	912	942	973	1003	1034
1125	565	594	624	654	684	713	743	773	803	832	862	892	921	951	981	1011
1150	552	582	611	640	669	698	727	756	785	814	843	872	901	931	960	989

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 88%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 5
P = MAWP, kPa

Table S2.10.3.5 Metric (Page 1 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Buttstrap Triple-Riveted Joint

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	8.75	9	9.25	9.5	9.75	10	10.25	10.5	10.75	11	11.25	11.5	11.75	12	12.25	12.5
300	3901	4013	4124	4236	4347	4459	4570	4682	4793	4905	5016	5127	5239	5350	5462	5573
325	3601	3704	3807	3910	4013	4116	4219	4321	4424	4527	4630	4733	4836	4939	5042	5145
350	3344	3440	3535	3631	3726	3822	3917	4013	4108	4204	4299	4395	4491	4586	4682	4777
375	3121	3210	3299	3389	3478	3567	3656	3745	3834	3924	4013	4102	4191	4280	4369	4459
400	2926	3010	3093	3177	3260	3344	3428	3511	3595	3678	3762	3846	3929	4013	4096	4180
425	2754	2833	2911	2990	3069	3147	3226	3305	3383	3462	3541	3619	3698	3777	3855	3934
450	2601	2675	2750	2824	2898	2972	3047	3121	3195	3270	3344	3418	3493	3567	3641	3716
475	2464	2534	2605	2675	2746	2816	2886	2957	3027	3098	3168	3238	3309	3379	3450	3520
500	2341	2408	2475	2541	2608	2675	2742	2809	2876	2943	3010	3076	3143	3210	3277	3344
525	2229	2293	2357	2420	2484	2548	2612	2675	2739	2803	2866	2930	2994	3057	3121	3185
550	2128	2189	2250	2310	2371	2432	2493	2554	2614	2675	2736	2797	2858	2918	2979	3040
575	2035	2094	2152	2210	2268	2326	2384	2443	2501	2559	2617	2675	2733	2792	2850	2908
600	1951	2006	2062	2118	2174	2229	2285	2341	2397	2452	2508	2564	2619	2675	2731	2787
625	1873	1926	1980	2033	2087	2140	2194	2247	2301	2354	2408	2461	2515	2568	2622	2675
650	1801	1852	1904	1955	2006	2058	2109	2161	2212	2264	2315	2367	2418	2469	2521	2572
675	1734	1783	1833	1883	1932	1982	2031	2081	2130	2180	2229	2279	2328	2378	2427	2477
700	1672	1720	1768	1815	1863	1911	1959	2006	2054	2102	2150	2197	2245	2293	2341	2389
725	1614	1660	1707	1753	1799	1845	1891	1937	1983	2029	2076	2122	2168	2214	2260	2306
750	1561	1605	1650	1694	1739	1783	1828	1873	1917	1962	2006	2051	2096	2140	2185	2229
775	1510	1553	1596	1640	1683	1726	1769	1812	1855	1899	1942	1985	2028	2071	2114	2157
800	1463	1505	1547	1588	1630	1672	1714	1756	1797	1839	1881	1923	1965	2006	2048	2090
825	1419	1459	1500	1540	1581	1621	1662	1702	1743	1783	1824	1865	1905	1946	1986	2027
850	1377	1416	1456	1495	1534	1574	1613	1652	1692	1731	1770	1810	1849	1888	1928	1967
875	1338	1376	1414	1452	1490	1529	1567	1605	1643	1682	1720	1758	1796	1834	1873	1911
900	1300	1338	1375	1412	1449	1486	1523	1561	1598	1635	1672	1709	1746	1783	1821	1858
925	1265	1301	1338	1374	1410	1446	1482	1518	1555	1591	1627	1663	1699	1735	1771	1808
950	1232	1267	1302	1338	1373	1408	1443	1478	1514	1549	1584	1619	1654	1690	1725	1760
975	1200	1235	1269	1303	1338	1372	1406	1440	1475	1509	1543	1578	1612	1646	1681	1715
1000	1170	1204	1237	1271	1304	1338	1371	1404	1438	1471	1505	1538	1572	1605	1639	1672
1025	1142	1174	1207	1240	1272	1305	1338	1370	1403	1435	1468	1501	1533	1566	1599	1631
1050	1115	1147	1178	1210	1242	1274	1306	1338	1369	1401	1433	1465	1497	1529	1561	1592
1075	1089	1120	1151	1182	1213	1244	1275	1306	1338	1369	1400	1431	1462	1493	1524	1555
1100	1064	1094	1125	1155	1186	1216	1246	1277	1307	1338	1368	1398	1429	1459	1490	1520
1125	1040	1070	1100	1130	1159	1189	1219	1248	1278	1308	1338	1367	1397	1427	1456	1486
1150	1018	1047	1076	1105	1134	1163	1192	1221	1250	1279	1309	1338	1367	1396	1425	1454

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 88%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 5
P = MAWP, kPa

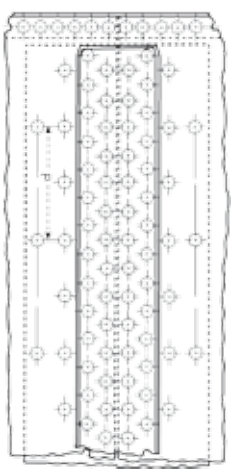
Table S2.10.3.5 Metric (Page 2 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Buttstrap Triple-Riveted Joint

TABLE S2.10.3.6

MAXIMUM ALLOWABLE WORKING PRESSURE FOR CYLINDRICAL COMPONENTS (BARREL)

For Buttstrap Quadruple-Riveted Joint

Shell ID	Minimum Thickness of Shell Plate																																
	0.19	0.2	0.21	0.22	0.23	0.24	0.25	0.26	0.27	0.28	0.29	0.3	0.31	0.32	0.33	0.34	0.35	0.36	0.37	0.38	0.39	0.4	0.41	0.42	0.43	0.44	0.45	0.46	0.47	0.48	0.49	0.5
12	327	345	362	379	396	414	431	448	465	483	500	517	534	551	569	586	603	620	638	655	672	689	707	724	741	758	776	793	810	827	844	862
13	302	318	334	350	366	382	398	414	430	445	461	477	493	509	525	541	557	573	589	604	620	636	652	668	684	700	716	732	748	764	779	795
14	281	295	310	325	340	355	369	384	399	414	428	443	458	473	487	502	517	532	547	561	576	591	606	620	635	650	665	679	694	709	724	739
15	262	276	290	303	317	331	345	358	372	386	400	414	427	441	455	469	483	496	510	524	538	551	565	579	593	607	620	634	648	662	676	689
16	246	259	271	284	297	310	323	336	349	362	375	388	401	414	427	439	452	465	478	491	504	517	530	543	556	569	582	595	607	620	633	646
17	231	243	255	268	280	292	304	316	328	341	353	365	377	389	401	414	426	438	450	462	474	487	499	511	523	535	547	560	572	584	596	608
18	218	230	241	253	264	276	287	299	310	322	333	345	356	368	379	391	402	414	425	437	448	460	471	483	494	506	517	528	540	551	563	574
19	207	218	229	239	250	261	272	283	294	305	316	327	337	348	359	370	381	392	403	414	424	435	446	457	468	479	490	501	512	522	533	544
20	196	207	217	227	238	248	259	269	279	290	300	310	321	331	341	352	362	372	383	393	403	414	424	434	445	455	465	476	486	496	507	517
21	187	197	207	217	226	236	246	256	266	276	286	295	305	315	325	335	345	355	364	374	384	394	404	414	423	433	443	453	463	473	483	492
22	179	188	197	207	216	226	235	244	254	263	273	282	291	301	310	320	329	338	348	357	367	376	385	395	404	414	423	432	442	451	461	470
23	171	180	189	198	207	216	225	234	243	252	261	270	279	288	297	306	315	324	333	342	351	360	369	378	387	396	405	414	423	432	441	450
24	164	172	181	190	198	207	215	224	233	241	250	259	267	276	284	293	302	310	319	327	336	345	353	362	371	379	388	396	405	414	422	431
25	157	165	174	182	190	199	207	215	223	232	240	248	256	265	273	281	290	298	306	314	323	331	339	347	356	364	372	381	389	397	405	414
26	151	159	167	175	183	191	199	207	215	223	231	239	247	255	262	270	278	286	294	302	310	318	326	334	342	350	358	366	374	382	390	398
27	146	153	161	169	176	184	191	199	207	214	222	230	237	245	253	260	268	276	283	291	299	306	314	322	329	337	345	352	360	368	375	383
28	140	148	155	162	170	177	185	192	199	207	214	222	229	236	244	251	259	266	273	281	288	295	303	310	318	325	332	340	347	355	362	369
29	135	143	150	157	164	171	178	185	193	200	207	214	221	228	235	242	250	257	264	271	278	285	292	300	307	314	321	328	335	342	349	357
30	131	138	145	152	159	165	172	179	186	193	200	207	214	221	227	234	241	248	255	262	269	276	283	290	296	303	310	317	324	331	338	345
31	127	133	140	147	153	160	167	173	180	187	193	200	207	213	220	227	233	240	247	253	260	267	274	280	287	294	300	307	314	320	327	334
32	123	129	136	142	149	155	162	168	174	181	187	194	200	207	213	220	226	233	239	246	252	259	265	271	278	284	291	297	304	310	317	323
33	119	125	132	138	144	150	157	163	169	175	182	188	194	201	207	213	219	226	232	238	244	251	257	263	269	276	282	288	295	301	307	313
34	116	122	128	134	140	146	152	158	164	170	176	182	189	195	201	207	213	219	225	231	237	243	249	255	262	268	274	280	286	292	298	304
35	112	118	124	130	136	142	148	154	160	165	171	177	183	189	195	201	207	213	219	225	230	236	242	248	254	260	266	272	278	284	290	295
36	109	115	121	126	132	138	144	149	155	161	167	172	178	184	190	195	201	207	213	218	224	230	236	241	247	253	259	264	270	276	281	287
37	106	112	117	123	129	134	140	145	151	156	162	168	173	179	184	190	196	201	207	212	218	224	229	235	240	246	252	257	263	268	274	279
38	103	109	114	120	125	131	136	141	147	152	158	163	169	174	180	185	190	196	201	207	212	218	223	229	234	239	245	250	256	261	267	272
39	101	106	111	117	122	127	133	138	143	148	154	159	164	170	175	180	186	191	196	201	207	212	217	223	228	233	239	244	249	255	260	265
40	98	103	109	114	119	124	129	134	140	145	150	155	160	165	171	176	181	186	191	196	202	207	212	217	222	227	233	238	243	248	253	259
41	96	101	106	111	116	121	126	131	136	141	146	151	156	161	166	171	177	182	187	192	197	202	207	212	217	222	227	232	237	242	247	252
42	94	98	103	108	113	118	123	128	133	138	143	148	153	158	162	167	172	177	182	187	192	197	202	207	212	217	222	226	231	236	241	246
43	91	96	101	106	111	115	120	125	130	135	139	144	149	154	159	164	168	173	178	183	188	192	197	202	207	212	216	221	226	231	236	240
44	89	94	99	103	108	113	118	122	127	132	136	141	146	150	155	160	165	169	174	179	183	188	193	197	202	207	212	216	221	226	230	235
45	87	92	97	101	106	110	115	119	124	129	133	138	142	147	152	156	161	165	170	175	179	184	188	193	198	202	207	211	216	221	225	230



TS = Tensile Strength (55,000)

t = Thickness of Cylindrical Component

TS x t x E/R x FS

R = Radius of Shell (inside diameter/2)

E = Joint Efficiency (94%)

FS = Factor of Safety (5)

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	4.75	5	5.25	5.5	5.75	6	6.25	6.5	6.75	7	7.25	7.5	7.75	8	8.25
300	2262	2381	2500	2619	2739	2858	2977	3096	3215	3334	3453	3572	3691	3810	3929
325	2088	2198	2308	2418	2528	2638	2748	2858	2968	3077	3187	3297	3407	3517	3627
350	1939	2041	2143	2245	2347	2449	2551	2653	2756	2858	2960	3062	3164	3266	3368
375	1810	1905	2000	2096	2191	2286	2381	2477	2572	2667	2762	2858	2953	3048	3143
400	1697	1786	1875	1965	2054	2143	2233	2322	2411	2500	2590	2679	2768	2858	2947
425	1597	1681	1765	1849	1933	2017	2101	2185	2269	2353	2437	2521	2605	2690	2774
450	1508	1588	1667	1746	1826	1905	1984	2064	2143	2223	2302	2381	2461	2540	2619
475	1429	1504	1579	1654	1730	1805	1880	1955	2030	2106	2181	2256	2331	2406	2482
500	1357	1429	1500	1572	1643	1715	1786	1857	1929	2000	2072	2143	2215	2286	2358
525	1293	1361	1429	1497	1565	1633	1701	1769	1837	1905	1973	2041	2109	2177	2245
550	1234	1299	1364	1429	1494	1559	1624	1689	1754	1818	1883	1948	2013	2078	2143
575	1180	1242	1305	1367	1429	1491	1553	1615	1677	1739	1802	1864	1926	1988	2050
600	1131	1191	1250	1310	1369	1429	1488	1548	1607	1667	1726	1786	1846	1905	1965
625	1086	1143	1200	1257	1314	1372	1429	1486	1543	1600	1657	1715	1772	1829	1886
650	1044	1099	1154	1209	1264	1319	1374	1429	1484	1539	1594	1649	1704	1759	1813
675	1005	1058	1111	1164	1217	1270	1323	1376	1429	1482	1535	1588	1640	1693	1746
700	970	1021	1072	1123	1174	1225	1276	1327	1378	1429	1480	1531	1582	1633	1684
725	936	985	1035	1084	1133	1182	1232	1281	1330	1380	1429	1478	1527	1577	1626
750	905	953	1000	1048	1095	1143	1191	1238	1286	1334	1381	1429	1476	1524	1572
775	876	922	968	1014	1060	1106	1152	1198	1244	1291	1337	1383	1429	1475	1521
800	848	893	938	982	1027	1072	1116	1161	1206	1250	1295	1340	1384	1429	1473
825	823	866	909	953	996	1039	1082	1126	1169	1212	1256	1299	1342	1386	1429
850	798	840	882	925	967	1009	1051	1093	1135	1177	1219	1261	1303	1345	1387
875	776	816	857	898	939	980	1021	1061	1102	1143	1184	1225	1266	1306	1347
900	754	794	833	873	913	953	992	1032	1072	1111	1151	1191	1230	1270	1310
925	734	772	811	850	888	927	965	1004	1043	1081	1120	1158	1197	1236	1274
950	714	752	790	827	865	902	940	978	1015	1053	1090	1128	1166	1203	1241
975	696	733	769	806	843	879	916	953	989	1026	1062	1099	1136	1172	1209
1000	679	714	750	786	822	857	893	929	964	1000	1036	1072	1107	1143	1179
1025	662	697	732	767	802	836	871	906	941	976	1011	1045	1080	1115	1150
1050	646	680	714	748	782	816	850	884	919	953	987	1021	1055	1089	1123
1075	631	665	698	731	764	797	831	864	897	930	964	997	1030	1063	1097
1100	617	649	682	714	747	779	812	844	877	909	942	974	1007	1039	1072
1125	603	635	667	699	730	762	794	826	857	889	921	953	984	1016	1048
1150	590	621	652	683	714	745	777	808	839	870	901	932	963	994	1025

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 94%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 5
P = MAWP, kPa

Table S2.10.3.6 Metric (Page 1 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Buttstrap Quadruple-Riveted Joint

Shell ID (mm)	Minimum Thickness of Shell Plate (mm)															
	8.75	9	9.25	9.5	9.75	10	10.25	10.5	10.75	11	11.25	11.5	11.75	12	12.25	12.5
300	4167	4286	4405	4525	4644	4763	4882	5001	5120	5239	5358	5477	5596	5715	5834	5953
325	3847	3957	4067	4176	4286	4396	4506	4616	4726	4836	4946	5056	5166	5276	5385	5495
350	3572	3674	3776	3878	3980	4082	4184	4286	4388	4491	4593	4695	4797	4899	5001	5103
375	3334	3429	3524	3620	3715	3810	3905	4001	4096	4191	4286	4382	4477	4572	4667	4763
400	3126	3215	3304	3393	3483	3572	3661	3751	3840	3929	4019	4108	4197	4286	4376	4465
425	2942	3026	3110	3194	3278	3362	3446	3530	3614	3698	3782	3866	3950	4034	4118	4202
450	2778	2858	2937	3016	3096	3175	3254	3334	3413	3493	3572	3651	3731	3810	3890	3969
475	2632	2707	2782	2858	2933	3008	3083	3158	3234	3309	3384	3459	3534	3610	3685	3760
500	2500	2572	2643	2715	2786	2858	2929	3000	3072	3143	3215	3286	3358	3429	3501	3572
525	2381	2449	2517	2585	2653	2722	2790	2858	2926	2994	3062	3130	3198	3266	3334	3402
550	2273	2338	2403	2468	2533	2598	2663	2728	2793	2858	2923	2987	3052	3117	3182	3247
575	2174	2236	2299	2361	2423	2485	2547	2609	2671	2733	2795	2858	2920	2982	3044	3106
600	2084	2143	2203	2262	2322	2381	2441	2500	2560	2619	2679	2739	2798	2858	2917	2977
625	2000	2057	2115	2172	2229	2286	2343	2400	2458	2515	2572	2629	2686	2743	2800	2858
650	1923	1978	2033	2088	2143	2198	2253	2308	2363	2418	2473	2528	2583	2638	2693	2748
675	1852	1905	1958	2011	2064	2117	2170	2223	2275	2328	2381	2434	2487	2540	2593	2646
700	1786	1837	1888	1939	1990	2041	2092	2143	2194	2245	2296	2347	2398	2449	2500	2551
725	1724	1774	1823	1872	1921	1971	2020	2069	2119	2168	2217	2266	2316	2365	2414	2463
750	1667	1715	1762	1810	1857	1905	1953	2000	2048	2096	2143	2191	2238	2286	2334	2381
775	1613	1659	1705	1751	1798	1844	1890	1936	1982	2028	2074	2120	2166	2212	2258	2305
800	1563	1607	1652	1697	1741	1786	1831	1875	1920	1965	2009	2054	2099	2143	2188	2233
825	1515	1559	1602	1645	1689	1732	1775	1818	1862	1905	1948	1992	2035	2078	2122	2165
850	1471	1513	1555	1597	1639	1681	1723	1765	1807	1849	1891	1933	1975	2017	2059	2101
875	1429	1470	1510	1551	1592	1633	1674	1715	1755	1796	1837	1878	1919	1959	2000	2041
900	1389	1429	1468	1508	1548	1588	1627	1667	1707	1746	1786	1826	1865	1905	1945	1984
925	1352	1390	1429	1467	1506	1545	1583	1622	1660	1699	1738	1776	1815	1854	1892	1931
950	1316	1354	1391	1429	1466	1504	1542	1579	1617	1654	1692	1730	1767	1805	1842	1880
975	1282	1319	1356	1392	1429	1465	1502	1539	1575	1612	1649	1685	1722	1759	1795	1832
1000	1250	1286	1322	1357	1393	1429	1465	1500	1536	1572	1607	1643	1679	1715	1750	1786
1025	1220	1255	1289	1324	1359	1394	1429	1464	1498	1533	1568	1603	1638	1673	1708	1742
1050	1191	1225	1259	1293	1327	1361	1395	1429	1463	1497	1531	1565	1599	1633	1667	1701
1075	1163	1196	1229	1263	1296	1329	1362	1396	1429	1462	1495	1528	1562	1595	1628	1661
1100	1137	1169	1201	1234	1266	1299	1331	1364	1396	1429	1461	1494	1526	1559	1591	1624
1125	1111	1143	1175	1207	1238	1270	1302	1334	1365	1397	1429	1461	1492	1524	1556	1588
1150	1087	1118	1149	1180	1211	1242	1273	1305	1336	1367	1398	1429	1460	1491	1522	1553

$$P = \frac{TS \cdot t \cdot E}{R \cdot FS}$$

TS = Tensile Strength 380,000 kPa
t = Thickness of Cylindrical Component, mm
E = Joint Efficiency 94%

R = Radius of Shell (inside Diameter/2), mm
FS = Factor of Safety 5
P= MAWP , KPa

Table S2.10.3.6 Metric (Page 2 of 2)
Maximum Allowable Working Pressure for Cylindrical Components (Barrel)
For Buttstrap Quadruple–Riveted Joint

S2.10.4 STAYED SURFACES

The maximum allowable working pressure for stayed flat plates and those parts which, by these rules, require staying as flat plates with stays or staybolts of uniform diameter, uniformly spaced, shall be calculated using the following formula or NBIC Part 2, Table S2.10.4.

When pitches of stays or staybolts of uniform diameter are symmetrical and form a rectangle, the equation may be replaced with the following equation:

$$P = \frac{2 \times t^2 \times S \times C}{t^2 + w^2}$$

See definitions of nomenclature in S2.10.6.

S2.10.4.1 STAYBOLTS

The maximum allowable working pressure for symmetrically spaced corroded staybolts will be calculated using the formula provided in either of the two following paragraphs or the accompanying tables. Equations calculate MAWP based on measuring the staybolt spacing on the stayed surface and the minimum diameter of the corroded staybolt.

(15) a) Iron Staybolt

Staybolts which are of iron or of unknown material shall be calculated using the following formula or Table S2.10.4.1-a. The table is based on a stress value of 7,500 psi (51.7 MPa) for staybolts. Refer to ASME Section 1, 1971 Edition, Table PG-23.3, for allowable loads for all staybolts.

$$p = \frac{\pi \left[\frac{d}{2}\right]^2 s}{p^2}$$

S = 7,500 psi (51.7 MPa)

b) Steel Staybolts

Staybolts of known, steel material shall be calculated using the following formula or Table S2.10.4.1-b. The table is based on a stress value of 11,300 psi (78.0 MPa) for staybolts. Refer to ASME Section 1, 1971 Addenda for allowable loads for all staybolts.

$$p = \frac{\pi \left[\frac{d}{2}\right]^2 s}{1.1 x p^2}$$

S = 11,300 psi (78.0 MPa)

(15) S2.10.4.2 BULGING

Stayed surfaces shall be examined and any deformations shall be measured and recorded. Deformations may be caused from freezing, localized overheating, broken staybolts, or extended use (cyclic activity). Deformations may by described as bulging, bagging, or pillow/mattress-effects. The bulged section depth is defined as the protrusion of the sheet beyond its original position.

a) Changes in deformations between inspections shall be noted and shall require additional evaluation to determine fitness for service.

b) The probable cause of the deformation shall be determined and, where possible, resolved. For example, overheating due to scale build-up requires removal of scale.

c) The amount of the bulging shall be measured:

1) If the depth of the bulge does not exceed 50% of plate thickness, then no further activity is required.

2) If the depth of the bulge is between 50% and 100% plate thickness, and thread engagement is not affected, then additional NDE is required.

Note: If ultrasonic thickness testing is performed (see S2.6.2 c)), then it is perfomed on a tight 1 in. (25 mm) grid to determine any thinning throughout the deformation. Any generalized thinning shall be used in the calculation of MAWP (see S2.6.2 b)). If the depth of the bulge exceeds the thickness of the plate, then repair is required.

d) The location of the deformations shall be examined. If the point of tangency of the curve in a bulge is within 't' of the edge of the staybolt head, then determination of thread engagement shall be made ('t' is defined in S2.10.6 and is the minimum thickness of the shell plate). Removal of one or more staybolts may be required to make this determination. Refer to figure NBIC Part 2, Figure S2.10.4.2 a).

1) Cracks, deformations, and/or missing portions of the threaded staybolt head may indicate a deformation of the plate at the staybolt.

e) The following guidelines apply where repair is required.

1) Plate may only be repaired using a flush patch, in accordance with NBIC Part 3, Supplement 2.

2) Where a deformation is to be repaired, all portions of the deformity shall be repaired. For example, for contigous bulging where only some bulges exceed allowable deformation, the entire bulged area shall be repaired (See Figure S2.10.4.2-b). Unrelated bulges seperated by non-deformed plate shall be independently evaluated.

FIGURE S2.10.4.2-A

POINT OF TANGENCY OF THE CURVE IN A BULGE WITHIN 't' OF THE EDGE OF THE STAYBOLT

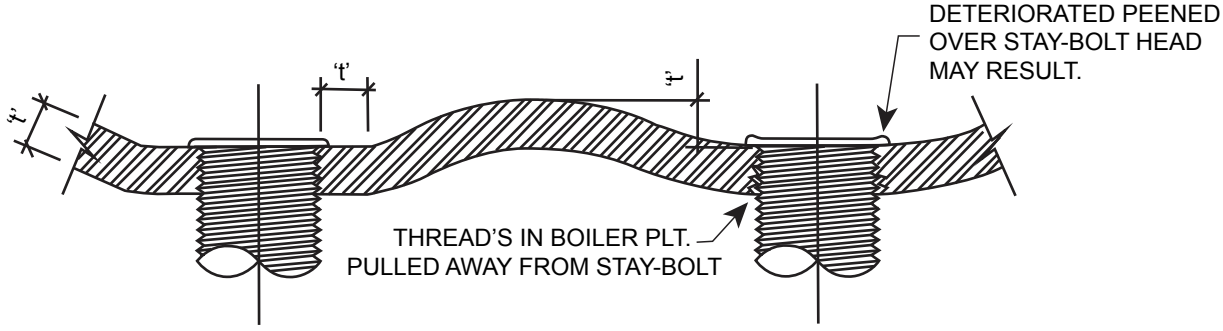


FIGURE S2.10.4.2 b)

CONTINUOUS BULGING WHERE ONLY SOME BULGES EXCEED ALLOWABLE DEFORMATION



Thickness of Stayed Surface, in.	Staybolt Spacing (Maximum Pitch, in.)																				
	3.5	3.625	3.75	3.875	4	4.125	4.25	4.375	4.5	4.625	4.75	4.875	5	5.125	5.25	5.375	5.5	5.625	5.75	5.875	6
0.19	85	80	74	70	65	61	58	55	52	49	46	44	42	40	38	36	35	33	32	30	29
0.20	95	88	82	77	72	68	64	61	57	54	51	49	46+	44	42	40	38	37	35	34	32
0.21	104	97	91	85	80	75	71	67	63	60	57	54	51	49	46	44	42	40	39	37	36
0.22	115	107	100	93	88	82	78	73	69	66	62	59	56	53	51	49	46	44	42	41	39
0.23	125	117	109	102	96	90	85	80	76	72	68	65	61	58	56	53	51	48	46	44	43
0.24	136	127	119	111	104	98	92	87	82	78	74	70	67	64	61	58	55	53	50	48	46
0.25	148	138	129	121	113	106	100	95	89	85	80	76	72	69	66	63	60	57	55	52	50
0.26	160	149	139	130	122	115	108	102	97	92	87	82	78	75	71	68	65	62	59	57	54
0.27	172	161	150	141	132	124	117	110	104	99	94	89	85	80	77	73	70	67	64	61	59
0.28	185	173	162	151	142	134	126	119	112	106	101	96	91	87	82	79	75	72	69	66	63
0.29	199	185	173	162	152	143	135	127	120	114	108	103	97	93	88	84	81	77	74	71	68
0.30	213	198	185	174	163	153	144	136	129	122	116	110	104	99	95	90	86	82	79	76	72
0.31	227	212	198	185	174	164	154	146	138	130	123	117	111	106	101	96	92	88	84	81	77
0.32	242	226	211	198	185	174	164	155	147	139	132	125	119	113	108	103	98	94	90	86	82
0.33	258	240	224	210	197	185	175	165	156	148	140	133	126	120	115	109	104	100	95	91	88
0.34	273	255	238	223	209	197	185	175	165	157	148	141	134	128	122	116	111	106	101	97	93
0.35	290	270	252	236	222	209	197	185	175	166	157	149	142	135	129	123	117	112	107	103	99
0.36	307	286	267	250	235	221	208	196	185	176	166	158	150	143	136	130	124	119	114	109	104
0.37	324	302	282	264	248	233	220	207	196	185	176	167	159	151	144	137	131	125	120	115	110
0.38	342	318	298	279	262	246	232	219	207	196	185	176	167	159	152	145	138	132	127	121	116
0.39	360	335	313	294	275	259	244	230	218	206	195	185	176	168	160	153	146	139	133	128	122
0.40	379	353	330	309	290	273	257	242	229	217	206	195	185	177	168	160	153	147	140	134	129
0.41	398	371	346	324	304	286	270	255	241	228	216	205	195	185	177	169	161	154	147	141	135
0.42	417	289	364	340	320	300	283	267	252	239	227	215	204	195	185	177	169	162	155	148	142
0.43	437	408	281	357	335	315	297	280	265	251	237	225	214	204	194	185	177	169	162	155	149
0.44	480	447	418	391	367	345	325	307	290	275	261	247	235	224	213	203	194	186	178	170	163
0.45	502	468	437	409	384	361	340	321	304	287	272	259	246	234	223	213	203	194	186	178	171
0.46	524	489	457	428	402	378	356	336	317	300	285	270	257	245	233	222	212	203	194	186	178
0.47	547	510	477	447	419	394	371	350	331	314	297	282	268	255	243	232	222	212	203	194	186
0.48	571	532	497	466	437	411	387	365	345	327	310	294	280	266	254	242	231	221	212	203	194

TS = Tensile Strength 55,000 psi

$$P = \frac{t^2 \cdot S \cdot C}{p^2}$$

For Thicknesses 0.4375 in. and less, C=2.1

t = Thickness of Stayed Surface, in.

For Thicknesses larger than 0.4375 in., C=2.2

S = 13,800 psi

MAWP is expressed in psi

Table S2.10.4 (US Customary Units) Maximum Allowable Working Pressure for Stayed Surfaces, Formula Per ASME Section I, PG-46.1

Thickness of Stayed Surfaces, mm	Staybolt Spacing (Maximum Pitch), mm																				
	89	92	95	98	102	105	108	111	114	117	121	124	127	130	133	137	140	143	146	149	152
5.00	630	589	553	519	479	452	428	405	384	364	341	324	309	295	282	266	254	244	234	225	216
5.25	694	650	609	573	529	499	471	446	423	402	376	358	341	325	311	293	281	269	258	248	238
5.50	762	713	669	628	580	547	517	490	464	441	412	392	374	357	341	322	308	295	283	272	261
5.75	833	779	731	687	634	598	565	535	508	482	451	429	409	390	373	351	337	323	309	297	285
6.00	907	849	796	748	690	651	616	583	553	525	491	467	445	425	406	383	366	351	337	323	311
6.25	984	921	863	811	749	707	668	632	600	569	532	507	483	461	441	415	398	381	366	351	337
6.50	1 064	996	934	878	810	765	723	684	649	616	576	548	523	499	477	449	430	412	395	380	365
6.75	1 148	1 074	1 007	946	874	824	779	738	699	664	621	591	564	538	514	484	464	445	426	409	393
7.00	1 234	1 155	1 083	1 018	940	887	838	793	752	714	668	636	606	578	553	521	499	478	459	440	423
7.25	1 324	1 239	1 162	1 093	1 008	951	899	851	807	766	716	682	650	620	593	559	535	513	492	472	454
7.50	1 417	1 326	1 243	1 168	1 079	1 018	962	911	863	820	766	730	696	664	634	598	573	549	526	505	486
7.75	1 513	1 416	1 328	1 248	1 152	1 087	1 027	973	922	875	818	779	743	709	677	638	611	586	562	540	519
8.00	1 612	1 509	1 415	1 329	1 227	1 158	1 095	1 036	982	933	872	830	792	756	722	680	651	624	599	575	553
8.25	1 714	1 604	1 505	1 414	1 305	1 232	1 164	1 102	1 045	992	927	883	842	803	768	723	693	664	637	612	588
8.50	1 820	1 703	1 597	1 501	1 385	1 307	1 236	1 170	1 109	1 053	984	937	894	853	815	768	735	705	676	649	624
8.75	1 928	1 805	1 692	1 590	1 468	1 385	1 310	1 240	1 175	1 116	1 043	993	947	904	863	814	779	747	717	688	661
9.00	2 040	1 909	1 791	1 683	1 553	1 466	1 385	1 312	1 243	1 180	1 104	1 051	1 002	956	914	861	814	790	758	728	699
9.25	2 155	2 017	1 891	1 777	1 641	1 548	1 463	1 685	1 313	1 247	1 166	1 110	1 058	1 010	965	909	871	835	801	769	736
9.50	2 273	2 127	1 995	1 875	1 731	1 633	1 544	1 461	1 385	1 315	1 230	1 171	1 116	1 065	1 018	959	919	880	845	811	779
9.75	2 394	2 241	2 101	1 975	1 823	1 720	1 626	1 539	1 459	1 385	1 295	1 233	1 176	1 122	1 072	1 010	986	927	890	854	821
10.00	2 519	2 357	2 211	2 077	1 918	1 810	1 710	1 619	1 535	1 475	1 363	1 297	1 237	1 180	1 128	1 063	1 018	976	936	899	863
10.25	2 646	2 476	2 322	2 182	2 015	1 901	1 797	1 701	1 613	1 531	1 432	1 363	1 300	1 240	1 185	1 117	1 069	1 025	983	944	907
10.50	2 777	2 599	2 437	2 290	2 114	1 995	1 886	1 785	1 692	1 607	1 502	1 430	1 634	1 301	1 243	1 172	1 122	1 076	1 032	991	952

TS = Tensile Strength 380 000 kPa

$$P = \frac{t^2 \cdot S \cdot C}{p^2}$$

For Thicknesses 11mm and less, C=2.1

t = Thickness of Stayed Surface, in.

For Thicknesses larger than 11 mm, C=2.2

S = 95 000 kPa

MAWP is expressed in kPa

Table S2.10.4 (Metric Units) Maximum Allowable Working Pressure for Stayed Surfaces, Formula Per ASME Section I, PG-46.1

Staybolt Spacing, in.	Actual Diameter of Corroded Staybolt, in.																						
	0.35	0.375	0.40	0.425	0.45	0.475	0.50	0.525	0.55	0.575	0.60	0.625	0.65	0.675	0.7	0.725	0.75	0.775	0.80	0.825	0.85	0.875	0.90
3.5	54	61	70	79	89	99	109	120	132	145	157	171	185	199	214	230	246	263	280	298	316	335	354
3.625	50	57	65	74	83	92	102	112	123	135	147	159	172	186	200	214	229	245	261	277	294	312	330
3.75	47	54	61	69	77	86	95	105	115	126	137	149	161	174	187	200	214	229	244	259	275	292	308
3.875	44	50	57	64	72	80	89	98	108	118	128	139	151	162	175	187	201	214	228	243	258	273	289
4	41	47	54	60	68	76	84	92	101	111	120	131	141	152	164	176	188	201	214	228	242	256	271
4.125	39	44	50	57	64	71	79	87	95	104	113	123	133	143	154	165	177	189	201	214	227	241	255
4.25	36	42	47	54	60	67	74	82	90	98	107	116	125	135	145	156	167	178	190	202	214	227	240
4.375	34	39	45	51	57	63	70	77	85	92	101	109	118	127	137	147	157	168	179	190	202	214	227
4.5	32	37	42	48	54	60	66	73	80	87	95	103	112	120	130	139	149	159	169	180	191	202	214
4.625	31	35	40	45	51	56	63	69	76	83	90	98	106	114	123	132	141	150	160	170	181	192	203
4.75	29	33	38	43	48	54	59	65	72	78	85	93	100	108	116	125	134	143	152	162	171	182	192
4.875	28	32	36	41	46	51	56	62	68	74	81	88	95	103	110	118	127	135	144	153	163	173	183
5	26	30	34	39	43	48	54	59	65	71	77	84	90	98	105	113	120	129	137	146	155	164	174
5.125	25	29	33	37	41	46	51	56	62	67	73	80	86	93	100	107	115	122	130	139	147	156	165
5.25	24	27	31	35	39	44	49	54	59	64	70	76	82	89	95	102	109	117	124	132	140	149	157
5.375	23	26	30	33	38	42	46	51	56	61	67	72	78	84	91	97	104	111	119	126	134	142	150
5.5	22	25	28	32	36	40	44	49	54	59	64	69	75	81	87	93	100	106	116	120	128	136	143
5.625	21	24	27	31	34	38	42	47	51	65	61	66	72	77	83	89	95	102	108	115	122	130	137
5.75	20	23	26	29	33	37	40	45	49	54	58	63	68	74	79	85	91	97	104	110	117	124	131
5.875	19	22	25	28	31	35	39	43	47	51	56	61	66	71	76	82	87	93	99	106	112	119	126
6	18	21	24	27	30	34	37	41	45	49	54	58	63	68	73	78	84	89	95	101	107	114	120
6.125	17	20	23	26	29	32	36	39	43	47	51	56	60	65	70	75	80	86	91	97	103	109	116
6.25	17	19	22	25	28	31	34	38	41	45	49	54	58	62	67	72	77	82	88	93	99	105	111
6.375	16	19	21	24	27	30	33	36	40	44	47	51	56	60	65	69	74	79	84	90	95	101	107
6.5	16	18	20	23	26	29	32	35	38	42	46	50	54	58	62	67	71	76	81	86	92	97	103
6.625	15	17	20	22	25	28	31	34	37	40	44	48	52	56	60	64	69	73	78	83	88	93	99
6.75	14	17	19	21	24	27	29	32	36	39	42	46	50	54	58	62	66	71	75	80	85	90	95
6.785	14	16	18	20	23	26	28	31	34	37	41	44	48	52	56	60	64	68	73	77	82	87	92
7	13	15	17	20	22	25	27	30	33	36	39	43	46	50	54	57	61	66	70	74	79	84	89

TS = 7,500 psi

P = MAWP psi

$$P = \frac{\pi \cdot d^2 \cdot TS}{1.1 \cdot 4 \cdot p^2}$$

d = Minimum diameter of corroded staybolt

p = Staybolt spacing, in.

Table S2.10.4.1 [US Customary Units]
Maximum Allowable Working Pressure Based on Load Carrying Capacity of a Single-Corroded Staybolt

Staybolt Spacing, in.	Actual Diameter of Corroded Staybolts, mm																								
	10	10.5	11	11.5	12	12.5	13	13.5	14	14.5	15	15.5	16	16.5	17	17.5	18	18.5	19	19.5	20	20.5	21	21.5	22
90	458	505	555	606	660	716	775	835	898	964	1 031	1 101	1 173	1 248	1 325	1 404	1 485	1 569	1 655	1 743	1 833	1 926	2 021	2 119	2 219
92.5	434	478	525	574	625	678	733	791	850	912	976	1 043	1 111	1 181	1 254	1 329	1 406	1 485	1 566	1 650	1 736	1 824	1 914	2 006	2 100
95	411	454	498	544	592	643	695	750	806	865	926	988	1 053	1 120	1 189	1 260	1 333	1 408	1 485	1 564	1 646	1 729	1 814	1 902	1 991
97.5	391	431	473	517	562	610	660	712	766	821	879	938	1 000	1 063	1 129	1 196	1 265	1 337	1 410	1 485	1 562	1 641	1 722	1 805	1 890
100	371	409	449	491	535	580	627	677	728	781	635	892	950	1 011	1 073	1 137	1 203	1 271	1 340	1 412	1 485	1 560	1 637	1 716	1 797
102.5	353	390	428	467	509	552	597	644	693	743	795	849	905	962	1 021	1 082	1 145	1 209	1 276	1 344	1 414	1 485	1 558	1 634	1 710
105	337	371	407	445	485	526	569	614	660	708	758	809	862	917	973	1 031	1 091	1 153	1 216	1 281	1 347	1 415	1 485	1 557	1 630
107.5	321	354	389	425	463	502	543	586	630	675	723	772	822	875	928	984	1 041	1 100	1 160	1 222	1 285	1 350	1 417	1 485	1 555
110	307	338	371	406	442	479	519	559	601	645	690	737	786	835	887	940	994	1 050	1 108	1 167	1 227	1 290	1 353	1 418	1 485
122.5	293	323	355	388	422	458	496	535	575	617	660	705	751	799	848	898	950	1 004	1 059	1 115	1 173	1 233	1 294	1 356	1 420
115	281	310	340	371	404	439	474	512	550	590	632	674	719	764	811	860	910	961	1 013	1 068	1 123	1 180	1 238	1 298	1 359
117.5	269	296	325	356	387	420	454	490	527	565	605	646	688	732	777	824	871	920	971	1 023	1 076	1 130	1 186	1 243	1 302
120	258	284	312	341	371	403	436	470	505	542	580	619	660	702	745	790	835	882	931	980	1 031	1 084	1 137	1 192	1 248
122.5	247	273	299	327	356	387	418	451	485	520	557	594	633	674	715	758	802	847	893	941	990	1 040	1 091	1 144	1 197
125	238	262	288	314	342	371	402	433	466	500	535	571	608	647	687	728	770	813	858	904	950	999	1 048	1 098	1 150
127.5	228	252	276	302	329	357	386	416	448	480	514	549	585	622	660	699	740	782	824	868	914	960	1 007	1 056	1 105
130	220	242	266	291	316	343	371	400	431	462	494	528	562	598	635	673	712	752	793	835	879	923	969	1 016	1 063
132.5	211	233	256	280	305	330	357	385	415	445	476	508	541	576	611	648	685	724	763	804	846	889	933	978	1 024
135	204	225	247	269	293	318	344	371	399	428	458	489	522	555	589	624	660	697	735	775	815	856	898	942	986
137.5	196	217	238	260	283	307	332	358	385	413	442	472	503	535	568	601	636	672	709	747	786	825	866	908	950
140	189	209	229	251	273	296	320	345	371	398	426	455	485	516	547	580	614	648	684	720	758	796	835	876	917
142.5	183	202	221	242	263	286	309	333	358	384	411	439	468	498	528	560	592	626	660	695	731	768	806	845	885
145	177	195	214	234	254	276	298	322	346	371	397	424	452	481	510	541	572	604	637	671	706	742	779	816	855
147.5	171	188	206	226	246	267	288	311	334	359	384	410	437	465	493	523	553	584	616	649	683	717	753	789	826
150	165	182	200	218	238	258	279	301	323	347	371	396	422	449	477	505	535	565	596	627	660	393	728	763	799
152.5	160	176	193	211	230	249	270	291	313	336	359	384	409	435	461	489	517	546	576	607	639	671	704	738	773
155	155	170	187	204	223	241	261	282	303	325	348	371	396	421	447	473	501	529	558	588	618	649	682	714	748
157.5	150	165	181	198	216	234	253	273	293	315	337	360	383	407	433	458	485	512	540	569	599	629	660	692	724
160	145	160	175	192	209	227	245	264	284	305	326	348	371	395	419	444	470	496	524	551	580	609	640	670	702
162.5	141	155	170	186	202	220	238	256	276	296	316	338	360	383	406	431	456	481	508	535	562	591	620	650	681
165	136	150	165	180	196	213	230	249	267	287	307	328	349	371	394	418	442	467	492	519	545	573	601	630	660
167.5	132	146	160	175	191	207	224	241	259	278	298	318	339	360	382	405	429	453	478	503	529	556	584	612	640
170	128	142	155	170	185	201	217	234	252	270	289	309	329	350	371	393	416	440	464	489	514	540	567	594	622
172.5	125	138	151	165	180	195	211	227	245	262	281	300	319	340	361	382	404	427	450	474	499	524	550	577	604
175	121	134	147	160	175	189	205	221	238	255	273	291	310	330	350	371	393	415	438	461	485	509	535	560	587
177.5	118	130	143	156	170	184	199	215	231	248	265	283	302	321	341	361	382	403	425	448	471	495	520	545	570
180	115	126	139	152	165	179	194	209	225	241	258	275	293	312	331	351	371	392	414	436	458	482	505	530	555

TS = 5 200 kPa

P = MAWP kPa

$$P = \frac{\pi \cdot d^2 \cdot TS}{1.1 \cdot 4 \cdot p^2}$$

d = Minimum diameter of corroded staybolt, mm

p = Staybolt spacing, mm

Table S2.10.4.1 [Metric Units]
Maximum Allowable Working Pressure Based on Load Carrying Capacity of a Single-Corroded Staybolt

Staybolt Spacing, in.	Actual Diameter of Corroded Iron Staybolts, in.																							
	0.35	0.375	0.4	0.425	0.45	0.475	0.5	1.525	0.55	0.575	0.6	0.625	0.65	0.675	0.7	0.725	0.75	0.775	0.8	0.825	0.85	0.875	0.9
3.5	81	93	105	119	133	149	165	182	199	218	237	257	278	300	323	346	370	396	422	448	476	504	533
3.625	75	86	98	111	124	139	153	169	186	203	221	240	259	280	301	323	345	369	393	418	444	470	497
3.75	70	81	92	104	116	129	143	158	174	190	207	224	242	261	281	302	323	345	367	390	415	439	465
3.875	66	76	86	97	109	121	134	148	163	178	193	210	227	245	263	282	302	323	344	366	388	411	435
4	62	71	81	91	102	114	126	139	153	167	182	197	213	230	247	265	284	303	323	343	364	386	408
4.125	58	67	76	86	96	107	119	131	143	157	171	185	200	216	232	249	267	285	303	323	343	363	384
4.25	55	63	71	81	90	101	112	123	135	148	161	174	189	204	219	235	251	268	286	304	323	342	362
4.375	52	59	67	76	85	95	105	116	128	139	152	165	178	192	207	222	237	253	270	287	305	323	341
4.5	49	56	64	72	81	90	100	110	121	132	143	156	168	182	195	209	224	239	255	271	288	305	323
4.625	46	53	60	68	76	85	94	104	114	125	136	147	159	172	185	198	212	227	241	257	273	289	306
4.75	32	37	42	47	53	59	65	72	79	86	94	102	110	119	128	137	147	157	167	178	189	200	211
4.875	30	35	40	45	50	56	62	68	75	82	89	97	105	113	121	130	139	149	159	169	179	190	201
5	29	33	38	43	48	53	59	65	71	78	85	92	100	107	115	124	133	142	151	160	170	180	191
5.125	27	32	36	41	45	51	56	62	68	74	81	88	95	102	110	118	126	135	144	153	162	172	182
5.25	26	30	34	39	43	48	53	59	65	71	77	83	90	97	105	112	120	128	137	145	154	164	173
5.375	25	29	33	37	41	46	51	56	32	67	73	82	86	93	100	107	115	122	130	139	147	156	165
5.5	24	27	31	35	39	44	49	54	59	64	70	76	82	89	95	102	110	117	125	133	141	149	158
5.625	23	26	30	34	38	42	47	51	56	62	67	73	79	85	91	98	105	112	119	127	135	143	151
5.75	22	25	29	32	36	40	45	49	54	59	64	70	75	81	87	94	100	107	114	121	129	136	144
5.875	21	24	27	31	35	39	43	47	52	56	61	67	72	78	84	90	96	103	109	116	123	131	138
6	20	23	26	30	33	37	41	45	49	54	59	64	69	75	80	86	92	98	105	111	118	125	133
6.125	19	22	25	28	32	35	39	43	47	52	57	61	66	72	77	83	88	94	100	107	113	120	127
6.25	18	21	23	27	31	34	38	42	46	50	54	59	64	69	74	79	85	91	97	103	109	115	122
6.375	18	20	23	26	29	33	36	40	44	48	52	57	61	66	71	76	82	87	93	99	105	111	117
6.5	17	20	22	25	28	31	35	38	42	46	50	54	59	64	68	73	78	84	89	95	101	107	113
6.625	16	19	21	24	27	30	34	37	41	44	48	52	57	61	66	71	75	81	86	91	97	103	109
6.75	16	18	21	23	26	29	32	36	39	43	47	51	55	59	63	68	73	78	83	88	93	99	105
6.875	15	18	20	23	25	28	31	34	38	41	45	49	53	57	61	66	70	75	80	85	90	95	101
7	15	17	19	22	24	27	30	33	36	40	43	47	51	55	59	63	68	72	77	82	87	92	97

$$P = \frac{\pi \left[\frac{d}{2}\right]^2 \cdot S}{p^2}$$

S = 7,500 psi

P = MAWP psi

p = staybolt spacing, in.

d = Minimum diameter of corroded staybolt, in.

Table S2.10.4.1.a [US Customary Units]
Maximum Allowable Working Pressure on the Load Carrying Capacity of a Single Corroded Staybolt

Staybolt Spacing, mm	Actual Diameter of Corroded Iron Staybolts, mm																								
	10	10.5	11	11.5	12	12.5	13	13.5	14	14.5	15	15.5	16	16.5	17	17.5	18	18.5	19	19.5	20	20.5	21	21.5	22
90	501	553	607	663	722	783	847	914	983	1 054	1 128	1 204	1 283	1 365	1 449	1 535	1 624	1 716	1 810	1 906	2 005	2 107	2 211	2 317	2 426
92.5	475	523	574	628	683	742	802	865	930	998	1 068	1 140	1 215	1 929	1 371	1 453	1 538	1 624	1 713	1 805	1 898	1 994	2 093	2 194	2 297
95	450	496	544	595	648	703	760	820	882	946	1 012	1 081	1 152	1 225	1 300	1 378	1 458	1 540	1 624	1 711	1 800	1 891	1 984	2 080	2 178
97.5	427	471	517	565	615	667	722	778	837	898	961	1 026	1 093	1 163	1 234	1 308	1 384	1 462	1 542	1 624	1 709	1 795	1 884	1 974	2 067
100	406	448	491	537	585	634	686	740	796	854	914	976	1 039	1 105	1 173	1 244	1 316	1 390	1 466	1 544	1 624	1 706	1 791	1 877	1 965
102.5	386	426	468	511	557	604	653	704	758	813	870	929	989	1 052	1 117	1 184	1 252	1 323	1 395	1 470	1 546	1 624	1 704	1 787	1 871
105	368	406	446	487	530	575	622	671	722	774	829	885	943	1 003	1 064	1 128	1 193	1 261	1 330	1 400	1 473	1 548	1 624	1 702	1 783
107.5	351	387	425	465	506	549	594	640	689	739	791	844	900	957	1 015	1 076	1 138	1 203	1 268	1 336	1 405	1 477	1 550	1 624	1 701
110	336	370	406	444	483	524	567	612	658	706	755	806	859	914	970	1 028	1 087	1 149	1 211	1 276	1 342	1 410	1 480	1 551	1 624
112.5	321	354	388	424	462	501	542	585	629	675	722	771	821	873	927	983	1 039	1 098	1 158	1 220	1 283	1 348	1 415	1 483	1 553
115	307	339	372	406	442	480	519	560	602	646	691	738	786	836	887	940	995	1 051	1 108	1 167	1 228	1 290	1 354	1 419	1 486
117.5	294	324	356	389	424	460	497	536	576	618	662	707	753	801	850	901	953	1 007	1 062	1 118	1 176	1 236	1 297	1 360	1 423
120	282	311	341	373	406	441	477	514	553	593	634	677	722	768	815	864	614	965	1 018	1 072	1 128	1 185	1 244	1 303	1 365
122.5	271	298	327	358	390	423	457	493	530	569	609	650	693	737	782	829	877	926	977	1 029	1 082	1 137	1 193	1 251	1 310
125	260	287	314	344	374	406	439	474	509	546	585	624	665	708	751	796	842	889	938	988	1 039	1 092	1 146	1 201	1 258
127.5	250	275	302	330	360	390	422	455	490	525	562	600	639	680	722	765	809	855	902	950	999	1 050	1 102	1 155	1 209
130	240	265	291	318	346	375	406	438	471	505	541	577	615	654	694	736	778	822	867	914	961	1 010	1 060	1 111	1 163
132.5	231	255	280	306	333	361	391	422	453	486	520	556	592	630	668	708	749	792	835	879	925	972	1 020	1 069	1 119
135	223	246	270	295	321	348	377	406	437	468	501	535	570	607	644	682	722	763	804	847	891	936	983	1 030	1 078
137.5	215	237	260	284	309	336	363	391	421	452	483	516	550	585	621	658	696	735	775	817	859	903	947	993	1 039
140	207	228	251	274	298	324	350	378	406	436	466	498	530	564	599	634	671	709	748	788	829	871	914	958	1 003
142.5	200	220	242	264	288	312	338	364	392	420	450	480	512	544	578	612	648	684	722	760	800	840	882	924	968
145	193	213	234	255	278	302	326	352	379	406	435	464	494	526	558	591	626	661	697	734	773	812	852	893	935
147.5	187	206	226	247	269	292	315	340	366	392	420	448	478	508	539	572	605	639	674	710	747	784	823	863	903
150	180	199	218	239	260	282	305	329	354	379	406	434	462	491	522	553	585	618	651	686	722	758	796	834	873
152.5	175	192	211	231	251	273	295	318	342	367	393	419	447	475	505	535	566	598	630	664	698	734	770	807	845
155	169	186	205	224	243	264	286	308	331	355	380	406	433	460	488	518	548	578	610	643	676	710	745	781	818
157.5	164	180	198	216	236	256	277	298	321	344	368	393	419	446	473	501	530	560	591	622	655	688	722	757	792
160	159	175	192	210	228	248	268	289	311	333	357	381	406	432	458	486	514	543	573	603	634	667	699	733	768
162.5	154	170	186	203	221	240	260	280	301	323	346	369	394	419	444	471	498	526	555	585	615	646	678	711	744
165	149	164	180	197	215	233	252	272	292	314	336	358	382	406	431	457	483	510	538	567	597	627	658	689	722
167.5	145	160	175	191	208	226	245	264	284	304	326	348	371	394	418	443	469	495	522	550	579	608	638	669	700
170	141	155	170	186	202	220	237	256	275	295	316	338	360	383	406	430	455	481	507	534	562	590	620	649	680
172.5	136	150	165	180	197	213	231	249	267	287	307	328	349	372	394	418	442	467	493	519	546	573	602	631	660
175	133	146	160	175	191	207	224	242	260	279	298	319	339	361	383	406	430	454	479	504	530	557	585	613	642
177.5	129	142	156	170	186	201	218	235	253	271	290	310	330	351	372	395	418	441	465	490	516	542	568	596	624
180	125	138	152	166	180	196	212	228	246	263	282	301	321	341	362	384	406	429	452	477	501	527	553	579	607

$$P = \frac{\pi \left[\frac{d}{2}\right]^2 \cdot S}{p^2}$$

S = 51 700 kPa

P = MAWP kPa

p = staybolt spacing, mm

d = Minimum diameter of corroded staybolt, mm

Table S2.10.4.1.a [Metric Units]
Maximum Allowable Working Pressure on the Load Carrying Capacity of a Single Corroded Staybolt

Staybolt Spacing, in.	Actual Diameter of Corroded Steel Staybolts, in.																							
	0.35	0.375	0.4	0.425	0.45	0.475	0.5	0.525	0.55	0.575	0.6	0.625	0.65	0.675	0.7	0.725	0.75	0.775	0.8	0.85	0.825	0.875	0.9
3.5	81	93	105	119	133	149	165	182	199	218	237	257	278	300	323	346	370	396	422	448	476	504	533
3.625	85	86	98	111	124	139	153	169	186	203	221	240	259	280	301	323	345	369	393	418	444	470	497
3.75	70	81	92	104	116	129	143	158	174	190	207	224	242	261	281	302	323	345	367	390	415	439	465
3.875	66	76	86	97	109	121	134	148	163	178	193	210	227	245	263	282	302	323	344	366	388	411	435
4	62	71	81	91	102	114	126	139	153	167	182	197	213	230	247	265	284	303	323	343	364	386	408
4.125	58	67	76	86	96	107	119	131	143	157	171	185	200	216	232	249	267	285	303	323	343	363	384
4.25	55	63	71	81	90	101	112	123	135	148	161	174	189	204	219	235	251	268	286	304	323	342	362
4.375	52	59	67	76	85	95	105	116	128	139	152	165	178	192	207	222	237	253	270	287	305	323	341
4.5	49	56	64	72	81	90	100	110	121	132	143	156	168	182	195	209	224	239	255	271	288	305	323
4.625	46	53	60	68	76	85	94	104	114	125	136	147	159	172	185	198	212	227	241	257	273	289	306
4.75	44	50	57	65	72	81	89	99	108	118	129	140	151	163	175	188	201	215	229	243	258	274	290
4.875	42	48	54	61	69	77	85	94	103	112	122	133	143	155	166	178	191	204	217	231	245	260	275
5	40	45	52	58	65	73	81	89	98	107	116	126	136	147	158	170	182	194	207	220	233	247	261
5.125	38	43	49	55	62	69	77	85	93	102	111	120	130	140	151	161	173	184	197	209	222	235	249
5.25	36	41	47	53	59	66	73	81	89	97	105	114	124	133	143	154	165	176	187	199	211	224	237
5.375	34	39	45	50	57	63	70	77	84	92	101	109	118	127	137	147	157	168	179	190	202	214	226
5.5	33	38	43	48	54	60	67	74	81	88	96	104	113	122	131	140	150	160	171	182	193	204	216
5.625	31	36	41	46	52	58	64	70	77	84	92	100	108	116	125	134	143	153	163	174	184	195	207
5.75	30	34	39	44	49	55	61	67	74	81	88	95	103	111	120	128	137	147	156	166	176	187	198
5.875	29	33	37	42	47	53	58	64	71	77	84	91	99	107	115	123	131	140	150	159	169	179	189
6	27	32	36	40	45	51	56	62	68	74	81	88	95	102	110	118	126	135	143	153	162	172	182
6.125	26	30	34	39	44	49	54	59	65	71	77	84	91	98	105	113	121	129	138	146	155	165	174
6.25	25	29	33	37	42	47	52	57	62	68	74	81	87	94	101	109	116	124	132	141	149	158	167
6.375	24	28	32	36	40	45	50	55	60	66	71	78	84	90	97	104	112	119	127	135	143	152	161
6.5	23	27	31	34	39	43	48	53	58	63	69	75	81	87	94	100	107	115	122	130	138	146	155
6.625	23	26	29	33	37	41	46	51	56	61	66	72	78	84	90	97	103	110	118	125	133	141	149
6.75	22	25	28	32	36	40	44	49	54	59	64	69	75	81	87	93	100	106	113	121	128	136	143
6.875	21	24	27	31	35	39	43	47	52	56	61	67	72	78	84	90	96	103	109	116	123	131	138
7	20	23	26	30	33	37	41	45	50	54	59	64	70	75	81	87	93	99	105	112	119	126	133

$$P = \frac{\pi \left[\frac{d}{2}\right]^2 \cdot S}{1.1 \cdot p^2}$$

S = 11,300 psi

P = MAWP psi

p = staybolt spacing, in.

d = Minimum diameter of corroded staybolt, in.

Table S2.10.4.1.b [US Customary Units]
Maximum Allowable Working Pressure on the Load Carrying Capacity of a Single Corroded Steel Staybolt

Staybolt Spacing, mm	Actual Diameter of Corroded Steel Staybolts, mm																								
	10	10.5	11	11.5	12	12.5	13	13.5	14	14.5	15	15.5	16	16.5	17	17.5	18	18.5	19	19.5	20	20.5	21	21.5	22
90	688	758	932	909	990	1 074	1 162	1 253	1 348	1 446	1 547	1 652	1 760	1 872	1 987	2 106	2 228	2 353	2 482	2 614	2 750	2 889	3 032	3 178	3 328
92.5	651	718	788	861	937	1 017	1 100	1 186	1 276	1 368	1 465	1 564	1 666	1 772	1 881	1 993	2 109	2 228	2 350	2 475	2 604	2 735	2 870	3 009	3 150
95	617	680	747	816	889	964	1 043	1 125	1 209	1 297	1 388	1 483	1 580	1 680	1 783	1 890	1 999	2 112	2 228	2 346	2 468	2 593	2 721	2 852	2 987
97.5	586	646	709	775	844	915	990	1 068	1 148	1 232	1 318	1 407	1 500	1 595	1 693	1 794	1 898	2 005	2 115	2 228	2 343	2 462	2 584	2 708	2 835
100	557	614	674	737	802	870	941	1 015	1 092	1 171	1 253	1 338	1 426	1 516	1 609	1 706	1 804	1 906	2 010	2 118	2 228	2 340	2 456	2 574	2 695
102.5	563	584	641	701	763	828	896	966	1 039	1 114	1 193	1 274	1 357	1 443	1 532	1 623	1 717	1 814	1 914	2 016	2 120	2 228	2 338	2 450	2 566
105	505	557	611	668	727	789	854	921	990	1 062	1 137	1 214	1 293	1 375	1 460	1 547	1 637	1 729	1 824	1 921	2 021	2 133	2 228	2 335	2 445
107.5	482	531	583	637	694	753	814	878	945	1 013	1 084	1 158	1 234	1 312	1 393	1 476	1 561	1 649	1 740	1 833	1 928	2 025	2 125	2 228	2 332
110	460	507	557	609	663	719	778	839	902	968	1 036	1 106	1 178	1 253	1 330	1 410	1 491	1 575	1 662	1 750	1 841	1 934	2 030	2 128	2 228
112.5	440	485	532	582	634	688	744	802	862	925	990	1 057	1 126	1 198	1 272	1 348	1 426	1 506	1 589	1 673	1 760	1 849	1 941	2 034	2 130
115	421	464	510	557	606	658	712	767	825	885	947	1 012	1 078	1 146	1 217	1 290	1 364	1 441	1 520	1 601	1 684	1 770	1 857	1 947	2 038
117.5	403	445	488	533	581	630	682	735	791	848	908	969	1 033	1 098	1 166	1 235	1 307	1 381	1 456	1 534	1 614	1 695	1 779	1 865	1 952
120	387	426	468	511	557	604	654	705	758	813	870	929	990	1 053	1 118	1 184	1 253	1 324	1 396	1 471	1 547	1 625	1 706	1 788	1 872
122.5	371	409	449	491	534	580	627	676	727	780	835	892	950	1 010	1 073	1 137	1 202	1 270	1 340	1 411	1 484	1 560	1 637	1 716	1 796
125	356	393	431	471	513	557	602	650	699	749	802	856	912	970	1 030	1 092	1 155	1 220	1 287	1 355	1 426	1 498	1 572	1 648	1 725
127.5	343	378	415	453	493	535	579	624	671	720	771	823	877	933	990	1 049	1 110	1 173	1 237	1 303	1 370	1 440	1 511	1 584	1 426
130	330	363	399	436	475	515	557	601	646	693	741	792	844	897	952	1 009	1 068	1 128	1 190	1 253	1 318	1 385	1 453	1 523	1 595
132.5	317	350	384	420	457	496	536	578	622	667	714	762	812	964	917	971	1 028	1 086	1 145	1 206	1 269	1 333	1 399	1 466	1 535
135	306	337	370	404	440	477	516	557	599	642	688	734	782	832	883	936	990	1 046	1 103	1 162	1 222	1 284	1 348	1 413	1 479
137.5	295	325	356	390	424	460	498	537	577	619	663	708	754	802	851	902	954	1 008	1 063	1 120	1 178	1 238	1 299	1 362	1 426
140	284	313	344	376	409	444	480	518	557	597	639	683	727	774	821	870	921	972	1 026	1 080	1 137	1 194	1 253	1 313	1 375
142.5	274	302	332	363	395	429	463	500	538	577	617	659	702	747	793	840	889	939	990	1 043	1 097	1 153	1 209	1 268	1 327
145	265	292	321	350	381	414	448	483	519	557	596	636	678	721	766	811	858	907	956	1 007	1 060	1 113	1 168	1 224	1 282
147.5	256	282	310	339	369	400	433	467	502	538	576	615	655	697	740	784	829	876	924	973	1 024	1 076	1 129	1 183	1 239
150	248	273	299	327	356	387	418	451	485	520	557	595	634	674	715	758	802	847	894	941	990	1 040	1 092	1 144	1 198
152.5	239	264	290	317	345	374	405	436	469	503	539	575	613	652	692	733	776	820	864	911	958	1 006	1 056	1 107	1 159
155	232	256	280	307	334	362	392	422	454	487	522	557	593	631	670	710	751	793	837	881	927	974	1 022	1 072	1 122
157.5	225	248	272	297	323	351	379	409	440	472	505	539	575	611	649	688	727	768	810	854	898	943	990	1 038	1 087
160	218	240	263	288	313	340	368	396	426	457	489	523	557	592	629	666	705	745	785	827	870	914	959	1 006	1 053
162.5	211	233	255	279	304	330	356	384	413	443	475	507	540	574	610	646	683	722	761	802	844	886	930	975	1 021
165	205	226	248	271	295	320	346	373	401	430	460	491	524	557	591	626	663	700	738	778	818	860	902	946	990
167.5	199	219	240	263	286	310	335	362	389	417	447	477	508	540	574	608	643	679	717	755	794	834	875	918	961
170	193	212	233	255	277	301	326	351	378	405	434	463	493	525	557	590	624	660	696	733	771	810	850	891	933
172.5	187	206	226	248	270	292	316	341	367	394	421	450	479	510	541	573	606	641	676	712	749	787	825	865	906
175	182	200	220	240	262	284	307	331	356	382	409	437	466	495	526	557	589	622	656	691	727	764	802	841	880
177.5	177	195	214	234	255	276	299	322	346	372	398	425	453	481	511	541	573	605	638	672	707	743	780	817	856
180	172	190	208	227	248	269	290	313	337	361	387	413	440	468	497	526	557	588	621	654	688	722	758	795	832

$$P = \frac{\pi \left[\frac{d}{2}\right]^2 \cdot S}{1.1 \cdot p^2}$$

S = 78 000 kPa

P = MAWP kPa

p = staybolt spacing, mm

d = Minimum diameter of corroded staybolt, mm

Table S2.10.4.1.b [Metric Units]
Maximum Allowable Working Pressure on the Load Carrying Capacity of a Single Corroded Steel Staybolt

S2.10.5 CONSTRUCTION CODE

To address the many pressure-related components and features of construction encountered in firetube boilers, a reprint of the 1971 Edition of Section I of *ASME Boiler Code*, Part PFT, is provided for information only. This section may be used for actual repairs/alterations and inspection/evaluation of boilers.

S2.10.6 NOMENCLATURE (15)

The nomenclature for the terms used in the above equations is:

p = maximum pitch measured (inches or mm) between straight lines, (horizontal, vertical, or inclined) passing through the centers of staybolts in different rows.
l = the pitch of stays in one row, passing through the center of staybolts, these lines may be horizontal, vertical, or inclined and measured in inches or mm.
w = the distance between two rows of staybolts, inches or mm.
h = the hypotenuse of a square or rectangle, defined as either $\sqrt{2p^2}$ or $\sqrt{l^2 + w^2}$, inches or mm.
d = minimum diameter of corroded stayblot, inches or mm
R = inside radius of the weakest course of shell or drum, in inches or mm.
TS= ultimate tensile strength of shell plates, psi (MPa)
t = minimum thickness of shell plate in the weakest course, inches or mm.
P = calculated MAWP psi (MPa).
S = maximum allowable stress value, psi (MPa).
C = 2.1 for welded stays or stays screwed through plates not over 7/16 in. (11 mm) in thickness with ends riveted over.
C = 2.2 for welded stays or stays screwed through plates over 7/16 in. (11 mm) in thickness with ends riveted over.
C = 2.5 for stays screwed through plates and fitted with single nuts outside of plate, or with inside and outside nuts, omitting washers.
C = 2.8 for stays with heads not less than 1.3 times the diameter of the stays screwed through plates, or made a taper fit and having the heads formed on the stays before installing them and not riveted over, said heads being made to have true bearing on the plate.
C = 3.2 for stays fitted with inside and outside nuts and outside washers where the diameter of washers is not less than 0.4p and thickness not less than t.

Note: The ends of stays fitted with nuts shall not be exposed to the direct radiant heat of the fire.

E = the efficiency of the longitudinal riveted joint.

See Table S2.10.6 for efficiencies (E), which are the average for the different types of riveted joints.

TABLE S2.10.6
EFFICIENCIES (E), AVERAGES FOR RIVETED JOINTS

Type of Riveting	Lap	Butt
Single	58	
Double	74	82
Triple	78	88
Quadruple		94

Note: The efficiency of a particular joint depends upon the strength of the plate and rivet, thickness of the plates, and the diameter of the rivets. The 1971 Edition of Section I of the ASME Code, Appendix A-1 through A-7, provides a method for calculating a specific joint efficiency that may be used with the concurrence of the Jurisdiction.

FS = Factor of safety

FS = 4 For stayed surfaces
FS = 6 For riveted lap joints
FS = 5 For riveted buttstrap joints

Note: A Jurisdiction may mandate a higher design margin or permit a lower design margin, but in no case may the factor of safety be less than four.

S2.10.7 LIMITATIONS

a) The maximum allowable working pressure shall be the lesser of that calculated in accordance with NBIC Part 2, S2.10, or the MAWP established by the original manufacturer.

b) The shell or drum of a boiler in which a "lap seam crack" extending parallel to the longitudinal joint and located either between or adjacent to rivet holes, when discovered along a longitudinal riveted joint for either butt or lap joint, shall be permanently discontinued for use under steam pressure, unless it is repaired with jurisdictional approval.

S2.11 BOILER INSPECTION GUIDELINE

a) The following form may be used as a guideline for documentation and inspection of historical boilers. Jurisdictions may require additional inspections and documentation to those noted in this guide. The owner or user and Inspector should be aware and understand jurisdictional requirements where the historical boiler will be operated.

Jurisdiction Number _____

Owner _____

Location _____

Make _____

Year _____

Engine No. _____

Heating Surface _____

Design Pressure _____

Current Operating Pressure _____

Inspector _____

Safety Valve(s) Setting _____

Total Safety Valve Capacity _____

b) As a minimum, the inspection shall include consideration of the following:

1) Smoke Box

a. Front Tubesheet

1. Check condition of front tubesheet and thickness around handhole openings.

2. Check condition of threaded openings and plugs.

3. Check condition of rivets between front tubesheet and barrel.

b. Tubes

1. Are tubes beaded back to the tubesheet?

2. Are there signs of leakage?

c. Check condition of smoke box shell (especially around lower surfaces).

d. Check inside condition of barrel and outside diameter of tubes for corrosion and scale.

e. Check back side of tubesheet (especially area in contact with handhole gasket and area where tubesheet joins barrel).

f. Check tubesheet supports (through stays, supports or strong backs).

g. Check inside rivet heads on lap or buttstrap joints, if possible.

h. Check front bolster (front axle) attachment points inside barrel. Note thinning of the lower smokebox section of the barrel is critical if the steering bolster attaches fully or partially to this thinned area.

2) Barrel (shell)

a. Check front bolster attachment points on the outside of the barrel, both within and without the present boundary.

b. Check condition of tubesheet rivets on outside of barrel.

c. Check condition of threaded openings and plugs in openings.

d. Check radius rod attachment point.

e. Check attachment points of studs, castings, brackets, accessories, etc.

f. Check piping and nozzle openings on shell (feedwater nozzles, steam outlet, water column, etc.).

g. Check handhole openings in barrel.

h. Lap seam or buttstrap

1. Check for leakage around riveted seams and joint rivets.

2. Confirm joint efficiency based on number of rows of rivets and type of joint.

i. Identify and check any external contour that does not appear normal.

j. Insulation or insulation jacket (lagging)

1. Does jacket cover any critical areas or make them difficult to observe? (Normally the jacket will need to be removed for inspection of the barrel.)

2. Is barrel pitted or corroded under jacket?

3) Wrapper Sheet

a. Check handhole openings (material thickness, gasket area, etc.).

b. Check for seepage around attachment points (wing sheets, axle supports, etc.).

c. Check condition of riveted seams joining wrapper to throat sheet and rear head.

d. Check condition of riveted seams joining throat sheet to barrel.

e. Check for external shapes or contours that do not appear normal.

f. Check for seepage around staybolt heads.

g. Check condition of staybolt heads.

h. Check condition of threaded openings. (May need to remove nipples and plugs).

i. Check internal surfaces for cracks, pits, material thickness, and scale.

j. Check staybolt thickness and condition.

k. Check for scale and mud buildup in waterlegs and wet bottoms.

l. Check for buildup of dirt and grease between or behind attaching brackets such as wing sheets.

m. For dry bottom boilers:

1. Check riveted seams at bottom of waterlegs in ash pan area (ogee ring).

2. Do you need to remove ash pans and grates to observe above seams?

3. Check condition of grate support brackets.

n. For wet bottom boilers:

1. Check ash pan area for pits and staybolt head condition.

2. Check inside bottom of wrapper and staybolt condition.

3. Check condition of lap seam in wrapper.

4. Check condition of ash pan drain tube if present.

5. Check condition of drain plug and plug threads.

6. Check condition of studs, especially studs holding hitches to the bottom sheet.

o. Check for condition of blowdown valve. Check for size and type.

4) Steam Dome

a. Check for condition of drain back holes in shell if possible.

b. Check condition of main steam stop valve.

c. Check condition of piping on the steam dome and the condition of the steam outlet piping on the steam dome.

d. Check condition of the steam dome seams and seams between the steam dome and the boiler shell.

1. Is seepage present?

2. Can interior seams be observed?

e. Check the condition of pressure gage.

1. Is there a siphon and what is its condition?

2. Is the gage readable from the operator's position?

3. Has the gage been calibrated or checked against another gage?

4. If a shutoff valve is present, its handle shall indicate open position.

5. Checked gage for correct range and pressure.

f. Check for condition of safety valve.

1. Does the safety valve have its own inlet/outlet piping with no intervening block valves and no possibility of isolation?

2. Check that the inlet pipe size is not smaller than the valve inlet size.

3. Check that the outlet pipe size is not smaller than the valve outlet size.

4. Is the safety valve a National Board capacity certified, ASME "V"/National Board "VR" stamped valve of proper set pressure and capacity rating for the boiler heating surface?

5. Does the safety valve have a try lever (hand lifting lever)?

6. Is the safety valve sealed with factory seals at the top pressure adjustment cap and at the blowdown ring adjustment point?

5) Water Column and Gage Glass

a. Is the gage glass calibrated to the level of the crownsheet?

b. Check condition of try-cocks, gage glass stop valves, gage glass drain valve, and water column drain valve.

c. Check condition of gage glass (cracks or scratches).

d. Check the upper and lower gage glass packing for signs of leakage.

6) Firebox

a. Check for bulging between staybolts and warping of the boiler plate (determine possible causes).

b. Check riveted seams around the fire door.

c. Check for sediment buildup over the fire door opening at the rear head.

d. Check for sediment buildup over the peephole opening in the wrapper sheet (where applicable).

e. Check condition of fusible plug. (The plug must be removed for observation.)

1. Is it stamped ASME standard?

2. Check condition of top surface for scale and bottom surface for tin corrosion. (May need to brush it off)

3. Check for signs of leakage between the tin center and brass casing.

f. When the fusible plug is removed, check crownsheet thickness at that location and thread condition. Are weld repairs required?

g. A fireside fusible plug must project a minimum of 3/4 in. (17.8 mm) into the waterside.

h. Fireside fusible plug may not extend into fire area more than 1 in. (25 mm).

i. A gage glass calibration can only be done when the crownsheet and fusible plug and gage glass can be seen and measured. A recommended minimum water level may be determined as follows: With engine (boiler) sitting on level ground and water just observable at the bottom of the gage glass, the crownsheet should be covered by at least 2-1/2 in. (64 mm) of water on a full-size boiler.

j. Check staybolt condition, especially near top surface of crownsheet.

k. Check through stays, strong backs, knee braces, etc., on rear head.

l. Check handhole openings, threaded openings and plugs in rear head.

m. Check condition of firebox tubesheet and check if tubes are beaded back to the tubesheet.

n. Check condition of staybolt heads inside the firebox.

o. Check condition or design of crownsheet. Is it flat-topped or able to trap water? Is it free of scale?

7) External Plumbing (see NBIC Part 2, S2.7.1)

a. Is black pipe (as opposed to galvanized pipe) used throughout?

b. Check for use of schedule 80 black pipe required between boiler and first valve.

c. Are fittings and valves of proper pressure rating for maximum allowable working pressure?

d. Are isolation valves present to shut off individual system lines (blower, injector, main steam, blowdown, etc.)?

e. Are two separate feedwater systems present and operable?

f. Check piping for freeze damage.

g. Are piping support brackets present where needed?

h. Fittings dates are to be stamped, stenciled, or recorded on boiler records (boiler log).

i. Piping shall have a 20-year life, except for the main steam line, which shall be evaluated periodically as to remaining service life. As an alternative, all boiler piping may be ultrasonically examined for adequate thickness to determine the remaining service life.

8) Ultrasonic Thickness Testing (every fifth year).

9) Hydrostatic Pressure Test (minimum every three years or as required by the Jurisdiction).

a. Hydrostatic pressure test should be between maximum calculated allowable working pressure and 1.25 times maximum allowable working pressure with metal temperature at 60°F-120°F. (16°C-49°C).

b. A calibrated pressure gage shall be used when hydrostatically pressure testing a boiler. The boiler gage may be compared (calibrated) with the calibrated pressure gage at this time.

c. All safety valves shall be removed during the hydrostatic testing of the boiler.

10) Safety Valve Testing

a. Safety valves should be removed from the boiler for testing and/or repair at intervals required by the Inspector or the Jurisdiction.

b. Safety valves may be try lever checked for operability with the boiler under steam pressure of at least 75% of the set pressure of the safety valve.

c. Safety valves may also be tested initially, periodically and after any repair or adjustment as noted in the External Operating Test listed below.

11) External Operating Test (every third year)

a. The safety valve should be tested by having the operator raise the boiler pressure to the safety valve popping point and popping point pressure and blowdown observed to be within manufacturer's tolerances.

b. Feedwater devices (two injectors, or one injector and one pump) tested for operability.

c. Gage glass stop and drain valves and gage cocks checked in service.

d. Blowdown valve(s) tested as operational and discharging to a safe location.

e. Operation of the steam engine by the operator satisfactory, including a driving test.

f. The external operating test to be recorded in the boiler records (boiler log).

S2.12 INITIAL BOILER CERTIFICATION REPORT FORM, see Pg.174

Form C-1 may be used to document the initial inspection for historical boilers. (Form C-1 is located at the end of this supplement.)

S2.13 GUIDELINES FOR HISTORICAL BOILER STORAGE

The historical boiler guidelines published herein list the general recommendations for storage of historical boilers. The exact procedures used by the owner/operator must be based on the conditions and facilities at the storage site.

S2.13.1 STORAGE METHODS

a) The methods for preparing a historical boiler for storage depend upon several factors, including:

1) The anticipated length of time the historical boiler will be stored;

2) Whether storage will be indoors or outdoors;

3) Anticipated weather conditions during the storage period;

4) The availability of climate-controlled storage;

5) Type of fuel used; and

6) Equipment available at the storage site.

b) Indoor storage can be categorized into two types: indoor with climate control and indoor without climate control.

c) Outdoor storage can also be categorized into two types: outdoors during a warm time of year or in a geographic location where it can reasonably be expected to be above freezing during storage, and outdoors during a time period or in a geographic location where it can be expected that freezing temperatures will occur during storage.

d) Historical boilers may be stored using the “wet method” or the “dry method.”

e) Before any method of storage, the boiler must be thoroughly washed out, with mud and scale removed from the mudring, crownsheet, bottom of the barrel, and the top of the firing door.

S2.13.1.1 WET STORAGE METHOD

a) When utilizing the “wet storage method,” the boiler is completely filled with treated water to exclude air.

Note: This method cannot be used if the historical boiler is exposed to freezing weather during storage.

b) Chemicals may be added to the storage water to further inhibit corrosion. However, depending on the chemical used, the treated water may have to be disposed of as a hazardous waste to prevent chemical contamination of the surrounding property.

c) The procedure applies only to the sections of the boiler that contain water. The firebox interior, cylinders, piping, and auxiliary equipment of the historical boilers still require draining, preservation, and dry storage.

S2.13.1.2 DRY STORAGE METHOD

a) When utilizing the “dry storage method” the boiler is completely emptied of water, dried out, and allowed to stand empty. Several variations of the “dry method” may be used. These include but are not limited to:

1) Airtight storage with a moisture absorbent placed in trays in the boiler;

2) Airtight storage with the boiler filled with inert gas to exclude oxygen; and

3) Open-air storage with the mudring washout plugs or handholes removed to enable air circulation for evaporation of formed moisture.

b) Each variation has positive and negative points that must be taken into account before use. If the boiler is filled with inert gas such as nitrogen, care must be taken because this method can result in asphyxiation of personnel if the gas escapes the boiler through a leaking valve, washout plug, or handhole and enters a pit, sump, or enclosed room. In addition, the boiler must be completely vented to remove gas, then tested and declared gas-free before personnel may enter.

c) Although the use of dry storage with several washout plugs or handholes removed for air circulation is the most common method, there are some potential drawbacks. The boiler interior may be subject to moisture forming from condensation created from humidity changes in the ambient air. Small animals may take up residence inside if screens are not used to cover handholes or washouts.

d) Before storage, the boiler must be thoroughly washed out, with mud and scale removed from the mudring, crownsheet, bottom of the barrel, and top of the firing door. Any mud or loose scale left in the boiler will retain moisture, leading to corrosion. After washing, water must be removed and the boiler dried before storage. A portable gas or electric heater placed in the firebox to aid evaporation and drying along with a vacuum used to siphon water out via the lower washout plugs or handholes is recommended.

Note: Use of the drying-out procedure of building a small wood fire in the firebox is not recommended because of the danger of overheating the firebox sheets.

e) The typical railroad dry storage method required blowdown of the boiler until empty while steam pressure registered on the gage and removal of the washout plugs or handholes while the shell plates were hot and there was no steam pressure. This allowed the heat remaining in the boiler plates to evaporate any remaining water in the boiler. However, this method may result in staybolt damage from temperature change and requires extreme care, if used.

f) Oil should not be applied to the interior surfaces of the boiler because it is difficult to remove. Further, the oil must be removed before steaming or it will form scale and contribute to foaming.

S2.13.2 RECOMMENDED GENERAL PRESERVATION PROCEDURES

a) When the historical boiler is under steam, inspect piping, fittings, and appliances for steam and water leaks that may introduce moisture into the lagging. Repair leaks as necessary and remove wet lagging insulation.

b) Remove grates and ash pan bottom if dry bottom. Remove washout plugs and handhole plates. Mark handhole plates and washout plugs for proper relocation.

c) Thoroughly wash the boiler and firebox and remove mud and scale from the mudring, crownsheet, bottom of the barrel, and top of the firing door. Any mud or loose scale left in the boiler will retain moisture leading to corrosion.

d) To protect the boiler interior during storage, dry the boiler by using compressed air to blow out as much water as possible. A portable heater placed in the firebox to warm the boiler to 200°F (95°C) along with a vacuum used to siphon water out via the lower washout plugs or handholes can aid evaporation and drying of any moisture that collects in low or impossible-to-drain locations without harming the sheets.

Caution: To prevent a buildup of steam pressure during the drying process, an opening in the upper part of the boiler should be opened to enable the moisture to escape. In addition, the driving wheels should be blocked and the throttle and cylinder cocks should be opened to permit any steam that forms to escape.

After drying, it will be necessary to either vent the boiler or to place containers of desiccant inside the boiler through the dome cap to absorb any condensation that may occur during storage. Venting the boiler to allow air circulation is accomplished by leaving two or more of the lower washout plugs or handholes out and opening the vent valve on the top of the boiler. A vent line consisting of two 90° elbows and pipe nipples should be installed in the vent valve to locate the opening to the downward direction in order to keep rain or snow from entering the open valve.

e) To prepare a historical boiler for storage, the following should be completed:

1) If the historical boiler will be stored outdoors, inspect the boiler jacket and confirm it is tight with no gaps leading into the lagging or shell. Pay close attention to areas at shell openings such as for studs, safety valves, etc. Repair gaps or damaged jacket sections as necessary. Consideration should be given to covering the entire historical boiler and equipment with a tarp. Otherwise, jacket openings should be covered to prevent the entrance of rain or snow. Where necessary, apply a waterproof covering over the exposed or open sections.

2) If the historical boiler will be stored outdoors, the smokestack should be sealed by applying a wood and sheet rubber cover held in place by clamps or a through bolt.

3) If the historical boiler will be stored outdoors, the safety valves should either be covered or removed, with plugs or caps installed in the holes if the valves are removed. The governor and lubricators should be covered.

4) Clean tubes using tube brush or scraper. After cleaning use a long air nozzle or vacuum to remove any loose coal or ash.

5) Empty and clean the smokebox and front tubesheet of all coal, ash, or burnt oil. This work is especially critical at the bottom section of the smokebox and front tubesheet rivet flange. The smokebox door should be sealed by applying a gasket or sealant and any other air openings in the smokebox sealed. The exhaust nozzle should be sealed by applying a wood and sheet rubber cover held in place by clamps.

6) Thoroughly clean the firebox sheets of coal, ash, and clinker.

7) The potential for corrosion of the smokebox interior, front tubesheet, and fireside of the firebox sheets can be further minimized by applying a coating of light oil, outdoor paint, or primer. Inspection of the smokebox, front tubesheet, and firebox sheet must be accomplished before painting since it will cover up many types of defects. The coating will burn off quickly when the historical boiler is returned to service.

8) Empty and completely clean the grates and ash pan of coal and ash. This work is especially critical at the sections between the grate bearers, rivets, and firebox sheets; and from the grate segment air openings.

9) Appliances and piping that might contain water or condensation should be drained and blown dry using dry compressed air. Remove injectors and store in a warm place. Refer to NBIC Part 2, S2.13.3, *Use of Compressed Air to Drain Historical Boiler Components*, for details.

10) The cylinder castings, valve cavities, and steam lines must be drained of moisture and blown dry. A typical method:

    Pressurizing the boiler with compressed air. Using the throttle to regulate the airflow, allow the air to blow through the dry pipe and discharge into the cylinders. The cylinder cocks must be open.

    Note: This may have to be performed several times to discharge the moisture from the cylinders and steam pipes.

    Refer to NBIC Part 2, S2.13.3, *Use of Compressed Air to Drain Historical Boiler Components*, for additional information.

11) Drain and wash tender water spaces. The tank should be inspected afterward and any remaining water removed by siphon or vacuum. When dry, spray the water space with outdoor paint or a commercial rust preventative. Oil should not be used. Drain and dry the tender tank hoses and clean screens.

12) On coal or wood burners, remove coal or wood. Spray any exposed surfaces of the tender fuel space with outdoor paint or a commercial rust preventative. If the historical boiler is to be stored outdoors for a long term, cover the coal space with a tarp or a roof.

13) After cleaning thoroughly, coat connecting rods, cross heads, valve gear, guides, piston rods, and exposed feedwater pump components with water-resistant grease or a rust preventative. If the historical boiler is to be stored outdoors for a long term, grease should be applied to junction of rod and pin in valve gear and rods to prevent water entering.

14) If the historical boiler is moved after this is applied, it will be necessary to reapply the coating to piston rods and guides.

    Note: Heavy oil or unrefined oil such as any of the Bunker types (Bunker 6, etc.) should not be used for preservation of any components because the sulfur contained in it can accelerate corrosion. Standard motor oil or journal oil will not stick to wetted surfaces. Surfaces to be so coated must be dry. If moisture is a problem, steam cylinder oil should be applied.

15) All openings in the boiler should be covered to ensure water and contaminants cannot enter the boiler. Handholes and plugs left out for air circulation should be covered with screen to prevent

small animals from entering and taking up residency in the boiler. Secure all openings and covers on the top of the water tender to prevent accidental opening with the potential for water and contaminants to enter.

16) If the historical boiler is to be stored outdoors with questionable or no security, remove and store all cab gages, water glasses, lubricators, brass handles, whistle, headlight, tools, spare parts, and any other items that thieves or vandals might attack.

17) Inspect stored historical boiler regularly for signs of rust, corrosion, damage, deterioration, vandalism, or animal invasion and immediately take any corrective measures necessary.

S2.13.3 USE OF COMPRESSED AIR TO DRAIN HISTORICAL BOILER COMPONENTS

a) The process of using air pressure to drain and empty auxiliary components such as the cylinders and piping completely of water offers several advantages over other methods.

b) The air compressor must be equipped with a suitable filter to enable it to supply oil-free air because the introduction of air that contains oil into the water/steam parts of the boiler will promote the formation of scale and water foaming when the historical boiler is returned to service.

c) The air compressor must be a large enough size to provide the volume and pressure of air required.

d) If the boiler is pressurized with compressed air, the air pressure must be raised slowly to prevent distorting or overstressing the firebox sheets or staybolts because the normal expansion of the boiler that occurs under steam pressure is not present when air pressure is used.

e) When pressurizing the boiler with air, the pressure should never exceed three-quarters of the maximum allowable working pressure. Air shall never be used for pressure testing the boiler.

f) Components are drained by pressurizing the boiler to one-half to three-quarters of the maximum allowable working pressure with compressed air, then operating each component individually until the exhaust from it contains no moisture.

g) When necessary, specific pipe lines can be drained by breaking the line at each end, attaching the air line to it directly, then blowing the line out.

S2.13.4 RETURN TO SERVICE

a) When returning a historical boiler to service, the boiler, firebox, and tender tank shall be ventilated to remove a potentially hazardous atmosphere from the firebox interior before personnel enter it. In addition, the atmosphere in the firebox shall be verified to be safe for human occupancy before personnel enter it. For the boiler this can be accomplished by removing the washout plugs or handholes and placing a fan or air blower on top of a steam dome opening to force air into the boiler. For the firebox this can be accomplished by opening the smokebox door and firebox door and placing a fan or air blower at either location to force air through. Failure to do this could result in asphyxiation of the first personnel to enter the boiler or firebox.

b) Perform a complete boiler flush to remove scale that has flaked off during storage as a result of the expansion and contraction of the metal due to temperature changes.

c) Clean handhole plate gasket surfaces (both boiler and handhole plate). These surfaces must be flat and free of scale, rust, and dirt in order to seal.

d) Inspect feedwater inlet connection to boiler. There should be a tee at each inlet; remove plug and inspect for lime deposits and clean if necessary. This should be done once a year; more often if conditions warrant it.

e) Remove gage glass and valves, and inspect these connections for lime deposits and clean if necessary. This should be done once a year; more often if conditions warrant it.

f) After inspection, replace glass (clean if necessary). Also inspect gage glass sealing washers and replace if necessary.

g) During cold weather, the historical boiler should be moved into a heated area and the boiler allowed to warm up in the air for several days until it is the same temperature as the air.

h) The initial fire-up should be done slowly to allow even heating of the boiler.

i) Before movement, the cylinder(s) should be warmed up by allowing a small quantity of steam to blow through them and out the cylinder cocks and exhaust passage(s). This is necessary to reduce the stress in the casting from thermal expansion of the metal.

j) Steam should be discharged through the cylinder cocks for several minutes to aid removal of any solvent, debris, or rust that may have formed in the steam pipes, cylinder, valve chest, and dry pipe.

k) All appliances should be tested under steam pressure before the historical boiler is moved or put under load.

S2.14 SAFETY PROCEDURES[4]

This chapter of text covers procedures in certain situations or emergencies that may occur.

S2.14.1 EXPERIENCE

a) Reading check lists and procedures can be of some value to get you thinking about what you are doing, but nothing can replace the experience gained by working beside conscientious and knowledgeable engineers. Ask questions, observe, read, listen, study, and think.

b) Safe operations depend upon thorough attention to detailed routines. Having procedures thought out, planned, and practiced before they are needed could minimize accidents and improve public safety. Know your abilities as well as the limitations of the machine that you are operating. In most cases knowing and keeping your machine in top operating condition can prevent most emergency situations from occurring. However, sometimes problems or situations beyond your control do occur. In any situation the first rule to remember is to keep a cool head. Haste and panic can never solve any emergency.

c) Don’t be afraid to ask for help or advice. A lot of shows and public demonstrations have a designated individual in the area to ensure safe operation and assistance should a problem arise.

S2.14.2 STOPPING ENGINE IN AN EMERGENCY

a) Know how to stop the engine suddenly. For example, if someone or something runs out in front of the engine or some problem happens with whatever it is belted up to:

   1) Close throttle.

   2) Reverse valve quadrant position.

   3) Open throttle for a moment (this will quickly stop your engine).

   4) Close throttle.

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5) Open cylinder cocks.

b) Steam traction engines do not have brakes, so this is a maneuver worth knowing and practicing. However, it should be practiced with the dome valve shut as this method of stopping the engine tends to be very hard on gears and castings. In regards to belt work, it is extremely important that total undivided attention be given to what it is belted up to. Be prepared to shut down quickly should something happen.

S2.14.3 WATER GLASS BREAKAGE

Having a properly guarded water glass will prevent objects from coming in contact with the glass. However, water glasses do break. If the machine is operating when water glass breakage occurs:

a) Close throttle.

b) Set valve quadrant to neutral (middle notch).

c) Disengage clutch.

d) Close damper.

e) Locate bottom water glass valve and shut off.

1) The first four procedures will be difficult if the water glass is mounted back by the operator's platform.

2) The bottom water glass valve is essential to locate and close first. This valve is below the waterline and can take the water dangerously close to the crownsheet if water is allowed to escape unchecked. This is where having the automatic type gage valves would be most desirable. Most traction engines do not have automatic-type gage valves. Caution must be exercised at this time because 300 °F (150 °C) steam and water will be spraying in every direction! There will be an inability to see much of anything except a cloud of water vapor. Use a shovel or a coat or something to deflect the spray to be able to find that lower valve.

f) Next, close the top gage valve; this one should just be blowing steam and obscuring visibility. There is no serious problem with steam being released because this valve is above the water line.

g) Next, use the try-cocks to determine water level of boiler. If bottom try-cock blows water, then inject water and replace water glass. However, if bottom try-cock does not blow water, and only blows steam, do not inject water and proceed to kill fire immediately. Do not move engine. Another method of determining the water level in the boiler other than using the try-cocks is to wet down a burlap sack and lay it on the barrel part of the boiler. Quickly pull it away and there will be a "sweat line" of where the actual water level is.

S2.14.4 RUNAWAY ENGINE AND GOVERNOR OVER SPEED

a) Probable cause: governor malfunction. Usually the governor belt either slips or breaks. Know the governor belt condition and keep its tension snug but not too tight. Also, packing nut could be too tight, causing a binding on valve spindle; more often this will cause the engine not to respond to load and usually will not "run away."

b) What to do in a runaway situation: Never leave the operator's platform while engine is at governed speed.

In the case of a runaway engine:

1) Quickly close the throttle;

2) Move forward/reverse lever to center of quadrant;

3) Open cylinder cocks;

4) Close dome valve; and

5) Close damper and steam down (this is not a boiler emergency; once the engine has stopped there should be no danger).

c) In the unlikely event the throttle were to jam in conjunction with governor malfunction:

1) Move forward/reverse lever to center of quadrant. This will stop the engine even though steam is still being sent to the valve chest;

2) Close the dome valve; this would be the same as closing the throttle. Steam flow would then be stopped and the engine should be safe;

3) Close damper and steam down.

S2.14.5 KILLING A FIRE

This is an important procedure to know, should a low water situation ever occur.

a) Close all dampers. This will stop incoming air, which supports fire. Capping the smokestack is an additional way of checking draft to fire. However, it will cause a lot of smoke to emit around fire door.

b) Shovel dry sand or dry earth on the fire; this should immediately cool the fire to a safe level. Have a pile of dry sand or dirt in or around the steam engine area should a situation occur. It is important to remember that when trying to extinguish a fire, never stir the fire; this will only intensify the fire's heat.

c) Close the fire door.

d) Close the dome valve.

e) Leave the engine alone. It is especially important not to move the engine as this could slosh water onto a possibly overheated crownsheet.

S2.14.6 INJECTOR PROBLEMS

Injector problems are the number one reason for boiler operation malfunctions. An injector can be a very sensitive device. The ability to identify the reasons why it's not working is the most important thing a steam engineer needs to know. The following are various problems and their causes.

a) Failure to raise water from supply tank.

1) Suction pipe clogged or tank supply valve turned off.

2) Leaks in suction pipe or hose, allowing air to enter above the level of water supply. A common problem when rubber or plastic hoses are used on suction side of injector.

3) Water supply too hot. Hot water will prevent injector from lifting water.

4) Obstruction in the lifting or combining tubes of the injector.

b) Injector lifts water but will not force it into the boiler.

1) Choked suction pipe or strainer/incomplete obstruction.

2) Supply valve not opened all the way.

3) Boiler valve closed.

4) Boiler check valve stuck closed.

5) Obstruction in delivery tube on injector.

6) Leaking injector overflow check valve.

7) Injector choked with lime.

c) Other injector problems.

1) Usually you have a hot injector because of improper operation. This is where a removable rubber hose on your water suction is handy. Remove hose, turn steam valve on to injector and put your thumb over suction side of injector. You should feel a smooth, steady suction. If not, wrap a rag around injector body and soak rag with cool water. Your objective is to cool down the injector. Now turn steam back on to injector, allowing cool air to suck into injector. At the same time, place suction hose back onto water supply line and it should go. Remember to tighten suction side connections so you don't lose your vacuum.

2) If injector still does not lift after following the previous instructions, it probably has some foreign matter in the lifting or combining tube. Simply remove bottom square nut on injector body, taking care not to lose flat washer that will come out with injector combining tube, clean and re-install. This should restore injector to working order.

3) When having injector problems, watch your injector overflow. Steam only and no water at overflow usually is an indication of a water lifting problem (no water to the injector). Steam and water at the overflow is usually a delivery problem, meaning your injector is lifting water but not forcing it into boiler.

4) The problem with delivery is usually associated with a stuck boiler check valve. After assuring yourself that the isolation valve to the boiler is open, try lightly tapping on the boiler check valve. More than likely though you will have to disassemble and clean boiler check valve; scale may be is holding the check valve from opening. This can be done with steam pressure on the boiler, providing the valve to the boiler holds pressure and the boiler check valve has been properly piped in. A boiler check valve may not close, causing steam and hot water to blow back through injector and into your feedwater tank. Again, you would have to turn off the valve to the boiler, disassemble and clean the check valve. If the injector will not force water into the boiler, there may be an obstruction in the delivery/combining tube of the injector. Remove bottom nut of the injector, disassemble and clean as explained above.

S2.14.7 FOAMING OR PRIMING BOILER

a) A foaming boiler is usually caused by dirty or impure water in the boiler. Oils, detergent, etc., are the biggest problems and have no business being on the waterside of a boiler. A good rule of thumb is, "If you wouldn't drink it, don't put it in your boiler." Foaming can be especially bad because you have no way of discerning your water level. The water glass and try-cocks will appear full. Foaming is usually really intensified with a heavy fire and a heavy engine load. Reduce or stop your engine load and reduce your fire until it settles down, steam down, wash out your boiler, and refill it with clean water. The first indication of a foaming or priming boiler is usually a "wet stack" and a discernable difference in the exhaust sound. Open cylinder cocks immediately and close throttle and determine your water level.

b) Priming is similar to foaming; you're pulling water into your engine. This is especially bad because it can wash the oil from valves and cylinders and risk severe damage to the engine. Priming is caused more from carrying too-high a water level. It also occurs from working steam while ascending and descending hills. Know the machine you are operating, and what the safe water level is.

c) If an engine starts priming (it will show a wet stack), open cylinder cocks, reduce throttle, get engine to level area, and determine the water level. If possible, safely blowdown boiler to proper water level. Ensure no bystanders are close-by for safety.

S2.14.8 HANDHOLE GASKET BLOWS OUT

a) Special care should be taken to ensure proper installation of handhole gaskets to prevent a blowout.

b) New gaskets need special attention on the first fire-up. When installing, ensure plate surface and mating surface on boiler are free of loose scale and debris. Firmly snug the gasket after it is properly centered on the handhole. Do not over-tighten as this tends to cut the gasket. A common cause of handhole gasket blowout is improper fitting of gasket to handhole plate. It is very important that the gasket fits center of handhole plate very snug. When steaming up, carefully "follow up" gaskets by ensuring nut stays snug. Special care must be exercised to ensure that there is no rotaton of the handhole plate or gasket. Caution should be used if boiler has any pressure built up on it. The best time to follow up on handhole gaskets is when steam is almost down after first fire-up. It is important to snug them up before boiler cools, because as a boiler cools, it forms a vacuum, and if handholes are loose, they can collapse and drain your boiler.

c) If a handhole gasket blows out:

1) Close damper. Prepare to steam down. If there is a large fire, be prepared to kill the fire. Depending on how fast the boiler is losing water and where on the boiler the handhole is leaking. Under no circumstance attempt to operate engine! Periodic operation of the injector is recommended to keep water level up until fire-down is complete.

2) Do not attempt to remove handhole plate and gasket until steam is down. Carefully remove handhole plate and gasket. Inspect for cause of blowout.

S2.14.9 TUBE BURST

Tubes will deteriorate and corrode over time. Usually a pit in the tube surface works its way through the tube and a pinhole develops. Rarely will a tube actually "burst". Usually just a small leak occurs. If the leak occurs on firebox end or if leak is a large one, it usually puts the fire out. Leave the engine on a level surface and let it cool down. If the leak is toward the smoke box end of the boiler, water will come out of the smoke box door. Watch water level, close damper and prepare to steam down, or kill the fire if it hasn't died out so already depending on how fast the boiler is losing water. Do not continue to operate the engine.

S2.14.10 LEAKING VALVES

Several situations can cause a leaking valve. The most common would be a piece of scale or debris between valve seat and valve disc/plug. Another reason would be a break between valve stem and disc/plug (on a globe-type valve). Assuming scale on the valve seat, try opening and closing the valve to try and dislodge any debris. If the valve is broken or disc/plug has pulled off the end of the valve stem, there is nothing that can be safely done. Determining when to steam down or kill the fire will depend on the rate which the boiler is losing water. In most cases a normal steam down procedure will be required.

S2.14.11 BROKEN PIPES

Broken pipes on an engine normally will not occur if engine has been piped with proper materials and correct procedures have been followed. Close attention should be paid to pipe and pipe fittings and their condition. However, should a pipe or pipe fitting break, carefully try and locate a up-line valve and isolate the break. Follow normal steam down procedures. If there is no up-line valve that can be shut off, kill the fire immediately.

S2.14.12 SAFETY VALVE PROBLEMS

Testing of this critical safety device should be done each time the boiler is fired up. This is essential to ensure its continued safe operation. In the event the safety valve does not open at its preset pressure and trying to manually trip open valve lever is unsuccessful, close the damper and follow steam-down procedure. After closing damper, start the injector. This will decrease the steam pressure. Under no circumstance should the blowdown valve be used to release pressure (blowing down will lower the water level considerably). Killing the fire should not be necessary provided the water level is at a safe level and the steam pressure is dropping from running the injector. Do not continue to run engine; remove the valve and send to a certified shop for repair or replace the valve.

S2.14.13 SAFETY VALVE OPENS BUT WILL NOT CLOSE

This problem is more prevalent than valves that don't open. There is no immediate danger in a safety valve that won't close; the boiler is only losing steam. Try to manually open the valve a few times under pressure. This may seat the valve. Bringing your steam pressure down by approximately 25 psi (170 kPa) will let the valve seat. If after dropping the pressure and it still does not seat, there may be an obstruction in the valve or a binding in the action of the valve. Follow normal steam-down procedure. Remove valve and send to a certified shop for repairs or replace the valve.

S2.14.14 LEAKING PIPE PLUGS

Usually threads were not properly cleaned before installation or thread tape/sealant was not properly applied. Under no circumstance should plugs be tightened with boiler under pressure. Usually the leak is very small and does not mean any immediate danger. Follow normal steam-down procedure.

S2.14.15 MELTED GRATES

a) Closing damper with a hot coal fire restricts air flow to the grates. Although it is rare for a grate to melt from this, it is possible to warp or ruin a good set of grates. Grates need air flow to keep them cool. Closing damper all the way with a hot coal fire should only be done in an emergency.

b) Carrying ashes too high in ash pan is usually the reason for melted grates. The hot coals in the ash pan touching the grates and the restricted air flow is going to damage the grates. In some cases a grate bar can entirely melt out leaving a huge hole in your fire bed and an intense fire burning in your ash pan. Follow normal steam-down procedure.

S2.15 TABLES AND FIGURES

a) TABLE S2.8.1, Minimum Pounds of Steam per hour per Square Foot of Heating Surfaces

b) TABLE S2.10.2, Sizes for Rivets Based on Plate Thickness

c) TABLE S2.10.3.1, Maximum Allowable Working Pressure for Cylindrical Components – Single-Riveted Lap Joint

d) TABLE S2.10.3.2, Maximum Allowable Working Pressure for Cylindrical Components – Double-Riveted Lap Joint

e) TABLE S2.10.3.3, Maximum Allowable Working Pressure for Cylindrical Components – Triple-Riveted Lap Joint

f) TABLE S2.10.3.4, Maximum Allowable Working Pressure for Cylindrical Components – Buttstrap Double- Riveted Lap Joint

g) TABLE S2.10.3.5, Maximum Allowable Working Pressure for Cylindrical Components – Buttstrap Triple-Riveted Lap Joint

h) TABLE S2.10.3.6, Maximum Allowable Working Pressure for Cylindrical Components – Buttstrap Quadruple-Riveted Lap Joint

i) TABLE S2.10.4, Maximum Allowable Working Pressure for Stayed Surfaces

j) TABLE S2.10.4.1, Maximum Allowable Working Pressure Based on Load Capacity of a Single-Riveted Staybolt

The National Board of Boiler and Pressure Vessel Inspectors
INITIAL BOILER CERTIFICATION REPORT (Form C-1)

BOILER INFORMATION	
JURISDICTION NO.	Owner
MANUFACTURER	Owner ADDRESS
YEAR BUILT	Owner CITY/STATE
BOILER TYPE	USER
ENGINE NO.	USER ADDRESS
OTHER NO.	USER CITY/STATE
HEATING SURFACE	OPERATOR & LICENSE NO.

BARREL INFORMATION	
INSIDE DIAMETER	SEAM TYPE
TUBE SIZE/NUMBER	SEAM EFFICIENCY (from Table S2.10.3)
TENSILE STRENGTH OF SHELL	MAXIMUM PITCH OF SEAM RIVETS
MIN. THICKNESS OF SHELL	JACKET FULLY REMOVED FOR INSPECTION
MIN. THICKNESS OF TUBESHEET	MAWP OF BARREL (from Table S2.10.3)

FIREBOX AND WRAPPER SHEET
STAYBOLT DIAMETER (Base of Threads) OF THINNEST STAYBOLT
STAYBOLT PITCH (Max) AT CROWNSHEET
TYPE OF STAYBOLT (Telltale?)
MINIMUM THICKNESS OF STAYED SURFACE
MAWP OF STAYED SURFACES (from Table S2.10.4.1)
TYPE OF BOTTOM (Ogee, Wet Bottom, etc.)
CONDITION OF THREADED MOUNTING STUDS
GRATES, GRATE SUPPORTS, DAMPERS, ASHPAN — SATISFACTORY?
CLEANED FOR INSPECTION?

SAFETY EQUIPMENT AND CONTROLS				
SAFETY VALVE (per S2.8.1)	MANUFACTURER	SET PRESSURE	CAPACITY	SIZE
FUSIBLE PLUG (per S2.8.4)	NEW “ASME” PLUG	OLD PLUG REMOVED FOR CROWN INSPECTION?		
FEED METHODS	INJECTOR(S) BRAND/SIZE	PUMP TYPE	PREHEATER TYPE	
WATER COLUMN		DRAIN	WATER LEVEL VERIFIED?	
GAGE GLASS (per S2.8.2)		GUARD	TYPE	
TRY-COCKS (per S2.8.3)		NUMBER	OPERABLE?	
PRESSURE GAGE (per S2.8.5)		DIAL RANGE	SIPHON TYPE	

INITIAL BOILER CERTIFICATION REPORT (Form C-1) *continued*

VALVES AND PIPING (per S2.9 and S2.9.1)	
MAIN STEAM (dome) VALVE	MAIN STEAM PIPING
THROTTLE VALVE	PIPE NIPPLES AT SHELL
FEEDLINE STOP VALVE(s)	FEEDLINE CHECK VALVES
FEEDWATER PIPING TO INJECTORS & PIPING	BLOWDOWN PIPING
STEAM PIPING TO INJECTORS & PIPING	BLOWDOWN VALVES
INJECTOR ISOLATION (steam & water) VALVES	PIPING SUPPORTS
BLOWER VALVE	BLOWER PIPING

EXISTING REPAIRS AND ALTERATIONS

EXTERNAL VISUAL INSPECTION FINDINGS

INTERNAL VISUAL INSPECTION FINDINGS

MAWP CALCULATIONS USING ULTRASONIC THICKNESS MEASUREMENTS	
BARREL: P = (TS x Tmin x E)/(R X FS) [per Table S2.10.3]	FIREBOX: P = (T^2 x S x C/Pitch Max^2) [per Table S2.10.4]
HYDROSTATIC PRESSURE TEST (per S2.6.1)	
TEST PRESSURE — PSI	TEST TEMPERATURE — °F
TEST DATE	TEST PROBLEMS

(Page 2)

INITIAL BOILER CERTIFICATION REPORT (Form C-1) *continued*

OPERATING INSPECTION AT PRESSURE	
ABSENCE OF LEAKS	TEST OF INJECTOR(S) & PUMP (if used)
TEST OF TRY-COCKS	OPERATION OF THROTTLE & GOVERNOR
TEST OF BLOWDOWN VALVE	TEST OF SAFETY VALVE(S)
	VALVE POPPING POINT & BLOWDOWN

NOTES

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This form may be obtained from The National Board of Boiler and Pressure Vessel Inspectors, 1055 Crupper Ave., Columbus, OH 43229 NB-405 Rev. 0

SUPPLEMENT 3
INSPECTION OF GRAPHITE PRESSURE EQUIPMENT

S3.1 SCOPE

a) The purpose of this supplement is to provide requirements for inservice inspection of pressure equipment manufactured from impervious graphite materials.

b) The impervious graphite (carbon, graphite, or graphite compound) used for the construction of graphite pressure vessels is a composite material, consisting of “raw” carbon or graphite that is impregnated with a resin using a tightly controlled pressure/heat cycle(s). The interaction between the raw material and the resin is the determining factor when considering the design characteristics of the material. The design characteristics include the strengths (flexural, compressive, and tensile), permeability, co-efficient of thermal expansion, thermal conductivity, and ultimately, the safe operating life of the vessel.

c) The process used in the manufacturing of the raw material is well documented. The expertise developed in this field allows for many different grades to be manufactured to meet the specific needs of various industries, including corrosive chemical-processing pressure vessels. In the chemical processing industry the properties of the raw material are dictated by the manufacturer of the impregnated material, based on the pressure/temperature cycle and the type of resin used for impregnation. The raw material requirements are defined and communicated to the manufacturer of the raw material. The cycle and resin type may vary from manufacturer to manufacturer, and also for each “grade” of impregnated material a manufacturer produces.

d) After over a century of experience with graphite pressure equipment, the essential variables of the process have been defined and apply universally to all manufacturers of impervious graphite equipment. Therefore, by requiring the essential variables of the resin impregnation cycle to be identified and verified, it is possible to assign a “lot” number to all certified materials at completion of the resin impregnation process. This can be done with the assurance of meaningful and consistent test results.

S3.2 APPLICATION

Due to inherent resistance to chemical attack, graphite pressure equipment is often used in corrosive applications, which may include lethal service.

S3.3 OPERATIONS

The owner should maintain controlled conditions for use of graphite pressure equipment, including the use of temperature and pressure recorders and/or operating logs. The owner should maintain operating procedures, and ensure that pressure and temperature are controlled. A thermal or pressure spike may damage the graphite or metal components.

S3.4 INSERVICE INSPECTION

a) The guidelines provided in NBIC Part 2, Section 1 shall apply to graphite pressure equipment, except as modified herein.

b) Graphite pressure vessels, pressure parts, and vessel components should receive an external visual examination biennially. All accessible surfaces should be chemically cleaned. Cleaning fluids containing strong oxidants should not be used.

c) Typical indicators that should necessitate graphite pressure equipment inspection, evaluation, and repair include:

1) Cross-contamination of either process or service fluids;

2) Obeservation of external leaking;

3) Observation of reduced rate or excessive pressure drop; and

4) Reduction of heat-transfer performance.

d) Cracks, bulges, blisters, delaminations, spalling conditions, and excessive erosion are cause for repair or replacement. Any surface discoloration should be recleaned and examined more closely to determine if a delamination or spalling condition exists.

e) Other typical discontinuities include chipping, erosion, baffle cutting due to vibration, and cement deterioration. All passageways are susceptible to fouling.

SUPPLEMENT 4
INSPECTION OF FIBER-REINFORCED THERMOSETTING PLASTIC PRESSURE EQUIPMENT

S4.1 SCOPE

This supplement provides specific guidelines for inspection of fiber-reinforced thermosetting plastic pressure equipment.

S4.2 INSERVICE INSPECTION

NBIC Part 1, Section 1, shall apply to inspection of fiber-reinforced plastic (FRP) equipment, except as modified herein. This supplement covers vessels and tanks only and was not written to cover piping and ductwork, although some of the information contained herein may be used for the inspection of piping and ductwork.

S4.3 GENERAL

a) Typical FRP equipment consists of the structural laminate (pressure-retaining material) and a liner (corrosion barrier) to protect the structural laminate (see NBIC Part 2, Figure S4.3). The structural laminate is defined as one or more layers of reinforced resin material bonded together. In addition to damage from mechanical sources, FRP material may be susceptible to damage from acids, alkalis, compounds containing fluorine, solvents, and hot, clean water.

b) For equipment fabricated with a liner, the primary purpose of a process side inspection is to ensure the integrity of the liner to prevent chemical attack and degradation of the structural laminate. For equipment fabricated without a liner, the purpose of a process side inspection is to determine the condition of the structural laminate.

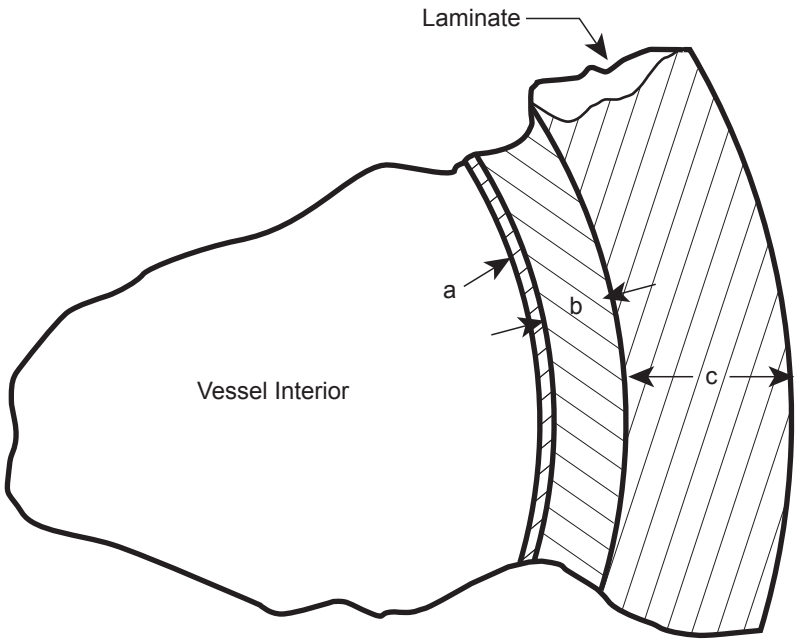
c) In addition to chemical attack, the laminate is also susceptible to damage from:

    1) Excessive service temperatures;

    2) Mechanical or service abuse; and

    3) Ultraviolet light (See NBIC Part 2, S4.7.2).

FIGURE S4.3
TYPICAL VESSEL SHELL



a	= innermost layer
b	= interior layer
c	= structural laminate
a + b	= corrosion barrier (liner)

S4.4 VISUAL EXAMINATION

a) Exposed surfaces shall be visually examined for defects and mechanical or environmental damage in the liner or the laminate. Classification and acceptance of any defects in the liner or laminate shall be according to NBIC Part 3, Table S4.12.

b) Defects to look for include:

1) Cracks;

2) Separation of secondary edges;

3) Leaks, especially around nozzles

4) Discolored areas;

5) Areas of mechanical damage, such as impacts or gouges;

6) Surface deterioration; fiber exposure;

7) Cracked or broken attachments;

8) Damage due to dynamic loading;

9) Defective supports;

10) Delaminations; and

11) Blisters.

S4.5 INSPECTOR QUALIFICATIONS

The "R" Stamp Holder's Inspector shall have the following qualifications:

a) No fewer than five years of current verifiable documented experience in an occupational function that has a direct relationship to reinforced thermoplastic (RTP) fabrication and inspection, following customer or national standards, and be directly involved in the following activities:

1) The development of plans, drawings, procedures, inspection requirements, acceptance criteria, and personnel qualification requirements;

2) Fabrication, construction, and supervision of personnel in the production of assemblies or subassemblies;

3) Detection and measurement of nonconformities by application of visual or other nondestructive evaluation processes to written procedures;

4) Supervision of personnel engaged in material and component examination;

5) Repairs of equipment or supervision of personnel performing repairs;

6) Preparation of written procedures for assembly, acceptance, nondestructive evaluation, or destructive tests;

7) Qualification of secondary bonders, laminators, and welders to applicable codes, standards, or specifications;

8) Operation techniques or activities used to fulfill quality control requirements for RTP fabrication or assembly; and

9) Train the occupational skills of fabrication or assembly of RTP equipment.

b) The Inspector shall meet the following visual and educational requirements:

1) Ability to read a Jaeger Type No. 1 standard chart at a distance of not less than 12 inches (305 mm);

2) Capability of distinguishing and differentiating contrast between colors;

3) Visual acuity which must be checked annually to ensure natural or corrected near distance vision; and

4) High school graduate or holder of a state- or military-approved high school equivalency diploma.

c) The employer of the Inspector shall certify that the employee complies with the above qualification requirements.

S4.6 ASSESSMENT OF INSTALLATION

An observation shall be made of the condition of the complete installation.

S4.6.1 PREPARATION

An observation shall be made of the condition of the complete installation, including maintenance and operation, as a guide in forming an opinion of the care the equipment receives. The history of the equipment shall be established, and shall include: date built, service history, maintenance, and a review of previous inspection records. Process conditions shall be reviewed to identify areas most likely to be attacked. Surface cleaning procedures and requirements shall also be reviewed.

S4.6.2 LEAKAGE

Any leak shall be thoroughly investigated and corrective action initiated. Repairs shall be in accordance with NBIC Part 3, Supplement 4, *Repair and Alteration of Fiber-Reinforced Thermosetting Plastic Pressure Equipment*.

S4.6.3 TOOLS

The following tools may be required by the inspector:

a) Adequate lighting, including overall lighting and a portable lamp for close inspections;

b) Handheld magnifying glass;

c) Barcol hardness tester;

d) Small pick or pen knife;

e) Small quantity of acetone and cotton swabs;

f) Camera with flash capability; and

g) Liquid penetrant testing kit.

S4.7 EXTERNAL INSPECTION

An external inspection is performed to determine if FRP pressure equipment is in a condition to operate safely.

S4.7.1 INSULATION OR OTHER COVERINGS

It is not necessary to remove insulation and corrosion resistant covers for examination of the pressure equipment, if the coverings show no sign of mechanical impact, gouging, scratching, leaks, etc., and there is no reason to suspect any unsafe condition behind them. Where insulation coverings are impervious, such as a sealed fiberglass jacket, it is recommended that weep or drain holes be installed at the bottom of the insulation jacket as a means to detect leakage.

S4.7.2 EXPOSED SURFACES

a) Exposed surfaces of pressure equipment are subject to mechanical, thermal, and environmental damage. Exposed surfaces may show damage from impact, gouging, abrasion, scratching, temperature excursions, etc. Sunlit areas may be degraded by ultraviolet light with a resulting change in surface color and increased fiber prominence, but with no loss in physical properties. Overheating may also cause a change in color.

b) The location of external damage should be noted so that the opposing internal surface at that location can be examined. For example, an impact load applied to the outer surface may be transmitted through the laminate, causing a star crack in the inner surface. See NBIC Part 2, Figure S4.7.2.

c) Areas that should be closely examined are:

1) Nozzle attachments;

2) Gusset attachments;

3) Flanges;

4) Secondary joints;

5) Hold-down lugs;

6) Lifting lugs; and

7) Attachments.

S4.7.3 STRUCTURAL ATTACHMENTS

a) Attachments of legs, saddles, skirts, or other components shall be examined for cracks where the component attaches to or contacts the vessel and the component itself. See NBIC Part 2, Figure S4.7.3-a.

b) Piping loads on nozzles may be excessive; therefore, all nozzles shall be closely examined for cracks as shown in NBIC Part 2, Figures S4.7.3-b and S4.7.3-c.

S4.8 INTERNAL INSPECTION

An internal inspection is performed to determine the condition of internal surfaces and the pressure integrity of the item.

S4.8.1 GENERAL

FRP surfaces shall be dry and clean for the inspection. Every effort shall be made to minimize damage to the liner during inspection. Defects to look for include:

a) Indentations;

b) Cracks;

c) Porosity;

d) Exposed fibers;

e) Lack of resin;

f) Delaminations;

g) Thinning at points of fluid impingement;

h) Blisters;

i) Scratches;

j) Gouges; and

k) Discolorations.

S4.8.2 SPECIFIC AREAS OF CONCERN

All surfaces shall be examined with both direct and oblique illumination. Color differences, opacity, stains, wetness, roughness, or any deviation from the original surface (original cutout sample) condition shall be noted and investigated. Liquid level lines shall be defined so the laminate condition in both the wet and dry zones can be determined. The following areas should be closely examined for cracks, porosity, or chemical attacks on the liner or laminate:

a) Fittings;

b) Changes in shape;

c) Baffles;

d) Secondary overlays;

e) Nozzles;

f) Cut edges; and

g) Supports/internal structures and areas of attachment.

S4.9 INSPECTION FREQUENCY

Frequency of inspections is established to determine how often inspections shall be performed to ensure safe operation of FRP equipment.

S4.9.1 NEWLY INSTALLED EQUIPMENT

a) The following factors should be considered when determining the frequency of inspection of FRP equipment that is new and recently placed into service.

   1) The distance between the FRP equipment and personnel or critical equipment;

   2) Substance contained in the vessel is of such a nature that if abruptly released it could threaten the health or safety of personnel;

   3) Contains chemicals or is subject to conditions known to degrade or shorten the life of FRP laminates;

   4) Past experience has shown that the service application warrants more frequent internal and external inspections; and

   5) Insurance or jurisdictional requirements.

b) FRP equipment should be externally inspected:

   1) Once every 2 to 3 years after introduction of process fluid. All findings are to be documented in the equipment inspection file for comparison to future inspection;

   2) If upsets outside the vessel design conditions in the process occur, external inspections shall be performed to ensure equipment integrity; or

   3) If prior experience (i.e., if equipment was recently replaced using same material/construction) dictates that inspection frequency other than that listed is acceptable (through previous inspections and records), then the inspection frequency may be altered.

c) FRP equipment should be internally inspected:

1) One year after the introduction of process fluid to establish any changes due to service and chemical environment;

2) After the initial first-year inspection, subsequent inspections are to be established based on those results. Subsequent inspection intervals shall be documented. It is suggested to document inspections using photographs;

3) When some conditions may exist where entry is prohibited and alternate means of inspection considered;

4) If prior experience (i.e., if equipment was recently replaced using same material/construction) dictates that inspection frequency other than that documented is acceptable, then the inspection frequency may be altered; or

5) If upsets outside the vessel design conditions in the process occur, internal inspections shall be performed to ensure equipment integrity.

S4.9.2 PREVIOUSLY REPAIRED OR ALTERED EQUIPMENT

a) The following factors should be considered when determining the frequency of inspection for FRP equipment.

1) The distance between the FRP equipment and personnel or critical equipment;

2) Substance contained in the vessel is of such a nature that if abruptly released it could threaten the health or safety of personnel;

3) Equipment contains chemicals or is subject to conditions known to degrade or shorten the life of FRP laminates;

4) Past experience has shown that the service application warrants more frequent internal and external inspections; and

5) Insurance or jurisdictional requirements.

b) FRP equipment should be externally inspected:

1) Annually — all findings are to be documented in the equipment inspection file for comparison to future inspection;

2) If upsets outside the vessel design conditions in the process occur, external inspections need be performed to ensure equipment integrity; or

3) If prior experience (i.e., if equipment was recently replaced using same material/construction) dictates that inspection frequency other than that listed is acceptable (through previous inspections and records), then the inspection frequency may be altered.

c) FRP equipment should be internally inspected:

1) One year after the introduction of process fluid to establish any changes due to service and chemical environment;

2) If upsets outside the vessel design conditions in the process occur, internal inspections need be performed to ensure equipment integrity;

3) Following the initial first-year inspection, subsequent inspections are to be established based on those documented results and the results documented. It is suggested to document the interior inspection using photographs;

4) If prior experience (i.e., if equipment was recently replaced using same material/construction) dictates that inspection frequency other than that listed is acceptable (through previous inspections and records), then the inspection frequency may be altered; or

5) Some conditions may exist where entry is prohibited and alternate means of inspection must be considered.

S4.10 PHOTOGRAPHS OF TYPICAL CONDITIONS

The figures listed in S4.11 contain photographs of typical conditions that may exist in inservice FRP vessels and piping. These surface conditions can be similar to or different from those encountered in practice. Also, differing causes of surface degradation can result in similar surface appearances.

Note: NBIC Part 2, Figures S4.7.2, S4.7.3-a, S4.7.3-b, and S4.10-j through S4.10-r, were reprinted with permission of the Copyright Owner, © MATERIALS TECHNOLOGY INSTITUTE, INC. (2002). The captions of the figures were revised by the NBIC Committee.

FIGURE S4.7.2

STAR CRACK IN CORRODED LINER. POSSIBLE CAUSE IS EXTERNAL IMPACT.

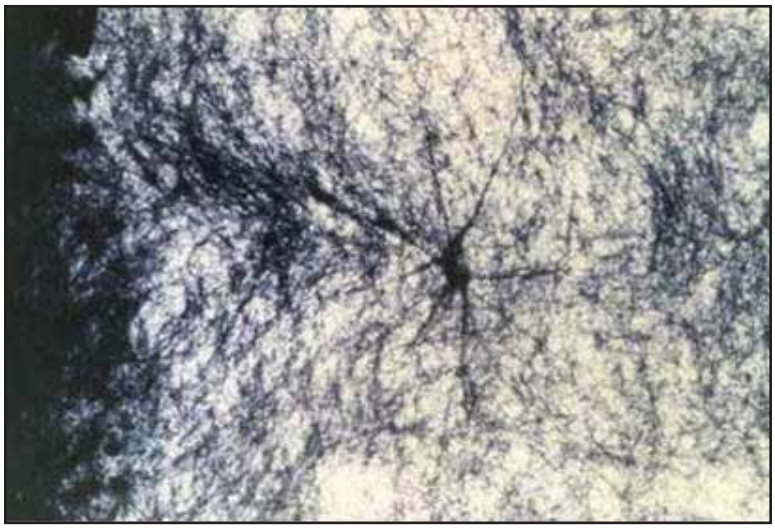


FIGURE S4.7.3-a

GUSSET CRACK. POSSIBLE CAUSES ARE EXCESSIVE LOAD DUE TO UNSUPPORTED VALVE, PIPE, OR OVERSTRESS AND AGE.



FIGURE S4.7.3-b

CRACKED FLANGE. POSSIBLE CAUSES ARE INCORRECT MATCH-UP OF FLANGES, OVER-TORQUE OF BOLTS AT FIT-UP, MANUFACTURING DEFECT, OR EXCESSIVE PIPING LOADS.



FIGURE S4.7.3-c

CRACKED FLANGE. POSSIBLE CAUSE IS BOLTING DISSIMILAR FLANGES TOGETHER (FULL-FACED FLANGE WITH RAISED-FACE FLANGE).



FIGURE S4.10-a

EXCESSIVE HEAT. POSSIBLE CAUSES ARE LOCALIZED HIGH-TEMPERATURE EXCURSIONS.



FIGURE S4.10-b

LAMINATE VOIDS AT OVERLAYS.

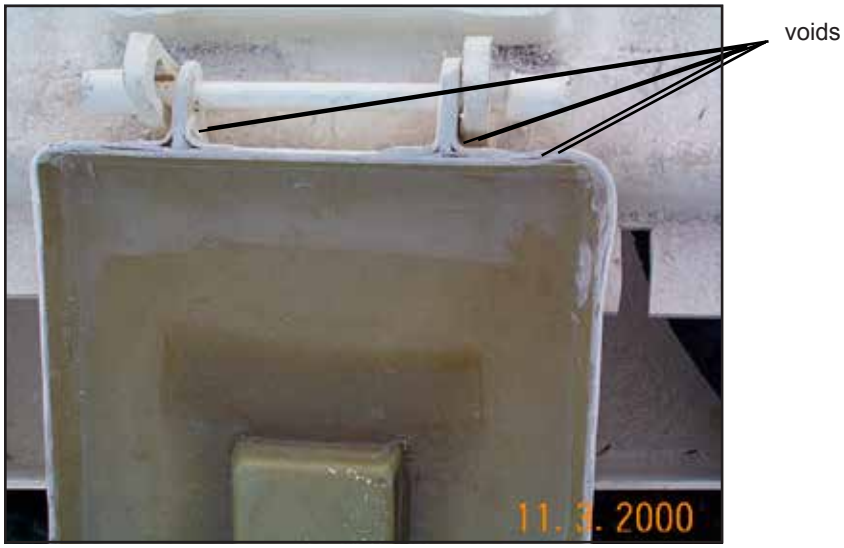


FIGURE S4.10-c

SURFACE DETERIORATIONS. POSSIBLE CAUSES ARE EXPOSURE TO HOT WATER AND/OR STEAM AND CHEMICAL ATTACK.



FIGURE S4.10-d

BLISTERS. POSSIBLE CAUSE IS EXPOSURE TO STEAM OR PURIFIED HOT WATER.



FIGURE S4.10-e

SURFACE EROSION. POSSIBLE CAUSES ARE HIGH FLOW RATE OF FLUIDS, EROSION DUE TO PARTICULATES IN FLUID, AND CHEMICAL ATTACK/SOFTENING OF RESIN.

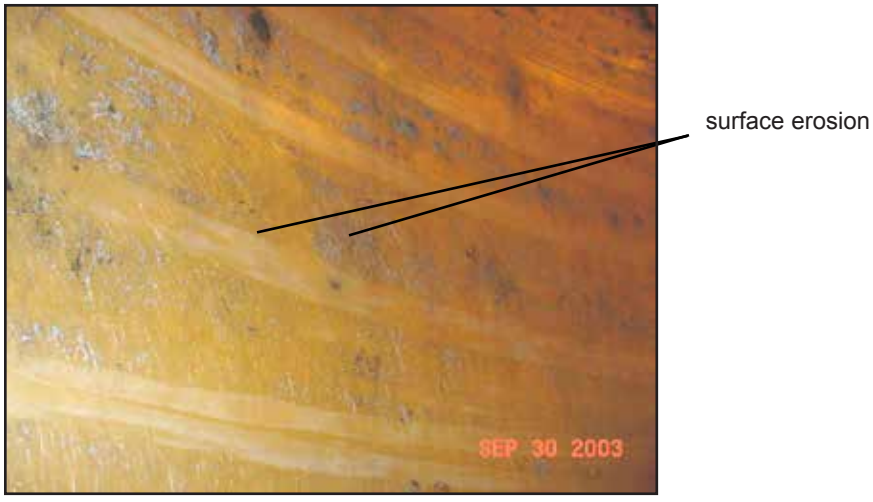


FIGURE S4.10-f
CORROSION/EROSION.



FIGURE S4.10-g
CRACKS. POSSIBLE CAUSE IS IMPACT FROM AN EXTERNAL SOURCE.



FIGURE S4.10-h

CORROSION (LOSS OF VEIL).

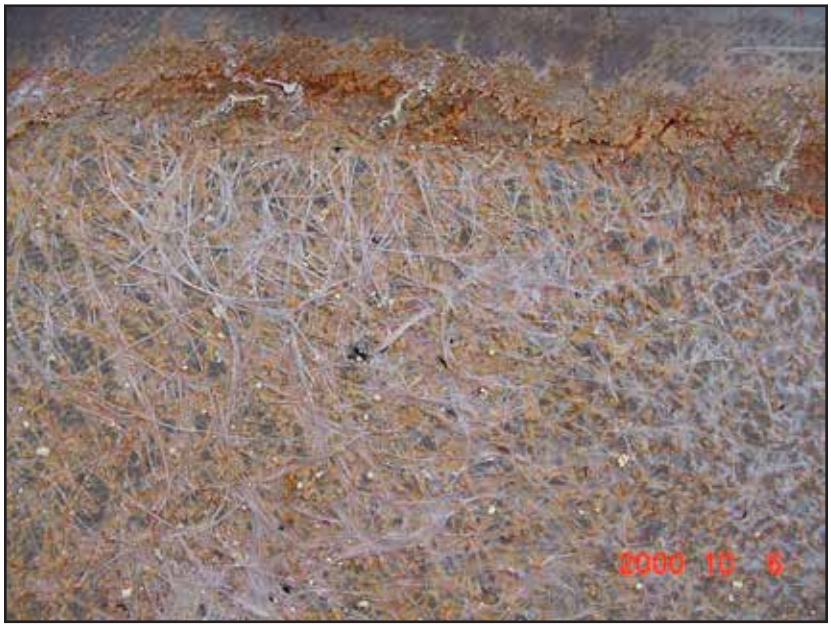


FIGURE S4.10-i

SHELL FRACTURE. POSSIBLE CAUSE IS EXTERIOR IMPACT.



FIGURE S4.10-j
CONCENTRATED SULFURIC ACID ATTACK.



FIGURE S4.10-k
BLISTER.

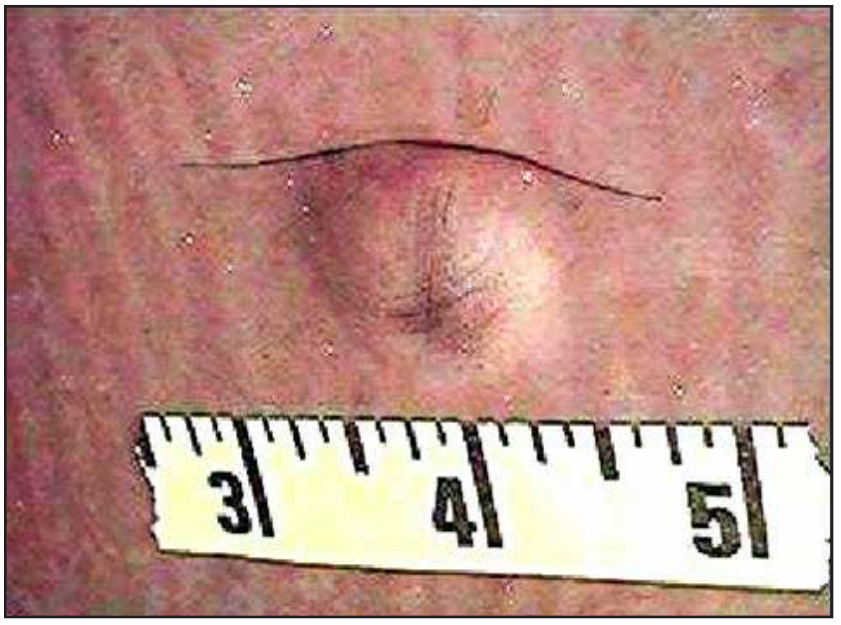


FIGURE S4.10-l

FIBER PROMINENCE. POSSIBLE CAUSE IS EXPOSURE TO SUNLIGHT AND NO UV PROTECTION.

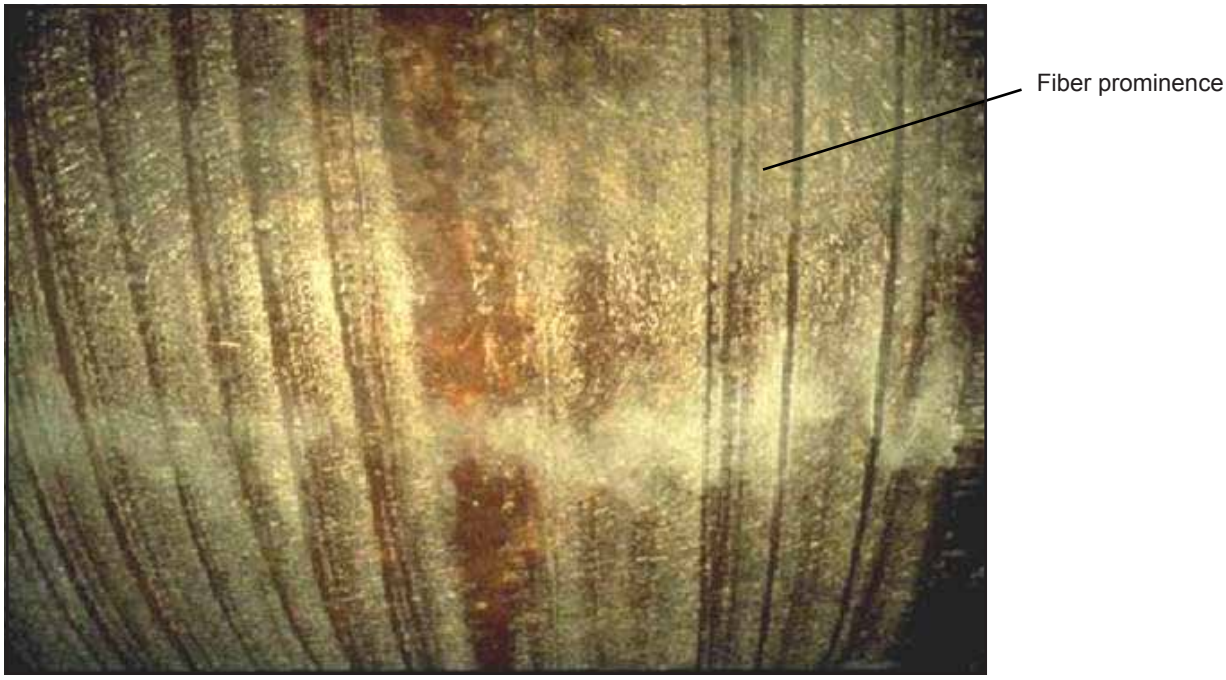


FIGURE S4.10-m

COLOR CHANGE.

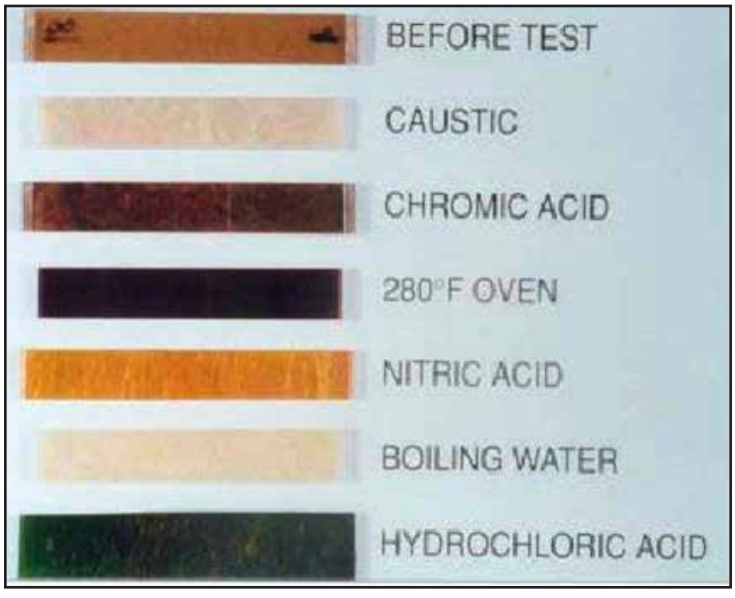


FIGURE S4.10-n

CUT EDGE EVALUATION.

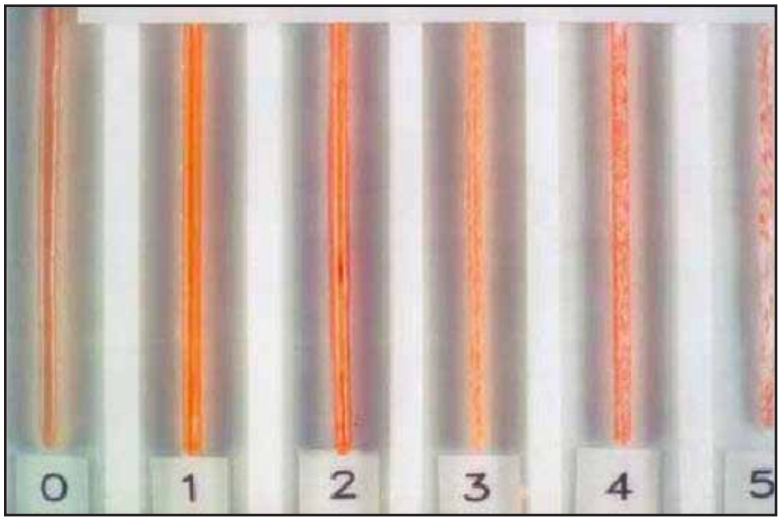


FIGURE S4.10-o

EROSION IN THE LINER.



FIGURE S4.10-p
GOUGE. POSSIBLE CAUSE IS MECHANICAL DAMAGE.



FIGURE S4.10-q
CRACKS AT THE KNUCKLE. POSSIBLE CAUSE IS INADEQUATE ANCHORING OF VESSEL.



FIGURE S4.10-r
SULFURIC ACID ATTACK AND THERMAL SHOCK.

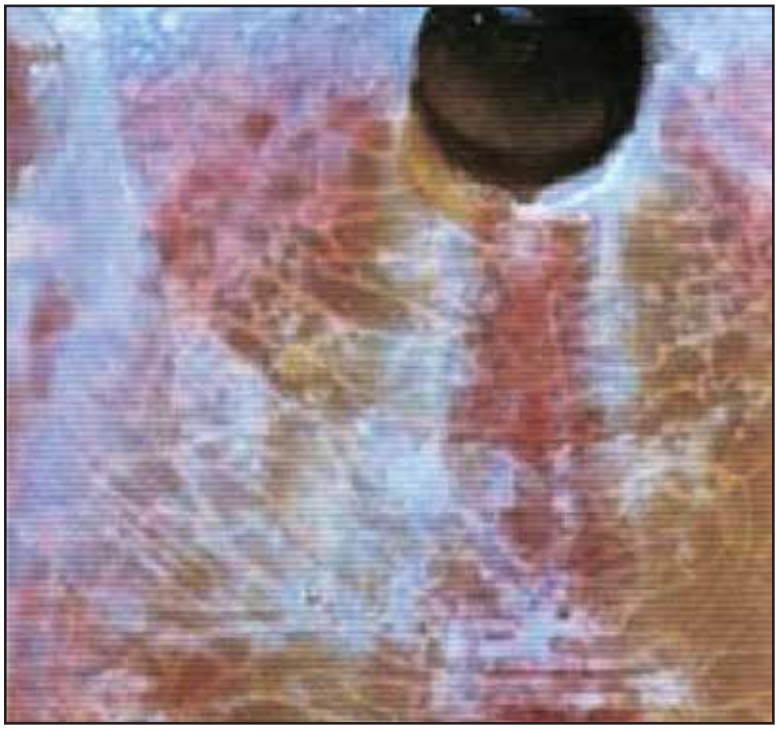


FIGURE S4.10-s
AIR BUBBLES BEHIND THE VEIL (SHOWN AFTER CHEMICAL EXPOSURE).

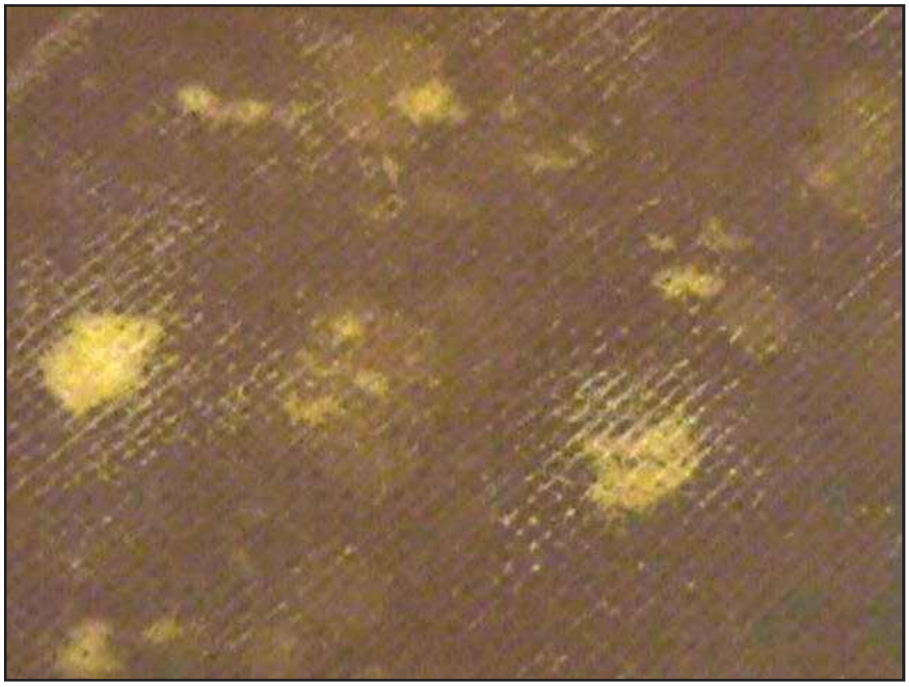


FIGURE S4.10-t

DELAMINATIONS AND BLISTERS. POSSIBLE CAUSES ARE EXPOSURE TO HIGH HEAT OR IMPROPER SURFACE PREPARATION OF LINER PRIOR TO STRUCTURAL APPLICATION.



FIGURE S4.10-u

FLANGE CRACKING.



FIGURE S4.10-v

ELASTOMERIC GASKET EXTRUDING. POSSIBLE CAUSES ARE EXCESSIVE BOLT TORQUE OR IMPROPER BOLTING SEQUENCE.



FIGURE S4.10-w

INCORRECT GUSSET ATTACHMENT. POSSIBLE CAUSES ARE GUSSETS NOT EXTENDING OUT FROM FLANGE A MINIMUM OF 30° FROM THE AXIS OF NOZZLE NECK, OR GUSSET ATTACHMENTS USED AS PART OF THE FLANGE THICKNESS.

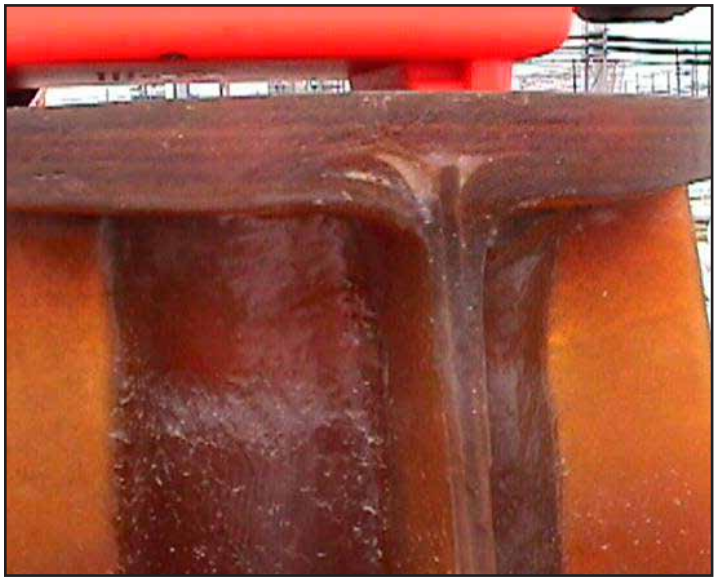


FIGURE S4.10-x
STAR CRACK. POSSIBLE CAUSE IS EXTERNAL IMPACT.

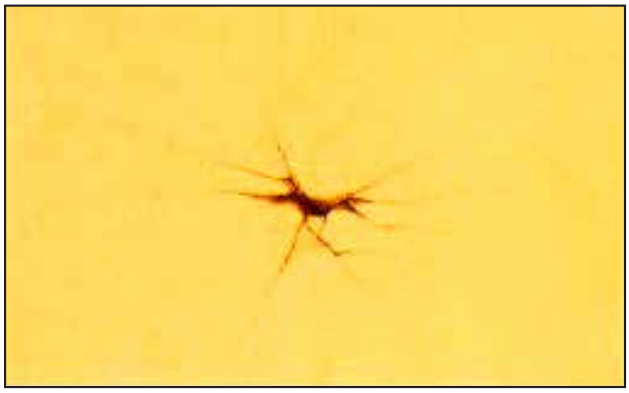


FIGURE S4.10-y
EXCESSIVE USE OF PUTTY.



S4.11 TABLES AND FIGURES

a) FIGURE S4.3, Typical vessel shell

b) FIGURE S4.7.2 , Star crack in corroded liner

c) FIGURE S4.7.3-a, Gusset crack

d) FIGURE S4.7.3-b, Cracked flange

e) FIGURE S4.7.3-c ,Cracked flange

f) FIGURE S4.10-a, Excessive heat

g) FIGURE S4.10-b, Laminate voids at overlays

h) FIGURE S4.10-c, surfaces deteriorations

i) FIGURE S4.10-d, Blisters

j) FIGURE S4.10-e, Surface corrosion

k) FIGURE S4.10-f, Corrosion/erosion

l) FIGURE S4.10-g, Cracks

m) FIGURE S4.10-h, Corrosion (loss of veil)

n) FIGURE S4.10-i, Shell fracture

o) FIGURE S4.10-j, Concentrated sulfuric acid attack

p) FIGURE S4.10-k, Blister

q) FIGURE S4.10-l, Fiber prominence

r) FIGURE S4.10-m, Color change

s) FIGURE S4.10-n, Cut edge evaluation

t) FIGURE S4.10-o, Erosion in liner

u) FIGURE S4.10-p, Gouge

v) FIGURE S4.10-q, Cracks at the knuckle

w) FIGURE S4.10-r, Sulfuric acid attack and thermal shock

x) FIGURE S4.10-s, Air bubbles behind the veil

y) FIGURE S4.10-t, Delaminations and blisters

z) FIGURE S4.10-u, Flange cracking

aa) FIGURE S4.10-v, Elastomeric gasket extruding

ab) FIGURE S4.10-w, Incorrect gusset attachment

ac) FIGURE S4.10-x, Star crack

ad) FIGURE S4.10-y, Excessive use of putty

SUPPLEMENT 5
INSPECTION OF YANKEE DRYERS (ROTATING CAST-IRON PRESSURE VESSELS) WITH FINISHED SHELL OUTER SURFACES

S5.1 SCOPE

a) This supplement describes guidelines for the inservice inspection of a Yankee dryer. A Yankee dryer is a rotating steam-pressurized cylindrical vessel commonly used in the paper industry, and is made of cast iron, finished to a high surface quality, and characterized by a center shaft connecting the heads.

b) Yankee dryers are primarily used in the production of tissue-type paper products. When used to produce machine-glazed (MG) paper, the dryer is termed an MG cylinder. A wet paper web is pressed onto the finished dryer surface using one or two pressure (pressing) rolls. Paper is dried through a combination of mechanical dewatering by the pressure roll(s); thermal drying by the pressurized Yankee dryer; and a steam-heated or fuel-fired hood. After drying, the paper web is removed from the dryer.

c) The dryer is typically manufactured in a range of outside diameters from 8 to 23 ft. (2.4 m to 7 m), widths from 8 to 28 ft. (2.4 m to 8.5 m), pressurized and heated with steam up to 160 psi (1,100 kPa), and rotated at speeds up to 7,000 ft./min (2,135 m/min). Typical pressure roll loads against the Yankee dryer are up to 600 pounds per linear inch (105 kN/m). A thermal load results from the drying process due to difference in temperature between internal and external shell surfaces. The dryer has an internal system to remove steam and condensate. These vessels can weigh up to 220 tons (200 tonnes).

d) The typical Yankee dryer is an assembly of several large castings. The shell is normally a gray iron casting, in accordance with ASME designation SA-278. Shells internally may be smooth bore or ribbed. Heads, center shafts, and journals may be gray cast iron, ductile cast iron, or steel.

S5.2 ASSESSMENT OF INSTALLATION

a) The Inspector verifies that the owner or user is properly controlling the operating conditions of the dryer. The Inspector does this by reviewing the owner's comprehensive assessments of the complete installation, operating environment, maintenance, and operating history.

b) The dryer is subjected to a variety of loads over its life. Some of the loads exist individually, while others are combined. Consideration of all the loads that can exist on a Yankee dryer is required to determine the maximum allowable operating parameters. There are four loads that combine during normal operation to create the maximum operating stresses, usually on the outside surface of the shell at the axial center line. These are:

1) Pressure load due to internal steam pressure;

2) Inertial load due to dryer rotation;

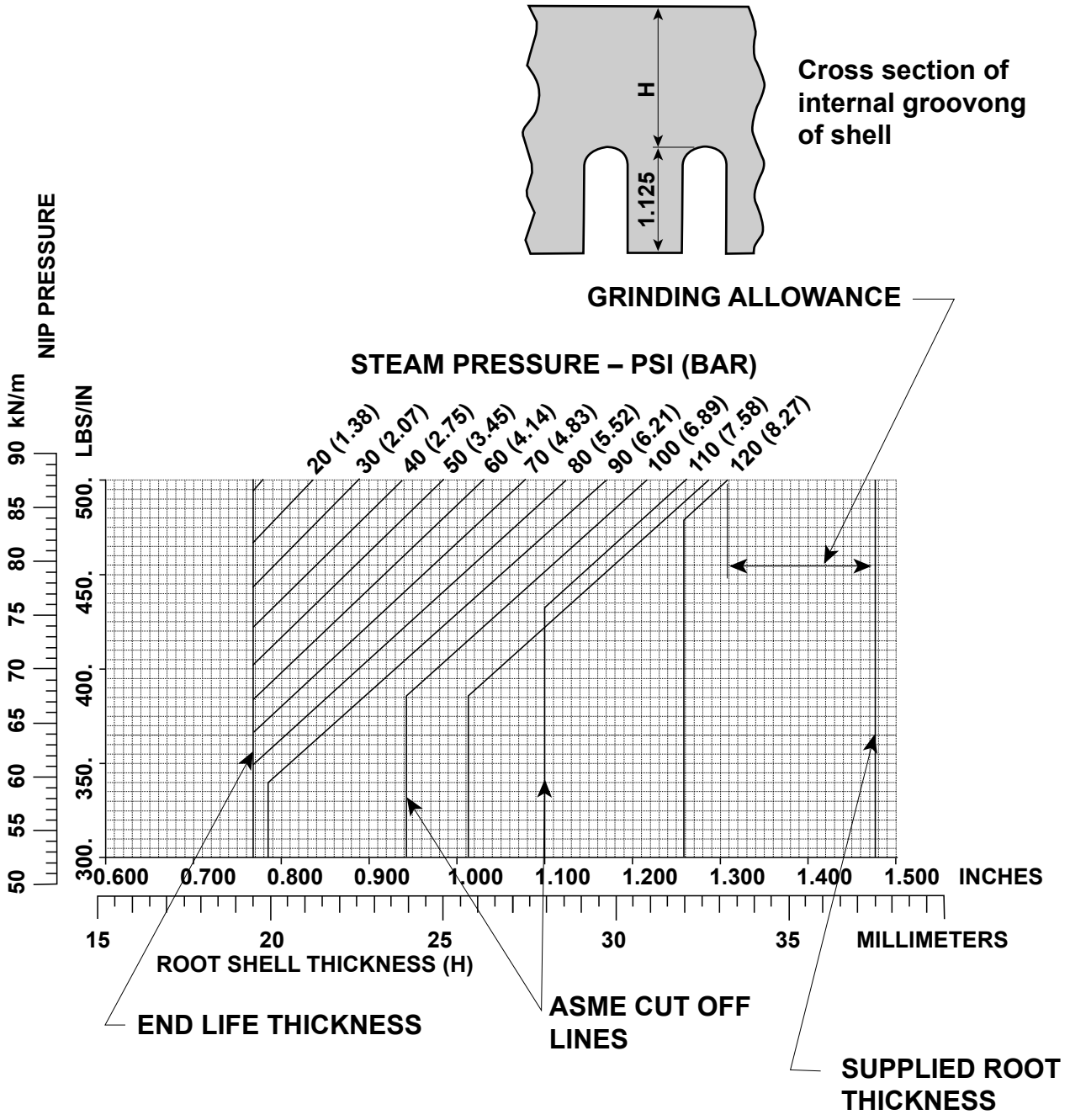
3) Thermal gradient load due to the drying of the web; and

4) Pressure roll load (line or nip load)[5] due to pressing the wet web onto the dryer.

c) Steam pressure, inertial, and thermal gradient loads impose steady-state stresses. These stresses typically change when the dryer shell thickness (effective thickness for ribbed dryers) is reduced to restore a paper-making surface, the grade of tissue is changed or speed of the dryer is changed.

5 Pressure roll load, line load, and nip load are terms that are used interchangeably to refer to the interaction between the pressure roll(s) and the Yankee dryer. It is called "nip" load because the pressure roll is rubber-covered and is pressed up against the Yankee with enough force to create a nip (or pinch) that forces the paper into line contact between the rolls and provides some mechanical dewatering. The paper then sticks onto the Yankee surface and follows the Yankee dryer for thermal dewatering by the steam-heated Yankee surface. This "nip load" is called a "line load" because the units are load (force) per length of line contact. The units are pounds per linear inch (PLI) and kilonewtons per meter (kN/m).

FIGURE S5.2
DE-RATE CURVE



d) The pressure roll(s) load imposes an alternating stress on the shell face. The resulting maximum stress is dependent on the magnitude of the alternating and steady-state stresses.

e) ASME Section VIII, Div. 1, only provides specific requirements for the analysis of pressure loads. Although the code requires analysis of other loads, no specific guidance for thermal, inertial, or pressure roll loads is provided. Hence, additional criteria must be applied by the manufacturer to account for all the steady-state and alternating stresses.

f) To maintain product quality, the dryer surface is periodically refurbished by grinding. This results in shell thickness reduction. Therefore, the manufacturer does not provide a single set of maximum allowable operating parameters relating steam pressure, rotational speed, and pressure roll load for a single design shell thickness. The manufacturer, or another qualified source acceptable to the Inspector, instead provides a series of curves that graphically defines these maximum allowable operating parameters across a range of shell thicknesses. This document is known as the “De-Rate Curve.” See NBIC Part 2, Figure S5.2.

g) In addition to the loads on the dryer due to normal operation, other nonstandard load events can occur. These nonstandard load events should be recorded in an operation or maintenance log. Examples of nonstandard load events include:

1) Excessive thermal load due to local or global heating rate during warm-up;

2) Excessive thermal load due to local or global cooling rate during shut-down;

3) Excessive thermal load due to inappropriate use or malfunctioning auxiliary heating devices causing localized heating;

4) Excessive thermal load due to the misapplication or uncontrolled application of water or other fluids for production, cleaning, or fire fighting; and

5) Impact load.

h) If nonstandard load events have occurred, then the Inspector should ensure that an appropriate assessment of the structural integrity on the dryer has been performed.

S5.2.1 DETERMINATION OF ALLOWABLE OPERATING PARAMETERS

a) A Yankee dryer is designed and intended to have its shell thickness reduced over the life of the vessel through routine wear and grinding. The Yankee dryer shell is ground on the outside surface to restore the quality or shape of the papermaking surface, essential to the manufacturing of tissue or other paper products.

b) Design documentation is required that dictates the maximum allowable operating parameters as shell thickness is reduced. Calculations used to determine those parameters are in accordance with ASME Code requirements for primary membrane stress and design criteria based upon other relevant stress categories; (e.g., fatigue and maximum principal stress). Calculation of these parameters requires that the respective stresses, resulting from the imposed loads, be compared to the appropriate material strength properties. Hence, knowledge of the applied stresses in the shell and the tensile and fatigue properties of the material are essential.

c) Yankee dryers are subjected to a variety of loads that create several categories of stress. Yankee dryers are designed such that the stress of greatest concern typically occurs on the outside surface at the axial centerline of the shell.

1) Steam Pressure Load — The internal steam pressure is one of the principal design loads applied to the Yankee dryer. The steam pressure expands the shell radially, causing a predominately circumferential membrane tensile stress. Because the shell is constrained radially by the heads at either end of the shell, the steam pressure also causes a primary bending stress in the vicinity of the head-to-shell joint. The ends of the shell are in tension on the inside and compression on the outside due to the steam pressure. The steam pressure also causes a bending stress in the heads.

2) Inertia Load — The rotation of the Yankee dryer causes a circumferential membrane stress in the shell similar to that caused by the steam pressure load. This stress is included in the design of the shell and increases with dryer diameter and speed.

3) Thermal Gradient Load — The wet sheet, applied to the shell, causes the outside surface to cool and creates a thermal gradient through the shell wall. This thermal gradient results in the outside surface being in tension and the inside surface in compression. With this cooling, the average shell temperature is less than the head temperature, which creates bending stresses on the ends of the shell and in the heads. The ends of the shell are in tension on the outside and compression on the inside.

   a. Other thermal loading also occurs on a Yankee dryer. The use of full width showers for a variety of papermaking purposes affects the shell similar to a wet sheet. The use of edge sprays produces high bending stress in the ends of the shell due to the mechanical restraint of the heads.

   b. Warm-up, cool-down, hot air impingement from the hood, moisture profiling devices, fire fighting, and wash-up can all produce non-uniform thermal stresses in the pressure-containing parts of the Yankee dryer. Heating or cooling different portions of the Yankee dryer at different rates causes these non-uniform stresses.

4) Line Load — The line load from the contacting pressure roll(s) results in an alternating, high cycle, bending stress in the shell. This stress is greatest at the centerline of the shell. The load of the pressure roll deflects the shell radially inward causing a circumferential compressive stress on the outside surface and a tensile stress on the inside. Because the shell has been deflected inward at the pressure roll nip, it bulges outward about 30 degrees on each side of the nip. The outward bulge causes a tensile stress on the outside shell surface at that location and a corresponding compressive stress on the inside. Since the shell is passing under the pressure roll, its surface is subjected to an alternating load every revolution.

S5.2.2 ADJUSTING THE MAXIMUM ALLOWABLE OPERATING PARAMETERS OF THE YANKEE DRYER DUE TO A REDUCTION IN SHELL THICKNESS FROM GRINDING OR MACHINING

a) The outside surface of the Yankee dryer shell is routinely ground to restore the quality of the papermaking surface. The papermaking surface degrades due to wear, corrosion, and local thinning. As the shell thickness is reduced, the maximum allowable operating parameters are adjusted. Adjustment of the maximum allowable operating parameters requires accurate shell thickness measurements.

b) Over the life of the Yankee dryer, the adjustment of the maximum allowable operating parameters will require that the original design pressure and/or the pressure roll line load be reduced. After the maximum allowable operating parameters are adjusted per the De-rate Curve, the appropriate load limiting devices are reset (e.g., steam safety relief valve, line load limiting device).

S5.2.3 DOCUMENTATION OF SHELL THICKNESS AND ADJUSTED MAXIMUM ALLOWABLE OPERATING PARAMETERS

a) Yankee dryers are designed and intended to have the shell thickness reduced over the life of the vessel as a result of routine wear and grinding. Yankee shell grinding is routinely performed to restore the quality or shape of the papermaking surface.

b) Design documentation, a De-rate Curve, is required, which dictates the maximum allowable operating parameters, based on imposed loads over a range of shell thickness. The documentation shall be obtained from the original dryer manufacturer or from another qualified source acceptable to the Inspector.

c) Yankee dryer shell grinding requires accurate shell thickness measurements in conjunction with the De-rate Curve in order to set load-limiting devices. The resulting shell thickness and maximum allowable operating parameters after grinding shall be documented, and the Inspector notified that load-limiting device settings have changed.

S5.3 CAUSES OF DETERIORATION AND DAMAGE

Three types of deterioration or damage typically encountered in Yankee dryers are local thinning, cracking, and corrosion. Many times, the mechanisms are interrelated, one being the precursor of another.

S5.3.1 LOCAL THINNING

a) Internally, a Local Thin Area (LTA) can occur on the pressure-retaining surfaces due to steam and condensate erosion, mechanical wear and impact, and removal of material flaws. These assume features ranging from broad shallow areas washed out by erosion, to more groove-like flaws, including gouges and indentations from contacting metal parts.

b) Externally, the process is typically one of wear-corrosion in circumferential bands. Except on the shell edges, local thinning never achieves significant depth because the papermaking process will tolerate only the smallest departure from surface contour. On the shell edges, beyond the papermaking surface, wear-corrosion may advance to comparatively greater depths. However, the stresses are far less in this area than under the papermaking surface, so the wear is inconsequential in considerations of load-carrying ability. Only in the instance of steam leakage between flanges has the resultant local thinning ever been implicated in Yankee failure.

c) Steam leakage is detrimental to the long-term structural integrity of the vessel, in that the escaping steam, under high velocity, erodes ever-widening paths in the cast-iron surfaces over which it passes, thinning the cross-section. Steam cutting of connecting bolts is another possible outcome. Either result reduces load-carrying capacity of the part. A safety hazard can also be created for operating personnel, who may be burned by the high-velocity steam jets.

d) Interface leakage, including joints and bolted connections.

    1) Joint Interface Corrosion
    Jacking forces, which develop from the expansion of corrosion products between head-to-shell flanges, cause flange separation and create leakage paths between the flanges and/or through the bolt holes.

    2) Insufficient Joint Clamping Force
    Through inadequate design, improper assembly, loss of washer/gasket, or stress corrosion cracking of connecting bolts, the clamping force between mating flanges is insufficient to retain internal pressure.

    3) Washer/Gasket Functional Loss
    Deterioration, caused by corrosion or expulsion, provides a path for escaping steam and condensate.

    4) Flange Machining Variation
    Variations in surface contour of flange faces may create leakage paths.

e) Through-Wall Leakage
Cast iron inherently exhibits shrinkage porosity. Where porosity linkages occur between internal and external surfaces, a path for steam leakage is made available. Such leakage is largely an operational issue, as holes are formed in the paper product, demanding expedient attention.

S5.3.2 CRACKING

Cracks in cast-iron parts are problematic because of the relatively low fracture toughness compared with standard, more ductile pressure vessel materials and because strengthening repair through welding is prohibited. Furthermore, Yankee dryers are subject to both low- and high-cycle fatigue loading. Consequently,

considerable emphasis is placed upon quality inspection for and timely remediation of cracks, the central causes of which (in Yankee dryers) are:

a) Overpressurization
As shell thickness is routinely diminished through time, Yankee dryers are designed to operate within the pressure limitations set down by ASME Section VIII and the safety factors inherent to the “De-rate Curve” calculated by the vessel manufacturer or equally qualified source. Failure to maintain operation within the steam pressure established by those criteria can, in the extreme, lead to cracking.

b) Pressure Roll Overload
Included in Yankee dryer shell design is a fatigue factor of safety. Exceeding allowable roll load, in combination with other stress-elevating or strength-reducing conditions, can precipitate fatigue cracking and failure.

S5.3.2.1 THROUGH JOINTS AND BOLTED CONNECTIONS

a) Joint Interface Corrosion
Jacking forces, which develop from the expansion of corrosion products between head-to-shell flanges, cause flange separation and create leakage paths between the flanges and/or through the bolt holes.

b) Insufficient Joint Clamping Force
Through inadequate design, improper assembly, loss of washer/gasket, or stress corrosion cracking of connecting bolts, the clamping force between mating flanges is insufficient to retain internal pressure.

c) Washer/Gasket Functional Loss
Deterioration, caused by corrosion or expulsion, provides a path for escaping steam and condensate.

d) Flange Machining Variation
Variations in surface contour of flange faces may create leakage paths.

S5.3.2.2 THROUGH-WALL LEAKAGE

Cast iron inherently exhibits shrinkage porosity. Where porosity linkages occur between internal and external surfaces, a path for steam leakage is made available. Such leakage in the shell is largely an operational issue, as holes are formed in the paper product, demanding expedient attention.

S5.3.2.3 IMPACT FROM OBJECTS PASSING THROUGH THE YANKEE/PRESSURE ROLL NIP

Because of cast iron’s low fracture toughness, it is especially intolerant of local, high-impact loads.

S5.3.2.4 STRESS MAGNIFICATION AROUND DRILLED HOLES

Surface defects, caused by porosity and indentations, are frequently repaired with driven plugs, having some level of interference fit. Pumping ports, threaded for a tapered pipe fitting, are often installed as a standard Yankee design feature for sealant injection into flange interfaces. When installed, both produce an area of increased stress, local to the hole’s edge. In the case of driven plugs, this stress can be exaggerated by excessive interference fits and by closely-grouped or overlapping plugs. Over-torque of threaded, tapered plugs can cause cracks to develop at the periphery of the hole.

S5.3.2.5 THERMAL STRESS AND/OR MICRO-STRUCTURAL CHANGE FROM EXCESSIVE LOCAL HEATING AND COOLING

Transient thermal stresses are usually the highest encountered by a Yankee dryer. Temperature differential through and between parts can be of such magnitude as to exceed the strength of the material. When abnormal thermal loads occur, nondestructive examination is crucial to ensure the vessel's fitness-for-service. Micro-structural change and transient thermal stresses, sufficiently high to cause cracking in Yankee dryers, have resulted, or could result, from:

a) Bearing failure;

b) Rapid warm-up;

c) Excessive steam temperature;

d) Heat from fires;

e) Application of water sprays to fight fires and remove paper jams;

f) Continuous and excessive local cooling from water sprays;

g) Operating heating or cooling systems while the Yankee dryer is stationary; (e.g., high-temperature air impingement hoods, infra-red heating devices, coating showers);

h) Welding and electrical arcs on cast-iron parts; and

i) Excessive local temperature due to improper thermal spray application.

S5.3.2.6 JOINT INTERFACE CORROSION

The products of corrosion occupy a larger volume than the base metal. The forces created by this expansion are sufficient to cause cracking in cast-iron flanges. Without remediation, expansion will continue until failure occurs. Corrosion products form in the presence of moisture in the crevice created between flanges, wherever the clamping force is insufficient to maintain contact between the mating surfaces.

S5.3.2.7 STRESS-CORROSION CRACKING OF STRUCTURAL BOLTS

Stress-corrosion cracking (SCC) is the result of the combination of a corroding agent, material sensitivity, tensile stress, and temperature. At stress levels sufficiently high to induce SCC in the presence of a corrosive medium, attack proceeds along or through grain boundaries perpendicular to the direction of maximum tensile stress. Cracking can initiate with little or no evidence of general corrosion.

S5.3.3 CORROSION

Corrosion culminates with a failure in component functionality by diminishing load-carrying capacity or by generating forces beyond the material's strength. In addition to SCC, corrosion-jacking (head to shell joint), wear-corrosion, and deterioration of washers described above, oxygen pitting, and general corrosion wastage need to be considered as potential failure causes. These latter two corrosion conditions are the result of inadequate boiler water treatment. Oxygen pitting has been encountered, but rarely.

S5.4 INSPECTIONS

a) Yankee dryers should be inspected on a routine-periodic basis. However, as a minimum, the Yankee dryer should be inspected internally and externally at least one time every two years.

b) As appropriate, the following items should be included:

1) Head-to-shell joint;

2) Shell out-of-roundness;

3) Shell centerline thickness;

4) Tilt of head flange;

5) Integrity and security of internal parts;

6) Spigot fit of flanged joints (head-to-shell, head-to-journal);

7) Integrity of structural bolts and studs; and

8) Previously identified areas of deterioration and damage.

c) When a nonstandard load event occurs, or a material non-conformity is noted, an inspection should be performed to assess fitness for continued service. This inspection may involve testing methods not typically used in routine inspections and may also involve removal of material samples for destructive testing.

S5.5 NONDESTRUCTIVE EXAMINATION

a) Nondestructive examination (NDE) methods shall be implemented by individuals qualified and experienced with the material to be tested using written NDE procedures. For Yankee dryers, cast-iron knowledge and experience are essential.

b) Typical nondestructive examination methods should be employed to determine indication length, depth, and orientation (sizing) of discontinuities in Yankee dryers. Magnetic particle, specifically the wet fluorescent method, and dye penetrant methods are applicable in the evaluation of surface-breaking indications. Ultrasonic testing is the standard method for evaluation of surface-breaking and embedded indications. Radiographic methods are useful in the evaluation of embedded indications. Acoustic emission testing can be used to locate and determine if a linear indication is active, i.e., propagating crack. Metallographic analysis is useful in differentiating between original casting discontinuities and cracks.

c) When nondestructive examination produces an indication, the indication is subject to interpretation as false, relevant, or non-relevant. If it has been interpreted as relevant, the necessary subsequent evaluation will result in a decision to accept, repair, replace, monitor, or adjust the maximum allowable operating parameters.

S5.6 PRESSURE TESTING

a) Water pressure testing in the field is not recommended because of the large size of the Yankee dryers and the resulting combined weight of the Yankee dryer and the water used in testing. This combined weight can lead to support structure overload. Several failures of Yankee dryers have occurred during field pressure testing using water. If this test must occur, the following review is recommended:

1) The testing area should be evaluated for maximum allowable loading, assuming the weight of the Yankee dryer, the weight of the water filling the Yankee dryer, and the weight of the support structure used to hold the Yankee dryer during the test.

2) The manufacturer should be contacted to provide information on building the Yankee dryer support structure for the water pressure test. Typically, the Yankee dryer is supported on saddles that contact the testing area and should be evaluated for maximum allowable loading, assuming the weight of the Yankee dryer, the weight of the water filling the Yankee dryer, and the weight of the support structure used to hold the Yankee dryer during the test.

3) The manufacturer should be contacted to provide information on building the Yankee dryer support structure for the water pressure test. Typically, the Yankee dryer is supported on saddles that contact the Yankee dryer shell at each end near the head-to-shell joint. The manufacturer can provide information on saddle sizing and location so that the Yankee dryer is properly supported for the test.

b) When pressure testing is desired to evaluate forms of deterioration, acoustic emission testing, with steam or air, is recommended. Typically, the test pressure used is the operating pressure.

S5.7 TABLES AND FIGURES

a) FIGURE S5.2, De-Rate Curve.

SUPPLEMENT 6
CONTINUED SERVICE AND INSPECTION OF DOT TRANSPORT TANKS

S6.1 SCOPE

This supplement provides rules for continued service inspections of transport tanks, i.e., cargo tanks, rail tanks, portable tanks, and ton tanks that transport dangerous goods as required in the Code of Federal Regulations, Title 49, Parts 100 through 185, and the United Nations Recommendations for Transport of Dangerous Goods-Model Regulations. This supplement, where applicable, shall be used in conjunction with other applicable Parts of the *National Board Inspection Code* (NBIC) and Section XII, *Transport Tanks*, of the *ASME Boiler and Pressure Vessel Code*.

S6.2 TERMINOLOGY

a) The terminology used in this supplement in some cases may be in conflict with terms and definitions normally used in the repair and alteration of pressure-retaining items. Considering these differences, this supplement in the Definition section has incorporated definitions and terms specified in CFR 49, Parts 100 through 185.

b) When conflicts are identified between this part and the regulations of the competent authority regarding the examination, inspection, testing, repair, and maintenance for the continued qualification of transport tanks, the regulations of the Competent Authority take precedence.

c) Rules for repairs and modifications of transport tanks are provided in NBIC Part 3, *Repairs and Alterations*, Supplement 6.

S6.3 ADMINISTRATION

a) The Competent Authority's requirements describe the frequency, scope, type of inspection (internal, external, or both), type of examination (nondestructive, spark test, etc.), and the documentation requirements for the inspection.

b) For transport tanks under the Jurisdiction of the Department of Transportation, the Registered Inspector shall have a thorough knowledge of the Code of Federal Regulations, Title 49, Parts 100 through 185.

S6.4 INSPECTION

This section will establish the appropriate methods to be used for continued service inspections. Inspections for repairs and modifications of transport tanks is located in NBIC Part 3, *Repairs and Alterations*, Supplement 6.

S6.4.1 SCOPE

This section describes the duties, qualifications, and responsibilities of the Registered Inspector, and the scope of inspection activities permitted.

S6.4.2 GENERAL REQUIREMENTS FOR INSPECTORS

a) The Inspector shall be a National Board recognized Inspector, i.e., Authorized Inspector (AI), Qualified Inspector (QI), Certified Individual (CI), or a Registered Inspector (RI). The Registered Inspector is a position established by CFR 49 Parts 100 through 185 for Continued Service Inspections. This individual's duties and responsibilities are subject to DOT and not ASME QAI-1.

b) For continued service inspections, the owner or user's Registered Inspector can be used to perform inspections and testing in accordance with the Code of Federal Regulations, Title 49, Parts 100 through 185, Transportation.

S6.4.3 REGISTRATION OF INSPECTORS

Each Registered Inspector performing duties and responsibilities for continued service inspections or inspections for repairs and modifications as specified in this section and 49 CFR Part 180 is required to meet the qualification requirements of NBIC Part 2, S6.4.4, S6.4.6 and S6.4.7, as applicable to be registered with DOT.

S6.4.4 QUALIFICATIONS OF INSPECTORS

Registered Inspector (RI) means a person registered with the US Department of Transportation (DOT) in accordance with Subpart F of Part 107 of 49 CFR who has the knowledge and ability to determine whether a cargo tank conforms to the applicable DOT specification. A Registered Inspector may or may not be an employee of the approved facility. In addition, Registered Inspector means a person who meets, at a minimum, any one of the following:

a) Has an engineering degree and one year of work experience;

b) Has an associate degree in engineering and two years of work experience;

c) Has a high school diploma or GED and three years of work experience; and

d) Has at least three years of experience in performing the duties of a Registered Inspector by September 1, 1991, and was registered with the DOT by December 31, 1995.

S6.4.5 CODES OF CONSTRUCTION

a) The Registered Inspector is responsible to ensure that all repairs or modifications (including re-rating) are performed in accordance with the original code of construction of the transport tank.

b) For repairs or modifications, the original code of construction for DOT vessels shall be either ASME Section VIII Division I or Section XII.

S6.4.6 INSPECTOR DUTIES FOR CONTINUED SERVICE INSPECTIONS

a) Inspectors performing Continued Service Inspections required by the Code of Federal Regulations (CFR), Title 49, Part 180 shall be a Registered Inspector. The Inspector shall satisfy the following requirements:

   1) Has satisfied DOT requirements as a Registered Inspector;

   2) Has successfully completed the National Board's web-based training program for Registered Inspectors and been issued a National Board certificate of completion;

   3) Has received authorization from DOT as a Registered Inspector; and

   4) Has been registered by DOT for the classification(s) of Transport Tanks to be inspected.

b) Inspectors performing Continued Service Inspections meeting the requirements of NBIC Part 2, S6.13 (Cargo Tanks), S6.14 (Portable Tanks), or S6.15 (Ton Tanks), and 49 CFR, Part 180 shall perform all inspections and tests required by this Section and any additional requirements, as applicable in 49CFR Part 180. The Inspections and tests shall be documented as follows:

1) All inspections and tests shall be conducted, as applicable, in accordance with NBIC Part 2, S6.13, S6.14, and S6.15;

2) All inspections and tests shall be documented in an Inspection Report as required by NBIC Part 2, S6.5;

3) All inspection and test reports shall be maintained by the owner, user, or shipper of the transport tank in accordance with NBIC Part 2, S6.5;

4) All inspection and test reports shall be available for review by an authorized representative of the Department of Transportation; and

c) The requirements for inspections are provided for each classification of transport tanks as specified in NBIC Part 2, S6.4.6.1, Cargo Tanks, S6.4.6.2, Portable Tanks and S6.4.6.3, Ton Tanks.

S6.4.6.1 INSPECTOR DUTIES FOR CONTINUED SERVICE INSPECTION OF CARGO TANKS

a) Cargo tanks constructed in accordance with a DOT Specification that are required to be tested or inspected can not be used for transportation until the required test or inspection has been successfully completed.

1) The Registered Inspector shall inspect cargo tanks in accordance with S6.13, and in conjunction with the requirements of 49 CFR Parts 180.401 through 180.417.

2) The Registered Inspector in the performance of their duties shall ensure that the following requirements for Periodic Inspection and test frequencies in S6.13 are properly satisfied as specified by:

a. Periodic Inspection and Test frequencies: NBIC Part 2, Table S6.13;

b. Pressure Test Requirements for Cargo Tank by specification: NBIC Part 2, Table S6.13.6.

b) Additional criteria for material thickness requirements for a cargo tank specification are listed, as applicable for material type (ferrous and non ferrous) in various tables in NBIC Part 2, S6.13.

S6.4.6.2 INSPECTOR DUTIES FOR CONTINUED SERVICE INSPECTION OF PORTABLE TANKS

a) Portable tanks constructed in accordance with DOT, United Nations (UN), or Inter Modal (IM) specifications that are required to be tested or inspected cannot be used for transportation until the required test or inspections have been successfully completed.

b) The Registered Inspector shall inspect portable tanks in accordance with NBIC Part 2, S6.14, in conjunction with the requirements of 49CFR, Parts 180.601 to 180.605.

c) The Registered Inspector in the performance of their duties shall ensure that the following requirements for Inspection Intervals and Pressure Test Requirements in NBIC Part 2, S6.14, are properly satisfied as specified by:

1) Inspection Intervals: NBIC Part 2, Table S6.14;

2) Pressure Testing Requirements: NBIC Part 2, Table S6.14.6.

S6.4.6.3 INSPECTOR DUTIES FOR CONTINUED SERVICE INSPECTIONS OF TON TANKS

a) Ton Tanks constructed in accordance with DOT 106A or DOT 110A requirements that are required to be tested and inspected cannot be used for transportation until the required test and inspection has been made.

b) The Registered Inspector, shall inspect ton tanks in accordance with NBIC Part 2, S6.15, in conjunction with the requirements of 49CFR, Part 180.519.

c) The Registered Inspector, in the performance of his or her duties, shall ensure that the requirements for Ton Tank Periodic Inspection and Test Frequencies in NBIC Part 2, Table S6.15.3 are properly satisfied.

d) Additional criteria for material thickness, safety valve, and acceptable material with acceptable tensile strength and elongation requirements for ton tanks, are listed in the following tables of NBIC Part 2, S6.15:

    1) Thickness of Plate and Safety Valve Requirements: NBIC Part 2, Table S6.15.1-a;

    2) Acceptable materials with acceptable tensile strength and elongation requirements: NBIC Part 2, Table S6.15.1-b.

S6.4.7 CONTINUED SERVICE, INSPECTION FOR DOT TRANSPORT TANKS SCOPE

This supplement details frequencies of testing requirements, type of tests required, acceptance criteria, and inspection reports of transport tanks.

S6.4.7.1 ADMINISTRATION

The Competent Authority's requirements describe the frequency, scope, type of inspection, and documentation requirements for the inspection and are noted in the US Code of Federal Regulations, Title 49 CFR, Parts 100 through 185.

S6.4.7.2 INSPECTION AND TEST REQUIRED FREQUENCIES

Inspection and frequencies for periodic testing of cargo tanks are found in NBIC Part 2, S6.13; portable tanks S6.14; and ton tanks S6.15.

S6.4.7.3 EXTERNAL VISUAL AND PRESSURE TESTS

External visual inspection tests shall be performed in accordance with NBIC Part 2, S6.13.1, for cargo tanks; S6.14.5 for portable tanks; and NBIC Part 2, S6.15.2, for ton tanks. The pressure tests for cargo tanks shall be as specified in S6.13.6; S6.14.6, for portable tanks; and NBIC Part 2, S6.15.3, for ton tanks.

S6.4.7.4 LEAK TIGHTNESS TESTING OF TRANSPORT TANKS

S6.4.7.4.1 CARGO TANKS

a) Each cargo tank must be tested for leaks in accordance with NBIC Part 2, Table S6.13, *Periodic Inspections and Tests,* and per the requirements in NBIC Part 2, S6.13.9. The minimum leakage test pressure of 80% of MAWP may be accepted by provisions of the Competent Authority (see 49 CFR 180.407[h]).

b) All external and accessible portions of piping up to the first closure when offered for transportation shall be tested for leak tightness.

1) All closure fittings must be in place during the leak tightness test.

2) The leak tightness test pressure must be maintained for at least 5 minutes.

3) All sources of leakage must be properly repaired.

4) A cargo tank that fails to retain leakage test pressure may not be returned to service as a specification cargo tank.

S6.4.7.4.2 PORTABLE TANKS

Each portable tank's piping must be tested for leaks in accordance with the inspection intervals in NBIC Part 2, Table S6.14, and per the procedures in NBIC Part 2, S6.14.6.

a) The minimum leakage test pressure is as specified in NBIC Part 2, Table S6.14.6.

b) All closure fittings must be in place during the leak tightness test.

c) The test pressure must be maintained for at least 5 minutes.

d) All sources of leakage must be properly repaired.

e) A portable tank that fails to retain leakage test pressure may not be returned to service as a specification portable tank.

S6.4.7.4.3 TON TANKS

Each ton tank shall be tested at intervals specified in NBIC Part 2, Table S6.15.3, by procedure at pressures specified for the classification of the tank.

S6.4.7.4.4 LEAK TIGHTNESS TESTING OF VALVES

S6.4.7.4.4.1 CARGO TANKS

Cargo tank valves shall be periodically visually inspected in accordance with the applicable provisions in NBIC Part 2, S6.13 and leak tested at time intervals specified in Table S6.13. This test should coincide with the leak test for piping as specified in NBIC Part 2, S6.4.7.4.1, and shall include:

a) All valves under pressure shall be leak tested at the pressure specified, for leakage through the valve, and externally (e.g., valve bonnet).

b) During the inspection a suitable method must be used for detecting the existence of leaks. This method must consist either of coating the entire surface of all joints under pressure with a solution of soap and water, or using other equally sensitive methods.

c) All emergency devices and valves including self-closing stop valves, excess flow valves and remote closure devices must be free from corrosion, distortion, erosion, and external damage that will prevent safe operation. Remote closure devices and self-closing stop valves must be functioned to demonstrate proper operation.

S6.4.7.4.4.2 PORTABLE TANKS

Portable tank valves shall be periodically visually inspected in accordance with the applicable provisions of NBIC Part 2, S6.14.3, and leak tested at time intervals specified in NBIC Part 2, S6.14. Leak tightness testing requirements are as specified in NBIC Part 2, Table S6.14.6, and shall include:

a) Piping, valves, and gaskets must be free from corroded areas, defects, and other conditions, including leakage, that might render the portable tank unsafe for filling, discharge, or transportation;

b) All emergency valves shall be free from corrosion, distortion, and any damage or defect that could prevent their normal operation;

c) Remote closure devices and self-closing stop valves must be operated to demonstrate proper function;

d) For testing of internal self-closing stop valves see Appendix A and B of 49CFR180; and

e) The intermediate periodic inspection and test shall include an internal and external inspection, unless exempted, and an external inspection of the portable tank and fittings, leakage test, and test for satisfactory operation of all service equipment.

S6.4.7.4.4.3 TON TANKS

Ton tank valves shall be periodically visually inspected in accordance with the applicable provisions of NBIC Part 2, S6.15.2 and leak tested in accordance with the provisions of NBIC Part 2, S6.15.3 and S6.15.3.1. This test should coincide with the tank retest intervals as stipulated in NBIC Part 2, Table S6.15.3.

S6.4.7.5 LEAK TIGHTNESS TESTING OF SAFETY RELIEF DEVICES

S6.4.7.5.1 CARGO TANKS

a) All reclosing pressure relief devices for cargo tanks shall be visually inspected per NBIC Part 2, S6.13.2 e) and pressure tested for leak tightness as stipulated in NBIC Part 2, S6.13.6 b) at frequencies specified in NBIC Part 2, Table S6.13.

   Note: When performing this test, all reclosing pressure relief valves, including emergency relief vents, and normal vents shall be removed for inspection and tested as follows:

b) Leakage test for any venting device required for the interval specified in NBIC Part 2, Table S6.13, must include testing the device in place, except that any venting device set to discharge at less than the leakage pressure must be removed or rendered inoperative during the test.

c) Non-reclosing relief device discs should be evaluated for replacement at the time of the pressure test intervals.

S6.4.7.5.2 PORTABLE TANKS

Portable tanks subject to a five-year periodic inspection and leak tightness test, except for DOT Specification 56 and 57 Portable Tanks, shall include:

a) All re-closing pressure relief devices must be removed from the tank and tested separately unless they can be tested while installed on the portable tank.

b) If a leakage test is specified being less than the MAWP, the re-closing pressure relief valves can be tested in place.

c) Visual inspection shall include all emergency devices to ensure that they are free from corrosion, distortion, and any damage or defects that could prevent the devices from operating as designed.

d) For Specification 57 Portable Tanks, during the air test, the pressure relief device may be removed or left in place. If the relief device is left in place during the test, the device's discharge opening shall be plugged. (See Special Requirements for testing of pressure relief devices for Specifications 51 and 56 Portable Tanks in NBIC Part 2, S6.14.6.2.)

e) For Specification 60 Portable Tanks, re-closing pressure relief devices may be removed from the tank and tested separately unless they can be tested while installed in the portable tank.

f) If portable tanks are fitted with non-reclosing relieving devices, consideration for replacing the discs for these devices should be evaluated at the time of the leak tightness test interval.

S6.4.7.5.3 TON TANKS

Each ton tank designed to be removed from tank cars for filling and emptying shall have their safety relief devices, if fitted, tested and subjected to a periodic inspection and test at frequencies established in NBIC Part 2, Table S6.15.3.

1) All pressure relief devices shall be retested by air or gas for the start-to-discharge and vapor tightness requirements.

2) For ton tanks fitted with rupture discs and fusible plugs, the inspection of these devices and disposition must be as described in NBIC Part 2, S6.15.3.3.

S6.4.7.6 TESTING OF MISCELLANEOUS PRESSURE PARTS

S6.4.7.6.1 CARGO TANKS

Cargo tanks provided with manholes (or handholes) shall be inspected in accordance with NBIC Part 2, S6.13.2 and all major structural attachments as defined in CFR180.407(d)(2)(viii), including the upper coupler (fifth wheel) assembly and ring stiffeners shall be inspected in accordance with NBIC Part 2, S6.13.3. Other miscellaneous items shall comply with the following:

a) Cargo tanks equipped with linings that protect the cargo tank from the commodity being transported shall be inspected, unless exempted, in accordance with the provisions of NBIC Part 2, S6.13.5.

b) For cargo tanks equipped with a heating system, the heating system shall be pressure tested as required by NBIC Part 2, S6.13.6.4.

c) Delivery hoses for MC330 and MC331 cargo tanks shall be leak tightness tested. Any conditions as noted in NBIC Part 2, S6.13.9, which exist for the delivery hose, shall be unacceptable and prevent its continued use.

d) New or replaced delivery hose assemblies shall meet all of the requirements of NBIC Part 2, S6.13.10. In addition to this requirement, for commodities transported in MC330 and MC331, the delivery hose assemblies may be installed or carried on the cargo tank. The operator is required to perform inspections as required in 49CFR180.416.

S6.4.7.6.2 PORTABLE TANKS

For portable tanks, the periodic visual inspection shall include:

a) The operation of tightening devices for manhole and handhole covers, or the gaskets are operative and there is no leakage at the manhole or handhole cover or gasket at leakage pressure.

b) The framework structural supports and the lifting device located on the portable tank shall be in satisfactory condition.

S6.4.7.6.3 TON TANKS

Visual inspection of ton tanks shall include damaged chimes or protective rings, if so fitted.

S6.4.7.7 ACCEPTANCE CRITERIA

All defects or deficiencies discovered during the inspection process of a transport tank shall be documented in the Inspection Report and discussed with the owner or user of the transport tank at the time of the inspection. Defects or deficiencies shall be corrected using appropriate methods, and tested prior to returning the transport tank to service. (See NBIC Part 2, S6.10)

S6.4.7.8 INSPECTION REPORT

S6.4.7.8.1 CARGO TANKS

Cargo tank Inspection Reports, as a minimum, shall include the information specified in NBIC Part 2, S6.13.6.7 and S6.13.8 (as applicable) and 49 CFR 180.417.

S6.4.7.8.2 PORTABLE TANKS

Portable tank Inspection Reports shall satisfy the requirements of NBIC Part 2, S6.14.9, in addition to those of 49 CFR Part 180.605.

S6.4.7.8.3 TON TANKS

Ton tank Inspection Reports shall satisfy the requirements of NBIC Part 2, S6.15.3.6 in addition to those of 49 CFR Part 180.519.

S6.5 STAMPING AND RECORD REQUIREMENTS FOR DOT TRANSPORT TANKS IN CONTINUED SERVICE

This section provides for preparation, distribution and maintenance of inspection records and stamping requirements for Continued Service Inspections of Transport Tanks, i.e., cargo tanks, portable tanks, and ton tanks.

S6.5.1 GENERAL

To ensure that transport tanks can maintain their authorization to transport hazardous materials by the mode of transport permitted by the competent authority (DOT), the specification transport tank's owner or user shall satisfy, as applicable, that the records and stamping requirements of this supplement and Code of Federal Regulations, Title 49, Part 180 (49 CFR 180) have been satisfied.

S6.5.2 STAMPING

a) Transport tanks represented as manufactured to a DOT specification or a United Nations (UN) standard shall be marked on a non-removable component of the transport tank with specification markings conforming to the applicable specification. The specification marking is required to be located in an unobstructed area with letters and numerals identifying the standard or specification. Unless otherwise specified by Part 178.3 of the Code of Federal Regulations, the markings must identify the name and address or symbol of the transport tank manufacturer or, where specifically authorized, the symbol of the approval agency certifying compliance with a UN standard.

b) Symbols required by the Department of Transportation (DOT) must be with the approval of the DOT Associate Administrator. Duplicative symbols are not authorized. Stamping and symbol requirements for transport tanks that are under different rules than CFR 49, Parts 100 through 185, shall comply with the applicable competent authority's rules and regulations.

c) The detailed markings, i.e., stamped, embossed, burned, printed, etc., size of the markings, capacities, etc., are specified in Part 178.3 of the Code of Federal Regulations, Title 49, as follows:

1) ASME-Stamped Transport Tanks

a. Transport tanks stamped with the ASME Section XII Code Symbol shall satisfy the applicable requirements of that code. Transport tanks manufactured prior to the adoption of ASME Section XII by the Competent Authority were manufactured in accordance with ASME Section VIII, Div. 1. Stamping with the ASME Section VIII, Div. 1 "U" Code Symbol Stamp is dependent on pressure and/or media limitations.

b. When the stamping on a transport tank becomes indistinct or the nameplate is lost or illegible, but traceability to the original transport tank is still possible. To satisfy this requirement, as a minimum, original source data from the manufacturer of the vessel or records in possession of the tank Owner should be used to establish traceablity to the stamping with the concurrence of the Inspector, and approval of the Competent Authority, and if required the Jurisdiction. The Inspector shall instruct the Owner or user to have the stamped data replaced. All restamping shall be done in accordance with the original code of construction (ASME Section XII, or ASME Section VIII, Div. 1, as applicable). Request for permission to restamp or replace the nameplate shall be made to the Competent Authority and, if required, the Jurisdiction. Application must be made on the *Replacement of Stamped Data Form*, NB-136 (See NBIC Part 2, 5.5.2). Proof of the stamping and other such data, as is available, shall be furnished with the request. When traceability cannot be established, the Competent Authority shall be contacted.

2) Restamping or replacement of nameplates

Restamping or replacement of the nameplate as authorized by the Competent Authority shall only be done in the presence of the Inspector, i.e., AI, QI, CI, or National Board Commissioned Inspector, as required by ASME Section XII and the applicable Modal Appendix, or as required by the Competent Authority. For transport tanks manufactured to ASME Section VIII, Division 1, restamping or replacement shall only by done in the presence of an Authorized Inspector or a National Board Commissioned Inspector.

S6.5.3 OWNER OR USER REQUIRED RECORDS FOR CARGO TANKS

a) Each owner or user of a DOT Specification cargo tank shall retain the appropriate ASME Manufacturer's Data Report, Form T-1, for Section XII Transport Tanks, or Form U-1A for Section VIII, Division 1 Pressure Vessels, and related papers certifying that the DOT Specification cargo tank identified in the documents was manufactured and tested in accordance with the applicable tank specification.

1) In addition to the appropriate ASME Manufacturer's Data Report, the required documents shall include any certification of emergency discharge control systems required by 49 CFR 173.315(n) or 49 CFR 180.405(m).

a. The Certificate of Compliance issued by the cargo tank motor vehicle manufacturer (CTMVM) and all preceding certificates issued by preceding manufacturers signed and dated by a Registered Inspector or Company Official or Design Certifying Engineer as required by 49 CFR 178.337-18(a)(1) or (a)(2) as appropriate. The certificate must contain a statement indicating whether or not the cargo tank was postweld heat treated for anhydrous ammonia service as specified in 49 CFR 178.337-1(f);

b. Cargo tank fabrication drawings;

c. Piping drawing that identifies the location, make, model, and size of each valve and the arrangement of all piping associated with the cargo tank motor vehicle;

d. Assembly drawing;

e. Pressure test report for the piping, valves and fittings;

f. Hose certification; and

g. Certification of emergency discharge control systems.

2) The documents required by 49 CFR shall be retained throughout ownership of the cargo tank and for one year after relinquishing ownership.

3) In the event of a change in ownership, the prior owner shall retain non-fading photocopies of these documents for one year.

4) Users of a cargo tank that are not the owner shall retain a copy of the vehicle certification report as long as the cargo tank motor vehicle is used by the user and for one year thereafter.

5) The required documents specified in this Section shall be maintained at the owner's or users' principal place of business, or at a location where the cargo tank is housed or maintained.

6) Items 4) and 5) do not apply if the user leases the cargo tank for less than 30 days.

b) For DOT Specification cargo tanks that were manufactured prior to September 1, 1995, that were not constructed to ASME Section VIII, Division 1 (Non Code Pressure Vessels), but wishes to certify the cargo tank to a DOT Specification Cargo Tank, the following shall be complied with:

1) The owner shall perform the appropriate tests and inspections as required by 49 CFR Part 178 under the direct supervision of a Registered Inspector to determine if the cargo tank conforms to the applicable specification.

2) Both the owner and the Registered Inspector shall certify that the cargo tank fully conforms to the applicable specification.

3) The owner shall maintain the certification as specified in this section.

c) For ASME stamped cargo tanks, the owner must have the manufacturer's certification and the appropriate ASME Manufacturer's Data Report on file.

1) If the owner does not have the manufacturer's certification and the appropriate ASME Manufacturer's Data Report, the following shall be satisfied:

a. If the pressure vessel of the cargo tank is registered with the National Board of Boiler and Pressure Vessel Inspectors (National Board), they shall obtain a copy of the Manufacturer's Data Report from the National Board.

b. If the pressure vessel of the cargo tank is not registered with the National Board, shall copy the cargo tank's identification and ASME Code nameplate information and retain this information in their files.

2) If the nameplate information is copied as identified in c) 1) b., the owner and the Registered Inspector shall certify that the pressure vessel of the cargo tank fully conforms to the DOT specification.

3) The owner shall retain all certification documents in accordance with retention periods specified in this supplement.

S6.5.3.1 REPORTING REQUIREMENTS BY THE OWNER OR USER OF TESTS AND INSPECTIONS OF DOT SPECIFICATION CARGO TANKS

The owner or user that performs the required test and the Registered Inspector that performs the inspection as specified at frequencies established in NBIC Part 2, Table S6.13, shall prepare a written report in English

that satisfies the requirements of NBIC Part 2, S6.13. Each test and inspection facility that fails a cargo tank based on a test or inspection report shall notify the Owner, register the report with the National Board, and provide a copy of the test report indicating the failure to the competent authority.

S6.5.3.2 DOT MARKING REQUIREMENTS FOR TESTS AND INSPECTIONS OF DOT SPECIFICATION CARGO TANKS

Each cargo tank that has successfully completed the test and inspection contained in NBIC Part 2, S6.13, shall be durably and legibly marked, in English. The markings shall comply with the following:

a) Date (month and year) of the type of test or inspection performed, subject to the following:

   1) Date shall be readily identifiable with the applicable test or inspection;

   2) Markings shall be 32 mm (1.25 in.) high, near the specification plate or anywhere on the front head of the cargo tank.

b) The type of test or inspection may be abbreviated as follows:

   1) “V” for external visual inspection;

   2) “I” for internal visual inspection;

   3) “P” for pressure test;

   4) “L” for lining inspection;

   5) “T” for thickness inspection;

   6) “K” for leakage test for a cargo tank tested to the requirements of NBIC Part 2, S6.13.9, except for cargo tanks subject to the requirements of NBIC Part 2, S6.13.9 d) 10); or

   7) “K-EPA27” for a cargo tank tested to the requirements of NBIC Part 2, S6.13.9 d) 10), that was manufactured after October 1, 2004.

c) For a cargo tank motor vehicle composed of multiple cargo tanks constructed to the same specification, which are tested and inspected at the same time, one set of test and inspection markings may be used to satisfy the requirements of NBIC Part 2, S6.5.3.2.

d) For a cargo tank motor vehicle composed of multiple cargo tanks constructed to different specifications, which are tested and inspected at different intervals, the test and inspection markings shall appear in the order of the cargo tank’s corresponding location, from front to rear.

S6.5.4 OWNER OR USER REQUIRED RECORDS FOR PORTABLE TANKS

a) The owner of each portable tank or their authorized agent shall retain a written record of the date and results of all required inspections and tests, including the ASME Manufacturer’s Data Report.

b) The written record, if applicable, shall indicate the name and address of the person that performed the inspection or test. The inspection and test shall comply with the requirements of the portable tank’s specification, as provided in 49 CFR, Part 178.

c) The owner shall maintain a copy of the ASME Manufacturer’s Data Report. He shall also maintain a certificate(s) that is signed by the manufacturer of the portable tank, and by the authorized design approval agency, as applicable indicating compliance with the applicable portable tank specification.

d) The signed certificate, including the ASME Manufacturer's Data Report, shall be maintained by the owner or their authorized agent during the time that the portable tank is used for service. DOT Specifications 56 and 57 portable tanks are exempt from this requirement.

S6.5.4.1 REPORTING OF PERIODIC AND INTERMEDIATE PERIODIC INSPECTION AND TESTS OF DOT SPECIFICATION PORTABLE TANKS

a) The user of portable tanks shall satisfy the requirements for Periodic and Intermediate Periodic Inspection and Tests of portable tanks as specified in Table S6.14 of this supplement and shall maintain the results of these tests as required in NBIC Part 2, S6.5.4.

b) The methods and procedures to be used in the performance of the required Intermediate Periodic and Inspections and Tests are specified in NBIC Part 2, S6.14.

S6.5.4.2 MARKING REQUIREMENTS FOR PERIODIC AND INTERMEDIATE INSPECTION AND TESTS FOR IM OR UN PORTABLE TANKS

Each IM or UN portable tank that has successfully completed the required Periodic or Intermediate Inspection and Test shall be durably and legibly marked, in English. The markings shall comply with the following:

a) Date (month and year) of the last pressure test;

b) Identification markings of the approval agency witnessing the test;

c) When required, the date (month and year) of the last visual inspection;

d) Markings shall be placed on or near the metal identification plate; and

e) Markings shall be 3 mm (0.118 in.) high when on the metal identification plate and 12 mm (0.47 in.) high when on the portable tank.

S6.5.4.3 DOT MARKING REQUIREMENTS FOR PERIODIC AND INTERMEDIATE INSPECTION AND TESTS OF DOT SPECIFICATION 51, 56, 57, OR 60 PORTABLE TANKS

Each DOT Specification 51, 56, 57, or 60 portable tank that has successfully completed the required Periodic or Intermediate Inspection and Test shall be durably and legibly marked, in English. The markings shall comply with the following:

a) Date (month and year) of the most recent test;

b) Markings shall be placed on or near the metal certification plate;

c) Markings shall be accordance with 49 CFR, Part 178.3; and

d) Letters and numerals shall not be less than 3 mm (0.118 in.) high, when on a metal certification plate and 12 mm (0.47 in.) on the portable tank, except that a portable tank manufactured under a previously authorized specification may continue to be marked with smaller markings if originally authorized under that specification (for example, DOT specification 57 portable tanks).

S6.5.5 OWNER OR USER REQUIRED REPORTS FOR DOT SPECIFICATION 106A AND DOT 110A TON TANKS

a) The owner or user of a DOT Specification ton tank shall retain the certificate of construction (AAR-Form 4-2) and related papers certifying that the manufacturer of the specification tank identified in the documents is in accordance with the applicable specification.

b) The owner or user shall retain the documents throughout the period of ownership of the specification ton tank and for one year thereafter.

c) Upon a change in ownership of the specification ton tank, the owner shall satisfy the requirements of Section 1.3.15 of the ARR Specification.

S6.5.5.1 REPORTING OF INSPECTION AND TESTS FOR DOT SPECIFICATION 106A AND DOT 110A TON TANKS

a) The owner or user shall inspect and test ton tanks at frequencies specified in NBIC Part 2, Table S6.15.3 and shall perform the inspections and tests in accordance with NBIC Part 2, S6.15.3.

b) The owner or user is required to develop a written record of the results of the pressure test and visual inspection and shall record the information on a suitable data sheet. Completed copies of these reports shall be retained by the owner and by the person performing the pressure test and visual inspection, as long as the ton tank is in service.

c) The required information to be recorded and checked on these data sheets is:

1) Date of test and inspection;

2) DOT Specification Number;

3) Ton tank identification (registered symbol and serial number);

4) Date of manufacturer and ownership symbol;

5) Type of protective coating (painted, etc.), and statement as to need for refinishing or recoating;

6) Conditions checked, i.e., leakage, corrosion, gouges, dents or digs, broken or damaged chime or protective ring, fire, fire damage, internal condition;

7) Test pressure;

8) Results of tests;

9) Disposition of ton tank (returned to service, returned to manufacturer for repair, or scraped); and

10) Identification of person conducting the retest or inspection.

d) If a Retest Inspection is required, the owner or user shall prepare a written report in accordance with NBIC Part 2, S6.15.3.6, of this supplement.

S6.5.5.2 DOT MARKING REQUIREMENTS FOR TESTS AND INSPECTION OF DOT SPECIFICATION 106A AND 110A TON TANKS

a) When a ton tank passes the required inspection and test with acceptable results, the tank car facility shall mark the following information on the ton tank:

1) Date of the inspection and test;

2) Due date of the next inspection and test;

3) The markings on the ton tank shall be in accordance with Appendix C of the ARR Specifications for Tank Cars.

b) When a tank car facility performs multiple inspections and tests at the same time, one date may be used to satisfy the requirements of NBIC Part 2, S6.5.5.2. Additionally, one date may be shown when multiple inspections and tests have the same due date.

S6.6 CORROSION AND FAILURE MECHANISMS IN TRANSPORT TANKS

An effective inspection and test program requires an understanding of the applicable potential failure mechanisms and the applicable inspection and test methods to ensure the continued structural integrity of a transport tank.

S6.6.1 SCOPE

This section provides an overview of the causes of deterioration and failure mechanisms in transport tanks. As provided in this overview, some forms of deterioration and failure mechanisms may include stress corrosion cracking, fatigue, and temperature gradients (brittle fracture behavior) applicable to transport tanks during their normal operation.

S6.6.2 GENERAL

a) This supplement includes a general discussion of mechanisms and effective inspection and test methods. Additionally, some specific guidance is given on how to evaluate the transport tanks for repairs, modifications, and continued service requirements.

b) There are a variety of inservice conditions that may cause deterioration of the materials used in the construction of transport tanks. These inservice conditions should be taken into consideration during any repair activity. Prior to any repair activity, it is important to identify the cause of the deterioration, and to prevent its recurrence.

S6.6.3 INTERNAL AND/OR EXTERNAL CORROSION

Internal and/or external wastage from corrosion is probably one of the most common causes of deterioration in transport tanks while in operation. All metals and alloys are susceptible to corrosion. Corrosion is deterioration that occurs when a metal reacts with its environment. Corrosion can be classified based on three factors. These factors are:

a) Nature

1) Wet — liquid or moisture present in the transport tank;

2) Dry — high temperatures that may be present in the transport tank;

b) Mechanism — electrochemical or direct chemical reactions; and

c) Appearance — either uniform or localized.

S6.6.3.1 TYPES OF CORROSION

To implement the proper corrective actions will depend on which factors caused the problems, making it important to diagnose the reason for failure. Early detection of corrosion problems are important to prevent failures and can be achieved by performing regular inspections and encouraging employees to be

observant and communicate their observations. The following types of corrosion mechanisms are commonly found in transport tanks:

a) Pitting Corrosion

Pitting corrosion is the formation of holes in an otherwise relatively un-attacked surface. Some of the characteristics of pitting corrosion are:

1) Usually a slow process causing isolated, scattered pitting over a small area that does not substantially weaken the transport tank. It could, however, eventually cause leakage;

2) In some cases, local corrosion pits can be caused by microbiological activity, commonly known as MIC (microbiologically influenced corrosion) attack; or

3) Generally, the area of the steel surrounding a corrosion pit from MIC will exhibit discoloration or a ring as evidence of a thriving bacteria colony.

b) Line Corrosion

This is a condition where pits are connected; or nearly connected to each other in a narrow band or line. Line corrosion frequently occurs in the interior surfaces of a transport tank at the following locations:

1) The liquid-vapor interface in the transport tank, or

2) The bottom of the transport tank.

c) General Corrosion

This is corrosion that covers a considerable area of the vessel surface of the transport tank. When this condition occurs, the owner or user of the transport tanks has to consider if this condition has compromised the continued safe operation of the transport tank. The following should be used in making this determination:

1) Inspect the affected area or areas to ensure that the required minimum thickness of the vessel is within acceptable limits; and

2) If the affected area's or areas' minimum thickness is below tolerance, depending on the degree of deterioration, restore the area or areas to the required thickness by using the weld buildup method or a flush patch.

d) Grooving Corrosion

This type of corrosion is a form of metal deterioration caused by localized corrosion, and may be accelerated by stress concentration. Grooving is generally noticed:

1) Adjacent to welded surfaces, and

2) On flange-mating surfaces.

e) Exfoliation and Selective Leaching

1) Exfoliation is a subsurface corrosion that begins on a clean surface, but spreads below the surface of the metal. This type of corrosion differs from pitting in that the damage to the metal exhibits a laminated appearance, recognized by a flaky and sometimes blistered surface.

2) Selective leaching results in the removal of one of the elements in an alloy material. This corrosion mechanism is detrimental because it yields a porous metal with poor mechanical properties.

f) Galvanic Corrosion

1) Occurs when two dissimilar metals come in contact with each other in the presence of an electrolyte (e.g., film of water containing dissolved oxygen, nitrogen, and carbon dioxide) constituting an electrolytic cell. The difference in galvanic potential between the two dissimilar materials creates a local electrical cell that may cause rapid corrosion of the less- noble metal. This corrosion mechanism becomes more active when there are large differences between the electrode potentials of the two metals.

2) Galvanic corrosion may also exist with relatively minor changes of alloy composition (e.g., between a weld metal and the base metal). Natural (e.g., an oxide coating on aluminum) or a protective coating may inhibit galvanic corrosion, but in most instances the metals or alloys must be selected on the basis of intrinsic resistance to corrosion.

3) In transport tanks, the effects of galvanic corrosion are most noticeable at welds or at flanged and bolted connections that have been exposed to contact with a fluid that is conductive.

g) Erosion/Corrosion

This type of damage mechanism is generally attributed to the movement of a corrodent over a metal surface that increases the rate of attack due to mechanical wear and corrosion. This type of damage mechanism is generally characterized as having an appearance of smooth bottomed shallow pit, and may also exhibit a directional pattern or surface texture related to the path taken by the corrodent. This deterioration would normally occur at locations where the transport tank is filled or emptied.

h) Crevice Corrosion

1) Environmental conditions in a crevice can, with time, become different from those on a nearby clean surface. A more aggressive environment may develop within the crevice and cause local corrosion. Crevice corrosion commonly can be found in:

a. Gasket surfaces;

b. Lap joints; and

c. Bolts and flanges.

2) Crevice corrosion can also be caused by dirt deposits, corrosion products, scratches in paint, etc.

3) To avoid or greatly reduce corrosion, the owner or user of transport tanks, when having a transport tank manufactured, can specify materials and protection methods (such as coating). By implementing proper selection of materials and protection methods, corrosive attack in transport tanks can be predicted and controlled. However, there may be unexpected failures as a result of one or more of the following:

a. Poor choice of materials used in transport tank repairs or new construction;

b. Operating conditions different from those anticipated in service;

c. Defective fabrication;

d. Improper design;

e. Inadequate maintenance; and

f. Defective material.

S6.6.4 FAILURE MECHANISMS

There are various failure mechanisms that can result in cracks or loss of structural integrity to transport tanks. The more common failure mechanisms described below are fatigue, mechanical, thermal, and corrosion induced brittle fracture and hydrogen embrittlement, as a result of poor handling practices during welded repairs.

a) Fatigue — Stress reversals (such as cyclic loading) in parts of transport tank equipment are common, particularly at points of high secondary stress. These stresses can originate adjacent to locations of weld repairs and from over-the-road vibratory stresses. If stresses are high and reversals frequent, failure of parts may occur because of mechanical fatigue crack propagation. Fatigue failures in transport tanks may also result from exposure to cyclic temperature and pressure changes. Locations where metals having different thermal coefficients of expansion that are joined by welding may be susceptible to thermal fatigue upon exposure to service temperature variations.

    1) In specific cases where the combined effects of exposure to a corrosive environment and cyclic loading occur together in a transport tank, the damage mechanism that can occur is corrosion assisted fatigue or simply corrosion fatigue.

    2) Corrosion fatigue crack propagation typically occurs along a straight direction, with minimal branching. Some sources of fatigue crack initiation are:

        a. At sharp corners;

        b. At openings in the transport tank; and

        c. At structural attachments.

b) Temperature — At subfreezing temperatures, water and some chemicals handled in transport tanks may freeze and cause failure. Carbon and low-alloy steels may be susceptible to brittle fracture, even at ambient temperatures. A number of failures have been attributed to brittle fracture of steels that were exposed to temperatures below their ductile-to-brittle transition temperature (DBTT) during a pressure test or hydrostatic test. However, most brittle fractures have occurred on the first application of a particular stress level (that is, the first hydrostatic test or overload).

    Special attention should be given to low-alloy steels because they are prone to temper embrittlement, which can result in a loss of toughness.

    Temper embrittlement is defined as a loss of ductility and notch toughness due to postweld heat treatment or high temperature service, above 370°C (700°F).

c) Hydrogen Embrittlement — A loss of strength and/or ductility in steels caused by atomic hydrogen dissolved in the steel. It is a low-temperature phenomenon, seldom encountered above 95°C (200°F), and most often occurs as a result of hydrogen evolved from aqueous corrosion reactions or hydrogen generated during welding. Weld underbead cracking (also know as delayed cracking and cold cracking) is also a form of hydrogen embrittlement; however, in this case, the hydrogen comes from the welding operation rather than from a corrosion reaction.

    1) Weld underbead cracking is caused by hydrogen dissolved in a hard, high-strength weld heat-affected zone. Use of low-hydrogen welding practices to minimize dissolved hydrogen, and/or use of high-preheat, and/or postweld heat treatment to reduce heat-affected zone hardness, will reduce the likelihood of weld underbead cracking in susceptible steel.

    2) Hydrogen embrittlement is reversible as long as no physical damage, e.g., cracking, has occurred in the steel. If the atomic hydrogen is removed from the steel before any damage occurs, for example by heating for a short time in the absence of hydrogen between 150°C (300°F) and 205°C (400°F), normal mechanical properties will be restored.

3) Welding procedures, repair methods, and inspection procedures must include careful consideration of potential failure in corrosive environments, including the various forms of hydrogen embrittlement.

d) Stress Corrosion Cracking (SCC) — Cracking of a metal caused by the combined action of stress and a corrosive environment. SCC only occurs with specific combinations of metal and environment. The stress required may be either applied or residual. Examples of stress corrosion cracking include chloride stress corrosion cracking of stainless steels in hot, aqueous chloride solutions; caustic cracking of carbon steel in hot sodium hydroxide solutions, and ammonia stress corrosion cracking of brass in ammonia solutions (season cracking).

1) Corrosivity alone is not a good indicator of the likelihood of a particular environment to cause SCC in a particular metal. Solutions that are highly corrosive to a material almost never promote SCC.

2) The principal variables affecting SCC are tensile stress, service temperature, solution chemistry, duration of exposure, and metal properties. Removing any one of these parameters sufficiently can reduce or eliminate the possibility of SCC occurring in service.

S6.7 CLASSIFICATION BOUNDARIES

Transport tanks are classified as Class 1, Class 2, and Class 3. The classification is established by the applicable Modal Appendix of ASME Section XII. Also contained in the Modal Appendix is the type of Inspector, i.e., Authorized Inspector, Qualified Inspector, and Certified Individual, that is permitted to perform the applicable fabrication inspection of the transport tank, i.e., cargo tank, tank car, portable tank, and ton tank. The classification of the transport tank, except for continued service inspections, determines the code of construction requirements for repairs or modifications.

S6.8 PRESSURE, TEMPERATURE, AND CAPACITY REQUIREMENTS FOR TRANSPORT TANKS

a) ASME Section XII has established pressure, temperature, and maximum thickness requirements for transport tanks as follows:

1) Pressure: full vacuum to 208 bar (full vacuum to 3,000 psia);

2) Temperature: -269°C to 343°C (-452°F to 650°F); and

3) Maximum material thickness: 38 mm (1-1/2 in.).

b) Transport tanks manufactured prior to the adoption of ASME Section XII by the Competent Authority were manufactured in accordance with ASME Section VIII, Div. 1. Transport tanks manufactured to this Code were required to be stamped with the “U” Code Symbol Stamp in accordance with Section VIII, Div. 1, if the design pressure of the transport tank was 241 kPa (35 psi) (depending on material being transported) and greater. If the design pressure was less than 241 kPa (35 psi) (depending on the media being transported), the transport tank was constructed in accordance with Section VIII, Div. 1, but not stamped with the “U” Code Symbol Stamp.

c) For these transport tanks, the requirements established in NBIC Part 2, for continued service inspection, repairs, or modifications shall apply, unless specifically exempted by the DOT.

S6.9 REFERENCES TO OTHER CODES AND STANDARDS

Other existing inspection codes, standards, and practices pertaining to the continued service inspection, i.e., CFR 49, Parts 100 through 185, ASME Section XII, etc., of transport tanks can provide useful information and references relative to the inspection techniques listed in this Appendix. Additionally, supplementary guidelines for assisting in the evaluation of inspection results and findings are also available. Some acceptable requirements and guidelines are as follows:

a) American Society of Mechanical Engineers — *ASME Boiler and Pressure Vessel Code*, Section VIII, Div. 1 (*Rules for Construction of Pressure Vessels*).

b) American Society of Mechanical Engineers:

   1) ASME Section V (*Nondestructive Examination*)

   2) ASME Section IX (*Welding and Brazing Qualifications*).

c) Code of Federal Regulations, Title 49, Parts 100 through 185, *Transportation*.

d) American Petroleum Institute — API 579, *Fitness for Service*.

e) ADR 2003, *European Agreement Concerning the International Carriage of Dangerous Goods by Road*. (Published by the UN Economic Commission for Europe, Information Service, Palais des Nations, C7-1211 Geneve, Suisse.)

f) CGA 6-4.1, *Cleaning Equipment for Oxygen Service*.

g) CGA S-1.2, *Pressure Relief Device Standard*, Part 2: *Cargo and Portable Tanks for Compressed Gases*. (Published by the Compressed Gas Association, Inc. [CGA], 4221 Walney Road, Chantilly, VA 20151.)

h) IMDG Code 2002, *International Maritime Dangerous Goods Code* (including Amendment 31-02. (Published by the International Maritime Organization [IMO], 4 Albert Embankment, London, SE1 7SR England.)

i) RID 2003, *Carriage of Dangerous Goods*. (Published by the Intergovernmental Organization for International Carriage by Rail [OTIF], Gyphenhubeliweg 30, C7-3006 Bern, Switzerland.)

j) *United Nations Recommendations on the Transport of Dangerous Goods – Modal Regulations.* (Published by the United Nations Publications, 2 UN Plaza, New York, New York 10017.)

k) SSPC Publication #91-12, *Coating and Lining Inspection Manual*. (Published by Steel Structures Painting Council, 4400 Fifth Avenue, Pittsburgh, PA 15212-2683.)

S6.10 CONCLUSION

a) During any continued service inspections or tests of transport tanks, performed by the Registered Inspector, the actual operating and maintenance requirements as specified in this Supplement shall be satisfied. The Registered Inspector shall determine, based on the applicable requirements of the *Code of Federal Regulations*, Title 49, Parts 100 through 185, and NBIC Part 2, Supplement 6, whether the transport tank can continue to be safely operated.

b) Defects or deficiencies in the condition, operation, and maintenance requirements of the transport tank, including piping, valves, fittings, etc., shall be discussed with the owner or user of the transport tank at the time of inspection. Defects or deficiencies shall be corrected using the appropriate methods prior to returning the transport tank to service.

S6.11 PERSONNEL SAFETY AND INSPECTION ACTIVITIES

a) Proper inspection of transport tanks may require pre-inspection planning. This planning should include development of an inspection plan that will satisfy the applicable technical requirements of this Part, the *Code of Federal Regulations*, Title 49, Parts 100 through 185, Transportation, and appropriate safety considerations. The inspection plan should also include the applicable failure and deterioration mechanisms, and inspection methods and the requirements of the applicable Competent Authority.

b) This supplement describes pre-inspection and post-inspection activities applicable to all transport tanks. Specific inspection requirements for transport tanks are identified in NBIC Part 2, S6.13 for Cargo Tanks, S6.14 for Portable Tanks, NBIC Part 2, S6.15 for Ton Tanks.

c) Personnel safety is the joint responsibility of the owner or user and the Registered Inspector. All applicable safety regulations shall be followed. This includes, if applicable, all governmental rules and regulations. owner's or user's personnel safety programs and/or safety programs by the Inspector's employer or similar regulations such as confined space requirements also apply.

S6.12 TRANSPORT TANK ENTRY REQUIREMENTS

a) No transport tank shall be entered until it has been properly prepared for inspection. The owner or user and the Inspector shall determine that the transport tank may be entered safely. This shall include:

   1) Potential hazards associated with the entry into the transport tank have been identified by the owner or user and are brought to the attention of the Inspector, along with acceptable means or methods for mitigating each of these hazards;

   2) Coordination of entry into the transport tank by the Inspector and the owner or user representative(s) working in or near the transport tanks;

   3) If personal protective equipment is required to enter the transport tank, the necessary equipment is available, and the Inspector is properly trained in its use; and

   4) An effective energy isolation program is in place and in effect that will prevent the unexpected release of energy or media to enter the transport tanks.

b) The Inspector shall be satisfied that a safe atmosphere exists before entering the transport tank. The oxygen content of breathable atmosphere shall be between 19.5% and 23.5%.

c) The Inspector shall not be permitted to enter an area if toxic, flammable, or inert gases or vapors are present and above acceptable limits without proper personal protective equipment. Protective equipment may include, among other items, protective outer clothing, gloves, eye protection, foot protection, and/or respirators.

d) The Inspector shall have proper training governing the selection and use of any personal protective clothing and equipment necessary, particularly related to respiratory protection if the testing of the atmosphere of the transport tank reveals any hazards. This requirement is to ensure that the inspection may be performed safely.

S6.12.1 PRE-INSPECTION ACTIVITIES

a) Prior to conducting the inspection, a review of the history of the transport tank and a general assessment of current conditions shall be performed. This shall include a review of information, such as:

   1) Date of the last inspection;

   2) Current Inspection Certificate;

3) ASME Code Name Plate and/or Specification;

4) If applicable, National Board registration number;

5) Serial number of identification marking of the transport tank;

6) Operating conditions and normal contents of the transport tank;

7) Previous inspection report or inspection certificates;

8) Records of wall thickness checks, especially where corrosion is a consideration; and

9) Observations of the condition of the complete transport tank, including, piping, fitting, valves, etc.

b) The following activities should be performed as required to support the inspection:

1) Verify the pressure gages, thermometers, and indicating devices are in proper calibration;

2) Ensure that all overpressure protection devices are in proper operation, and that they are operating as designed; and

3) Ensure that all structural attachments are free of defects and are operating as designed.

S6.12.2 PREPARATION FOR INTERNAL INSPECTION

The owner or user has the responsibility to prepare a transport tank for internal inspection. Requirements for safety including occupational safety and health regulations (federal, state, local, or other), the owner's or user's own safety program, and the safety programs of the Inspector's employer are applicable for inspections. The transport tank shall be prepared in the following manner or as deemed necessary by the Inspector.

a) When a transport tank is connected to a common header with other transport tanks or in a system where liquids or gases are present, the transport tank shall be isolated by closing, locking, and/or tagging stop valves in accordance with the owner's or user's procedures.

b) When toxic or flammable materials are involved, additional safety precautions should require removing pipe sections or blanking pipelines before entering the transport tank. The means of isolating the transport tank shall be acceptable to the Inspector and in compliance with applicable occupational safety and health regulations.

c) The transport tank shall be allowed to cool or warm to ambient temperature at a rate to avoid damage to the transport tank.

d) The transport tank shall be drained of all liquid and shall be purged of any toxic or flammable gases or other contaminants that were contained in the transport tank. Mechanical ventilation using a fresh air blower or fan shall be started after the purging operation and maintained until all pockets of "dead air" that may contain toxic or flammable or inert gases are reduced to acceptable limits. During the air purging and ventilation of the transport tank involved with flammable gases, the concentration of the vapor in air should pass through the flammable range before a safe atmosphere is obtained. All necessary precautions shall be taken to eliminate the possibility of explosion or fire.

e) Manhole, if applicable, and handhole plates, washout plugs, inspection plugs, and any other item requested by the Inspector shall be removed.

f) The Inspector shall not enter a transport tank until all safety precautions have been taken. The temperature of the transport tank shall be such that the inspection personnel will not be exposed to excessive heat or cold. The transport tank should be cleaned as necessary.

g) A qualified person (attendant) shall remain outside the transport tank at the point of entry while the Inspector is inside and shall monitor activities inside and outside and communicate with the Inspector as necessary. The attendant shall have means of summoning rescue assistance, if needed, and to facilitate rescue procedures for those inside the transport tank without personally entering the transport tank.

Note: If a transport tank has not been properly prepared for an internal inspection, the Inspector shall decline to make the inspection.

S6.12.3 POST-INSPECTION ACTIVITIES

a) Any defects or deficiencies in the condition, operation, and maintenance practices of the transport tank and auxiliary equipment shall be reported to the owner or user, including recommendations for correction.

b) Documentation of inspections shall contain pertinent data such as a description of the transport tank, classification (Class 1, 2, or 3), the transport tank identification number, inspection intervals, date of inspection, type of inspection, or type of test performed, and any other information required by the Competent Authority. The Inspector shall sign, date, and note any deficiencies, comments, or recommendations on the inspection report. The Inspector should retain and distribute copies of the inspection report as required.

S6.13 INSPECTION AND TESTS OF CARGO TANKS

All cargo tanks shall be examined and tested at frequencies specified in NBIC Part 2, Table S6.13. The examination and tests shall provide for a visual external, visual internal, leakage test, pressure test, thickness test, and lining test. It should be noted that the information in NBIC Part 2, Table S6.13 is a summary of United States Code of Federal Regulations, Title 49, Part 180. The user shall compare the requirements provided with Part 180 to ensure full compliance.

TABLE S6.13
PERIODIC INSPECTIONS AND TESTS

Test or Inspection (cargo tank specification, configuration, and service)	Date by which first test must be completed (see Note 1)	Interval period after first test
External Visual Inspection		
All cargo tanks designed to be loaded by vacuum with full opening rear heads	September 1, 1991	6 Months
All other cargo tanks	September 1, 1991	1 Year
Internal Visual Inspection		
All insulated cargo tanks, except MC 330, MC 331, & MC 338 (see Note 4)	September 1, 1991	1 Year
All cargo tanks transporting lading corrosive to the tank	September 1, 1991	1 Year
All other cargo tanks, except MC 338	September 1, 1995	5 Years
Lining Inspection		
All lined cargo tanks transporting lading corrosive to the tank	September 1, 1991	1 Year
Leakage Test		
MC 330 and MC 331 cargo tanks in chlorine service	September 1, 1991	2 Years
All other cargo tanks, except MC 338	September 1, 1991	1 Year
Pressure Test		
Hydrostatic or Pneumatic (see Notes 2 and 3)	—	—
All cargo tanks which are insulated with no manhole or insulated and lined, except MC 338	September 1, 1991	1 Year
All cargo tanks designed to be loaded by vacuum with full opening heads	September 1, 1992	2 Years
MC 330 and MC 331 cargo tanks in chlorine service	September 1, 1992	2 Years
All other cargo tanks	September 1, 1995	5 Years
Thickness Test		
All unlined cargo tanks transporting material corrosive to the tank, except MC 338	September 1, 1992	2 Years

Note 1:

If a cargo tank is subject to an applicable inspection or test requirement under the regulations in effect on December 30, 1990, and the due date (as specified by a requirement in effect on December 30, 1990) for completing the required test occurs before the compliance date listed in the Table, the earlier date applies.

Note 2:

Pressure testing is not required for MC 300 and MC 331 cargo tanks in dedicated sodium metal service.

Note 3:

Pressure testing is not required for uninsulated lined cargo tanks with a design pressure of MAWP 103 kPa (15 psi) or less, which receive an external visual inspection and lining inspection at least once each year.

Note 4:

Insulated cargo tanks equipped with manholes or inspection openings may receive either an internal visual inspection in conjunction with the external visual inspection or a hydrostatic or pneumatic test of the cargo tank.

S6.13.1 VISUAL EXTERNAL INSPECTION

a) Visual inspections are required of the complete cargo tank as required in NBIC Part 2, Table S6.13. The visual inspection shall include the heads, shell, nozzle connections, support attachments, all welded seams (longitudinal and circumferential), nozzle attachment welds, support, piping, appurtenances, structural attachments, and any attachment welds for possible defects. The visual inspection shall include a thorough examination for scratches that affect the pressure-retaining capabilities of the cargo tank, dents, leaks, distortions, corroded or abraded areas, and any other condition that would affect the safe operation of the cargo tank. If the cargo tank is able to be externally inspected, this must be noted in the inspection report of the cargo tank.

b) If the cargo tank is insulated and equipped with an internal lining, the following inspections shall be performed:

   1) Insulated cargo tanks — If the insulation on the cargo tank precludes a complete and thorough external visual inspection, the cargo tank shall be subjected to an internal visual inspection, if equipped with a manhole or inspection openings. This inspection shall include all internal surfaces, including welds, nozzle attachments, and, if equipped, baffles, internal stiffeners, surge protection devices for defects, corrosion, and missing or loose attachment;

   2) Lined or coated, or those designed to preclude an internal visual inspection — If the cargo tank is externally lined, coated, or of a design that would prevent a complete and thorough external visual examination, the internal areas of the cargo tank that are not obstructed by the lining or coating shall be internally inspected;

   3) Lined or coated, or those so designed to preclude access to the internal surfaces — The cargo tank shall be subjected to a hydrostatic or pneumatic test in accordance with NBIC Part 2, S6.13.6;

   4) All corroded or abraded areas of a cargo tank wall must be thickness tested in accordance with the following procedures:

      a. Measurements must be made using a device capable of accurately measuring thickness within ± 0.051 mm (± 0.002 of an inch);

      b. Any individual performing thickness testing must be trained in the proper use of the thickness testing device in accordance with the testing device manufacturer's instructions;

      c. The minimum thickness requirements for the heads, shell baffle, and bulkhead, when used as tank reinforcement, shall meet the minimum thickness requirements for inservice requirements for cargo tank specifications MC 300, MC 303, MC 304, MC 306, MC 307, MC 310, MC 311 transport tanks, and MC 312 cargo tanks constructed of steel, steel alloys, aluminum, and aluminum alloys are based on 90% of the minimum manufactured thickness. Table S6.13.1-a, provides minimum inservice minimum thicknesses for steel and steel alloys. Table S6.13.1-b provides minimum thicknesses for aluminum and aluminum alloys.

TABLE S6.13.1-a

(15) INSERVICE MINIMUM THICKNESSES FOR STEEL AND STEEL ALLOYS

Minimum manufactured thickness (US "Manufacturers' Standard Gage for Steel Sheets" or inches)	Nominal decimal equivalent, mm (inches)	Inservice minimum reference, mm (inches)
19 gage	1.06 (0.0418)	0.97 (0.038)
18 gage	1.21 (0.0478)	1.09 (0.043)
17 gage	1.37 (0.0538)	1.22 (0.048)
16 gage	1.52 (0.0598)	1.37 (0.054)
15 gage	1.71 (0.0673)	1.55 (0.061)
14 gage	1.90 (0.0747)	1.70 (0.067)
13 gage	2.28 (0.0897)	2.06 (0.081)
12 gage	2.66 (0.1046)	2.39 (0.094)
11 gage	3.04 (0.1196)	2.74 (0.108)
10 gage	3.42 (0.1345)	3.07 (0.121)
9 gage	3.80 (0.1495)	3.43 (0.135)
8 gage	4.18 (0.1644)	3.76 (0.148)
7 gage	4.55 (0.1793)	4.09 (0.161)
3/16 inch	4.76 (0.1875)	4.29 (0.169)
1/4 inch	6.35 (0.2500)	5.72 (0.225)
5/16 inch	7.94 (0.3125)	7.14 (0.281)
3/8 inch	9.53 (0.3750)	8.59 (0.338)

TABLE S6.13.1-b
INSERVICE MINIMUM THICKNESSES FOR ALUMINUM AND ALUMINUM ALLOYS

Minimum manufactured thickness, mm (inches)	Inservice minimum thickness, mm (inches)
1.98 (0.078)	1.78 (0.070)
2.21 (0.087)	1.98 (0.078)
2.44 (0.096)	2.18 (0.086)
2.77 (0.109)	2.49 (0.098)
3.30 (0.130)	2.97 (0.117)
3.58 (0.141)	3.23 (0.127)
3.84 (0.151)	3.45 (0.136)
4.37 (0.172)	3.94 (0.155)
4.39 (0.173)	3.96 (0.156)
4.93 (0.194)	4.44 (0.175)
5.49 (0.216)	4.93 (0.194)
6.02 (0.237)	5.41 (0.213)
6.86 (0.270)	6.17 (0.243)
9.14 (0.360)	8.23 (0.324)
11.40 (0.450)	10.30 (0.405)
13.70 (0.540)	12.30 (0.486)

S6.13.2 INSPECTION OF PIPING, VALVES, AND MANHOLES

The cargo tank piping, valves, and gaskets must be carefully inspected for corroded areas and the piping system and valve attachment welds or threads must be inspected for corrosion, leakage, or any other defects that might render the cargo tank unsafe for transportation service. This examination shall include:

a) All devices for securing manhole covers must be in satisfactory working condition, and the area must not show any evidence of leakage at either the manhole cover or the manhole gasket;

   1) When inspecting gaskets on any full opening of the cargo tank, the inspector should visually examine the gasket for defects to include cracks and/or splits that may prevent the gasket material from sealing properly;

   2) If the gasket shows any evidence of cuts or cracks that are likely to cause failure, the gasket shall be replaced;

b) All emergency devices and valves including self-closing stop valves, excess flow valves, and remote closure devices must be free of corrosion, distortion, erosion, and any external damage that will prevent safe operation of the cargo tank. Remote closure devices and self-closing stop valves must be operated during inspection to demonstrate that the devices are operating as designed;

c) Any missing bolts, nuts, and fusible links or elements shall be replaced. Loose bolts and nuts must be tightened;

d) All re-closing pressure relief valves shall be externally inspected for any corrosion or damage that might prevent the device from operating as designed;

1) All re-closing pressure relief valves on cargo tanks carrying lading corrosive to the pressure relief valve shall be removed from the cargo tank for inspection and testing;

2) Each re-closing pressure relief valve required to be removed and tested as specified in d) 1) above must open at the required test pressure and reseat to a leak-tight condition at 90% of the set-to-discharge pressure or the pressure prescribed for the applicable cargo tank specifications.

S6.13.3 INSPECTION OF APPURTENANCES AND STRUCTURAL ATTACHMENTS

a) Major appurtenances, as defined in CFR 49, 180.407 (d)(2)(viii), include but are not limited to suspension system attachments, connecting structures, and those elements of the upper coupler (kingpin) assembly that can be inspected without dismantling the upper coupler (kingpin) assembly. Major appurtenances shall be inspected for any corrosion or damage that might prevent safe operations.

b) If the cargo tank transports lading that is corrosive to the cargo tank, the upper coupler (kingpin) assembly must be inspected at least once in a two-year period. The upper coupler (kingpin) shall be removed for inspection of the following:

1) Corroded and abraded areas;

2) Dents;

3) Distortions;

4) Weld failures; and

5) Any other condition that might render the cargo tank unsafe for transportation service.

c) If the cargo tank is constructed of mild-or high-strength low-alloy steel and employs ring stiffeners or other appurtenances that create air cavities adjacent to the ring stiffeners or other appurtenances to the cargo tank's shell and these areas cannot be visually externally inspected, then the following shall be performed:

1) A thickness test on the stiffener rings shall be performed at least once every two years of at least four symmetrically distributed readings to establish an average thickness for the ring stiffener or appurtenance. The thickness requirements are specified in NBIC Part 2, Tables S6.13.1-a or S6.13.1-b, as applicable;

2) If any of the thickness testing readings for the ring stiffeners are less than the average thickness by more than 10%, thickness testing must be performed from inside the transport tank on the area of the tank wall covered by the appurtenance or ring stiffener. If the results of the thickness test of the transport tank fail to conform to the minimum thickness requirements prescribed for the design as manufactured, the tank must be repaired or removed from hazardous material service. The owner of the transport tank can de-rate the tank to transport authorized material and reduced maximum weight of lading, reduce pressure, or a combination thereof under the following conditions:

a. The reduced loadings, based on the cargo tank's design conditions and material thicknesses, are appropriate for the reduced loading conditions. This reduced loading shall be certified by a Design Certifying Engineer, and a revised manufacturer's certificate shall be issued reflecting these reduced loading conditions;

b. The cargo tank motor vehicle's manufacturer's nameplate shall be revised to reflect the reduced limits;

c. If a. and b. above cannot be satisfied, the owner of the cargo tank should not return the cargo tank to hazardous material service. The owner shall remove, or obliterate, or in a secure manner cover the tank's specification plate; and

d. The Inspector shall record the results of the thickness test on the cargo tank's inspection report.

S6.13.4 VISUAL INTERNAL INSPECTION

When performing an internal visual inspection of a cargo tank and the cargo tank is equipped with a manhole or an inspection opening, the Inspector shall examine the internal surfaces for corroded and abraded areas, dents, distortions, defects in welds, and any other conditions that might render the cargo tank unsafe for transportation service. As a minimum the inspection shall include:

a) The internal surfaces of the cargo tank shell and heads, and appurtenances such as baffles, clips, pads, piping or other internals;

b) Linings or coatings installed to prevent corrosion to the cargo tank wall shall be inspected in accordance with NBIC Part 2, S6.13.5 and Table S6.13.4;

c) When baffle assemblies prevent access required to perform the inspection of the interior surfaces of the cargo tanks or other interior appurtenances, either the entire baffle assembly or part thereof shall be detached to allow access or, other alternative means of inspection such as the use of boroscopes or cameras must be utilized;

d) For cargo tanks equipped with baffle assemblies, the baffle panels and the means of their attachment to the cargo tank wall shall be inspected for: weld defects, cracks, corrosion, deterioration at point of attachment, loose bolting, distortion or any other condition that might affect the structural integrity of the baffle assembly:

   1) Baffle panels that cannot be inspected, as installed, shall be detached or removed for inspection;

   2) Cracked or corroded baffle clips shall be replaced with material whose properties are equivalent to the material used for the cargo tank wall or material approved by a Design Certifying Engineer;

   3) For baffle clips welded directly to the cargo tank wall on tanks constructed of quenched and tempered steel, the clip shall be examined for cracks using surface Non Destructive Examination (NDE) methods such as PT and MT. The attachment weld to the cargo tank wall shall be examined for cracks using the Wet Fluorescent Magnetic Particle method. NDE must be in accordance with Section V of the ASME Code;

   4) Damaged or worn baffle panels shall be repaired or replaced. Particular attention must be given to bolt holes that are enlarged from original shape or size. Bolting that is worn shall be replaced;

e) If the cargo tank is not equipped with a manhole or inspection opening, or is welded closed and the cargo tank has not transported a lading that is corrosive to the cargo tank wall, it shall be subjected to a pressure test as provided in NBIC Part 2, Tables S6.13.4 and S6.13.6.

TABLE S6.13.4
PERIODIC INSPECTIONS AND TESTS

Test or Inspection (cargo tank specification, configuration, and service)	Test and Inspection Interval After Original Certification Date
External Visual Inspection	
All cargo tanks designed to be loaded by vacuum with full opening rear heads	6 Months
All other cargo tanks	1 Year
Internal Visual Inspection	
All insulated cargo tanks, except MC 330, MC 331, & MC 338	1 Year
All cargo tanks transporting lading corrosive to the tank	1 Year
All other cargo tanks, except MC 338	5 Years
Lining Inspection	
All lined cargo tanks transporting lading corrosive to the cargo tank	1 Year
Leakage Test	
MC 330 and MC 331 cargo tanks in chlorine service	2 Years
All other cargo tanks, except MC 338	1 Year
Pressure Test (Note 1: sodium metal; Note 2: MAWP < 15 psig)	
All cargo tanks which are insulated with no manhole or insulated and lined, except MC 338	1 Year
All cargo tanks designed to be loaded by full vacuum with full opening in the rear head of the cargo tank	2 Years
MC 330 and MC 331 cargo tanks in chlorine service	2 Years
All other cargo tanks	5 Years
Thickness Test	
All unlined cargo tanks in corrosive service, except MC 338	2 Years

Note 1:

Pressure testing is not required for MC 300 and MC 331 cargo tanks in dedicated sodium metal service.

Note 2:

Pressure testing is not required for uninsulated lined cargo tanks with a design pressure of MAWP 103 kPa (15 psi) or less, which receive an external visual inspection and lining inspection at least once each year.

S6.13.5 LINING INSPECTIONS

Cargo tank linings include rubber linings and linings other than rubber (elastomeric materials) that are used to protect the tank from corrosion or other harmful effects of the lading material being transported. The inspection requirements are:

a) Rubber linings must be inspected for holes by using a high-frequency spark tester, as described in this section. If holes are found, they must be repaired using equipment and procedures prescribed by the lining manufacturer or lining installer;

b) Linings other than rubber (elastomeric materials) must be inspected and tested in accordance with procedures using equipment and procedures prescribed by the lining manufacturer or lining installers; and

c) If degraded or defective areas of the cargo tank lining are discovered, the lining in these areas shall be removed and the thickness of the cargo tank wall area under the lining defect shall be tested in accordance with the following:

    1) Measurements shall be made using a device capable of accurately measuring thickness to within ± 0.051 mm (± 0.002 of an inch);

    2) The individuals performing the thickness test must be trained in the proper use of the thickness testing device in accordance with the manufacturer's instructions; and

    3) The minimum inservice thickness requirements for series MC 300 cargo tanks for steel and steel alloy and aluminum and aluminum alloy material is specified in NBIC Part 2, Tables S6.13.1-a and S6.13.1-b.

S6.13.6 PRESSURE TESTS

Cargo tanks may be tested by either the hydrostatic or pneumatic test method. When performing a pressure test, the test procedure shall include the test method (hydrostatic or pneumatic) used for the cargo tank, and the test shall include all appurtenances, all baffles, bulkheads, and upper coupler (fifth wheel) that comprise the cargo tank and shall be pressure tested at pressures established in NBIC Part 2, Table S6.13.6. The pressure test procedure shall include the following:

a) The pressure test shall be performed in accordance with a test pressure that includes provision for the inspector to perform an internal and external visual inspection of all surfaces of the cargo tank. For MC 338 cargo tanks, and cargo tanks not equipped with a manhole, an internal visual inspection is not required.

    1) The visual external inspection shall be conducted while the cargo tank is under test pressure.

    2) The visual internal inspection shall be conducted after the pressure test is completed.

b) When performing the pressure test all self-closing pressure relief valves, including emergency relief vents, and normal vents shall be removed for inspection and test, except for line safety devices that may be removed or left in place.

    1) Each self-closing pressure relief valve that is an emergency relief vent shall be capable of opening at the required set pressure and seat to a leak-tight condition at 90% of the set-to-discharge pressure, or the pressure prescribed for the applicable cargo tank. It should be noted that self-closing pressure relief valves not tested or failing the pressure test must be repaired or replaced;

    2) Normal vents 6.895 kPa (1 psig) shall be tested according to the testing criteria established by the valve manufacturer.

c) If the cargo tank is not carrying a corrosive lading, all areas that are covered by the upper coupler (fifth wheel) assembly must be inspected for corroded, abraded areas, dents, distortions, defects in welds, and any other condition that might render the tank unsafe for transport service. The upper coupler (fifth wheel) assembly must be removed from the cargo tank for this inspection.

d) If the cargo tank motor vehicle has multiple cargo tanks, each cargo tank shall be tested separately. The adjacent cargo tanks shall be empty and at atmospheric pressure.

e) When performing the hydrostatic or pneumatic test, the following requirements shall be specified in the test procedure:

1) All closures, except the pressure relief device, shall be in place during the test;

2) All required loading and unloading venting devices that are rated less than the test pressure may be removed during the test, or:

a. If the venting devices are not removed, the device shall be rendered inoperative by clamps, plugs, or other equally effective restraining devices;

b. The restraining devices shall not prevent detection of leaks or damage of the venting device and shall be removed immediately after the test.

TABLE S6.13.6
PRESSURE TEST REQUIREMENTS

Cargo Tank Specification	Test Pressure
MC 300, MC 301, MC 302, MC 303, MC 305, and MC 306	20.7 kPa (3 psig) or design pressure, whichever is greater
MC 304 and MC 307	275.8 kPa (40 psig) or 1.5 times design pressure, whichever is greater
MC 310, MC 311, and MC 312	20.7 kPa (3 psig) or 1.5 times design pressure, whichever is greater
MC 330 and MC 331	1.5 times either MAWP or the re-rated pressure, whichever is applicable
MC 338	1.25 times either MAWP or the re-rated pressure, whichever is applicable
DOT 406	34.5 kPa (5 psig) or 1.5 times the MAWP, whichever is greater
DOT 407	275.8 kPa (40 psig) or 1.5 times the MAWP, whichever is greater
DOT 412	1.5 times the MAWP

S6.13.6.1 HYDROSTATIC OR PNEUMATIC TEST METHOD

a) The owner or user of the cargo tank may apply either the hydrostatic or pneumatic test method to satisfy the requirements of the pressure test specified in NBIC Part 2, Table S6.13.4.

b) If the hydrostatic test method is used, the cargo tank shall be completely filled including, if equipped, its dome with water or other liquids having similar viscosity. During the hydrostatic test, the Inspector shall:

1) Ensure that the cargo tank is completely filled and free of any air pockets. During this operation, the liquid should flow freely out of the cargo tank's test vent;

2) Ensure that the temperature of the test media does not exceed 38°C (100°F);

3) Ensure that the test pressure cannot exceed the test pressures specified in NBIC Part 2, Table S6.13.6;

4) Ascertain that the test pressure shall be maintained for a minimum of 10 minutes; and

5) Visually examine the cargo tank for leakage, bulging or other defects. If any of the preceding occurs, terminate the test, drain the cargo tank, and evaluate the cargo tank's capabilities for repair or replacement of the affected areas.

c) If the owner and/or user elect to use the pneumatic test method, precaution should be employed due to the possibility of failure of the cargo tank under pneumatic test pressure conditions. The test area should be limited to the authorized personnel only and the test personnel shall be experienced in the pneumatic testing method. The pneumatic test pressure for the cargo tank shall be:

1) Gradually increased to one-half the test pressure;

2) After reaching one-half the test pressure, the test pressure shall be increased at a rate of approximately one-tenth of the test pressure until the test pressure is reached. The test pressure shall not exceed the test pressures specified in NBIC Part 2, Table S6.13.6;

3) When the test pressure is reached, the test pressure shall be held for a least 5 minutes, then reduced to the MAWP of the cargo tank;

4) At MAWP the inspector shall examine the cargo tank for any leakage, bulging, or any other defects; and

5) Visually examine the cargo tank for leakage, bulging, or other defects. If any of the preceeding occurs, terminate the test, drain the cargo tank of all air or inert gas, and evaluate the cargo tank's suitability for repairs or replacement of the affected areas.

S6.13.6.2 PRESSURE TESTING INSULATED CARGO TANKS

a) When pressure testing an insulated cargo tank, the insulations and jacketing are not required to be removed, unless it is not possible to reach the test pressure and maintain a condition of pressure equilibrium after the test pressure is reached, or the vacuum integrity cannot be maintained in the insulation space.

b) For MC 338 cargo tanks that transport refrigerated liquid, flammable gas, or oxygen, if the cargo tank is opened for any reason, the cleanliness of the cargo tank shall be verified prior to closure as required by CFR Title 49, Part 178.338-15.

S6.13.6.3 PRESSURE TESTING CARGO TANKS CONSTRUCTED OF QUENCHED AND TEMPERED STEELS

When testing MC 330 and MC 331 cargo tanks constructed of quenched and tempered steels, in accordance with ASME Section XII, Modal Appendix 1, and for cargo tanks constructed prior to the adoption of ASME Section XII, Part UHT of ASME Section VIII, Div. 1, or constructed of other quenched and tempered steel, without postweld heat treatment, used for the transportation of anhydrous ammonia or any other hazardous material that are subject to stress corrosion cracking, and the transportation of liquefied petroleum gas, the following is required:

a) The cargo tanks must be subjected to an internal visual inspection of all internal surfaces of the cargo tank using the wet fluorescent magnetic particle examination method immediately prior to performing the required pressure test;

b) The fluorescent magnetic particle examination has to be performed in accordance with ASME Section V.

c) The required pressure test as specified in NBIC Part 2, Table S6.13.4 shall be required.

S6.13.6.4 PRESSURE TESTING CARGO TANKS EQUIPPED WITH A HEATING SYSTEM

If the cargo tank is equipped with a heating system, employing a medium such as, but not limited to, steam or hot water hydrostatically, pressure is as follows:

a) The cargo tank must be tested at least once every 5 years;

b) The test pressure for the heating system shall be at least to the maximum system design operating pressure;

c) The test pressure shall be maintained for a least 5 minutes; and

d) If the heating system employs flues for heating the lading, the flues must be tested to ensure that the lading cannot leak into the flues or into the atmosphere.

S6.13.6.5 EXCEPTIONS TO PRESSURE TESTING

a) MC 330 and MC 331 cargo tanks that are in dedicated sodium metal service are not required to be pressure tested.

b) Un-insulated cargo tanks, with a design pressure or MAWP of 103 kPa (15 psig) or less, which can be externally visually inspected and a lining inspection at least once every 5 years, are not required to be pressure tested.

S6.13.6.6 ACCEPTANCE CRITERIA

a) The acceptance criteria for the hydrostatic or pneumatic pressure test of the heating system is based on the cargo tank's capabilities to successfully pass the pressure test, without showing evidence of permanent distortion or other evidence of weakness that might render the cargo tank unsafe for transportation service.

b) If the cargo tank does not satisfy the requirements for the pressure test of the heating system identified in a) above, the cargo tank cannot be returned to transportation service, unless:

   1) Cargo tanks with a heating system, which does not hold pressure, should remain inservice as an unheated cargo tank, if the heating system remains in place and is structurally sound and no lading may leak into the heating system; and

   2) The specification information for the heating system on the nameplate is changed to indicate that the cargo tank has no working heating system.

S6.13.6.7 INSPECTION REPORT

a) The Inspector shall prepare a written inspection report that identifies the results of the pressure test and specifies the following:

   1) Manufacturer's serial number of the cargo tank;

   2) Name of the cargo tank manufacturer;

   3) DOT or MC specification number;

   4) MAWP of the cargo tank;

   5) Minimum thickness of the head and shell of the cargo tank;

   6) Identify whether the cargo tank is lined, insulated, or both; and

   7) Identify if the cargo tank is for special service, i.e., transport material corrosive to the cargo tank, dedicated service, etc.

b) The written inspection report shall provide for the following additional information:

   1) The type of test or inspection performed;

   2) Date of the test or inspection (month and year).

c) Listing of all items tested or inspected, including information about pressure relief valve:

1) If the relief valve is removed, inspected and tested, or replaced;

2) If applicable, the type of device;

3) Set to discharge pressure at which the device will reseat; or

4) If the device was reinstalled, repaired, or replaced.

d) Information regarding the inspection of the upper coupler (fifth wheel) assembly, and when applicable:

1) If the coupler assembly (fifth wheel) was visually inspected in place; or

2) If the coupler assembly (fifth wheel) was removed for examination.

e) Information regarding leakage, and type of pressure test (hydrostatic or pneumatic);

f) The test pressure and holding time during the test;

g) Location of defects found and the method of repair;

h) Minimum thickness of the cargo tank's heads and shells, as specified in NBIC Part 2, Table S6.13.1-a or Table S6.13.1-b, as applicable;

1) Name and address of the person performing the test;

2) Registration number of the facility or person performing the test;

3) Continued qualification statement, such as:

a. "Cargo tank meets the requirements of DOT specification identified in this report."

b. "Cargo tank fails to meet the requirements of the DOT specification identified in this report.

i) DOT registration number of the Registered Inspector, and dated signature of the Registered Inspector and the cargo tank owner.

j) The owner and the motor carrier shall retain a copy of the test and inspection reports until the next test or inspection of the same type is successfully completed. This requirement does not apply to a motor carrier leasing a cargo tank for fewer than 30 days.

S6.13.7 ADDITIONAL REQUIREMENTS FOR MC 330 AND MC 331 CARGO TANKS

After completion of the pressure test, each motor carrier operating a Specification MC 330 and MC 331 cargo tank in anhydrous ammonia, liquefied petroleum gas, or any other service that is prone to stress corrosion cracking, shall make a written report containing the following information:

a) Carrier's name, address of principal place of business, and telephone number;

b) Complete identification plate data required by Specification MC 330 and MC 331 cargo tanks, including data required by the *ASME Boiler and Pressure Vessel Code*;

c) Carrier's equipment number;

d) Statement indicating whether or not the cargo tank was stress relieved after fabrication;

e) Name and address of the person performing the test and date of the test;

f) Statement of the nature and severity of any defects found. As a minimum, the information shall include:

1) Identification of the location of the defects detected, such as in weld, heat-affected zone, the liquid phase, the vapor phase, or the head to shell seam; or

2) If no defects or damage were discovered, this also shall be reported.

g) Statement indicating the methods employed to make repairs; that made the repairs; and the date the repairs were completed. If the cargo tank was stress relieved after the repairs were completed, whether full or local stress relieving was performed;

h) Statement of the disposition of the cargo tank, such as:

1) "cargo tank scrapped"; or

2) "cargo tank returned to service."

i) Statement as to whether or not the cargo tank is used in anhydrous ammonia service that is subject to stress corrosion cracking. If the cargo tank had been used in anhydrous ammonia service since the last report, the owner has to provide a statement in the report indicating whether each shipment of ammonia was certified by its shipper as containing at least 0.2% water by weight.

j) A copy of the written inspection report must be retained by the carrier at its principal place of business during the period the cargo tank is in the carrier's service and for one year thereafter.

k) Upon written request to, and with the approval of the Field Administrator, Regional Service Center, and Federal Motor Carrier Safety Administration for the region in which a motor carrier has its principal place of business, the carrier may maintain the reports at a regional or terminal office.

S6.13.8 CERTIFICATES AND REPORTS

a) Each person offering a DOT specification cargo tank for sale or lease must provide the purchaser or lessee with the following:

1) A copy of the cargo tank certificate of compliance;

2) If applicable, a copy of the record of repair, modification, stretching, or rebarrelling; and

3) The most recent inspection and test reports.

b) Copies of the documents and reports identified in a) above must be provided to the lessee if the cargo tank is leased for more than 30 days.

S6.13.9 LEAKAGE TEST

When leakage testing is required by NBIC Part 2, Table S6.13.4, the test shall include testing the product piping with all valves and accessories in place and operative, except that any venting devices set to discharge at less than the leakage test pressure must be removed or rendered inoperative during the test. The leakage test shall include:

a) All internal or external self-closing stop valves must be tested for leakage;

b) Each cargo tank of a multi-cargo tank motor vehicle must be tested with the adjacent cargo tanks empty and at atmospheric pressure;

c) The leakage test shall be maintained for a minimum of 5 minutes;

d) Cargo tanks in liquefied compressed gas service shall be:

1) Inspected externally for leaks during the leakage test;

2) Suitable safeguards must be provided to protect personnel should a failure occur, as follows:

   a. Cargo tanks may be leakage tested with the hazardous material in the cargo tank during the test;

   b. The leakage test pressure shall not be less than 80% of the MAWP marked on the specification plate, unless the cargo tank has a MAWP of 690 kPa (60 psig) or more, in which case it should be leakage tested at its maximum normal operating pressure provided it is in dedicated service or services;

   c. MC 330 or MC 331 cargo tanks in dedicated liquefied petroleum gas service may be leakage tested at not less than 414 kPa (60 psig);

   d. An operator of a MC 330 or MC 331 cargo tank and a non-specification cargo tank equipped with a meter should check leak tightness of the internal self-closing stop valve by conducting a meter creep test; and

   e. A non-specification cargo tank is a cargo tank that conforms and is marked in conformance with the edition of the ASME Code in effect when the cargo tank was fabricated and should be used for the transportation of liquefied petroleum gas, provided the cargo tank satisfies the following:

      1. The cargo tank has a minimum design pressure no lower than 172 kPa (250 psig);

      2. The cargo tank has a water capacity of 13,250 l (3,500 gallons) or less.

3) The cargo tank has been manufactured in accordance with the ASME Code prior to January 1, 1981. This requirement requires the cargo tank to be stamped with the ASME Code Symbol Stamp and documented on an ASME Manufacturer's Data Report;

4) The cargo tank shall conform to the applicable provisions of NFPA 58, except if NFPA is inconsistent with the requirements of Parts 178 and 180 of Title 49;

5) The cargo tank shall be leakage tested in accordance with NBIC Part 2, Table S6.13.4;

6) MC 330 and MC 331 cargo tanks in dedicated service for anhydrous ammonia may be leakage tested at not less than 414 kPa (60 psig);

7) Non-specification cargo tanks must be leakage tested at pressure of not less than 16.6 kPa (2.4 psig), if the cargo tanks comply with one of the following:

   a. For the transport of petroleum products that have a liquid capacity of 13,250 l (3,500 gal); and

   b. Permanently secured non-bulk tanks to a motor vehicle and protected against leakage or damage in the event of turnover, having a liquid capacity of less than 450 l (119 gal), used for transportation of a flammable liquid petroleum product.

8) The cargo tank is used to transport petroleum distillate fuels that are equipped with vapor collection equipment and should be leakage tested in accordance with the Environmental Protection Agency's "Model 27-Determination of Vapor Tightness of Gasoline Delivery Tank Using Pressure-Vacuum Test," as follows:

   a. The test method and procedures and maximum allowable pressure and vacuum changes are in 40 CFR 63.425(e)(1);

   b. The hydrostatic test alternative, using liquid in Environmental Protection Agency's "Method 27-Determination of Vapor Tightness of Gasoline Delivery Tank Using Pressure-Vacuum Test" should not be used to satisfy the leak testing requirements of this Section. The test shall be conducted using air; and

c. Cargo tanks equipped with vapor collection equipment should be leakage tested in accordance with 8) b. above.

9) Cargo tanks that fail to retain leakage test pressure shall not be returned to service as a specification cargo tank, unless all sources of leakage are properly repaired prior to returning the cargo tank to hazardous material service.

10) It is required that after July 1, 2000, that the Registered Inspector who performs inspections on MC 330 and MC 331 cargo tanks inspect the delivery hose assembly and the piping system of the cargo tank under leakage test pressure utilizing the rejection criteria for cargo tanks unloading liquefied compressed gas. It should be noted that an operator should remove and replace damaged sections or correct defects discovered as provided in NBIC Part 2, S6.13.10. If any of the following is discovered, it is cause for rejection:

a. No operator shall use a delivery hose assembly for liquefied compressed gas if it is determined that any of the following conditions exist:

1. Damage to the hose cover that exposes the reinforcement;

2. If the wire braid reinforcement is kinked or flattened so as to permanently deform the wire braid;

3. Soft spots when the hose is not under pressure, or any loose outer covering on the hose;

4. Damaged, slipping, or excessively worn hose couplings; and

5. Loose or missing bolts or fastenings on the bolted hose coupling assembly.

b. No operator can use a cargo tank with a piping system for unloading liquefied compressed gases if any of the following conditions exist:

1. Any external leaks identifiable without the use of instruments;

2. Bolting that is loose, missing, or severely corroded;

3. Manual stop valves that will not actuate; and

4. Rubber hose flexible connectors with any of the following conditions:

aa. Damage to the hose cover that exposes the reinforcement;

bb. If the wire braid reinforcement is kinked or flattened so as to permanently deform the wire braid;

cc. Soft spots when the hose is under pressure, or any loose outer covering on the hose;

dd. Damaged, slipping, or excessively worn hose couplings;

ee. Loose or missing bolts or fastenings on the bolted hose coupling assembly;

ff. Stainless steel flexible connectors with damaged reinforcement braid;

gg. Internal self-closing stop valves that fail to close or that permit leakage through the valve detectable without the use of instruments; or

hh. Pipes or joints that are severely corroded.

S6.13.10 NEW OR REPLACED DELIVERY HOSE ASSEMBLIES

The operator shall repair hose assemblies and place the cargo tank back in service if retested successfully in accordance with the following:

a) The new and/or replaced hose assembly is tested at a minimum of 120% of the hose's MAWP;

b) The operator shall visually examine the delivery hose assembly while it's under pressure;

c) If the test is successful, the operator shall ensure that the delivery hose assembly is permanently marked with the month and year of the test; and

d) It should be noted that after July 1, 2000, the operator shall complete a record documenting the test and inspection, which shall include the following:

   1) The date and signature of the Inspector that performed the inspection;

   2) The owner of the hose assembly;

   3) The hose identification number;

   4) The date of the original delivery of the hose assembly and tests;

   5) Notes of any defects observed;

   6) Any repairs that may have been made; and

   7) Identification in the written report that the delivery hose assembly passed or failed the tests and inspections.

S6.13.10.1 THICKNESS TESTING

a) Thickness testing of the head and shell of unlined cargo tanks used for the transportation of materials corrosive to the cargo tank shall be measured at least once every two years.

b) Cargo tanks measuring less than the sum of the minimum prescribed thickness in NBIC Part 2, Tables S6.13.1-a or S6.13.1-b, as applicable, plus one-fifth of the original corrosion allowance, shall be tested annually.

S6.13.10.2 TESTING CRITERIA

The testing criteria that shall be used for these requirements are as follows:

a) The measuring device shall be capable of accurately measuring thickness to within ± .50mm (.002 inch);

b) The individuals performing thickness testing shall be trained in the proper use of the thickness testing device used in accordance with the testing device manufacturer's instructions;

c) Thickness testing shall be performed in the following areas, as a minimum:

   1) Areas of the tank shell and heads, including around any piping that retains lading;

   2) Areas of high shell stress, such as the bottom center of the cargo tank;

   3) Areas near openings;

   4) Areas around weld joints;

5) Areas around shell reinforcements;

6) Areas around appurtenance attachments;

7) Areas near the upper coupler (fifth wheel) assembly attachments;

8) Areas near suspension system attachments and connecting structures;

9) Known thin areas in the tank shell and nominal liquid level lines; and

10) Connecting structures joining multiple cargo tanks of carbon steel in a self-supporting cargo tank motor vehicle.

S6.13.10.3 THICKNESS REQUIREMENTS

a) The minimum thickness for MC 300, MC 301, MC 302, MC 303, MC 304, MC 305, MC 306, MC 307, MC 310, and MC 312 cargo tanks are determined based on the definition of minimum thickness defined in CFR, Title 49, Part 178.320(a).

b) NBIC Part 2, Tables S6.13.1-a and S6.13.1-b, identify the “Inservice Minimum Thickness” values to determine the minimum thickness for the referenced cargo tank.

c) The tables are divided into three columns. The column headed “Minimum Manufactured Thickness” indicates the minimum values required for new construction of DOT 400 series cargo tanks.

d) The “Inservice Minimum Thicknesses” for cargo tanks specified in (a) above are based on 90% of the manufactured thickness specified in the DOT Specification, rounded off to three places.

S6.13.11 CARGO TANKS THAT NO LONGER CONFORM TO THE MINIMUM THICKNESS REQUIREMENTS IN NBIC PART 2, TABLES S6.13.1-a AND S6.13.1-b

If a cargo tank does not conform to the minimum thickness requirements in NBIC Part 2, Tables S6.13.1-a and S6.13.1-b, for the design as manufactured, the cargo tank should be used at a reduced maximum weight of lading or reduced MAWP, or combinations thereof, provided the following are met:

a) The cargo tank’s design and thickness are appropriate for the reduced loadings conditions as follows:

1) The cargo tank’s design and thickness for the appropriate reduced loading shall be certified by a Design Certifying Engineer;

2) A revised manufacturer’s certificate shall be issued; and

3) The cargo tank’s motor vehicle’s nameplate shall reflect the revised service limits.

b) It is required if a cargo tank no longer conforms with the minimum thickness requirements prescribed in the specification, that the cargo tank cannot be returned to hazardous material service. The cargo tank’s specification plate shall be removed, obliterated, or covered in a secure manner. The inspector shall require that the cargo tank is calculated to identify the thickness of the material as required in NBIC Part 2, S6.13.10.1 and S6.13.10.2, of this Section.

c) MC cargo tanks constructed prior to October 1, 2003, require the minimum thickness, minus the corrosion allowance as provided on the Manufacturer’s Data Report; and

d) MC cargo tanks constructed after October 1, 2003, require the minimum thickness will be the value indicated on the specification plate of the cargo tank. If no corrosion allowance is indicated on the Manufacturer’s Data Report, then the thickness of the cargo tank shall be the thickness of the material of construction indicated on the Manufacturer’s Data Report, with no corrosion allowance.

S6.13.11.1 MINIMUM THICKNESS FOR 400-SERIES CARGO TANKS

400 series cargo tanks are required to satisfy the minimum thickness requirements as established in Part 178.320(a) of Title 49 for DOT 406 cargo tanks, Part 178.347.2 of Title 49 for DOT 407 cargo tanks and Part 178.348.2 of Title 49 for DOT 412 cargo tanks.

S6.13.11.2 DOT 406 CARGO TANKS

a) It is required that all head, shell, bulkhead, and baffle materials used in the construction of DOT 406 cargo tanks satisfy Parts A and B of Section II of the *ASME Boiler and Pressure Vessel Code*,except that the following materials are authorized for cargo tanks constructed in accordance with *ASME Boiler and Pressure Vessel Code* that are not stamped with the "U" Code Symbol Stamp must be constructed out of ASTM materials permitted in Part 178.345-2 of Title 49. These materials are as follows:

   1) ASTM A 569,

   2) ASTM A 570,

   3) ASTM A 572,

   4) ASTM A 607,

   5) ASTM A 622,

   6) ASTM A 656, and

   7) ASTM A 715.

b) Aluminum alloys suitable for fusion welding and conforming with the O, H 32, or H 34 temper of one of the following ASTM Specifications may be used for cargo tanks constructed in accordance with the *ASME Boiler and Pressure Vessel Code*:

   1) ASTM B 209, Alloy 5052,

   2) ASTM B 209, Alloy 5086,

   3) ASTM B 209, Alloy 5154,

   4) ASTM B 209, Alloy 5254,

   5) ASTM B 209, Alloy 5454, and

   6) ASTM B 209, Alloy 5652.

c) All heads, bulkheads, and baffles must be of O temper (annealed) or stronger temper. All shell material shall be of H 32, or H 34 temper, except that the lower ultimate strength temper should be used if the minimum shell thicknesses in the tables are increased in proportion to the lesser ultimate strength.

d) NBIC Part 2, Table S6.13.11.2-a, specifies the minimum thickness requirements for heads or bulkheads and baffles when used as tank reinforcement that is based on the volume capacity in liters per mm (gallons per inch) of length for MC 406 cargo tanks constructed out of Mild Steel (MS), High-Strength Low -Alloy Steel (HSLA), Austenitic Stainless Steel (SS), or Aluminum (AL).

e) NBIC Part 2, Table S6.13.11.2-b specifies the minimum thickness requirements for shell based on the cargo tank motor vehicle rated capacity in gallons when the cargo tank is constructed out of Mild Steel (MS), High-Strength Low-Alloy Steel (HSLA), Austenitic Stainless Steel (SS), or Aluminum (AL). The thickness requirements in these tables are specified in decimal of a mm (inch) after forming.

TABLE S6.13.11.2 -a
MINIMUM THICKNESS FOR HEADS

Materials	Volume capacity in liter per mm of length (gallons per inch of length)								
	14 (0.21) or less			Over 14 to 23 (0.21 to 0.36)			Over 23 (0.36)		
	MS	HSLA SS	AL	MS	HSLA SS	AL	MS	HSLA SS	AL
Thickness, mm (in.)	2.54 (.100)	2.54 d(.100)	4.06 (0.160)	2.92 (0.115)	3.94 (.155)	4.39 (0.173)	3.28 (.129)	3.28 (.129)	4.75 (0.187)

TABLE S6.13.11.2-b
MINIMUM THICKNESS FOR SHELLS, IN. (MM)

Cargo tank motor vehicle rated capacity in liters (gallons)	MS	SS/HSLA	AL
More than 0 to at least 4,500 (0 to 17,000)	2.54 (0.100)	2.54 (0.100)	3.84 (0.151)
More than 4,500 to at least 8,000 (17,000 to 30,300)	2.92 (0.115)	2.54 (0.100)	4.06 (0.160)
More than 8,000 to at least 14,000 (30,300 to 53,000)	3.28 (0.129)	3.28 (0.129)	4.39 (0.173)
More than 14,000 (53,000)	3.63 (0.143)	3.63 (0.143)	4.75 (0.187)
Note: The maximum distance between bulkhead, baffles, or ring stiffeners shall not exceed 1,525 mm (60 inches)			

S6.13.11.3 DOT 407 CARGO TANKS

a) It is required that the type of materials used for DOT 407 cargo tanks, depending on the type of media being transferred be either Mild Steel (MS), High-Strength Low-Alloy Steel (HSLA), Austenitic Stainless Steel (SS), or Aluminum.

b) The minimum required thicknesses of materials specified in NBIC Part 2, Table S6.13.11.3-a, for DOT 407 cargo tanks, when the minimum thickness requirements are based on the volume capacity in liters per sq mm (gallons per square inch) for the cargo tank's heads, or bulkheads and baffles, when these items are used for reinforcement purposes. All thicknesses are expressed in decimals of a mm (inch) after forming.

c) The minimum required thicknesses of materials are specified in NBIC Part 2, Table S6.13.11.3-b, for DOT 407 cargo tanks, when the minimum thickness requirements are based on the volume capacity in liters per sq. mm (gallons per square inch) for the cargo tank shell. All thicknesses are expressed in decimals of a mm (inch) after forming.

TABLE S6.13.11.3-a
MINIMUM THICKNESS FOR HEADS (DOT 407), MM (IN.)

Volume capacity sq. mm (in gal./sq. in. l/)	10 (0.122) or less	Over 10 to 14 (0.122 to 0.171)	Over 14 to 18 (0.171 to 0.22)	Over 18 to 22 (0.22 to 0.268)	Over 22 to 26 (0.268 to 0.317)	Over 26 to 30 (0.317 to 0.365)	Over 30 (0.365)
Thickness (MS)	2.54 (0.100)	2.54 (0.100)	2.92 (0.115)	3.28 (0.129)	3.28 (0.129)	3.63 (0.143)	3.96 (0.156)
Thickness (HSLA)	2.54 (0.100)	2.54 (0.100)	2.92 (0.115)	3.28 (0.129)	3.28 (0.129)	3.63 (0.143)	3.96 (0.156)
Thickness (SS)	2.54 (0.100)	2.54 (0.100)	2.92 (0.115)	3.28 (0.129)	3.28 (0.129)	3.63 (0.143)	3.96 (0.156)
Thickness (A)	4.06 (0.160)	4.06 (0.160)	4.39 (0.173)	4.75 (0.187)	4.92 (0.194)	5.49 (0.216)	6.02 (0.237)

TABLE S6.13.11.3-b
MINIMUM THICKNESS FOR SHELLS (DOT 407), MM (IN.)

Volume capacity in gal./sq. in. (l/sq. mm)	10 (0.122) or less	Over 10 to 14 (0.122 to 0.171)	Over 14 to 18 (0.171 to 0.22)	Over 18 to 22 (0.22 to 0.268)	Over 22 to 26 (0.268 to 0.317)	Over 26 to 30 (0.317 to 0.365)	Over 30 (0.365)
Thickness (MS)	2.54 (0.100)	2.54 (0.100)	2.92 (0.115)	3.28 (0.129)	3.28 (0.129)	3.63 (0.143)	3.96 (0.156)
Thickness (HSLA)	2.54 (0.100)	2.54 (0.100)	2.92 (0.115)	3.28 (0.129)	3.28 (0.129)	3.63 (0.143)	3.96 (0.156)
Thickness (SS)	2.54 (0.100)	2.54 (0.100)	2.92 (0.115)	3.28 (0.129)	3.28 (0.129)	3.63 (0.143)	3.96 (0.156)
Thickness (A)	3.84 (0.151)	3.84 (0.151)	4.06 (0.160)	4.39 (0.173)	4.92 (0.194)	5.49 (0.216)	6.02 (0.237)

S6.13.11.4 DOT 412 CARGO TANKS

a) It is required that the type of materials used for DOT cargo tanks, depending on the type of media being transferred be either Mild Steel (MS), High-Strength Low-Alloy Steel (HSLA), Austenitic Stainless Steel (SS), or Aluminum.

b) The minimum required thickness of materials are specified in NBIC Part 2, Table S6.13.11.4-a, for DOT 412 cargo tanks, when the minimum thicknesses requirements are based on the volume capacity in liters per sq mm (gallons per square inch) for cargo tank heads, or bulkheads and baffles, when these items are used for reinforcement purposes. All thicknesses are expressed in decimals of mm (inch) after forming.

c) The minimum required thicknesses of materials are specified in NBIC Part 2, Table S6.13.11.4-b, for DOT 412 cargo tanks, when the minimum thickness requirements are based on the volume capacity in liters per sq mm (gallons per square inch) for the cargo tank's shell. All thicknesses are expressed in decimals of mm (inch) after forming.

TABLE S6.13.11.4-a

MINIMUM THICKNESS FOR HEADS (DOT 412)

Volume Capacity (gallons per inch)	10 or less				Over 10 to 14				Over 14 to 18			18 and over		
Lading density at 60°F in lbs/gal.	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs	Over 16 lbs	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs	Over 16 lbs	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs
Thickness (inch), steel	0.100	0.129	0.157	0.187	0.129	0.157	0.187	0.250	0.157	0.250	0.250	0.157	0.250	0.312
Thickness (inch), aluminum	0.144	0.187	0.227	0.270	0.187	0.227	0.270	0.360	0.227	0.360	0.360	0.227	0.360	0.450

TABLE S6.13.11.4 M-a

MINIMUM THICKNESS FOR HEADS (DOT 412)

Volume Capacity (liters per millimeter)	0.122 l/mm or less				Over 0.122 to 0.21 l/mm				Over 0.21 to 0.22 l/mm			0.22 l/mm and over		
Lading density at 15°C in kg/l	1.2 kg/l and less	Over 1.2 to 1.6 kg/l	Over 1.6 to 1.9 kg/l	Over 1.9 kg/l	1.2 kg/l and less	Over 1.2 to 1.6 kg/l	Over 1.6 to 1.9 kg/l	Over 1.9 kg/l	1.2 kg/l and less	Over 1.2 to 1.6 kg/l	Over 1.6 to 1.9 kg/l	1.2 kg/l and less	Over 1.2 to 1.6 kg/l	Over 1.6 to 1.9 kg/l
Thickness (mm), steel	2.54	3.28	3.99	4.75	3.28	3.99	4.75	6.35	3.99	6.35	6.35	3.99	6.35	7.92
Thickness (mm), aluminum	3.66	4.75	5.77	6.86	4.75	5.77	6.86	9.14	5.77	9.14	9.14	5.77	9.14	11.4

TABLE S6.13.11.4-b

MINIMUM THICKNESS FOR SHELLS (DOT 412)

Volume capacity (gallons per inch)	10 or less				Over 10 to 14				Over 14 to 18			18 and over		
Lading density at 60°F in pounds per gallon	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs	Over 16 lbs	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs	Over 16 lbs	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs	10 lbs and less	Over 10 to 13 lbs	Over 13 to 16 lbs
Thickness (inch), steel Distances between heads (and bulkheads, baffles, and ring stiffeners when used as tank reinforcement					0.129	0.157	0.187	0.250	0.157	0.250	0.250	0.157	0.250	0.312
36 in. or less	0.100	0.129	0.157	0.187	0.100	0.129	0.157	0.187	0.100	0.129	0.157	0.129	0.157	0.187
Over 36 in. to 54 in.	0.100	0.129	0.157	0.187	0.100	0.129	0.157	0.187	0.129	0.157	0.187	0.157	0.250	0.250
Over 54 in. to 60 in.	0.100	0.129	0.157	0.187	0.129	0.157	0.187	0.250	0.157	0.250	0.250	0.187	0.250	0.312
Thickness (inch), aluminum Distances between heads (and bulkheads, baffles, and ring stiffeners when used as tank reinforcement	0.144	0.187	0.227	0.270	0.187	0.227	0.270	0.360	0.227	0.360	0.360	0.227	0.360	0.450
36 in. or less	0.144	0.187	0.227	0.270	0.144	0.187	0.227	0.270	0.144	0.187	0.227	0.187	0.227	0.270
Over 36 in. to 54 in.	0.144	0.187	0.227	0.270	0.144	0.187	0.227	0.270	0.187	0.227	0.270	0.157	0.360	0.360
Over 54 in. to 60 in.	0.144	0.187	0.227	0.270	0.187	0.227	0.270	0.360	0.227	0.360	0.360	0.270	0.360	0.450

TABLE S6.13.11.4 M-b

MINIMUM THICKNESS FOR SHELLS (DOT 412)

Volume capacity (liters per millimeter)	0.122 or less				Over 0.122 to 0.21				Over 0.21 to 0.22			0.22 and over		
Lading density at 15°F in kilograms per liter	1.2 kgs and less	Over 1.2 to 1.6 kgs	Over 1.6 to 1.9 kgs	Over 1.9 kgs	1.2 kgs and less	Over 1.2 to 1.6 kgs	Over 1.6 to 1.9 kgs	Over 1.9 kgs	1.2 kgs and less	Over 1.2 to 1.6 kgs	Over 1.6 to 1.9 kgs	1.2 kgs and less	Over 1.2 to 1.6 kgs	Over 1.6 to 1.9 kgs
Thickness (mm), steel; Distances between heads (and bulkheads, baffles, and ring stiffeners when used as tank reinforcement					3.28	3.99	4.75	6.35	3.99	6.35	6.35	3.99	6.35	7.92
914 mm or less	2.54	3.28	3.99	4.75	2.54	3.28	3.94	4.75	2.54	3.28	3.99	3.28	3.99	4.75
Over 914 mm to 1,372 mm	2.54	3.28	3.99	4.75	2.54	3.28	3.94	4.75	3.28	3.99	4.75	3.99	6.35	6.35
Over 1,372 mm to 1,524 mm	2.54	3.28	3.99	4.75	3.28	3.94	4.75	6.35	3.99	6.35	6.35	4.75	6.35	7.92
Thickness (mm), aluminum; Distances between heads (and bulkheads, baffles, and ring stiffeners when used as tank reinforcement	3.66	4.75	5.77	6.86	4.75	5.77	6.86	9.14	5.77	9.14	9.14	5.77	9.14	11.4
914 mm or less	3.66	4.75	5.77	6.86	3.66	4.75	5.77	6.86	3.66	4.75	5.77	3.66	5.77	6.86
Over 914 mm to 1,372 mm	3.66	4.75	5.77	6.86	3.66	4.75	5.77	6.86	4.75	5.77	6.86	3.99	9.14	9.14
Over 1,372 to 1,524 mm	3.66	4.75	5.77	6.86	4.75	5.77	6.86	9.14	5.77	9.14	9.14	6.86	9.14	11.4

S6.14 INSPECTION AND TESTS OF PORTABLE TANKS

a) For hazardous material ladings, all portable tanks shall be inspected and tested at frequencies specified in NBIC Part 2, Table S6.14. The inspection and tests shall include visual inspection of external and internal surfaces, leak test, pressure test, thickness measurements, and lining test. It should be noted that the information in NBIC Part 2, S6.14, is a summary of CFR Title 49, Part 180.601 through Part 180.605. The user is responsible for full compliance with the requirements in CFR Title 49, Part 180.601 through Part 180.605.

b) All portable tanks shall be visually inspected (internally, unless otherwise noted, and externally) for any condition that might render the portable tank unsafe for transportation service. The inspection shall include:

   1) Inspection of the shell for pitting, corrosion or abrasions, dents, distortions or abrasions, defects in welds, or any other conditions, including leakage; and

   2) Inspection of the piping, valves, and gaskets for corroded areas, defects, and other conditions, including leakage that may be unsafe during filling and discharge or transportation.

c) In addition to the required frequencies established in NBIC Part 2, Table S6.14, it is required that portable tanks be inspected and tested when any of the following occurs:

   1) The portable tank has been in an accident and has been damaged to an extent that may adversely affect the portable tank's ability to retain hazardous materials;

   2) The portable tank has been out of hazardous material transportation service for a period of one year or more;

   3) The portable tank has been modified from its original design specification; and

   4) The portable tank is in an unsafe operating condition based on the existence of observed damage, leaks, or missing safety devices, etc.

TABLE S6.14
INSPECTION INTERVALS

Specification	Periodic Inspection and Test[1]	Intermediate Periodic Inspection and Test[2]
IM or UN Portable Tanks once placed in service	5 years	2-1/2 years
DOT 51 Portable Tanks	5 years	—
DOT 56 or DOT 57 Portable Tanks (The first periodic inspection and test is required 4 years after being placed into service and each 2-1/2 years thereafter.)	2-1/2 years	—
DOT 60 Portable Tanks (The first periodic inspection and test is required 4 years after being placed into service and then per the schedule to the right.)	For the first 12 years of service.....2 years	After 12 years of service.....yearly

1 Retesting is not required on a rubber-lined tank, except before relining.

2 For IM and UN Portable Tanks, periodic inspection and test shall include at least an internal and external inspection of the portable tank and fittings, taking into account the hazardous material intended to be transported.

S6.14.1 PERIODIC INSPECTION AND TEST

Portable tanks shall be tested and inspected in accordance with the frequency set forth in NBIC Part 2, Table S6.14 and the procedures set forth in NBIC Part 2, S6.14.3 through S6.14.6.4.

S6.14.2 INTERMEDIATE PERIODIC INSPECTION AND TEST

a) Intermediate periodic inspections and testing shall be performed in accordance with NBIC Part 2, Table S6.14. The intermediate periodic inspection and testing shall include:

   1) An external and an internal inspection of the portable tank and its fittings taking into account the hazardous materials being transported;

   2) A leakage test of the transport tank; and

   3) A test for satisfactory operation of all service equipment;

b) When inspecting portable tanks equipped with sheathing and thermal insulation, etc., the insulation need only be removed to the extent required for a reliable appraisal of the condition of the portable tank;

c) For portable tanks intended for the transportation of a single hazardous material, the internal inspection may be waived if the portable tank is subjected to a leakage test that is performed in accordance with NBIC Part 2, S6.14.3 of this section prior to each filling;

d) Portable tanks used for dedicated transportation of refrigerated liquefied gases that are not fitted with inspection openings are exempt from the internal inspection requirements, but shall be externally inspected.

S6.14.3 INTERNAL AND EXTERNAL INSPECTIONS

All portable tanks that are subject to five-year periodic inspection and testing (pressure test) are required to be inspected, both internally, unless exempt, and externally. The internal and external inspection shall include:

a) Sheathing, thermal insulation, etc. The sheathing and thermal insulation need only be removed to the extent required for reliable appraisal of the condition of the portable tank;

b) Except for DOT Specification 56 and 57 portable tanks, all re-closing pressure relief devices must be removed from the tank and tested separately unless they can be tested while installed on the portable tank;

c) For portable tanks where the shell and equipment have been pressure tested separately after assembly, the portable tank shall be subjected to a leakage test and effectively tested and inspected for corrosion;

d) Portable tanks used for the transportation of refrigerated, liquefied gases are exempt from the internal inspection and the hydrostatic test or other pressure test during the five-year periodic inspection if the portable tank was originally tested to a minimum test pressure of 1.3 times the design pressure using inert gas and provided that;

   1) The portable tank and its appurtenances were constructed to ASME Section XII, or ASME Section VIII, Division 1; the portable tank shall be inspected in accordance with the applicable requirements of this Code;

   2) Portable tanks shall be either hydrostatically or pneumatically tested with the formula 1.5 x design pressure + static head + 101 kPa (14.7 psi), if the tank is designed for external pressure;

   3) The portable tank shall be subjected to either a hydrostatic or pneumatic test at a test pressure of 1.5 x the sum of the design pressure + the static head of lading + 101 kPa (14.7 psi), if subjected to external vacuum. If the portable tank is constructed in accordance with ASME Section XII or Part UHT of ASME Section VIII, Div. 1, the test pressure shall be twice the design pressure; and

   4) A pneumatic test may be used in lieu of a hydrostatic test if the following conditions are met:

      a. The owner or user has taken necessary precautions to ensure the safety of the inspection and test personnel;

      b. The pneumatic test pressure shall be reached gradually by increasing the test pressure to one-half of the test pressure. Once this pressure is reached, the test pressure will be increased in increments of approximately one-tenth of the test pressure until the required test pressure is reached; and

      c. When the test pressure is reached, the test pressure shall be reduced to at least four-fifths of the test pressure and held for a sufficient time to permit inspection of the portable tank.

S6.14.4 EXCEPTIONAL INSPECTION AND TEST

a) Exceptional inspection and test is necessary when a portable tank shows evidence of damage, corroded areas, or leakage, or other conditions that indicate a deficiency that could affect the integrity of the portable tank.

b) The extent of the exceptional inspection and test shall depend on the amount of deterioration of the portable tank. The exceptional inspection and test shall include the requirements of NBIC Part 2, S6.14.3 of this section.

c) Pressure relief devices do not need to be included in this test unless there is reason to believe the relief device has been affected by damage or deterioration.

S6.14.5 INTERNAL AND EXTERNAL INSPECTION PROCEDURE

An internal and external inspection, when required, shall be performed by the owner or user. The inspection shall be conducted by the Inspector. This individual shall ensure that the portable tank is safe for continued transportation service. The Inspector shall evaluate the results of the inspection and report the applicable findings. The inspection shall include:

a) Inspection of the shell for pitting, corrosion or abrasions, dents, distortions, defects in welds, or any other conditions, including leakage;

b) Inspection of the piping, valves, and gaskets for corroded areas, defects, and other conditions, including leakage that might make the portable tank unsafe for filling, discharge, or transportation;

c) Ensuring that the tightening devices for manhole covers are operative, and there is no leakage at the manhole cover or gasket;

d) Checking for any missing or loose bolts or nuts on any flanged connections including piping flanges, pressure relief device connections, or blank flanges. If any bolts are loose or missing, these shall be tightened or replaced;

e) Checking all emergency devices and valves to ensure that they are free from corrosion, distortion, and any damage or defects that could prevent the devices from operating as designed;

f) Ensuring all remote closures and self-closing stop valves are operated to demonstrate their proper operation;

g) Ensuring the required markings on the portable tanks are legible and in accordance with the applicable requirements of CFR Title 49, Part 178.3, and Part 180.605; and

h) Ensuring the framework, supports, and the arrangements for lifting the portable tank are in a satisfactory condition.

S6.14.6 PRESSURE TEST PROCEDURES FOR SPECIFICATION 51, 57, 60, IM OR UN PORTABLE TANKS

This Section provides the requirements for pressure test procedures for Specification 51, 57, 60, IM or UN Portable Tanks as provided in CFR Title 49, Part 180.605(h). Pressure test requirements for Specification 51, 57, 60, IM and UN Portable Tanks are identified in NBIC Part 2, Table S6.14.6 of this Subsection.

TABLE S6.14.6
PRESSURE TESTING REQUIREMENTS

Specification	Leak Test	Hydrostatic	Pneumatic	Test Media	Minimum Test Pressure
51 and 56	—	X	X	Liquid or Air	14 kPa (2 psi) or at least 1-1/2 times the design pressure, whichever is greater
51 and 56 used to transport refrigerated liquefied gas	X	X	X	Liquid or Air	90% of the Maximum Allowable Working Pressure
51 and 56 for the transport of all other materials	—	X	X	Liquid or Air	25% of the Maximum Allowable Working Pressure
57	X	—	—	—	21 kPa (3 psi) to the entire tank
60	—	—	—	Water or other similar liquid	413 kPa (60 psig)
UN nonrefrigerated gases	—	—	—	Water	130% of Maximum Allowable Working Pressure
UN refrigerated gases	—	X	X	Water or Air	1.3 times design pressure
IM refrigerated or nonrefrigerated liquefied gases	—	X	X	Water or Air	150% of the Maximum Allowable Working Pressure

S6.14.6.1 SPECIFICATION 57 PORTABLE TANKS

a) Specification 57 portable tanks shall be leak tested by a minimum sustained air pressure of at least 21 kPa (3 psig) applied to the entire tank.

b) During each air pressure test, the entire surface of all joints, whether welded or threaded, shall be coated with or immersed in a solution of soap and water, heavy oil, or other material suitable for the purpose of detecting leaks.

c) The test pressure shall be held for a minimum of 5 minutes plus any additional time required to examine all portions of the portable tank.

d) During the air test, the pressure relief device may be removed or left in place. If the relief device is left in place during the test, the device's discharge opening shall be plugged.

e) All closure fittings must be in place during the pressure test.

f) If the portable tank is lagged or insulated, the lagging or insulation does not have to be removed if it is possible to maintain the required test pressure at a constant temperature with the portable tank disconnected from the source of pressure.

S6.14.6.2 SPECIFICATION 51 OR 56 PORTABLE TANKS

a) Specification 51 or 56 portable tanks shall be tested using either air or liquid. The minimum test pressure shall be at least 14 kPa (2 psig) or at least one and one-half times the maximum allowable working pressure (or re-rated pressure) of the portable tank. The greater test pressure shall be used.

b) The leak testing of all refrigerated liquefied gas tanks shall be performed at 90% of the maximum allowable working pressure of the portable tank.

c) Leak testing for all other portable tanks shall be at a test pressure of at least 25% of the maximum allowable working pressure of the portable tank.

d) If the portable tank is hydrostatically tested, the entire surface of the portable tank shall be inspected for leaks. This includes all welded joints and threaded connections. The requirements below shall be followed for hydrostatic testing:

1) The hydrostatic test pressure shall be held for a minimum of 5 minutes plus any additional time required to complete the inspection;

2) The pressure relief device should be removed or left in place during the hydrostatic test. If the relief device is left in place during the test, the device shall be isolated to prevent the relief device from discharging in accordance with the device manufacturer's recommendations;

3) It is required for DOT 51 specification tanks that the relief valve be removed during the pressure test; and

4) All closure fittings shall remain in place during the hydrostatic test.

e) If the portable tank is pressure tested by air, during the test all surfaces of welded joints and thread connections of the portable tank shall be inspected for leaks and the following procedure shall be followed:

1) All welded joints and threaded connections shall be coated with or immersed in a solution of soap and water, or heavy oil or other material suitable for the purpose of detecting leaks;

2) The air test pressure shall be held for a minimum of 5 minutes. This time period should be increased if so required by the Inspector;

3) The pressure relief device should be removed or left in place during the air test. If the relief device is left in place during the test, the device shall be isolated to prevent the pressure relief device from discharging in accordance with the device manufacturer's recommendations;

4) For Specification 51 portable tanks, the relief device shall be removed during the pressure test; and

5) All closure fittings shall remain in place during the air test.

f) If the portable tank is lagged or insulated and the pressure test performed is either hydrostatic or pneumatic, it is not necessary to remove the lagging or insulation for pressure testing provided the decay in test pressure can be measured at a constant temperature while the portable tank is disconnected from the source of pressure.

S6.14.6.3 SPECIFICATION 60 PORTABLE TANKS

Specification 60 portable tanks shall be tested by completely filling the portable tank with water or other liquid having a similar viscosity. The test procedure shall include:

a) The temperature of the liquid shall not exceed 37.7°C (100°F) during the test;

b) The test pressure applied shall be at least 413 kPa (60 psig);

c) The test pressure shall be maintained for a minimum of 10 minutes. This time period may be increased if required by the Inspector;

d) During the 10-minute time period, the portable tank shall be capable of maintaining the test pressure with no evidence of leakage;

e) All closures shall be left in place while the pressure test is being performed;

f) The pressure gage shall be located at the tip of the vessel during the test; and

g) Re-closing pressure relief devices must be removed from the tank and tested separately unless they can be tested while installed on the portable tank.

S6.14.6.4 SPECIFICATION IM OR UN PORTABLE TANKS

All Specification IM or UN portable tanks, except for UN portable tanks used for non-refrigerated and refrigerated liquefied gases, and all piping, valves, and accessories, except pressure relief devices, shall be hydrostatically tested with water, or other liquid similar in density and viscosity as follows:

a) All IM portable tanks used for non-refrigerated and refrigerated liquid gases shall be hydrostatically tested with water to a pressure of not less than 150% of the portable tanks maximum allowable working pressure;

b) All UN portable tanks used for the transportation of non-refrigerated liquefied gases shall be hydrostatically tested, with water to a pressure not less than 130% of the portable tanks maximum allowable working pressure.

    1) UN portable tanks used for the transportation of refrigerated gases should be tested either hydrostatically or pneumatically using an inert gas to a pressure of not less than 1.3 times the design pressure of the portable tank.

    2) If the portable tank is subjected to the pneumatic test method, the owner or user shall take necessary precautions for the safety of the inspection and test personnel.

    3) The pneumatic test pressure shall be reached gradually by increasing the test pressure to one-half of the test pressure. Once this pressure is reached, the test pressure will be increased in increments of approximately one-tenth of the test pressure until the required test pressure is reached.

    4) When the test pressure is reached, the pressure shall be reduced to a value equal to four-fifths of the test pressure and held for a sufficient time to permit the inspection for leaks.

c) The minimum test pressure of IM and UN portable tanks is determined on the basis of the hazardous materials that are intended to be transported in the portable tank as required by CFR Title 49, Part 172.101.

d) For liquid, solid, and non-refrigerated gases, the minimum test pressure for a specific hazardous material is provided in the applicable “T” Codes assigned for a particular hazardous material, as specified in CFR Title 49, Part 172.102 Tables. See NBIC Part 2, Table S6.14.6.4.

e) While the portable tank is under test pressure, it shall be inspected for leakage, distortion, or any other condition that might render the portable tank unsafe for service.

f) If a portable tank fails to meet the requirements of the pressure test or if during the pressure test there are any of the following conditions, the portable tank shall be removed from transportation service, unless the portable tank is adequately repaired and, thereafter, a successful pressure test is conducted in accordance with this Section.

    1) Any permanent distortion of the portable tank exceeding that permitted by the applicable specification;

    2) Any leakage; or

    3) Any deficiencies that would render the portable tank unsafe for transportation.

g) The approval agency shall witness the hydrostatic or pneumatic tests.

h) If the portable tank is damaged or a deficiency is discovered that might render the portable tank unsafe, the tank shall be repaired to a satisfactory condition. This test shall be witnessed by the applicable approval agency. As a minimum, the repair procedures shall include:

1) Retesting to the original pressure test requirements.

2) If the hydrostatic or pneumatic test is successful, the witnessing approval agency shall apply its name, identifying mark, or identifying number on the portable tank's nameplate as required in NBIC Part 2, S6.14.7;

i) All thermal cutting or welding on the shell of IM or UN portable tanks shall be done in accordance with this Section. After completion of the thermal cutting or welding operation, a pressure test shall be performed to the requirements of the portable tank's original test requirements.

TABLE S6.14.6.4
"T" CODES

T1 to T22	For liquid and solid hazardous materials of Classes 3 through 9 that are transported in portable tanks.1
T23	Applies to self-reactive substances of Division 4.1 and organic peroxides of Division 5.2.
T50	Applies to liquefied compressed gases.
1 Note: Class numbers of hazardous materials listed in CFR 49, Part 173.2.	

S6.14.7 INSPECTION AND TEST MARKINGS FOR IM OR UN PORTABLE TANKS

a) Each IM or UN portable tank shall be durably and legibly marked, in English, with the date (month and year) of the last pressure test.

b) The identifying agency shall witness the test, when required, and the date of the last visual inspection.

c) The markings required on the portable tank's identification plate shall be identified as follows:

1) Placed on or near the metal identification plate;

2) The size of the letters and numerals on the plate shall be no less than 3 mm (0.1 inches) high; and

3) If the letters and numerals are stamped into the portable tank's shell, they shall be at least 12 mm (0.5 inches) high.

S6.14.8 INSPECTION AND TEST MARKINGS FOR SPECIFICATION DOT 51, 56, 57, OR 60

a) Each Specification DOT 51, 56, 57, or 60 portable tank shall be durably and legibly marked, in English, with the date (month and year) of the most recent periodic test.

b) The markings shall be placed near the metal certification plate and shall be in accordance with the following:

1) Shall be marked on a non-removable component of the portable tank that identifies the specification markings;

2) Located in an unobstructed area with letters and numerals identifying the standard or specification, (e.g., UN 1A1, DOT 4B240ET, etc.);

3) Shall identify the name and address or symbol of the portable tank manufacturer or, where specifically authorized, the symbol of the approval agency certifying compliance with the UN standard;

4) The markings shall be stamped, embossed, burned, printed, or otherwise marked on the portable tank to provide adequate accessibility, permanency, contrast, and legibility, so as to be readily apparent and understood; and

5) The letters and numerals shall be at least 3 mm (0.1 inches) high if stamped on a plate, and shall be at least 12.0 mm (0.5 inches) high when stamped on the portable tank's shell.

S6.14.9 RECORD RETENTION

The owner of each portable tank or his authorized agent shall retain a written report of the date and results of all required inspections and tests, including the following:

a) If applicable, the ASME Manufacturer's Data Report (U-1 or U1A Forms);

b) The name and address of the person performing the inspection and/or test in accordance with the applicable specification;

c) The Manufacturer's Data Report including a certificate(s) signed by the manufacturer;

d) The authorized agency, as applicable, indicating compliance with the applicable specification of the portable tank; and

e) The records shall be retained in the owner's files or should be retained by the owner's authorized agent during the time that the portable tank is used. These records do not have to be maintained for DOT 56 and DOT 57 Specification tanks.

S6.15 GENERAL REQUIREMENTS FOR DOT SPECIFICATION 106A AND 110A TANK CARS (TON TANKS)

All Specification DOT 106A and DOT 110A multi-unit ton tanks shall be cylindrical, circular in cross-section and shall have heads of an approved design, with all fittings, i.e., couplings, nozzles, etc., located in the heads of the tank.

S6.15.1 SPECIAL PROVISIONS FOR TON TANKS

49 CFR, Section 179.300, has specific criteria for ton tanks that shall be met to satisfy DOT Specification 106A and 110A. The limitations are as follows:

a) Ton tanks shall have a water containing capacity of at least 0.68 tonne (1500 pounds), but in no case can the water containing capacity of the ton tank exceed 1.18 tonnes (2600 pounds);

b) Ton tanks shall not be insulated;

c) Thickness of plates for DOT Specifications 106A and 110A ton tanks shall be in accordance with NBIC Part 2, Table S6.15.1-a;

d) The maximum carbon content for carbon steel used in the fabrication of ton tanks shall not exceed 0.31%;

e) Permitted materials can be either an ASME, SA material, or an ASTM Material permitted by NBIC Part 2, Table S6.15.1-b;

f) DOT Specification 106A ton tanks shall only use forged-welded heads, convex to pressure. The forged-welded heads shall be torispherical with an inside radius not greater than the inside diameter of the shell. The heads shall be one piece, hot formed in one heat so as to provide a straight flange at least 100 mm (4 inches) long. The heads must have a snug fit into the shell;

g) DOT Specification 110A ton tanks shall only use fusion-welded heads formed concave to pressure. The fusion-welded heads shall be an ellipsoid of 2:1 ratio and shall be of one piece, hot formed in one heat so as to provide a straight flange at least 38 mm (1-1/2 inches) long;

h) All longitudinal welded joints on DOT Specification 106A and DOT Specification 110A ton tanks shall be a fusion weld. DOT Specification 106A ton tank head-to-shell attachments shall be a forged-welded joint.[6] DOT Specification 110A ton tank head-to-shell attachments shall be a fusion weld;

i) Postweld heat treatment is required after welding for all DOT Specification 106A and Specification 110A ton tanks;

j) DOT Specification 106A and DOT Specification 110A ton tanks shall be of such a design as to afford maximum protection to any fitting or attachment to the head, including loading and unloading valves. The protection housing[5] shall not project beyond the end of the ton tanks and shall be securely fastened to the tank head;

k) If applicable, siphon pipes and their couplings on the inside of the ton tank's head and lugs on the outside of the tank head for attaching valve protection housing shall be fusion welded prior to performing postweld heat treatment;

l) DOT Specification 106A and DOT Specification 110A ton tanks are required to be equipped with one or more approved types of pressure relief devices. The devices shall be made out of metal and the pressure relief devices shall not be subject to rapid deterioration by the lading. The device's inlet fitting to the tank shall be a screw-type fitting and installed or attached directly into the ton tank's head or attached to the head by other approved methods. For thread connections, the following shall apply:

   1) The threaded connections for all openings shall be in compliance with the National Gas Taper Threads (NGT);

   2) Pressure relief devices shall be set for start-to-discharge, and rupture discs shall burst at a pressure not exceeding the pressure identified in NBIC Part 2, Table S6.15.1-a; and

m) Fusible plugs, if used, shall be required to relieve the pressure from the tank at a temperature not exceeding 79°C (175°F) and shall be vapor tight at a temperature not exceeding 54°C (130°F).

6 The forged-welded joint shall be thoroughly hammered or rolled to ensure a sound weld.

TABLE S6.15.1-a

THICKNESS OF PLATES AND SAFETY VALVE REQUIREMENTS

DOT Specification	106A500-X	106A800-X	110A500-W	110600-W	110A800-W	110A1000-W
Minimum required bursting pressure, MPa (psig)	None Specified	None Specified	8.62 (1,250)	10.34 (1,500)	13.8 (2,000)	17.2 (2,500)
Minimum thickness shell, mm (inches), Test Pressure (See CFR 179.300-15), MPa (psig)	10.3 (13/32) 3.45 (500)	17.5 (11/16) 5.52 (800)	8.7 (11/32) 3.45 (500)	9.5 (3/8) 4.41 (600)	11.9 (15/32) 5.52 (800)	15.1 (19/32) 6.89 (1,000)
Start-to-discharge, or burst pressure (maximum MPa (psig))	2.59 (375)	4.14 (600)	2.59 (375)	3.10 (450)	4.14 (600)	4.83 (700)

TABLE S6.15.1-b

ACCEPTABLE MATERIALS WITH ACCEPTABLE TENSILE STRENGTH AND ELONGATION REQUIREMENTS

Material Specification	Minimum Tensile Strength MPa (psi) in the welded condition. *These values are to be used in the design calculations.*	Minimum Elongation in 50 mm (2 in.) (percent) in the welded condition. *These values are to be used in the design calculations.*
ASTM A 240 type 304	517 (75,000)	25
ASTM A 240 type 304L	483 (70,000)	25
ASTM A 240 type 316	517 (75,000)	25
ASTM A 240 type 316L	483 (70,000)	25
ASTM A 240 type 321	517 (75,000)	25
ASTM A 285 Gr. A	310 (45,000)	29
ASTM A 285 Gr. B	345 (50,000)	20
ASTM A 285 Gr. C	380 (55,000)	20
ASTM A 515 Gr. 65	448 (65,000)	20
ASTM A 515 Gr. 70	483 (70,000)	20
ASTM A 516 Gr. 70	483 (70,000)	20

S6.15.2 VISUAL INSPECTION OF TON TANKS

Without any regard to any other periodic inspection and test requirements, a ton tank shall be visually inspected for evidence of any:

a) Defects in welds;

b) Abrasions;

c) Corrosion;

d) Cracks;

e) Dents;

f) Distortions; or

g) Any other conditions that might make the ton tank unsafe for transportation.

S6.15.3 INSPECTION AND TESTS OF DOT SPECIFICATION 106A AND DOT SPECIFICATION 110A TON TANKS

Each ton tank shall be retested by subjecting the ton tank to a hydrostatic test in accordance with NBIC Part 2, Table S6.15.3. The hydrostatic test shall include an evaluation of the tank's permanent expansion. As a minimum, the hydrostatic test and the expansion procedure shall include:

a) The hydrostatic test pressure shall be maintained for a minimum of 30 seconds. This time period may be extended as long as necessary to secure complete expansion of the ton tank.

b) The pressure gage used for the hydrostatic test shall be accurate within 1% of the range of the pressure gage. The accuracy of the pressure gage shall be verified prior to performing the hydrostatic test.

c) The expansion test procedure shall include the following requirements:

1) The expansion shall be recorded in cubic centimeters;

2) Permanent volumetric expansion shall not exceed 10% of the total volumetric expansion at the test pressure; and

3) The expansion gage shall be accurate within one percent of the hydrostatic test pressure.

d) The ton tank shall not show any signs of leakage or stress during the hydrostatic and expansion test.

e) The retest may be made at any time during the calendar year the retest falls due.

TABLE S6.15.3

TON TANK PERIODIC INSPECTION AND TEST FREQUENCIES

	Retest Interval, years		Minimum Retest Pressure, MPa (psig)		Pressure Relief Valve Pressure, MPa (psig)	
DOT Specification	Tank	Pressure Relief Device	Tank Hydrostatic Expansion	Tank Air Test	Start-to-Discharge	Vapor Tight
106A500	5	2	500 (3.45)	100 (0.69)	375 (2.59)	300 (2.07)
106A500X	5	2	500 (3.45)	100 (0.69)	375 (2.59)	300 (2.07)
106A800	5	2	800 (5.52)	100 (0.69)	600 (4.14)	480 (3.31)
106A800X	5	2	800 (5.52)	100 (0.69)	600 (4.14)	480 (3.31)
106A800NCI	5	2	800 (5.52)	100 (0.69)	600 (4.14)	480 (3.31)
110A500-W	5	2	500 (3.45)	100 (0.69)	375 (2.59)	300 (2.07)
110A600-W	5	2	600 (4.41)	100 (0.69)	500 (3.45)	360 (2.48)
110A800-W	5	2	800 (5.52)	100 (0.69)	600 (4.14)	480 (3.31)
110A1000-W	5	2	1,000 (6.89)	100 (0.69)	750 (5.17)	600 (4.41)

S6.15.3.1 AIR TESTS

a) All specification DOT 106A and DOT 110A ton tanks, in addition to the hydrostatic test shall be subjected to an air test at frequencies and pressures specified in NBIC Part 2, Table S6.15.3.

b) The air test shall be under positive control to ensure safety to all inspection and test personnel.

c) Any leakage observed will require the ton tank to be repaired and retested prior to placing the ton tank back into service.

S6.15.3.2 PRESSURE RELIEF DEVICE TESTING

All pressure relief devices shall be retested by air or gas for the start-to-discharge and vapor tightness requirements at frequencies and pressures specified in NBIC Part 2, Table S6.15.3.

S6.15.3.3 RUPTURE DISCS AND FUSIBLE PLUGS

All rupture discs required by NBIC Part 2, S6.15.1 l) 2), and fusible plugs required by NBIC Part 2, S6.15.1 m), shall be removed from the ton tank and inspected. The inspection shall include but not be limited to the following:

a) All rupture discs shall be inspected for corrosion, leakage, and manufacturer tolerances;

b) All fusible plugs shall be inspected for corrosion, loose, or deteriorated temperature sensitive materials; and

c) Any indication specified in a) and b) above will require the rupture disc or fusible plug to be replaced with devices specified in NBIC Part 2, S6.15.1 l) 2) and S6.15.1) m).

S6.15.3.4 SUCCESSFUL COMPLETION OF THE PERIODIC RETESTING

If the results of the periodic retest are successful, the ton tank shall be plainly and permanently stamped on one head or chime of each ton tank. The stamping shall include:

a) The month and year of the test followed by a “V”, and

b) Dates of previous tests and all prescribed markings shall not be removed. Previous dates and markings on the ton tank’s head or chime shall be legible.

S6.15.3.5 EXEMPTIONS TO PERIODIC HYDROSTATIC RETESTING

Ton tanks that satisfy DOT 106A and DOT 110A and are used exclusively for transporting fluorinated hydrocarbons and mixtures thereof, and are free from corroding components related to the ton tank, may be exempted from the periodic hydrostatic retest if:

a) The ton tank is given a complete internal and external visual inspection of all heads, shells, nozzles, couplings, pressure relief devices, i.e. pressure relief valves and rupture discs and fusible plugs for deterioration and leakage.

b) The visual internal and external inspection is performed by qualified personnel, i.e., Registered Inspector, employee of the owner or user, etc.

S6.15.3.6 RECORD OF RETEST INSPECTION

The owner or the person performing the required pressure test and visual inspection is required to retain a written record of the results as long as the ton tank is in service. The written report shall identify the following:

a) Date of the test and inspection;

b) DOT Specification Number of the ton tank;

c) Ton tank identification: registered symbol and serial number, date of manufacture, and ownership symbol;

d) Type of protective coating, i.e., painting, etc.;

e) Statement as to the need for refinishing or recoating the ton tank;

f) Conditions checked for:

1) Leakage;

2) Corrosion;

3) Gouges;

4) Dents or dings;

5) Broken or damaged chimes, or protective rings;

6) Fire damage;

7) Internal conditions;

8) Test pressure; and

9) The written report shall also identify the results of the test:

a. Disposition of the tank, i.e., returned to service, returned to the manufacturer for repair, or scrapped; and

b. Identification of the person performing the retest or inspection.

S6.15.4 STAMPING REQUIREMENTS OF DOT 106A AND DOT 110A TON TANKS

To identify compliance with CFR 179.300-1, each DOT 106A and DOT 110A ton tank shall be plainly and permanently stamped with letters and figures 10 mm (3/8 in.) high on valve end chime of the ton tank's head. The minimum requirements for the stamping are as follows:

a) DOT Specification Number;

b) Material and cladding material, if any. This information shall be stamped directly below the DOT Specification Number;

c) Owner's or builder's identifying symbol and serial number. This information shall be stamped directly below the material identification stamping. The owner's or builder's symbol shall be registered with the Bureau of Explosions (duplications are not authorized);

d) Inspector's official mark. This information shall be stamped directly below the owner's or builder's symbol;

e) Date of the original ton tank test (month and year). Provisions should be made that subsequent tests may easily be added thereto;

f) Water capacity of the ton tank in kilograms (pounds); and

g) A duplicate of the stamping that satisfies a) through f) should be used if the plate is made of brass and is permanently attached to the ton tank's head.

S6.16 PRESSURE RELIEF DEVICES

S6.16.1 SCOPE

This Section provides details for the application, continued service inspection, and repair of pressure relief devices specified for overpressure protection of transport tanks.

Pressure relief devices are provided for all transport tanks to prevent internal pressure from exceeding design values. They may also be provided to prevent excessive internal vacuum. Overpressure protection may be provided by reclosing pressure relief valves, non-reclosing devices such as rupture disks or breaking bar or breaking pin valves, or combinations of pressure relief valves and non-reclosing devices.

S6.16.2 SAFETY CONSIDERATIONS

When inspections of pressure relief devices are being performed, Inspectors should be aware that tests of these devices involve the discharge of the test fluid, which can result in high-velocity fluid flow, possible high -or low-temperature fluids, and high noise levels. If a test is being performed with the service fluid, it should be a fluid that is safe for discharge and not toxic or hazardous. Due to the nature of fluids being transported, most testing will involve removing the device from the transport tank and testing it on a test stand. (See NBIC Part 2, S6.12.1, Pre-Inspection Activities.)

S6.16.3 INSTALLATION PROVISIONS

Incorrect installation of a pressure relief device can have a detrimental effect on device performance. The following provisions shall be followed when installing pressure relief devices on transport tanks:

a) Inlet piping shall have an area at least equal to the pressure relief device inlet size with no restrictions which can affect flow through the device;

b) Pressure relief devices shall be installed to be in communication with the vapor space of the tank in its normal transport orientation as near as practicable on the longitudinal center line, and in the center of the tank;

c) If discharge piping is provided, it shall have an area at least equal to the pressure relief device, be as short and straight as possible, and of a length that will not affect the pressure relief device flow performance. It will typically discharge upward, and should be directed away from personnel that may be around the tank at ground level;

d) Provisions for protection of the outlet of pressure relief devices from contamination from the effects of rain, weather, etc., shall be provided. Where rain caps are provided, the fit shall not be tight enough to affect the valve performance;

e) Pressure relief devices may be installed inside a protective housing consisting of mechanical elements designed to protect the valve during roll-over events. These elements shall not obstruct the outlet of the device;

f) If a rupture disk is used in combination with a pressure relief valve, it shall be located inboard of the pressure relief valve;

g) When a rupture disk is used in combination with a pressure relief valve, a device to detect leakage through the rupture disk, or actuation of the rupture disk, shall be provided. These devices detect leakage or actuation by observation of the accumution of pressure between the disk and the pressure relief valve, and shall consist of a needle valve, try-cock, tell-tale indicator or pressure gage. Where a valve is provided, it shall be closed during normal operation. Leaking disks or disks, which have discharged, shall be replaced as soon as possible; and

h) Block valves shall not be used on either device inlets or outlets.

S6.16.4 PRESSURE RELIEF DEVICE INSPECTION

For pressure relief valves, inspection shall consist of an External and Internal Visual Inspection and a Pressure Test to determine valve function. For non-reclosing pressure relief devices, inspection shall consist of an external and internal visual inspection as well.

S6.16.5 SCHEDULE OF INSPECTIONS

Pressure relief devices shall be inspected at the frequency as required by NBIC Part 2, Tables S6.13.4, S6.14, or S6.15.3. For both an External Visual Inspection and a Pressure Test, the frequency of inspection for pressure relief devices shall be the same as the frequency required for inspection of the transport tank itself.

S6.16.6 EXTERNAL VISUAL INSPECTION OF PRESSURE RELIEF DEVICES

The following items shall be inspected during the External Visual Inspection.

a) Pressure relief device nameplate data shall be reviewed, and the marked device set pressure compared to the transport tank data. The pressure relief device set pressure shall not exceed the tank maximum allowable working pressure (MAWP) except as permitted by the applicable transport tank specification appendix.

b) Where seals are provided to seal external adjustments of pressure relief valves, the seal must be intact and bear the identification of the organization responsible for performing the adjustment. If the valve has been repaired or reset, it must bear a supplemental nameplate identifying the organization responsible for the repair or resetting.

c) Valves that have the set pressure adjustment permanently sealed, by means such as a rivet or roll pin through the adjustment, shall be checked to ensure there has been no tampering with the set pressure adjustment.

d) Check for evidence of leakage through the valve. For a valve installed with a rupture disk at the inlet, the rupture disk leakage detection device shall be checked for signs of leakage through the disk. When possible, this inspection should be performed with normal transport tank operating pressure present.

e) All connecting bolting shall be present and tight.

f) Evidence of rust or corrosion of the pressure relief device shall be investigated.

g) Where drain holes are provided on the side of the valve, check that the drain holes are not plugged.

h) Check that a valve spindle restraint (test gag) has not been left in place after pressure testing of the transport tank; and

i) Check for proper orientation of rupture disk devices. These devices will have a flow direction arrow or other designation such as inlet or vent side to designate the flow direction. Installation of rupture disk devices in the reverse direction can cause a disk to burst at a higher pressure than its marked burst pressure.

S6.16.7 PRESSURE TESTING OF PRESSURE RELIEF VALVES

A check of pressure relief valve operation shall be performed to ensure the valve is functioning properly. This testing shall be performed at the time of the transport tank pressure test when the tank pressure test will necessitate removal of the pressure relief valve. When the valve is removed for testing, the connection on the transport tank shall be inspected for corrosion or deposits which could block or reduce the connection area.

a) Prior to the test, the inlet and outlet passages of the valve shall be visually inspected for corrosion or deposits of material which could affect valve operation.

b) The test fluid shall be air or other suitable non-hazardous gas.

c) The valve shall be installed on a test stand and a calibrated test gage of suitable range shall be used.

d) Valves shall be tested for the following operational characteristics:

    1) Seat Leakage: The test pressure shall be increased to seat leakage test pressure at which there should be no leakage as determined by a bubble test. This pressure will typically be 90% of the stamped set pressure or the pressure prescribed for the applicable transport tank specification. There shall be no audible or visible leakage at the specified seat leakage test pressure.

    2) Set Pressure: The set pressure definition used by the valve manufacturer to originally set the valve shall be determined, and shall be used during evaluations of valve performance. For most transport tank valves this will usually be the “start” to “discharge” pressure which is the pressure at which the first audible discharge is detected. The test pressure shall be increased until the set pressure is determined. The valve shall open within the tolerance for set pressure as specified by the applicable transport tank specification.

    3) Re-seal pressure: The test pressure shall then be decreased and the pressure at which the valve reseals shall be recorded. The valve shall reseal at or above the pressure specified by the applicable transport tank specification, or above the normal transport tank operating pressure; and

    4) It is recommended that the test sequence be repeated several times to ensure repeatable valve performance. Erratic performance may indicate damage to the valve, including damage or deposits on the seating surface.

e) The results of testing shall be documented and be made available to the Inspector.

f) Testing shall be performed by trained individuals from an organization acceptable to the Competent Authority.

S6.16.8 CORRECTION OF DEFECTS

Any failure of the valve to meet applicable test specifications shall be brought to the attention of the Inspector and owner, and steps shall be taken to correct the defect. If repairs are required they shall be performed by a qualified organization acceptable to the Competent Authority.

When a valve is to be repaired, it shall be completely disassembled, cleaned, all parts inspected, and repaired as necessary. It shall then be tested and all adjustments resealed with a seal identifying the repair organization. Parts replaced shall be from the valve manufacturer or meet the valve manufacturer’s specifications. Where soft goods such as gaskets, o-rings, and other seals are replaced, new parts shall be used.

Repairs shall be identified with a repair nameplate which includes the organization responsible for the repair, date of the repair, and a unique identifier, identifying repair documentation. The goal of the repair is to bring the valve back to a “like new” condition.

A valve found to be defective may be replaced by a new valve or previously repaired valve. Care shall be taken to ensure that the replacement valve meets the same requirements as the valve being replaced.

S6.16.9 INSPECTION OF RUPTURE DISKS AND NON-RECLOSING DEVICES

Rupture disks and other non-reclosing devices cannot be tested. In lieu of the required pressure test for a pressure relief valve, the disk and disk holder must be removed from the transport tank and the disk inlet and outlet surfaces visually inspected. (This is considered the “Internal Inspection.”) Signs of corrosion, damage, or deposits will require that the rupture disk be replaced.

A program to periodically replace rupture disks is recommended to prevent premature disk opening during normal operation. This can be caused by corrosion or deterioration of the disk or fatigue of the disk material due to cyclic operation of the transport tank and vibration during normal operation. The rupture disk manufacturer may have recommendations for the frequency of disk replacement. Replacement disks shall have the same specifications for burst pressure and coincident temperature as the disk being replaced, unless the service conditions for the transport vessel are being changed. It is recommended that replacement disks be specified by the complete disk description including model number, burst pressure, and coincident temperature, and the lot number from the disk being replaced. Disks and disk holders from different manufacturers shall not be interchanged.

S6.17 DEFINITIONS

These definitions shall be used in conjunction with those of Section 9 of the NBIC. Where conflicts between the two arise, those listed below shall prevail.

Approval — A written authorization, including a competent authority approval from the Associate Administrator or other designated department official, to perform a function for which prior authorization by the Associate Administrator is required.

Approval Agency — An organization or a person designated by the DOT to certify packaging as having been designed, manufactured, tested, modified, marked, or maintained in compliance with applicable DOT regulations.

Approved — Approval issued or recognized by the department unless otherwise specifically indicated.

Appurtenance — Any attachment to a cargo tank that has no lading retention or containment function and provides no structural support to the cargo tank.

Associate Administrator — The Associate Administrator for Hazardous Materials Safety, Research, and Special Programs Administration.

Atmospheric gas — Air, nitrogen, oxygen, argon, krypton, neon, and xenon.

Attachments — Structural members means the suspension sub-frame, accident protection structures, external circumferential reinforcements, support framing, and kingpin sub-frame (upper coupling).

Attachments, Light Weight — Welded to a cargo tank wall such as a conduit clip, brake line clip, skirting structure, lamp mounting bracing, or placard holder.

Authorized Inspector (AI) — An inspector regularly employed by an ASME-accredited Authorized Inspection Agency (AIA) who has been qualified accordingto ASME developed criteria, to perform inspections under the rules of any Jurisdiction that has adopted the ASME Code.

Baffle — A nonliquid-tight transverse partition device that deflects, checks, or regulates fluid motion in a tank.

Bar — 1 BAR = 100 kPa (14.5 psi).

Bottle — An inner packaging having a neck of relatively smaller cross-section than the body and an opening capable of holding a closure for retention of the contents.

Bottom Shell — That portion of a tank car surface, excluding the head ends of the tank car, that lies within two feet, measured circumferentially, of the bottom longitudinal center line of the tank car tank.

Bulk Packaging — A packaging other than the vessel or a barge, including a transport vehicle or freight container, in which hazardous materials are loaded with no intermediate form of containment and which has:

a) A maximum capacity greater than 450 l (119 gallons) as a receptacle for a liquid;

b) A maximum net mass greater than 400 kg (882 pounds) and a maximum capacity greater than 450 l (119 gallons) as a receptacle for a solid; or

c) A water capacity greater than 454 kg (1,000 pounds) as a receptacle for a gas.

Bulkhead — A liquid-tight transverse closure at the ends of or between (compartment) cargo tanks.

Cargo Tank — A bulk packaging which:

a) Is a tank intended primarily for the carriage of liquids or gases and includes appurtenances, reinforcements, fittings, and closures;

b) Is permanently attached to or forms a part of a motor vehicle, or is not permanently attached to a motor vehicle but which, by reason of its size, construction, or attachment to a motor vehicle is loaded or unloaded without being removed from the motor vehicle; and

c) Is not fabricated under a specification for cylinders, portable tanks, tank cars, or multi-unit tank car tanks.

Cargo Tank Motor Vehicle — A motor vehicle with one or more cargo tanks permanently attached to or forming an integral part of the motor vehicle.

Carrier — A person engaged in the transportation of passengers or property by:

a) Land or water, as a common, contract, or private carrier; or

b) Civil aircraft.

Certified Individual — An individual that is qualified and certified by a manufacturer accredited by ASME to construct Class 3 Section XII Transport Tanks.

Combination Packaging — A combination of packaging for transport purposes, consisting of one or more inner packaging secured in a non-bulk outer packaging. It does not include a composite packaging.

Combustible Liquid — Any liquid that does not meet the definition of any other hazard class specified in 173.129 of Title 49 and has a flash point above 60.5°C (141.5°F) and below 93°C (100°F).

Competent Authority — A national agency responsible under its national law for the control or regulation of a particular aspect of the transportation of hazardous materials. In the United States, the Associate Administrator of the US Department of Transportation is the Competent Authority.

Composite Packaging — A packaging consisting of an outer package and an inner receptacle so constructed that the inner receptacle and the outer package are integral. Once assembled, it remains an integrated single unit. It is filled, stored, shipped, and emptied as such.

Compressed Gas in Solution — A non-liquefied compressed gas that is dissolved in a solvent.

Constructed and Certified in Accordance with the ASME Code — A cargo tank that is constructed and stamped in accordance with the ASME Code and is inspected and certified by an Authorized Inspector, Qualified Inspector, or a Certified Individual.

Corrosive Material — A liquid or solid that causes full thickness destruction of human skin at the site of contact within a specified period of time. A liquid that has a severe corrosion rate on steel or aluminum based on the criteria in 173.173(c) (3) of Title 49 is also a corrosive material.

Cryogenic Liquid — A refrigerated liquefied gas having a boiling point colder than -90°C (-130°F) at 101.3 kPa (14.7 psia) absolute.

Design Certification — That each cargo tank or cargo tank motor vehicle design type, including its required accident damage protection device, must be certified to conform to the specification requirements by a Design Certifying Engineer who is registered with the department. An accident damage protection device is a rear-end protection, overturn protection, or piping protection.

Design Certifying Engineer — A person registerd with the department in accordance with Subpart F of Part 107 of 49 CFR who has the knowledge and ability to perform stress analysis of pressure vessels and otherwise determine whether a cargo tank design and construction meets the applicable DOT specification. In addition, Design Certifiying Engineer means a person who meets, at a minimum, any one of the following:

a) Has an engineering degree and one year of work experience in cargo tank structural or mechanical design;

b) Is currently registered as a professional engineer by the appropriate authority of a state of the United States or a province of Canada; or

c) Has at least three years experience in performing the duties of a Design Certifying Engineer by September 1, 1991, and was registered with the department by December 31, 1995.

Design Type — One or more cargo tanks that are made:

a) To the same specification;

b) By the same manufacturer;

c) To the same engineering drawings and calculations, except for minor variations in piping that do not affect the lading retention capabilities of the cargo tank;

d) Of the same materials of constructions;

e) To the same cross-sectional dimensions;

f) To a length varying by no more than 5 percent;

g) With the volume varying by no more than 5 percent (due to the change in length only); and

h) For the purposes of 178.338 of Title 49 only, with the same insulation system.

DOT or Department — US Department of Transportation.

Elevated Temperatures Material — A material which, when offered for transportation or transported in a bulk packaging:

a) Is in a liquid phase and at a temperature at or above 100°C (212°F);

b) Is in a liquid phase with a flash point at or above 37.8°C (100°F) that is intentionally heated and offered for transportation, or transported at or above the flash point; or

c) Is in a solid phase and at a temperature at or above 240°C (464°F).

Extreme Dynamic Loadings — The maximum loading of a cargo tank motor vehicle may experience during its expected life, excluding accident loadings resulting from an accident, such as overturn or collision.

Flammable Gas — Any material that is a gas at 20°C (68°F) or less and 101.3 kPa (14.7 psia) of pressure [a material that has a boiling point of 20°C (68°F) or less at 101.3 kPa (14.7 psia)] which:

a) Is ignitable at 101.3kPa (14.7 psia) when in a mixtue of 13% or less by volume with air; or

b) Has a flammable range at 101.3kPa (14.7 psia) with air of at least 12% regardless of the lower limit. Except for aerosols, the limits specified in paragraphs 1) and 2) shall be determined at 101.3kPa (14.7 psia) of pressure and a temperature of 20°C (68°F) in accordance with the ASTM E681-85, *Standard Test Method for Concentration Limits of Flammability of Chemicals*, or other equivalent method approved by the Associate Administrator, Hazardous Material Safety.

Gas — A material that has a vapor pressure greater than 300 kPa (43.5 psia) at 50°C (122°F) or is completely gaseous at 20°C (68°F) at a standard pressure of 101.3 kPa (14.7 psia).

Gross Weight or Gross — The weight of a packaging plus the weight of its contents.

Hazardous Class — The category of hazard assigned to a hazardous material under the definitional criteria of Part 173 of Title 49 and the provisions of the 172.101 Table. A material should meet the defining criteria for more than one hazard class but is assigned to only one hazard class.

Hazardous Material — A substance or material that the Secretary of Transportation has determined is capable of posing an unreasonable risk to health, safety, and property when transported in commerce and has been designated as hazardous under section 5103 of Federal Hazardous Law (49 U.S.C. 5103). The term includes hazardous substances, hazardous wastes, marine pollutants, elevated temperature materials, materials designated as hazardous in the Hazardous Material Table (49 CFR 172.101), and materials that meet the defining criteria for hazard classes and divisions of 173 of subchapter C of 171.8 of Title 49.

Hazardous Zones — One of four levels of hazard (Hazard Zones A through D) as assigned to gases, as specified in 173.116(a) of Title 49, and one of two levels of hazard (Hazard Zones A and B) assigned to liquids that are poisonous by inhalation as specified in 173.133(a) of Title 49. A hazard zone is based on the LC 50 value for acute inhalation toxicity of gases and vapors.

High Pressure Liquefied Gas — A gas with a critical temperature between -50°C (-58°F) and + 65°C (149°F).

Inner Packaging — A packaging for which an outer packaging is required for transport. It does not include the inner receptacle of a composite packaging.

Inner Receptacle — A receptacle that requires an outer packaging in order to perform its containment function. The inner receptacle should be an inner packaging of a combination packaging or the inner receptacle of a composite packaging.

Inspection Pressure — The pressure used to determine leak tightness of the cargo tank when testing with pneumatic or hydrostatic pressure.

Lading — The hazardous material contained in the cargo tank.

Liquefied Compressed Gas — a gas which, when packaged under pressure for transportation, is partially liquid at temperatures above -50°C (-58°F).

Liquid — A material, other than an elevated temperature material, with a melting point or initial melting point of 20°C (68°F) or lower at a standard pressure of 101.3 kPa (14.7 psig). Liquid Phase means a material that meets the definition of liquid when evaluated at the higher of the temperature at which it is offered for transportation or at which it is transported, not at the 37.8°C (100°F) temperature specified in ASTM D 4359-84.

Low-Pressure Liquefied Gas — A gas with a critical temperature above + 65°C (149°F).

Manufacturer — Any person engaged in the manufacture of a DOT specification cargo tank, cargo tank motor vehicle, or cargo tank equipment that forms part of the cargo tank wall. This term includes attaching a cargo tank to a motor vehicle or to a motor vehicle suspension component that involves welding on a cargo tank wall. A manufacturer must register with the department in accordance Subpart F of Part 107 in Subpart A of 49 CFR.

Marking — A descriptive name, identification number, instructions, cautions, weight, specification, or UN marks, or combinations thereof, required by Title 49 on outer packaging or hazardous materials.

Mode — Any of the following transportation methods: rail, highway, air, or water.

Modification — Any change to the original design and construction of a cargo tank or a cargo tank motor vehicle that affects its structural integrity or lading retention capability including changes to equipment certified as part of an emergency discharge control system. Any modification that involves welding on the cargo tank wall must also meet all requirements for “Repair” as defined in this section. Excluded from this category are the following:

a) A change to motor vehicle equipment such as lights, truck, or tractor power train components, steering, and brake systems, suspension parts, and changes to appurtenances, such as fender attachments, lighting brackets, ladder brackets; and

b) Replacement of components such as valves, vents, and fittings with a component of a similar design and of the same size.

Motor Vehicle — A vehicle, machine, tractor, trailer, or semi-trailer, or any combination thereof, propelled or drawn by mechanical power and used upon the highways in the transportation of passengers or property. It does not include a vehicle operated exclusively on a rail or rails or a trolley bus operated by electric power derived from a fixed overhead wire, furnishing local passenger transportation similar to street-railway service.

Multi-Specification Cargo Tank Motor Vehicle — A cargo tank with two or more cargo tanks fabricated to more than one cargo tank specification.

Non-Liquefied Compressed Gas — When packaged under pressure for transportation is entirely gaseous at -50°C (-58°F) with a critical temperature less than or equal to -50°C (-58°F).

Normal Operating Loading — A cargo tank motor vehicle equipped with two or more cargo tanks fabricated to more than one cargo tank specification.

Operator — A person who controls the use of aircraft, vessel, or vehicle.

Outer Packaging — The outermost enclosure of a composite or combination packaging together with any absorbent material, cushioning, and any other components necessary to contain and protect inner receptacles or inner packaging.

Owner — The person who owns a cargo tank motor vehicle used for the transportation of hazardous materials, or that person’s authorized agent.

Packaging — A receptacle and any other components or materials necessary for the receptacle to perform its containment function in conformance with the minimum packing requirements of Title 49.

Packing Group — A grouping according to the degree of danger present by hazardous materials. Packing Group I indicates great danger; Packing Group II indicates medium danger; Packing Group III indicates minor danger.

Person — An individual, firm, co-partnership, corporation, company, association, or joint-stock (including any trustee, receiver, assignee, or similar representative); or any government or Indian tribe (or an agency or instrumentality of any government or Indian tribe) that transports hazardous material to further a commercial enterprise or offers a hazardous material for transportation in commerce.

Poisonous Gas — A material that is a gas at 20°C (68°F) or less and a pressure of 101.3 kPa (14.7 psia) a material that has a boiling point of 20°C (68°F) or less at 101.3 kPa (14.7 psia) and which:

a) Is known to be so toxic to humans as to pose a hazard to health during transportation; or

b) In the absence of adequate data on human toxicity, is presumed to be toxic to humans because when tested on laboratory animals it has an LC50.

Poisonous Material — A material, other than a gas, which is known to be so toxic to humans as to afford a hazard to health during transportation, or which in the absence of adequate data on human toxicity.

Portable Tanks — A bulk packaging (except cylinders having a water capacity of 454 kg (1,000 lb) or less) designated primarily to be loaded onto, or on, or temporarily attached to, a transport vehicle or ship and equipped with skids, mountings, or accessories to facilitate handling of the tank by mechanical means. It does not include a cargo tank, tank car, multi-unit tank car tanks, or trailers carrying 3AX, 3AAX, or 3T cylinders.

psi — Pounds per square inch.

psia — Pounds per square inch absolute.

psig — Pounds per square inch gage.

Qualified Inspector — An Inspector regularly employed by an ASME Qualified Inspection Organization (QIO) who has been qualified to ASME developed criteria by a written examination, to perfom inspections under the rules of any jurisdiction that has adopted the ASME Code. The QI shall not be in the employ of the manufacturer. See ASME XII, TG-410.

Rail Car — A car designed to carry freight or nonpassenger personnel by rail, and includes a box car, flat car, gondola car, hopper car, tank car, and occupied caboose.

Rebarrelling — Replacing more than 50% of the combined shell and head material of a cargo tank.

Receptacle — A containment vessel for receiving and holding materials, including any means of closing.

Registered Inspector (RI) — A person registered with the department in accordance with Subpart F of Part 107 of 49 CFR who has the knowledge and ability to determine whether a cargo tank conforms with the applicable DOT specification. In addition, Registered Inspector means a person who meets, at a minimum, any one of the following:

a) Has an engineering degree and one year of work experience;

b) Has an associate degree in engineering and two years of work experience;

c) Has a high school diploma or General Equivalency Diploma and three years work experience; or

d) Has at least three years experience performing the duties of a Registered Inspector by September 1,

1991, and was registered with the DOT by December 31, 1995.

Repair — Any welding on a cargo tank wall done to return a cargo tank or a cargo tank motor vehicle to its orginial design and construction specification, or to a condition prescribed for a later equivalent specification in effect at the time of the repair. Excluded from this category are the following:

a) A change to motor vehicle equipment such as lights, truck, or tractor power train components. Steering and brake systems, suspension parts, and changes to appurtenances, such as fender attachments, lighting brackets, ladder brackets;

b) Replacement of components such as valves, vents, and fittings with a component of a similar design and of the same size; and

c) Replacement of an appurtenance by welding to a mounting pad.

Replacement of a Barrel — To replace the existing tank on a motor vehicle chassis with an unused (new) tank.

SCF (standard cubic foot) — One cubic foot of gas measured at 16°C (60°F) and 10 kPa (14.7 psi).

Single Packaging — A nonbulk packaging other than a combination packaging.

Solid — A material that is not a gas or liquid.

Solution — Any homogenous liquid mixture of two or more chemical compounds or elements that will not undergo any segregation under conditions normal to transportation.

Specification Packaging — A packaging conforming to one of the specifications or standards for packaging in Part 178 or Part 179 of Title 49.

Strong Outside Container — The outermost enclosure that provides protection against the unintentional release of its contents under conditions normally incident to transportation.

Tanks — A container, consisting of a shell and heads that form the pressure vessel having opening designed to accept pressure tight fittings or closure, excluding any appurtenances, reinforcements, fittings, or closures.

Test Pressure — The pressure to which a tank is subjected to determine structural integrity.

Top Shell — The tank car surface, excluding the head ends and bottom shell of the tank car.

Transport Vehicle — A cargo-car-carrying vehicle such as an automobile, van, tractor, truck, semi trailer, tank car, or rail car used for the transportation of cargo by any mode. Each cargo-carrying body (trailer, rail car, etc.) is a separate transport vehicle.

UFC — Uniform Freight Classification.

UN — United Nations.

UN Portable Tank — An intermodal tank having a capacity of more than 450 l (119 gal.). It includes a shell fitted with service equipment and structural equipment, including stabilizing members external to the shell and skids, mountings, or accessories to facilitate mechanical handling. A UN portable tank must be capable of being filled and discharged without the removal of its structural equipment and must be capable of being lifted when full. Cargo tanks, rail tank car tanks, nonmetallic tanks, nonspecification tanks, bulk bins, and IBC's and packaging made to cylinder specifications are not UN portable tanks.

UN Recommendation — The UN Recommendations on the Transport of Dangerous Goods.

UN Standard Packaging — A conforming to standards in the UN Recommendations.

Vessel — Includes every description of watercraft, used or capable of being used, as a means of transportation on the water.

Viscous Liquid — A liquid material that has a measured viscosity in excess of 2,500 centistokes at 25°C (77°F), when determined in accordance with the procedures specified in ASTM Method D 445-72 “Kinematic Viscosity of Transparent and Opaque Liquids (and the Calculation of Dynamic Viscosity),” or ASTM Method D 1200-70 “Viscosity of Paints, Varnishes, and Lacquers by Ford Viscosity Cup.”

S6.18 TABLES AND FIGURES

a) TABLE S6.13, Periodic Inspections and Tests

b) TABLE S6.13-a, Inservice Minimum Thickness for Steel and Steel Alloys

c) TABLE S6.13-b, Inservice Minimum Thickness for Aluminum and Aluminum Alloys

d) TABLE S6.13.4, Periodic Inspections and Tests

e) TABLE S6.13.6, Pressure Test Requirements

f) TABLE 6.13.11.2-a, Minimum Thickness for Heads

g) TABLE S6.13.11.2-b, Minimum Thickness for Shells, in.

h) TABLE S6.13.11.3-a, Minimum Thickness for Heads, (DOT 407) mm

i) TABLE S6.13.11.3-b, Minimum Thickness for Shells, (DOT407) mm

j) TABLE S6.13.11.4 M-a, Minimum Thickness for Heads (DOT 412)

k) TABLE S6.13.11.4-b, Minimum Thickness for Heads (DOT 412)

l) TABLE S6.13.11.4 M-b, Minimum Thickness for Heads (DOT 412)

m) TABLE S6.14, Inspection Intervals

n) TABLE S6.14.6, Pressure Testing Requirements

o) TABLE S6.14.6.4, “T” Codes

p) TABLE S6.15.1-a, Thickness of Plates and Safety Valve Requirements

q) TABLE S6.15.1b, Acceptable Materials with Acceptable Tensile Strength and Elongation Requirements

r) TABLE S6.15.3, Ton Tank Periodic Inspection and Test Frequencies

SUPPLEMENT 7
INSPECTION OF PRESSURE VESSELS IN LIQUEFIED PETROLEUM GAS SERVICE

S7.1 SCOPE

a) Containers designed for storing liquefied petroleum gas (LPG) can be stationary or can be mounted on skids. LPG is generally considered to be non-corrosive to the interior of the vessel. NBIC Part 2, Supplement 7 is provided for guidance of a general nature for the owner, user, or jurisdictional authority. There may be occasions where more detailed procedures will be required such as changing from one service to another (e.g., above ground to underground; or containers that are commercially refurbished).

b) The application of this supplement to underground containers will only be necessary when evidence of structural damage to the vessel has been observed, leakage has been determined, or the tank has been dug up, and is to be reinstalled. Special consideration will be given to containers that are going to be commercially refurbished (see NBIC Part 2, S7.9).

S7.2 PRE-INSPECTION ACTIVITIES

a) A review of the known history of the container should be performed. This should include a review of information, such as:

   1) Operating conditions;

   2) Historical contents of the vessel;

   3) Results of any previous inspection;

   4) Current jurisdictional inspection certificate, if required;

   5) ASME Code symbol stamping or mark of code of construction, if required; and

   6) National Board and/or jurisdictional registration number, if required.

b) The container shall be sufficiently cleaned to allow for visual inspection. For commercially refurbished containers see NBIC Part 2, S7.9.

S7.3 INSERVICE INSPECTION FOR VESSELS IN LP GAS SERVICE

The type of inspection given to pressure vessels should take into consideration the condition of the vessel and the environment in which it operates. The inspection may be external or internal, and use a variety of nondestructive examination methods. Where there is no reason to suspect an unsafe condition or where there are no inspection openings, internal inspections need not be performed. When service conditions change from one service to another, i.e. above ground to underground; or containers that are commercially refurbished, an internal inspection may be required. The external inspection may be performed when the container is pressurized or depressurized, but shall provide the necessary information that the essential sections of the vessel are of a condition to operate.

S7.3.1 NONDESTRUCTIVE EXAMINATION (NDE)

Listed below are a variety of methods that may be employed to assess the condition of the pressure vessel. These examination methods should be implemented by experienced and qualified individuals. Generally, some form of surface preparation will be required prior to the use of these examination methods: visual, magnetic particle, liquid penetrant, ultrasonic, radiography, radioscopy, eddy current, metallographic

examination, and acoustic emission. When there is doubt as to the extent of a defect or detrimental condition found in a container, additional NDE may be required.

S7.4 EXTERNAL INSPECTION

The container shall be inspected for corrosion, distortion, cracking, or other conditions as described in this section. In addition, the following should be reviewed, where applicable:

a) Insulation or Coating

If the insulation or coating is in good condition and there is no reason to suspect an unsafe condition behind it, then it is not necessary to remove the insulation or coating in order to inspect the vessel. However, it may be advisable to remove a small portion of the insulation or coating in order to determine its condition and the condition of the container surface. For commercially refurbished containers see NBIC Part 2, S7.9.

b) Evidence of Leakage

Any leakage of vapor or liquid shall be investigated. Leakage coming from behind insulation or coating, supports, or evidence of past leakage shall be thoroughly investigated by removing any insulation necessary until the source is established.

c) Structural Attachments

The pressure vessel mountings should be checked for adequate allowance for expansion and contraction, such as provided by slotted bolt holes or unobstructed saddle mountings. Attachments of legs, saddles, skirts, or other supports should be examined for distortion or cracks at welds.

d) Vessel Connections

Components that are exterior to the vessel and are accessible without disassembly shall be inspected as described in this paragraph. Manholes, reinforcing plates, nozzles, couplings, or other connections shall be examined for cracks, deformation, or other defects. Bolts or nuts should be examined for corrosion or defects. Weep holes in reinforcing plates shall remain open to provide visual evidence of leakage as well as to prevent pressure buildup between the vessel and the reinforcing plate. Accessible flange faces should be examined for distortion. It is not intended that flanges or other connections be opened unless there is evidence of corrosion to justify opening the connection.

e) Fire Damage

Pressure vessels shall be carefully inspected for evidence of fire damage. The extent of fire damage determines the repair that is necessary, if any. (See NBIC Part 2, S7.7).

S7.5 INTERNAL INSPECTION

When there is a reason to suspect an unsafe condition, the suspect parts of the vessel shall be inspected and evaluated.

The vessel shall be prepared and determined to be gas-free and suitable for human entry prior to internal inspection. (See NBIC Part 2, 2.3.4).

S7.6 LEAKS

Leakage is unacceptable. When leaks are identified, the vessel shall be removed from service until repaired by a qualified repair organization or permanently removed from service.

S7.7 FIRE DAMAGE

a) Vessels in which bulging exceeds the limits of NBIC Part 2, S7.8.3 or distortion that exceeds the limits of the original code of construction (e.g., ASME Section VIII, Div. 1), shall be removed from service until repaired by a qualified repair organization or permanently removed from service.

b) Common evidence of exposure to fire is:

1) Charring or burning of the paint or other protective coat;

2) Burning or scarring of the metal;

3) Distortion; or

4) Burning or melting of the valves.

c) A pressure vessel that has been subjected to action of fire shall be removed from service until it has been properly evaluated. The general intent of this requirement is to remove from service pressure vessels which have been subject to action of fire that has changed the metallurgical structure or the strength properties of the steel. Visual examination with emphasis given to the condition of the protective coating can be used to evaluate exposure from a fire. This is normally determined by visual examination as described above with particular emphasis given to the condition of the protective coating. If there is evidence that the protective coating has been burned off any portion of the pressure vessel surface, or if the pressure vessel is burned, warped, or distorted, it is assumed that the pressure vessel has been overheated. If, however, the protective coating is only smudged, discolored, or blistered, and is found by examination to be intact underneath, the pressure vessel shall not be considered affected within the scope of this requirement. Containers that have been involved in a fire and show no distortion shall be requalified for continued service by retesting using the liquid pressure test procedure applicable at the time of original fabrication.

d) Subject to the acceptance of the Jurisdiction and the Inspector, alternate methods of pressure testing may be used.

S7.8 ACCEPTANCE CRITERIA

The acceptance criteria for LPG vessels is based on successfully passing inspections without showing conditions beyond the limits shown below.

S7.8.1 CRACKS

Cracks in the pressure boundary (e.g., heads, shells, welds) are unacceptable. When a crack is identified, the vessel shall be removed from service until the crack is repaired by a qualified repair organization or permanently retired from service. (See NBIC Part 3, Repairs and Alterations).

S7.8.2 DENTS

a) Shells

The maximum mean dent diameter in shells shall not exceed 5% of the shell diameter, and the maximum depth of the dent shall not exceed 5% of the mean dent diameter. The mean dent diameter is defined as the average of the maximum dent diameter and the minimum dent diameter. If any portion of the dent is closer to a weld than 5% of the shell diameter, the dent shall be treated as a dent in a weld area, see b) below.

b) Welds

The maximum mean dent diameter on welds (i.e., part of the deformation includes a weld) shall not exceed 10% of the shell diameter. The maximum depth shall not exceed 5% of the mean dent diameter.

c) Head

The maximum mean dent diameter on heads shall not exceed 10% of the shell diameter. The maximum depth shall not exceed 5% of the mean dent diameter. The use of a template may be required to measure dents on heads.

d) When dents are identified which exceed the limits set forth in these paragraphs, the vessel shall be removed from service until the dents are repaired by a qualified repair organization or permanently retired from service.

S7.8.3 BULGES

a) Shells

If a bulge is suspected, the circumference shall be measured at the suspect location and in several places remote from the suspect location. The variation between measurements shall not exceed 1%.

b) Heads

1) If a bulge is suspected, the radius of curvature shall be measured by the use of templates. At any point the radius of curvature shall not exceed 1.25% of the diameter for the specified shape of the head.

2) When bulges are identified that exceed the limits set forth in these paragraphs, the vessel shall be removed from service until the bulges are repaired by a qualified repair organization or permanently retired from service.

S7.8.4 CUTS OR GOUGES

When a cut or a gouge exceeds 25% of the thickness of the vessel, the vessel shall be removed from service until it is repaired by a qualified repair organization or permanently removed from service.

S7.8.5 CORROSION

a) Line and Crevice Corrosion

For line and crevice corrosion, the depth of the corrosion shall not exceed 25% of the original wall thickness.

b) Isolated Pitting

Isolated pits may be disregarded provided that:

1) Their depth is not more than 25% the required thickness of the container wall;

2) The total area of the pits does not exceed 7 sq. in. (4,500 sq. mm) within any 8 in. (200 mm) diameter circle; and

3) The sum of their dimensions along any straight line within this circle does not exceed 2 in. (50 mm).

c) General Corrosion

For a corroded area of considerable size, the thickness along the most damaged area may be averaged over a length not exceeding 10 in. (250 mm). The thickness at the thinnest point shall not be less than 75% of the required wall thickness, and the average shall not be less than 90% of the required wall thickness. When general corrosion is identified that exceeds the limits set forth in this paragraph, the pressure vessel shall be removed from service until it is repaired by a qualified "R" Stamp holder or permanently removed from service unless an acceptable for service evaluation is performed in accordance with NBIC Part 2, 4.4.

S7.8.6 ANHYDROUS AMMONIA SERVICE

Containers that have been previously used in anhydrous ammonia service shall not be converted to LPG service. Any blue coloring of the brass valves indicates that the container has been in anhydrous ammonia service.

S7.9 ASME LPG CONTAINERS LESS THAN 2000 GALLONS BEING REFURBISHED BY A COMMERCIAL SOURCE.

Commercially refurbished containers are used containers that are temporarily taken out of service for repair and or renewal and sent to a company which specializes in this type of work. Because the history of some of these containers is unknown, special attention shall be given to inspection and repair before returning any of these containers back to service. ASME LPG containers less than 2,000 gal. (7,570 l) may be refurbished subject to the following conditions:

a) A complete external inspection shall be completed under the guidelines of this supplement. If any defects are found, as defined in S7.8.1 through S7.8.5, the defect shall be repaired under NBIC Part 3, Repairs and Alterations, by qualified personnel or permanently removed from service;

b) Containers that have been previously used in anhydrous ammonia service shall not be converted to LPG service. See NBIC Part 2, S7.8.6;

c) The coating on the outside of the container shall be removed down to bare metal so that an inspection can be performed under the guidelines of this supplement; and

d) Verify that there is no internal corrosion if the tank has had its valves removed or is known to have been out of service for an extended period.

(15) S7.10 REQUIREMENTS FOR CHANGE OF SERVICE FROM ABOVE GROUND TO UNDERGROUND SERVICE

ASME LPG storage vessels may be altered from above ground (AG) service to underground (UG) service subject to the following conditions.

a) Vessels that have been previously used in anhydrous ammonia service are not permitted to be converted to LPG service.

b) The outside surface of the vessel shall be cleaned to bare metal for an external inspection of the vessel under the guidelines of this supplement. Prior to placing underground, the outside surface of the vessel shall be prepared consistent with the paint manufactures specification and coated with a coating suitable for UG service. Any touch-up coating shall be the same coating material. All corrosion shall be repaired in accordance with the NBIC.

c) Verify that there is no internal corrosion due to valves having been removed while the container is out or service.

d) Any unused connections located on the vessel shall be closed by seal welding around a forged plug or removed using a flush patch. If a flush patch is used the material shall be the same material thickness and material grade as the original code of construction.

e) All connections on top of the vessel, except for the liquid withdrawal opening, shall be replaced with a riser pipe with multi-valve suitable for UG LPG service. The valve shall be enclosed in a protective housing and placed underground in accordance with jurisdictional requirements.

f) The liquid withdrawal opening shall be located within the protective housing.

g) The liquid level tube in the multivalve shall be the length required according to jurisdictional requirements.

h) The NBIC nameplate shall be made of stainless steel and continuous welded to the vessel wall. The nameplate shall also have the information from the original nameplate. This shall include the manufactures name, container serial number, National Board number, (if registered with the National Board) MAWP, year built, head and shell thickness, be stamped for “UG service”, the “liquid level tube length = inches” and the National Board “R” stamp. The original manufacturer’s nameplate shall remain attached to the vessel. See Part 2, Section 5.2 of this Part and NBIC, Part 3, Section 5.7 for additional stamping requirements.

i) The support legs and lifting lugs may remain in place and shall be welded around the entire periphery to prevent crevices that create a potential area for corrosion. Unused attachments shall be removed and welds ground flush.

j) A connection shall be added for the attachment of an anode for cathodic protection, per NFPA, 58 .

k) All welding shall be performed by a holder of a current “R” Certificate of Authorization, using a qualified welding procedure.

SUPPLEMENT 8
PRESSURE DIFFERENTIAL BETWEEN SAFETY OR SAFETY RELIEF VALVE SETTING AND BOILER OR PRESSURE VESSEL OPERATING PRESSURE

S8.1 SCOPE

If a safety valve or safety relief valve is subjected to pressure at or near its set pressure, it will tend to weep or simmer, and deposits may accumulate in the seat and disk area. Eventually, this can cause the valve to freeze closed and thereafter the valve could fail to open at the set pressure. Unless the source of pressure to the boiler or pressure vessel is interrupted, the pressure could exceed the rupture pressure of the vessel. It is important that the pressure differential between the valve set pressure and the boiler or pressure vessel operating pressure is sufficiently large to prevent the valve from weeping or simmering.

S8.2 HOT-WATER HEATING BOILERS

For hot-water heating boilers, the recommended pressure differential between the pressure relief valve set pressure and the boiler operating pressure should be at least 10 psi (70 kPa), or 25% of the boiler operating pressure, whichever is greater. Two examples follow:

a) If the safety relief valve of a hot-water heating boiler is set to open at 30 psi (200 kPa), the boiler operating pressure should not exceed 20 psi (140 kPa).

b) If the safety relief valve of a hot water heating boiler is set to open at 100 psi (700 kPa), the boiler operating pressure should not exceed 75 psi (520 kPa). Section IV of the ASME Code does not require that safety relief valves used on hot water heating boilers have a specified blowdown. Therefore, to help ensure that the safety relief valve will close tightly after opening and when the boiler pressure is reduced to the normal operating pressure, the pressure at which the valve closes should be well above the operating pressure of the boiler.

S8.3 STEAM HEATING BOILERS

For steam heating boilers, the recommended pressure differential between the safety valve set pressure and boiler operating pressure should be at least 5 psi (35 kPa), i.e., the boiler operating pressure should not exceed 10 psi (70 kPa).

Since some absorption-type refrigeration systems use the steam heating boiler for their operation, the boiler operating pressure may exceed 10 psi (70 kPa). If the boiler operating pressure is greater than 10 psi (70 kPa), it should not exceed 15 psi (100 kPa), minus the blowdown pressure of the safety valve.

This recommendation can be verified by increasing the steam pressure in the boiler until the safety valve pops, then slowly reducing the pressure until it closes, to ensure that this closing pressure is above the operating pressure.

S8.4 POWER BOILERS

For power boilers (steam), the recommended pressure differentials between the safety valve set pressure and the boiler operating pressure (see NBIC Part 2, Table S8.4).

TABLE S8.4

MINIMUM PRESSURE DIFFERENTIAL AS PERCENTAGE OF BOILER DESIGN PRESSURE

DESIGN PRESSURE :		
	over 15 psi to 300 psi 10% but not less than 7 psi	(100 KPa to 2.10 MPa) (50 KPa)
	over 300 psi to 1,000 psi 7% but not less than 30 psi	(2.14 MPa to 6.89 MPa) (200 KPa)
	over 1000 psi to 2,000 psi 5% but not less than 70 psi	(6.89 MPa to 13.8 MPa) (480 KPa)
	over 2,000 psi per designer's judgment	(13.8 MPa)

Note 1:
Above 2,000 psi (13.8 MPa) the pressure differential between operating pressure and the maximum allowable working pressure is a matter for the designer's judgement, taking into consideration such factors as satisfactory operating experience and the intended service conditions.

Note 2:
Safety relief valves in hot water service are more susceptible to damage and subsequent leakage than safety valves relieving steam. It is recommended that the maximum allowable working pressure of the boiler and safety relief valve setting for high-temperature hot-water boilers be selected substantially higher than the desired operating pressure, so as to minimize the time the safety relief valve must lift.

S8.5 PRESSURE VESSELS

Due to the variety of service conditions and the various designs of pressure relief valves, only general guidelines can be given regarding differentials between the set pressure of the valve and the operating pressure of the vessel. Operating difficulty will be minimized by providing an adequate differential for the application. The following is general advisory information on the characteristics of the intended service and of the pressure relief valves that may bear on the proper pressure differential selection for a given application. These considerations should be reviewed early in the system design since they may dictate the maximum allowable working pressure of the system.

To minimize operational problems it is imperative that the user consider not only normal operating conditions of the fluids (liquids or gases), pressures, and temperatures, but also start-up and shutdown conditions, process upsets, anticipated ambient conditions, instrument response time,and pressure surges due to quick-closing valves, etc. When such conditions are not considered, the pressure relief devices may become, in effect, a pressure controller, a duty for which they were not designed. Additional consideration should be given to the hazard and pollution associated with the release of the fluid. Larger differentials may be appropriate for fluids which are toxic, corrosive, or exceptionally valuable.

The blowdown characteristics and capabilities are the first consideration in selecting a compatible valve and operating margin. After a self-actuated release of pressure, the valve must be capable of reclosing above the normal operating pressure. For example: if the valve is set at 100 psi (700 kPa) with a 7% blowdown, it will close at 93 psi (640 kPa). The operating pressure must be maintained below 93 psi (640 kPa) in order to prevent leakage or flow from a partially open valve. Users should exercise caution regarding the blowdown adjustment of large, spring-loaded valves. Test facilities, whether owned by the manufacturer, repair house, or user, may not have sufficient capacity to accurately verify the blowdown setting. The setting cannot be considered accurate unless made in the field on an actual installation.

Pilot operated valves represent a special case from the standpoint of both blowdown and tightness. The pilot portion of some pilot operated valves can be set at blowdowns as short as 2%. This characteristic is not, however, reflected in the operation of the main valve in all cases. The main valve can vary considerably from the pilot depending on the location of the two components in the system. If the pilot is installed remotely from the main valve, significant time and pressure lags can occur, but reseating of the pilot ensures reseating of the main valve. The pressure drop in connecting piping between the pilot and the main valve must not be excessive, otherwise the operation of the main valve will be adversely affected.

Tightness capability is another factor affecting valve selection, whether spring-loaded or pilot operated. Tightness varies somewhat depending on whether metal or resilient seats are specified and also on such factors as corrosion and temperature. The required tightness and test method should be specified to comply at a pressure not lower than the normal operating pressure of the process. It should be remembered that any degree of tightness obtained should not be considered permanent. Service operation of a valve almost invariably reduces the degree of tightness.

The following minimum pressure differentials are recommended unless the safety or safety relief valve has been designed or tested in a specific or similar service and a smaller differential has been recommended by the manufacturer:

a) For set pressures up to 70 psi (480 kPa), the recommended pressure differential is 5 psi (35 kPa);

b) For set pressure between 70 and 1,000 psi (480 kPa and 6.89 MPa), the recommended pressure differential is 10% of set pressure; and

c) For set pressures above 1,000 psi (6.89MPa), the recommended pressure differential is 7% of set pressure.

SUPPLEMENT 9
REQUIREMENTS FOR CHANGE OF SERVICE

(15)

S9.1 SCOPE

(15)

This supplement provides requirements and guidelines to be followed when a change of service or service type is made to a pressure-retaining item.

Whenever there is a change of service, the jurisdiction where the pressure-retaining item is to be operated shall be notified for acceptance. Any specific jurisdictional requirements shall be met.

S9.2 CLASSIFICATION OF SERVICE CHANGES

(15)

S9.2.1 SERVICE CONTENTS

(15)

A change in service contents is considered to be any modification to the commodity or contents that the pressure-retaining item was originally intended to contain when the pressure-retaining item was constructed.

For example, a change:

a) From LP gas service to air receiver service.

b) From lethal to non lethal service.

S9.2.2 SERVICE TYPE OR CHANGE OF USAGE

(15)

A change in service type is considered to be a change of how the pressure-retaining item is being used.

For example, a change:

a) From above ground service to underground service for LP gas tanks.

b) From mobile or transport use to stationary use.

S9.3 FACTORS TO CONSIDER

(15)

Before a change of service is to be made, the owner or user shall consider and evaluate the effects of the new operating conditions or environment on the existing condition and suitability for service of the pressure-retaining item. Various factors will have an impact on the reliability of the pressure-retaining item in its new service environment. Changes can be successfully adopted providing there is an understanding of the effect on the pressure-retaining item. However, there are some cases where changes are detrimental to the existing pressure-retaining item. The owner or user should seek technical guidance of experienced personnel in appropriate areas affected by the change of service (e.g. design, metallurgy, or operations of the pressure retaining item).

The following is a listing of criteria that should be evaluated as appropriate. The criterion is not limited to that listed herein. Other factors may be considered as necessary;

a) Design Consideration:

    1) Thickness of existing vessel material.

    2) Vessel or system flow rate or pressure.

    3) Weight of vessel with new contents.

4) Existing or additional loads imposed on nozzles and highly stressed areas.

5) Change in pressure or temperature, and cycling.

6) Compliance to product or industry standards, such as ANSI K61, API 579, or NFPA 58.

b) Material Consideration:

1) Chemical and mechanical properties of existing material or any new material to be added or replaced to ensure it has the required strength and toughness to withstand the pressure and temperature effects of the new environment.

2) Effects of erosion or corrosion.

3) Time dependent effects on service life - creep or fatigue, or both effects combined.

c) Environment

1) Physical condition of the pressure-retaining item.

2) Overpressure protection needs.

3) Regulatory environment – Verification of compliance to new or existing jurisdictional rules or regulations.

4) Vessel cleanliness – When changing lading fluids or contents consideration should be given to cleaning or decontaminating the vessel as appropriate.

d) Operational History

1) A review of current and past operational logs or records should be made to ensure that no conditions existed where any further use would render the pressure-retaining item hazardous or otherwise unsafe.

2) Records to be obtained and reviewed would include Manufacturer's Data Reports, Repair and Alteration Forms, Inspection reports, etc.

e) Repairs and Alterations Made:

A review of any repairs, alterations, reratings, or reconfigurations that have been performed on the pressure-retaining item, so as to ensure that they will not have a detrimental impact on the intended use.

f) Proposed Rework

1) Any physical work to be performed to restore the material to the existing or intended state or to meet any requirements for the new operating conditions.

2) Repairs and alterations shall be performed in accordance with NBIC Part 3, *Repair and Alterations*.

3) The effects of heat applied as a result of welding or heat treatment on the material or shaped parts.

4) The method and extent of any physical or non destructive examination should be considered.

5) Any physical testing or pressure testing to be performed to determine or verify leak tightness or structural integrity of the pressure-retaining item.

6) The pressure-retaining item shall meet the code requirements for the new environment at the time of change.

g) Documentation

1) Review existing records that are required to satisfy customer, user, or legal requirements.

2) Review the need for any marking, stamping, or labeling required for the intended service.

3) Review the need for developing or revising an inspection plan to ensure safe operation. Refer to Part 2, Section 1.5.2.1, *Inspection Plan*.

S9.4 SOME EXAMPLES FOR CHANGE OF SERVICE (15)

Table S9.4 lists examples of what constitutes a change in service and some factors to consider. Note: This list is not all inclusive. There may be other service changes not mentioned.

The listing of "Factors to Consider" is also not all inclusive. There may be other elements that can influence the safe and reliable operation of the pressure retaining item.

The owner shall check with the Jurisdiction where the pressure retaining item is to operate in the new environment, and review local building codes, laws, and regulations for additional requirements or prohibitions against a change of service.

TABLE S9.4

EXAMPLES OF CHANGE OF SERVICE CONDITIONS

Change	Some Factors to Consider
LP Gas to Ammonia	• PWHT of Vessel During Construction Wet-fluorescent magnetic particle testing (WFMT) on all internal surfaces • Internal access of vessel is necessary, may need to install manhole • NFPA 58 should be consulted
Ammonia to LP gas	• NFPA-58 should be consulted. i.e. restriction on maximum volume • Wet-fluorescent magnetic particle testing (WFMT) on all internal surfaces • Internal access of vessel is necessary., may need to install manhole • Also see, NBIC Part 2, 2.3.6.4
LP gas service: from above ground to underground	• Requires alterations (additional nozzles) • Corrosion protection • See NFPA 58
LP gas to air receiver	• Assurance of vessel cleanliness, i.e. removal of mercaptan • Appropriateness and number of inspection and drain openings • Corrosion allowance
Boiler Service: steam to hot water	• Nozzles may require modification for water inlet and outlet • Change of Pressure Relief Device

Change	Some Factors to Consider
Boiler Service: High-Pressure to Low-Pressure	• Controls required by the LP boiler code • Safety Valve Change • Need for larger openings for steam outlets and safety relief valves
Sulfur Dioxide Service Sweet to Sour Gas Service	• Concern Over Hydrogen Cracking
Inert to Oxidizing or Reducing Atmosphere	• Inspection for Damage mechinisims that may be present from previous service life that is detrimental to the vessel in the new environment • Cleanliness of Hydrocarbons
Lethal Service to Non-Lethal	• Design Conditions and suitability for service
DOT Railcars of ICC Transport Tanks to Stationary Service	• Prohibited by DOT regulations for permanent service • Temporary stationary service prohibited as per NFPA • Inspection or damage mechanisms that may be present from previous service life that is detrimental to the vessel in the new environment

(15) S9.5 DOCUMENTATION OF CHANGE OF SERVICE

Any records, forms, or reports required documenting the change of service event that may be required by contract or the jurisdiction where the pressure retaining item operates shall be completed. Such documentation should be retained by the owner or user for future reference or use as needed.

SUPPLEMENT 10 (15)
INSPECTION OF STATIONARY HIGH-PRESSURE (3,000-15,000 psi) (21-103 MPa) COMPOSITE PRESSURE VESSELS

S10.1 SCOPE (15)

This supplement provides specific guidelines for inspection of high-pressure composite pressure vessels, hereafter referred to as vessels. This supplement is applicable to pressure vessels with a design pressure that exceeds 3,000 psi (21 MPa) but not greater than 15,000 psi (103 MPa), and is applicable to the following four types of pressure vessels:

a) Metallic vessel with a hoop Fiber Reinforced Plastic (FRP) wrap over the straight shell cylindrical part of the vessel (both load sharing).

b) Fully wrapped FRP vessel with a non-load sharing metallic liner.

c) Fully wrapped FRP vessel with a non-load sharing non-metallic liner.

d) Fully wrapped FRP vessel with load sharing metallic liner.

This supplement is intended for inspection of ASME Section X, Class III, vessels and ASME Section VIII, Division 3, Composite Reinforced Pressure Vessels (CRPVs). However, it may be used for inspection of similar vessels manufactured to other construction codes with approval of the jurisdiction in which the vessels are installed.

S10.2 GENERAL (15)

a) High-pressure composite vessels are used for the storage of fluids at pressures up to 15,000 psi (103 MPa). Composite vessels consist of the FRP laminate with load sharing or non-load sharing metallic shells/liners, or nonmetallic liners. The FRP laminate with load sharing metallic liners form the pressure retaining system. The FRP laminate is the pressure-retaining material for composite vessels with non-load sharing metallic and nonmetallic liners. The purpose of the non-load sharing metallic and the nonmetallic liners is to minimize the permeation of fluids through the vessel wall.

b) Fluids stored in vessels are considered to be non corrosive to the materials used for vessel construction. The laminate is susceptible to damage from:

   1) External chemical attack.

   2) External mechanical damage(i.e. abrasion, impact, cuts, dents, etc.).

   3) Structural damage (i.e. over pressurization, distortion, bulging, etc.).

   4) Environmental degradation [i.e. ultraviolet (if there is no pigmented coating or protective layer), ice, etc.].

   5) Fire or excessive heat.

S10.3 INSPECTOR QUALIFICATIONS (15)

a) The Inspector referenced in this supplement is a National Board Commissioned Inspector.

b) The Inspector shall be familiar with vessel construction and qualified by training and experience to conduct such inspections. The Inspector should have a thorough understanding of all required inspections, tests, test apparatus, inspection procedures, and inspection techniques and equipment applicable to

the types of vessels to be inspected. The Inspector should have basic knowledge of the vessel material types and properties. Refer to NBIC Part 2, S4.2 and S4.5.

c) The acoustic emission technician conducting the examination required per S10.5(c) and in accordance with S10.10 shall be certified per the guidelines of ASNT SNT-TC-1A or CP-189 AE Level II or III. A technician performing this test shall have training in and experience with measuring C_e and C_f in composites and identifying wave modes.

(15) S10.4 INSPECTION FREQUENCY

a) Initial Inspection

The vessel shall be given an external visual examination by the Inspector or the Authority having jurisdiction where the vessel is installed and during the initial filling operation. The examination shall check for any damage during installation prior to initial filling and for any leaks or damage during and at the conclusion of filling.

b) Subsequent Filling Inspections

Before each refilling of the vessel, the manager of the facility shall visually examine the vessel exterior for damage or leaks. Refilling operations shall be suspended if any damage or leaks are detected and the vessel shall be emptied and subsequently inspected by the Inspector to determine if the vessel shall remain in service.

c) Periodic Inspection

Within 30 days of the anniversary of the initial operation of the vessel during each year of its service life, the vessel shall be externally examined by the Inspector or the Authority having jurisdiction where the vessel is installed. Internal inspections shall only be required if any of the conditions of S10.9 a) are met. These examinations are in addition to the periodic acoustic emission examination requirements of S10.5 c).

(15) S10.5 INSERVICE INSPECTION

a) NBIC Part 2, Section 1, of this part shall apply to inspection of high-pressure vessels, except as modified herein. This supplement covers vessels, and is not intended to cover piping and ductwork, although some of the information in this supplement may be used for the inspection of piping and ductwork.

b) The inspection and testing for exposed load sharing metallic portions of vessels shall be in accordance with NBIC Part 2, Section 2.3.

c) All composite vessels shall have an initial acoustic emission examination per S10.10 after the first three years from the date of manufacture. Thereafter, vessels shall have a maximum examination interval of fiveyears which may be more frequent based on the results of any external inspection per S10.8 or internal inspections per S10.9.

All vessels shall be subject to the periodic inspection frequency given in S10.4.

(15) S10.6 ASSESSMENT OF INSTALLATION

a) The visual examination of the vessel requires that all exposed surfaces of the vessel are examined to identify any degradation, defects, mechanical damage, or environmental damage on the surface of the vessel.

The causes of damage to vessels are:

1) abrasion damage;

2) cut damage;

3) impact damage;

4) structural damage;

5) chemical or environmental exposure damage or degradation; and

6) heat or fire damage.

The types of damage found are:

1) cracks;

2) discolored areas;

3) gouges and impact damage;

4) leaks;

5) fiber exposure;

6) blisters;

7) delaminations;

8) surface degradation; and

9) broken supports.

b) The visual examination of the vessel requires that the identity of the vessel must be verified. This should include the construction code (ASME) to which the vessel was constructed, vessel serial number, maximum allowable operating pressure, date of manufacture, vessel manufacturer, date of expiration of the service life of the vessel, and any other pertinent information shown on the vessel or available from vessel documents. The overall condition of the vessel should be noted.

S10.7 VISUAL EXAMINATION (15)

a) Acceptable Damage

Acceptable damage or degradation is minor, normally found in service, and considered to be cosmetic. This level of damage or degradation does not reduce the structural integrity of the vessel. This level of damage or degradation should not have any adverse effect on the continued safe use of the vessel. This level of damage or degradation does not require any repair to be performed at the time of in-service inspection. When there is an external, non load bearing, sacrificial layer of filaments on the vessel, any damage or degradation should be limited to this layer. Damage or degradation of the structural wall shall not exceed the limits specified in Tables S10.7-a or S10.7-b.

b) Rejectable Damage (Condemned—Not Repairable)

Rejectable damage or degradation is so severe that structural integrity of the vessel is sufficiently reduced so that the vessel is considered unfit for continued service and shall be condemned and removed from service. No repair is authorized for vessels with rejectable damage or degradation.

c) Acceptance Criteria

Certain, specific types of damage can be identified by the external in-service visual examination. Indications of certain types and sizes may not significantly reduce the structural integrity of the vessel and may be acceptable so the vessel can be left in service. Other types and larger sizes of damages

may reduce the structural integrity of the vessel and the vessel shall be condemned and removed from service. Tables S10.7-a or S10.7-b are a summary of the acceptance/rejection criteria for the indications that are found by external examination of the vessel.

d) Fitness for service

1) If a visual examination reveals that a vessel does not meet all criteria of Table S10.7-a or S10.7-b satisfactorily, it shall be taken out of service immediately, and either be condemned or a fitness for service examination be conducted by the original vessel manufacturer or legal successor who must also hold a National Board "R" certificate. When the vessel is taken out of service, its contents shall be immediately safely vented or transferred to another storage vessel per the owner's written safety procedures.

2) If a fitness for service examination is to be conducted, the original vessel manufacturer shall be contacted as soon as possible after the rejectable defects have been found. The manufacturer shall then determine the vessel fitness-for-service by applicable techniques, (e.g., acoustic emission testing, ultrasonic testing, and/or other feasible methods). The manufacturer shall have documentation that the evaluation method(s) used is satisfactory for determining the condition of the vessel. Repairs to the outer protective layer may be made by a "R" certificate holder other than the original manufacturer following the original manufacturer's instructions.

3) Determination of fitness for service is restricted to original manufacturer or legal successor.

(15) **TABLE S10.7-a**

VISUAL ACCEPTANCE/REJECTION CRITERIA FOR COMPOSITE PRESSURE VESSELS (U.S. CUSTOMARY UNITS)

Type of Degradation or Damage	Description of Degradation or Damage	Acceptable Level of Degradation or Damage	Rejectable Level of Degradation or Damage
Abrasion	Abrasion is damage to the filaments caused by wearing or rubbing of the surface by friction.	Less than 0.050 in. depth in the pressure bearing thickness.	≥ 0.050 in. depth in the pressure bearing thickness.
Cuts	Linear indications flaws caused by an impact with a sharp object.	Less than 0.050 in. depth in the pressure bearing thickness.	≥ 0.050 in. depth in the pressure bearing thickness.
Impact Damage	Damage to the vessel caused by striking the vessel with an object or by being dropped. This may be indicated by discoloration of the composite or broken filaments and/or cracking.	Slight damage that causes a frosted appearance or hairline cracking of the resin in the impact area.	Any permanent deformation of the vessel or damaged filaments.
Delamination	Lifting or separation of the filaments due to impact, a cut, or fabrication error.	Minor delamination of the exterior coating.	Any loose filament ends showing on the surface. Any bulging due to interior delaminations.

Type of Degradation or Damage	Description of Degradation or Damage	Acceptable Level of Degradation or Damage	Rejectable Level of Degradation or Damage
Heat or Fire Damage	Discoloration, charring or distortion of the composite due to temperatures beyond the curing temperature of the composite.	Merely soiled by soot or other debris, such that the cylinder can be washed with no residue.	Any evidence of thermal degradation or discoloration or distortion.
Structural Damage – bulging, distortion, depressions	Change in shape of the vessel due to sever impact or dropping.	None	Any visible distortion, bulging, or depression.
Chemical attack	Environmental exposure that causes a change in the composite or failure of the filaments.	Any attack that can be cleaned off and that leaves no residue.	Any permanent discoloration or loss or softening of material under the exterior coat.
Cracks	Sharp, linear indications	None	None
Scratches/Gouges	Sharp, linear indications caused by mechanical damage.	Less than 0.050 in. depth in the pressure bearing thickness No structural fibers cut or broken.	≥ 0.050 in. depth in the pressure bearing thickness or structural fibers cut or broken.
Soot	A deposit on the composite caused by thermal or environmental exposure.	Soot that washes off and leaves no residue.	Any permanent marking that will not wash off the surface under the exterior coating.
Over pressurization	Excessive pressure due to operational malfunction.	None reported	Any report of pressurization beyond the MAWP or any indication of distortion.
Corrosion	Degradation of the composite due to exposure to specific corrosive environments.	None visible	Any surface damage to structural identified as corrosion. (See Note 2)
Dents	A depression in the exterior of the vessel caused by impact or dropping.	< 1/16 in. in depth	Any dents with a depth ≥ 1/16 in. Or with a diameter greater than 2 inches.
Reported collision, accident, or fire	Damage to the vessel caused by unanticipated excursion from normally expected operating conditions.	None reported	Any indication or report of impact or heat damage.
Environmental Damage or Weathering	Ultraviolet or other environmental attack under the exterior coating..	None	Any discoloration that can not be washed off. (See Note 2)

Type of Degradation or Damage	Description of Degradation or Damage	Acceptable Level of Degradation or Damage	Rejectable Level of Degradation or Damage
Damage to a protective or sacrificial layer	Abrasion, cuts, chemical attack, scratches/gouges, corrosion, environmental damage, or crazing that are limited only to the protective or sacrificial layer.	The depth of any damage to the protective or sacrificial layer that does not exceed the thickness of the protective or sacrificial layer plus 0.050 inch.	The depth of any damage to the protective or sacrificial layer that exceeds the thickness of the protective or sacrificial layer plus 0.050 inch.
Crazing	Hairline surface cracks only in the composite resin.	Light hairline cracks only in the resin.	Any damage to the filaments.

Note 1:

Only damage beyond the sacrificial or coated layer should be considered, and that any damage to sacrificial or coated layers should be repaired by suitable techniques (i.e. epoxy filler). Refer to Manufacturer's Data Report for sacrificial layer thickness.

Note 2:

Washing off UV scale will accelerate attack into lower composite layers. For this reason, if there is superficial UV damage the affected area should be cleaned and painted with a UV tolerant paint. If broken, frayed, or separated fibers to the non sacrificial layer, are discovered during the cleaning process then the vessel shall be condemned.

(15) **TABLE S10.7-b**

VISUAL ACCEPTANCE/REJECTION CRITERIA FOR COMPOSITE PRESSURE VESSELS (SI UNITS)

Type of Degradation or Damage	Description of Degradation or Damage	Acceptable Level of Degradation or Damage	Rejectable Level of Degradation or Damage
Abrasion	Abrasion is damage to the filaments caused by wearing or rubbing of the surface by friction.	Less than 1.3 mm. depth in the pressure bearing thickness.	≥ 1.3 mm depth in the pressure bearing thickness.
Cuts	Linear indications flaws caused by an impact with a sharp object.	Less than 1.3 mm. depth in the pressure bearing thickness.	≥1.3 mm depth in the pressure bearing thickness.
Impact Damage	Damage to the vessel caused by striking the vessel with an object or by being dropped. This may be indicated by discoloration of the composite or broken filaments and/or cracking.	Slight damage that causes a frosted appearance or hairline cracking of the resin in the impact area.	Any permanent deformation of the vessel or damaged filaments.
Delamination	Lifting or separation of the filaments due to impact, a cut, or fabrication error.	Minor delamination of the exterior coating.	Any loose filament ends showing on the surface. Any bulging due to interior delaminations.

Type of Degradation or Damage	Description of Degradation or Damage	Acceptable Level of Degradation or Damage	Rejectable Level of Degradation or Damage
Heat or Fire Damage	Discoloration, charring or distortion of the composite due to temperatures beyond the curing temperature of the composite.	Merely soiled by soot or other debris, such that the cylinder can be washed with no residue.	Any evidence of thermal degradation or discoloration or distortion.
Structural Damage – bulging, distortion, depressions	Change in shape of the vessel due to sever impact or dropping.	None	Any visible distortion, bulging, or depression.
Chemical attack	Environmental exposure that causes a change in the composite or failure of the filaments.	Any attack that can be cleaned off and that leaves no residue.	Any permanent discoloration or loss or softening of material under the exterior coat.
Cracks	Sharp, linear indications	None	None
Scratches/Gouges	Sharp, linear indications caused by mechanical damage.	Less than 1.3 mm depth in the pressure bearing thickness No structural fibers cut or broken.	≥ 1.3 mm depth in the pressure bearing thickness or structural fibers cut or broken.
Soot	A deposit on the composite caused by thermal or environmental exposure.	Soot that washes off and leaves no residue.	Any permanent marking that will not wash off the surface under the exterior coating.
Over pressurization	Excessive pressure due to operational malfunction.	None reported	Any report of pressurization beyond the MAWP or any indication of distortion.
Corrosion	Degradation of the composite due to exposure to specific corrosive environments.	None visible	Any surface damage to structural identified as corrosion.
Dents	A depression in the exterior of the vessel caused by impact or dropping.	< 1.6 mm depth	Any dents with a depth ≥ 1.6 mm Or with a diameter greater than 51 mm.
Reported collision, accident, or fire	Damage to the vessel caused by unanticipated excursion from normally expected operating conditions.	None reported	Any indication or report of impact or heat damage.
Environmental Damage or Weathering	Ultraviolet or other environmental attack under the exterior coating.	None	Any discoloration that can not be washed off. (See Note 2)

Type of Degradation or Damage	Description of Degradation or Damage	Acceptable Level of Degradation or Damage	Rejectable Level of Degradation or Damage
Damage to a protective or sacrificial layer	Abrasion, cuts, chemical attack, scratches/gouges, corrosion, environmental damage, or crazing that are limited only to the protective or sacrificial layer.	The depth of any damage to the protective or sacrificial layer that does not exceed the thickness of the protective or sacrificial layer plus 1.3 mm.	The depth of any damage to the protective or sacrificial layer that exceeds the thickness of the protective or sacrificial layer plus1.3 mm.
Crazing	Hairline surface cracks only in the composite resin.	Light hairline cracks only in the resin.	Any damage to the filaments.

Note 1:

Only damage beyond the sacrificial or coated layer should be considered, and that any damage to sacrificial or coated layers should be repaired by suitable techniques (e.g., epoxy filler). Refer to Manufacturer's Data Report for sacrificial layer thickness.

Note 2:

Washing off UV scale will accelerate attack into lower composite layers.. For this reason, if there is superficial UV damage the affected area should be cleaned and painted with a UV tolerant paint. If broken, frayed, or separated fibers to the non sacrificial layer, are discovered during the cleaning process then the vessel shall be condemned.

(15) S10.8 EXTERNAL INSPECTION

a) Vessel Service Life

Vessels have been designed and manufactured for a limited lifetime; this is indicated on the vessel marking. This marking should first be checked to ensure that such vessels are within their designated service lifetime.

b) Identification of External Damage

The external surface should be inspected for damage to the laminate. Damage is classified into two levels as shown in Table S10.7-a or Table S10.7-b of this supplement. The acceptance/rejection criteria shown in Table S10.7-a or Table S10.7-b of this supplement shall be followed, as a minimum.

The external surface of the vessel is subject to mechanical, thermal, and environmental damage. The external surface of a vessel may show damage from impacts, gouging, abrasion, scratching, temperature excursions, etc. Areas of the surface that are exposed to sunlight may be degraded by ultraviolet light which results in change in the color of the surface and may make the fibers more visible. This discoloration does not indicate a loss in physical properties of the fibers. Overheating may also cause a change in color. The size (area or length and depth) and location of all external damage shall be noted. Vessel support structures and attachments should be examined for damage such as cracks, deformation, or structural failure.

c) Types of External Damage

1) General

Several types of damage to the exterior of vessels have been identified. Examples of specific type of damage are described below. The acceptance/rejection criteria for each type of damage are described in Table S10.7-a or Table S10.7-b of this supplement.

2) Abrasion Damage

Abrasion damage is caused by grinding or rubbing away of the exterior of the vessel. Minor abrasion damage to the protective outer coating or paint will not reduce the structural integrity of the vessel. Abrasion that results in flat spots on the surface of the vessel may indicate loss of composite fiber overwrap thickness.

3) Damage from Cuts

Cuts or gouges are caused by contact with sharp objects in such a way as to cut into the composite overwrap, reducing its thickness at that point.

4) Impact Damage

Impact damage may appear as hairline cracks in the resin, delamination, or cuts of the composite fiber overwrap.

5) Delamination

Delamination is a separation of layers of fibers of the composite overwrap. It may also appear as a discoloration or a blister beneath the surface of the fiber.

6) Heat or Fire Damage

Heat or fire damage may be evident by discoloration, charring or burning of the composite fiber overwrap, labels, or paint. If there is any suspicion of damage, the vessel shall be qualified fit for service using an acoustic emission examination.

7) Structural Damage

Structural damage will be evidenced by bulging, distortion, or depressions on the surface of the vessel.

8) Chemical Attack

Some chemicals are known to cause damage to composite materials. Environmental exposure or direct contact with solvents, acids, bases, alcohols, and general corrosives can cause damage to vessels. Long-term contact with water can also contribute to corrosive damage. Chemicals can dissolve, corrode, remove, or destroy vessel materials. Chemical attack can result in a significant loss of strength in the composite material. Chemical attack can appear as discoloration and in more extreme cases the composite overwrap can feel soft when touched. If there is any suspicion of damage, the vessel shall be re-qualified using acoustic emission examination.

S10.9 INTERNAL EXAMINATION (15)

a) Requirements for Internal Visual Examination

Internal visual examination is normally not required. When vessels have been filled only with pure fluids, corrosion of the interior of the liner should not occur. Internal visual examination of the tanks should only be carried out when:

1) There is evidence that any commodity except a pure fluid has been introduced into the tank. In particular, any evidence that water, moisture, compressor cleaning solvents, or other corrosive agents have been introduced into the vessel will require an internal visual examination.

2) There is evidence of structural damage to the vessel, such as denting or bulging.

3) The vessel valve is removed for maintenance or other reason. Internal examination in this case is limited to examination of the threads and sealing surface. When an internal visual examination is conducted, the following procedures should be followed.

b) Identification of Internal Damage

1) Vessels with Metallic Liners

For vessels with metallic liners, the objective of the internal visual examination is primarily to detect the presence of any corrosion or corrosion cracks.

The internal surface of the vessel shall be examined with adequate illumination to identify any degradation or defects present. Any foreign matter or corrosion products should be removed from the interior of the vessel to facilitate inspection. Any chemical solutions used in the interior of the vessel should be selected to ensure that they do not adversely affect the liner or composite overwrap materials. After cleaning the vessel should be thoroughly dried before it is examined.

All interior surfaces of the vessel should be examined for any color differences, stains, wetness, roughness, or cracks. The location of any degradation should be noted.

Any vessel showing significant internal corrosion, dents or cracks should be removed from service.

2) Vessels with Non-metallic Liners or No Liners

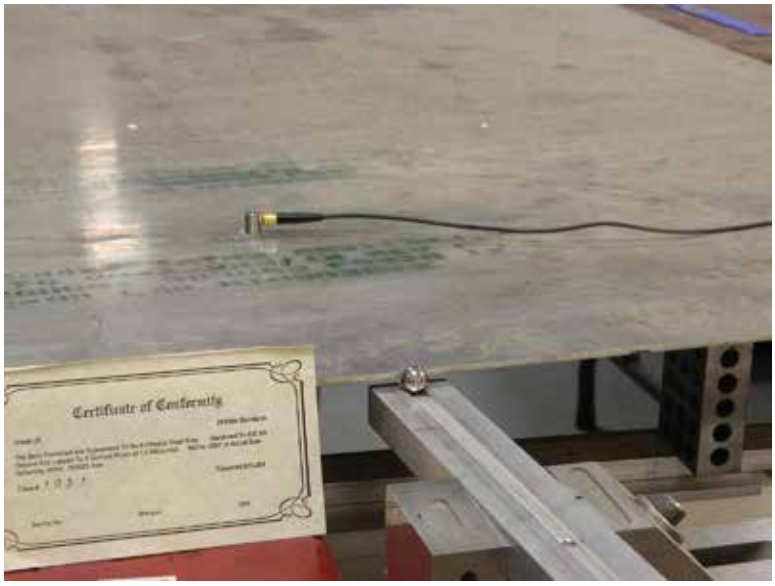
Vessels with non-metallic liners may show corrosion on the plastic liner or metal boss ends. Vessels with non-metallic liners or no liners may also show internal degradation in the form of cracks, pitting, exposed laminate, or porosity.

The internal surface of vessels should be examined with adequate illumination to identify any degradation or defects present. Any foreign matter or corrosion products should be removed from the interior of the vessel to facilitate examination. Chemical solutions used in the interior of the vessel should be selected to ensure they do not adversely affect the liner or composite overwrap materials. After cleaning the vessel should be thoroughly dried before it is examined.

The Inspector should look for cracks, porosity, indentations, exposed fibers, blisters, and any other indication of degradation of the liner and/or laminate. Deterioration of the liner may include softening of the matrix or exposed fibers.

S10.10 ACOUSTIC EMISSION EXAMINATION (15)

FIGURE S10.10 (15)
ROLLING BALL IMPACT CALIBRATION SETUP



S10.10.1 USE AND TEST OBJECTIVES (15)

All high-pressure composite pressure vessels shall be subject to an acoustic emission (AE) examination to detect damage that may occur while the vessel is in service. This method may be used in conjunction with the normal filling procedure.

S10.10.2 TEST PROCEDURE (15)

AE transducers shall be acoustically coupled to the vessel under test and connected to waveform recording equipment. Waveforms shall be recorded and stored on digital media as the vessel is pressurized. All analysis shall be done on the waveforms. The waveforms of interest are the E (Extensional Mode) and F (Flexural Mode) plate waves.

Prior to pressurization, the velocities of the earliest arriving frequency in the E wave and the latest arriving frequency in the F wave shall be measured in the circumferential direction in order to characterize the material and set the sample time (the length of the wave window).

The E and F waves must be digitized and stored for analysis. The test pressure shall be recorded simultaneously with the AE events. Permanent storage of the waveforms is required for the life of the vessel.

S10.10.3 EQUIPMENT (15)

a) Testing System

A testing system shall consist of:

1) sensors;

2) preamplifiers;

3) high pass and low pass filters;

4) amplifier;

5) A/D (analog-to-digital) converters;

6) a computer program for the collection of data;

7) computer and monitor for the display of data; and

8) a computer program for analysis of data.

Examination of the waveforms event by event must always be possible and the waveforms for each event must correspond precisely with the pressure and time data during the test. The computer program shall be capable of detecting the first arrival channel. This is critical to the acceptance criteria below.

Sensors and recording equipment shall be checked for a current calibration sticker or a current certificate of calibration.

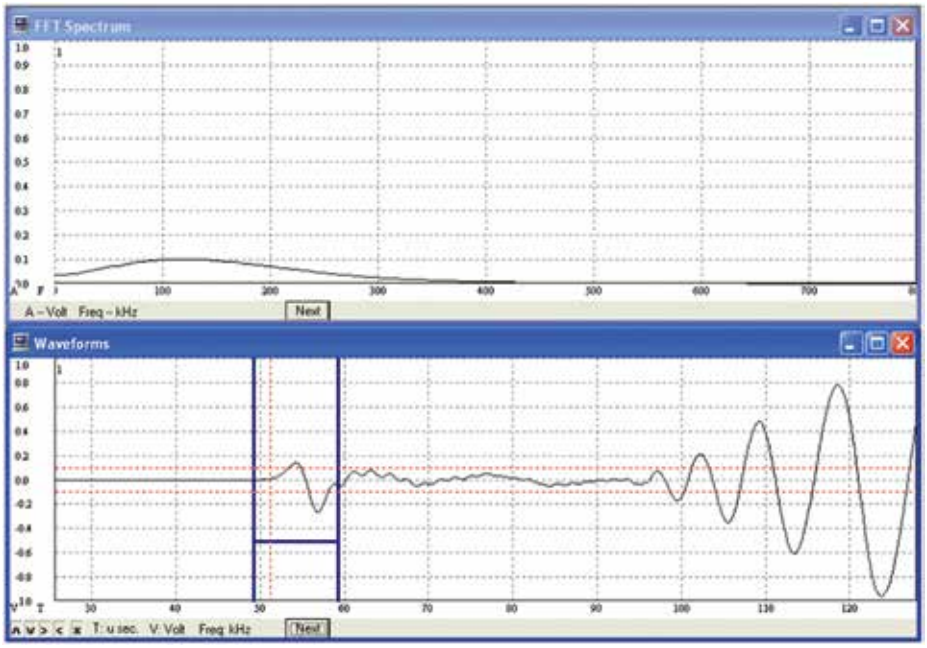
b) Sensor Calibration

Sensors shall have a flat frequency response from 50 kHz to 400 kHz. Deviation from flat response (signal coloration) shall be corrected by using a sensitivity curve obtained with a Michelson interferometer calibration system similar to the apparatus used by NIST (National Institute for Standards and Technology). Sensors shall have a diameter no greater than 0.5 in. (13 mm) for the active part of the sensor face. The aperture effect must be taken into account. Sensor sensitivity shall be at least 0.1 V/nm.

c) Scaling Fiber Break Energy

The wave energy shall be computed by the formula:

(15) **FIGURE S10.10.3**
FRONT END WAVEFORM



$$u = \int v^2 \, dt/z$$

which is the formula for computing energy in the AE signal, where V is the voltage in volts (V) and Z is the input impedance in ohms (Ω). A rolling ball impactor shall be used to create an acoustical impulse in an aluminum plate. The measured energy in the wave shall be used to scale the fiber break energy. This scaling is illustrated later on.

The impact setup, an example of which is shown in Figure S10.10, shall be arranged as follows. The steel ball shall be ½ inch (13 mm) in diameter. The steel ball is a type typically used in machine shops for measuring taper and is commercially available. The ball shall made of chrome steel alloy hardened to R/C 63, ground and lapped to a surface finish of 1.5 micro-inch (0.0000381 mm), within 0.0001 inch (0.0025 mm) of actual size and sphericity within 0.000025 inch (0.00064 mm). The plate shall be made of 7075 T6 aluminum, be at least 4 ft x 4 ft (1200 mm X 1200 mm) in size, the larger the better to avoid reflections, be 1/8 inch (3.2 mm) in thickness and be simply supported by steel blocks. The inclined plane shall be aluminum with a machined square groove 3/8 inch (9.5 mm) wide which supports the ball and guides it to the impact point. The top surface of the inclined plane shall be positioned next to the edge of the plate and stationed below the lower edge of the plate such that the ball impacts with equal parts of the ball projecting above and below the plane of the plate. A mechanical release mechanism shall be used to release the ball down the plane.

The ball roll length shall be 12 inch (305 mm) and the inclined plane angle shall be 6 degrees. The impact produces an impulse that propagates to sensors coupled to the surface of the plate 12 inches (305 mm) away from the edge. The sensors shall be coupled to the plate with vacuum grease. The energy of the leading edge of the impulse, known as the wave front shall be measured. The vertical position of the ball impact point shall be adjusted gradually in order to “peak up” the acoustical signal, much as is done in ultrasonic testing where the angle is varied slightly to peak up the response. The center frequency of the first cycle of the E wave shall be confirmed as 125 kHz ± 10 kHz. See Figure S10.10.3. The energy value in joules of the first half cycle of the E wave shall be used to scale the fiber break energy in criterion 2, as illustrated there. This shall be an “end to end” calibration meaning that the energy shall be measured using the complete AE instrumentation (sensor, cables, preamplifiers, amplifiers, filters and digitizer) that are to be used in the actual testing situation.

Front end of waveform created by rolling ball impact calibration setup described herein. Fast Fourier transform (FFT) shows center frequency of first cycle is approximately 125kHz. The energy linearity of the complete AE instrumentation (sensor, cables, preamplifiers, amplifiers, filters and digitizer) shall be measured by using different roll lengths of 8, 12 and 16 inches (203, 305, and 406 mm). The start of the E wave shall be from the first cycle of the waveform recognizable as the front end of the E wave to the end of the E wave which shall be taken as 10 microsecond (μs) later. (The time was calculated from the dispersion curves for the specified aluminum plate.) A linear regression shall be applied to the energy data and a goodness of fit $R^2 > 0.9$ shall be obtained.

d) Preamplifiers and Amplifiers - See ASME Section V, Article 11.

e) Filters

A high pass filter of 20 kHz shall be used. A low pass filter shall be applied to prevent digital aliasing that occurs if frequencies higher than the Nyquist frequency (half the sampling rate) are in the signal.

f) A/D

The sampling speed and memory depth (wave window length) are dictated by the test requirements and calculated as follows: Vessel length = L inches (meters). Use C_E = 0.2 in./μs (5080 m/s) and C_F = 0.05 in./μs (1270 m/s), the speeds of the first arriving frequency in the E wave and last arriving frequency in the F wave, respectively, as a guide. The actual dispersion curves for the material shall be used if available.

L / C_E = T1 μs. This is when the first part of the direct E wave will arrive.

L / C_F = T2 μs. This is when the last part of the direct F wave will arrive.

(T2 – T1) x.1.5 is the minimum waveform window time and allows for pretrigger time.

The recording shall be quiescent before front end of the E wave arrives. This is called a “clean front end”. Clean is defined in S10.10.6 b) 2) below.

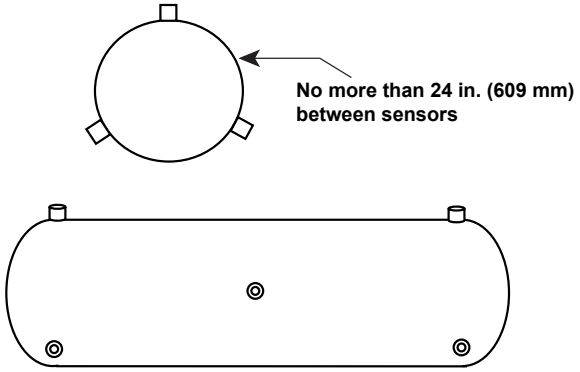
The sampling rate, or sampling speed, shall be such that aliasing does not occur.

The recording system (consisting of all amplifiers, filters and digitizers beyond the sensor) shall be calibrated by using a 20 cycle long tone burst with 0.1 V amplitude at 100, 200, 300, and 400 kHz. The system shall display an energy of $u = \frac{v^2\,NT}{2Z}$ joules at each frequency, where V=0.1 volts, N = 20, Z is the preamplifier input impedance in ohms (Ω) and T is the period of the cycle in seconds (s).

(15) S10.10.4 SENSOR PLACEMENT

At least two sensors shall be used in any AE test regardless of vessel size so that electromagnetic interference (EMI) is easily detected by simultaneity of arrival. Sensors shall be placed at equal distances around the circumference of the vessel on the cylindrical portion of the vessel adjacent to the tangent point of the dome such that the distance between sensors does not exceed 24 in. (610 mm). Adjacent rings of sensors shall be offset by ½ a cycle. For example, if the first ring of sensors is placed at 0, 120, and 240 degrees, the second ring of sensors is placed at 60, 180, and 300 degrees. This pattern shall be continued along the vessel length at evenly spaced intervals, such intervals not to exceed 24 in. (610 mm), until the other end of the vessel is reached. See Figure S10.10.4. The diameter referred to is the external diameter of a vessel.

(15) **FIGURE S10.10.4**
SENSOR SPACING AND PATTERN



Maximum distance between sensors in the axial and circumferential directions shall not exceed 24 inches (609 mm) unless it is demonstrated that the essential data can still be obtained using a greater distance and the authority having the jurisdiction concurs.

This spacing allows for capturing the higher frequency components of the acoustic emission impulses and high channel count wave recording systems are readily available.

S10.10.5 TEST PROCEDURE (15)

Couple sensors to vessel and connect to the testing equipment per ASME Section V Article 11. Connect pressure transducer to the recorder. Conduct sensor performance checks prior to test to verify proper operation and good coupling to the vessel. The E and F waveforms shall be observed by breaking pencil lead at approximately 8 in. (200 mm) and 16 in. (410 mm) from a sensor along the fiber direction. All calibration data shall be recorded.

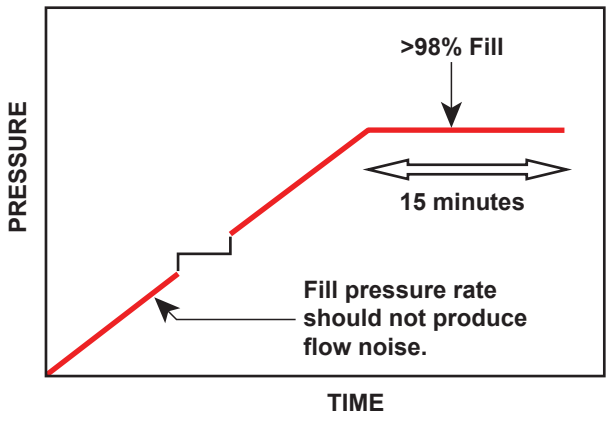
Recording threshold shall be 60 dB ref 1 μV at the transducer.

Performance checks shall be carried out by pencil lead breaks (Pentel 0.3 mm, 2H) six inches (150 mm) from each transducer in the axial direction of the cylinder and a break at the center of each group of four sensors.

Pressurize vessel to >98% of normal fill pressure and monitor AE during pressurization and for 15 minutes after fill pressure is reached. See Figure S10.10.5 for a schematic of the pressurization scheme. If at any time during fill the fill rate is too high in that it causes flow noise, decrease fill rate until flow noise disappears. Record events during pressurization and for 15 minutes after fill pressure is reached and save the data. Then conduct a post-test performance check and save data. Test temperature shall be between 50°F (10°C) and 120°F (49°C).

A threshold of 60 dBAE ref 1 μV at the sensor shall be used during all phases of testing.

FIGURE S10.10.5 (15)
TYPICAL PRESSURIZATION PLAN WHEN FILLING VESSELS



AE shall be monitored for 15 min after operating fill pressure is reached.

S10.10.6 ACCEPT/REJECT CRITERIA (15)

a) Stability Criterion

Theory of AE Monitoring of high-pressure composite pressure vessels for stability– A stable vessel will exhibit cumulative curves with exponentially decaying curvature. The shape of the cumulative events curve is similar for pressure vessels made of fiberglass, aramid and carbon fiber that exhibit a fiber dominated failure mode. This is essentially a test that demonstrates the composite is not progressing to failure at the hold pressure.

b) Analysis Procedure

Data will include matrix splits, matrix cracks, fiber breaks, and matrix chirps due to fracture surface fretting, and fiber/matrix debonding. Extraneous noise, identified by waveform characteristics, may also be included in the data.

1) Filter data to eliminate any external noise such as electromagnetic interference (EMI), mechanical rubbing, flow noise, etc. Identify noise events by their shape, spectral characteristics, or other information known about the test such as a temporally associated disturbance due to the pressurization system or test fixturing. EMI is characterized by a lack of any mechanical wave propagation characteristics, particularly a lack of dispersion being apparent. EMI can be further identified by simultaneity of arrival on more than one channel. The two criteria shall be considered together to ensure it's not simply an event that happened to be centered between the sensors. Mechanical rubbing frequencies are usually very low and can be determined by experiment. There should be no flow noise. If the vessel, or a fitting, leaks, this will compromise the data as AE is very sensitive to leaks. Leak noise is characterized by waves that look uniform across the entire length of the waveform window. If a leak occurs during the load hold, the test must be redone. Flow noise is characterized by waves that fill the waveform window.

2) Use only events that have clean front ends and in which first arrival channel can be determined. Clean means having a pre-trigger energy of less than 0.01×10^{-10} joules. Energy is computed by the integral of the voltage squared over time.

3) Plot first arrival cumulative events versus time. Plots shall always show the pressure data.

4) Apply exponential fits by channel for pressure hold time and display both data and fit. The values are determined by the fit to $y = A_e^{Bt} + C$.

The B value is the shape factor of the cumulative curves. C is an intercept and A is a scale factor. The time t shall be equal intervals during the hold with events binned by time interval. Record exponents and goodness of fit (R2). Plot energy decay curves. One third or one fourth of hold time shall be used for event energy binning (cumulative energy). The formula is $y=A_e^{Bt}$.

The sequence of energy values must monotonically decrease.

This is similar to using other energy criteria, such as Historic Index. A sequence that is not properly decreasing will be indicated by a low R^2 value.

5) Save all plots (all channels) to report document.

6) Record exponents and R^2 values.

7) Vessel B Values

a. Vessel B values shall be tracked and compiled in order to develop a statistically significant database.

b. B is the critical value that measures the frequency of occurrence of events during pressure hold.

c. Not every vessel will have the exact same B value.

d. Data on B values should cluster.

S10.10.6.1 THE CRITERIA GIVEN BELOW APPLY TO EACH INDIVIDUAL SENSOR ON THE VESSEL (15)

a) The stability criteria as described above shall be met. (Also see ASME Section X Mandatory Appendix 8.) Any vessel that does not meet the stability criteria must be removed from service. The criteria are:

1) Cumulative Event Decay Rate $-0.1 < B < -0.0001$, $R^2 \geq 0.80$

2) Cumulative Energy Decay Rate $-0.2 < B < -0.001$, $R^2 \geq 0.80$

If these criteria are not met, the vessel does not pass. The vessel may be retested. An AE Level III examiner must review the data from the initial testing and the subsequent loading test before the vessel can be passed. Retest loadings shall follow the original pressurization rates and pressures and use a threshold of 60 dBAE. If the vessel fails the criteria again, the vessel shall not be certified by the Inspector as meeting the provisions of this section.

b) Events that occur at the higher loads during pressurization having significant energy in the frequency band f > 300 kHz are due to fiber bundle, or partial bundle, breaks. These should not be present at operating pressure in a vessel that has been tested to a much higher pressures and is now operated at the much lower service pressure. For fiber bundles to break in the upper twenty percent of load during the test cycle or while holding at operating pressure, the vessel has a severe stress concentration and shall be removed from service.

S10.10.7 FIBER BREAKAGE CRITERION (15)

a) Analysis Procedure

In order to determine if fiber bundle breakage has occurred during the filling operation the frequency spectra of the direct E and F waves shall be examined and the energies in certain frequency ranges shall be computed as given below.

b) Definitions

Energies (U) in the ranges are defined as:

50 – 400 kHz: U_0

100 – 200 kHz: U_1

250 – 400 kHz: U_2

The criteria for determining The criteria for determining if high frequency spectrum events have occurred is given by the following formulas:

$U_0 / (UF_{BB}) \geq 10\%$

$U_2 / (U_1 + U_2) \geq 15\%$

$U_2 / U_0 \geq 10\%$

U_{FBB} is the energy of a fiber bundle break calculated using the average breaking strength from the manufacturer's data or independent test data. The manufacturer's data shall be used if available. The formula that shall be used for calculating average fiber break energy in joules (J) is

$$U_{FB} = \frac{E * A * l * \varepsilon^2}{2}$$

where E is the Young's modulus of the fiber in pascals (Pa), ε is the strain to failure of the fiber, A is area of the fiber in square meters (m^2), and l is the ineffective fiber length in meters (m) for the fiber and matrix combination. If the ineffective length is not readily available, four times the fiber diameter shall be used. Set U_{FBB} = 100 x U_{FB}, where U_{FB} has been calculated and scaled by the rolling ball impact energy as in the examples below. If these criteria are met, fiber bundle break damage has occurred during the test and the vessel shall be removed from service.

c) Example of Fiber Break Energy Calculation Suppose d = 7 μm, *E* = 69.6 GPa and ε = 0.01 (average breaking strain) for some carbon fiber. Using $A = \pi d^2/4$ and / = 4d,

$$U_{FB} = \frac{E * A * l * \varepsilon^2}{2}$$

$$U_{FB} = \frac{E69.6 * 10^9\ Pa * \pi * \frac{(7 * 10^{-6}m)^2}{4} * 2.8 * 10^{-5}m * (0.01)^2}{2}$$

$$U_{FB} = 3.75 * 10^{-9} j$$

d) Example of Scaling Calculation

Suppose that the rolling ball impact (RBI) acoustical energy measured by a particular high fidelity AE transducer is U^{AE}_{RBI} = 5 x 10^{-10} J and the impact energy U_{RBI} = 1.9 x 10^{-3} J (due to gravity). Suppose d = 7 μm, *E* = 69.6 GPa and ε = 0.01 (average breaking strain) for some carbon fiber. Using $A = \pi d^2/4$ and l = 4d, U_{FB} = 3x10^{-8} J. A carbon fiber with a break energy of U_{FB} = 3x10^{-8} J would correspond to a wave energy.

$$U^{AE}_{FB} = U_{FB} \text{ x } U^{AE}_{RBI} / U_{RBI}$$

$$U^{AE}_{FB} = 3x10^{-8}\text{ J x 5 x } 10^{-10}\text{ J / 1.9 x 10-}^{-3}\text{ J}$$

$$U^{AE}_{FB} = 7.9 \text{ x } 10^{-15}\text{ J.}$$

This is the number that is used to calculate the value of U_{FBB} that is used in the fiber break criterion in the second acceptance criterion and the energy acceptance criterion in the third criterion below.

e) Amplifier Gain Correction

All energies shall be corrected for gain. (20 dB gain increases apparent energy 100 times and 40 dB gain 10,000 times.)

Fiber break waves may look similar to matrix event waves in time space but in frequency space the difference is clear. A fiber break is a very fast source, while a matrix crack evolves much more slowly due to greater than ten to one difference in their tensile moduli. The speed of the fiber break produces the high frequencies, much higher than a matrix crack event can produce. Frequencies higher than 2 MHz have been observed in proximity to a fiber break, however these very high frequencies are attenuated rapidly as the wave propagates. Practically speaking, the observation of frequencies above 300 kHz, combined with certain other characteristics of the frequency spectrum and pressure level, is enough to confirm a fiber break. It should also be noted that it is fiber bundle breaks that are usually detected in structural testing and not the breaking of individual fibers. The energies of individual fiber breaks are very small, about 3x10^{-8} Joules for T-300 carbon fibers for example.

S10.10.8 FRICTION BETWEEN FRACTURE SURFACES (15)

Friction between fracture surfaces plays a very important role in understanding AE in fatigue testing. It is an indicator of the presence of damage because it is produced by the frictional rubbing between existing and newly created fracture surfaces. Even the presence of fiber bundle breakage can be detected by examining the waveforms produced by frictional acoustic emission or FRAE. Increasing FRAE intensity throughout a pressure cycle means more and more damage has occurred.

Therefore, for a vessel to be acceptable no AE event shall have an energy greater than (F) x U_{FB} at anytime during the test. F is the acoustic emission allowance factor. The smaller the allowance factor, the more conservative the test. An F = 10^4 shall be used in this testing. It is the equivalent of three plus fiber tows, each tow consisting of 3,000 fibers, breaking simultaneously near a given transducer.

S10.10.9 BACKGROUND ENERGY (15)

Background energy of any channel shall not exceed 10 times the quiescent background energy of that channel. After fill pressure is reached, any oscillation in background energy with a factor of two excursions between minima and maxima shows that the vessel is struggling to handle the pressure. Pressure shall be reduced immediately and the vessel removed from service.

S10.11 DOCUMENT RETENTION (15)

a) The vessel owner shall retain a copy of the Manufacturer's Data Report for the life of the vessel.

b) After satisfactory completion of the periodic in-service inspection, vessels shall be permanently marked or labeled with date of the inspection, signature of the Inspector, and date of the next periodic in-service inspection.

c) The vessel owner shall retain a copy of the in-service inspection report for the life of the vessel.

PART 2, SECTION 7
INSPECTION — NBIC POLICY FOR METRICATION

7.1 GENERAL

This policy provides guidance for the use of US customary units and metric units. Throughout the NBIC, metric units are identified and placed in parentheses after the US customary units referenced in the text and associated tables. For each repair or alteration performed, selection of units shall be based on the units used in the original code of construction. For example, items constructed using US customary units shall be repaired or altered using US customary units. The same example applies to items constructed using metric units. Whichever units are selected, those units are to be used consistently throughout each repair or alteration. Consistent use of units includes all aspects of work required for repairs or alterations (i.e. materials, design, procedures, testing, documentation, and stamping, etc.).

7.2 EQUIVALENT RATIONALE

The rationale taken to convert metric units and US customary units involves knowing the difference between a *soft* conversion and a *hard* conversion. A soft conversion is an exact conversion. A hard conversion is simply performing a soft conversion and then rounding off within a range of intended precision. When values specified in the NBIC are intended to be approximate values, a hard conversion is provided. If an exact value is needed to maintain safety or required based on using good engineering judgment, then a soft conversion will be used. In general, approximate accuracy is acceptable for most repairs or alterations performed using the requirements of the NBIC. Therefore, within the NBIC, metric equivalent units are primarily hard conversions.

The following examples are provided for further clarification and understanding of soft conversions versus hard conversions:

Example 1: Using 1 in. = 25.4 mm;
12 in. = 304.8 mm (soft conversion)

Example 2: Using the above conversion, a hard conversion may be 300 mm or 305 mm depending on the degree of precision needed.

7.3 PROCEDURE FOR CONVERSION

The following guidelines shall be used to convert between US customary units and metric units within the text of the NBIC:

a) All US customary units will be converted using a soft conversion;

b) Soft conversion calculations will be reviewed for accuracy;

c) Based on specified value in the NBIC, an appropriate degree of precision shall be identified;

d) Once the degree of precision is decided, rounding up or down may be applied to each soft conversion in order to obtain a hard conversion; and

e) Use of hard conversion units shall be used consistently throughout the NBIC wherever soft conversions are not required.

Note: Care shall be taken to minimize percentage difference between units.

7.4 REFERENCING TABLES

The following tables are provided for guidance and convenience when converting between US customary units and metric units. See NBIC Part 1, 2, 3, Tables 7.4-a through 7.4-j.

TABLE 7.4-a
SOFT CONVERSION FACTORS (US X FACTOR = METRIC)

US Customary	Metric	Factor
in.	mm	25.4
ft.	m	0.3048
$in.^2$	mm^2	645.16
$ft.^2$	m^2	0.09290304
$in.^3$	mm^3	16,387.064
$ft.^3$	m^3	0.02831685
US gal.	m^3	0.003785412
US gal.	liters	3.785412
psi	MPa	0.0068948
psi	kPa	6.894757
ft-lb	J	1.355818
°F	°C	5/9 x (°F–32)
R	K	5/9
lbm	kg	0.4535924
lbf	N	4.448222
in.-lb	N-mm	112.98484
ft.-lb	N-m	1.3558181
ksi√in	MPa√m	1.0988434
Btu/hr	W	0.2930711
lb/ft^3	kg/m^3	16.018463
in.-wc	kPa	0.249089

Note:

The actual pressure corresponding to the height of a vertical column of fluid depends on the local gravitational field and the density of the fluid, which in turn depends upon the temperature. This conversion factor is the conventional value adopted by ISO. The conversion assumes a standard gravitational field (gn – 9.80665 N/kg) and a density of water equal to 1,000 kg/m^3. NBIC Part 1, 2, 3, 7.4-a through 7.4-j.

Temperature shall be converted to within 1°C as shown in NBIC Part 1, 2, 3, Table 7.4-b.

TABLE 7.4-b
TEMPERATURE EQUIVALENTS

Temperature °F	Temperature °C
60	16
70	21
100	38
120	49
350	177
400	204
450	232
800	427
1,150	621

Fractions of an inch shall be converted according to NBIC Part 1, 2, 3, Table 7.4-c. Even increments of inches are in even multiples of 25 mm. For example, 40 inches is equivalent to 1,000 mm. Intermediate values may be interpolated rather than converting and rounding to the nearest mm.

TABLE 7.4-c
US FRACTIONS/METRIC EQUIVALENTS

Inches	Millimeters
1/32	0.8
3/64	1.2
1/16	1.5
3/32	2.5
1/8	3
5/32	4
3/16	5
7/32	5.5
1/4	6
5/16	8
3/8	10
7/16	11
1/2	13
9/16	14
5/8	16
11/16	17
3/4	19
7/8	22
1	25

For nominal pipe sizes, the following relationships were used as shown in NBIC Parts 1, 2 or 3, Table 7.4-d.

TABLE 7.4-d
PIPE SIZES/EQUIVALENT

US Customary Practice	Metric Practice
NPS 1/8	DN 6
NPS 1/4	DN 8
NPS 3/8	DN 10
NPS 1/2	DN 15
NPS 3/4	DN 20
NPS 1	DN 25
NPS 1-1/4	DN 32
NPS 1-1/2	DN 40
NPS 2	DN 50
NPS 2-1/2	DN 65
NPS 3	DN 80
NPS 3-1/2	DN 90
NPS 4	DN 100
NPS 5	DN125
NPS 6	DN 150
NPS 8	DN 200
NPS 10	DN 250
NPS 12	DN 300
NPS 14	DN 350
NPS 16	DN 400
NPS 18	DN 450
NPS 20	DN 500
NPS 22	DN 550
NPS 24	DN 600
NPS 26	DN 650
NPS 28	DN 700
NPS 30	DN 750
NPS 32	DN 800
NPS 34	DN 850
NPS 36	DN 900
NPS 38	DN 950
NPS 40	DN 1000
NPS 42	DN 1050
NPS 44	DN 1100
NPS 46	DN 1150
NPS 48	DN 1200
NPS 50	DN 1250
NPS 52	DN 1300
NPS 54	DN 1350
NPS 56	DN 1400
NPS 58	DN 1450
NPS 60	DN 1500

Areas in square inches (in^2) were converted to square mm (mm^2) and areas in square feet (ft^2) were converted to square meters (m^2). See examples in NBIC Parts 1, 2 or 3, Tables 7.4-e and 7.4-f.

TABLE 7.4-e

Area (US Customary)	Area (Metric)
3 in^2	650 mm^2
6 in^2	3,900 mm^2
10 in^2	6,500 mm^2

TABLE 7.4-f

Area (US Customary)	Area (Metric)
5 ft^2	0.46 mm^2

Volumes in cubic inches ($in.^3$) were converted to cubic mm **(**mm^3**)** and volumes in cubic feet (ft^3) were converted to cubic meters (m^3). See examples in NBIC Parts 1, 2 or 3, Tables 7.4-g and 7.4-h.

TABLE 7.4-g

Volume (US Customary)	Volume (Metric)
1 in^3	16,000 mm^3
6 in^3	96,000 mm^3
10 in^3	160,000 mm^3

TABLE 7.4-h

Volume (US Customary)	Volume (Metric)
5 ft^3	0.14 m^3

Although the pressure should always be in MPa for calculations, there are cases where other units are used in the text. For example, kPa is used for small pressures. Also, rounding was to two significant figures. See examples in Table 7.4-i. (Note that 14.7 psi converts to 101 kPa, while 15 psi converts to 100 kPa. While this may seem at first glance to be an anomaly, it is consistent with the rounding philosophy.)

TABLE 7.4-i
PRESSURE/EQUIVALENTS

Pressure (US Customary)	Pressure (Metric)
0.5 psi	3 kPa
2 psi	15 kPa
3 psi	20 kPa
10 psi	70 kPa
15 psi	100 kPa
30 psi	200 kPa
50 psi	350 kPa
100 psi	700 kPa
150 psi	1.03 MPa
200 psi	1.38 MPa
250 psi	1.72 MPa
300 psi	2.10 MPa
350 psi	2.40 MPa
400 psi	2.8 MPa
500 psi	3.45 MPa
600 psi	4.14 MPa
1,200 psi	8.27 MPa
1,500 psi	10.34 MPa

TABLE 7.4-j

Strength (US Customary)	Strength (Metric)
95,000 psi	655 MPa

Material properties that are expressed in psi or ksi (e.g., allowable stress, yield and tensile strength, elastic modulus) were generally converted to MPa to three significant figures. See example in NBIC Parts 1, 2 or 3, Table 7.4-h.

PART 2, SECTION 8
INSPECTION — PREPARATION OF TECHNICAL INQUIRIES TO THE *NATIONAL BOARD INSPECTION CODE* COMMITTEE

8.1 INTRODUCTION

The NBIC Committee meets regularly to consider written requests for interpretations and revisions to the code rules. This section provides guidance to code users for submitting technical inquiries to the Committee. Technical inquires include requests for additions to the code rules and requests for code Interpretations, as described below.

a) Code Revisions
Code revisions are considered to accommodate technological developments, address administrative requirements, or to clarify code intent.

b) Code Interpretations
Code Interpretations provide clarification of the meaning of existing rules in the code, and are also presented in question and reply format. Interpretations do not introduce new requirements. In cases where existing code text does not fully convey the meaning that was intended, and revision of the rules is required to support an Interpretation, an intent Interpretation will be issued and the code will be revised. As a matter of published policy, the National Board does not approve, certify, or endorse any item, construction, propriety device or activity and, accordingly, inquiries requiring such consideration will be returned. Moreover, the National Board does not act as a consultant on specific engineering problems or on the general application or understanding of the code rules.

Inquiries that do not comply with the provisions of this section or that do not provide sufficient information for the Committee's full understanding may result in the request being returned to the inquirer with no action.

8.2 INQUIRY FORMAT

Inquiries submitted to the Committee shall include:

a) Purpose
Specify one of the following:

1) Revision of present code rules;

2) New or additional code rules; or

3) code Interpretation.

b) Background
Provide concisely the information needed for the Committee's understanding of the inquiry, being sure to include reference to the applicable Code Edition, Addenda, paragraphs, figures, and tables. Provide a copy of the specific referenced portions of the code.

c) Presentations
The inquirer may attend a meeting of the Committee to make a formal presentation or to answer questions from the Committee members with regard to the inquiry. Attendance at a Committee meeting shall be at the expense of the inquirer. The inquirer's attendance or lack of attendance at a meeting shall not be a basis for acceptance or rejection of the inquiry by the Committee.

8.3 CODE REVISIONS OR ADDITIONS

Request for code revisions or additions shall provide the following:

a) Proposed Revisions or Additions
For revisions, identify the rules of the code that require revision and submit a copy of the appropriate rules as they appear in the code, marked up with the proposed revision. For additions, provide the recommended wording referenced to the existing code rules.

b) Statement of Need
Provide a brief explanation of the need for the revision or addition.

c) Background Information
Provide background information to support the revision or addition, including any data or changes in technology that form the basis for the request that will allow the Committee to adequately evaluate the proposed revision or addition. Sketches, tables, figures, and graphs should be submitted as appropriate. When applicable, identify any pertinent paragraph in the code that would be affected by the revision or addition and identify paragraphs in the code that reference the paragraphs that are to be revised or added.

8.4 CODE INTERPRETATIONS

Requests for code Interpretations shall provide the following:

a) Inquiry
Provide a condensed and precise question, omitting superfluous background information and, when possible, composed in such a way that a “yes” or a “no” reply, with brief provisos if needed, is acceptable. The question should be technically and editorially correct.

b) Reply
Provide a proposed reply that will clearly and concisely answer the inquiry question. Preferably the reply should be “yes” or “no” with brief provisos, if needed.

c) Background Information
Provide any background information that will assist the committee in understanding the proposed Inquiry and Reply Requests for Code Interpretations must be limited to an interpretation of the particular requirement in the code. The Committee cannot consider consulting type requests such as:

1) A review of calculations, design drawings, welding qualifications, or descriptions of equipment or Parts to determine compliance with code requirements;

2) A request for assistance in performing any code-prescribed functions relating to, but not limited to, material selection, designs, calculations, fabrication, inspection, pressure testing, or installation;

3) A request seeking the rationale for code requirements.

8.5 SUBMITTALS

Submittals to and responses from the Committee shall meet the following criteria:

a) Submittal
Inquiries from code users shall be in English and preferably be submitted in typewritten form; however, legible handwritten inquiries will be considered. They shall include the name, address, telephone number, fax number, and email address, if available, of the inquirer and be mailed to the following address:

Secretary, NBIC Committee
The National Board of Boiler and
Pressure Vessel Inspectors
1055 Crupper Avenue
Columbus, OH 43229

As an alternative, inquiries may be submitted via fax or email to:
Secretary NBIC Committee
Fax: 614.847.1828
Email: *NBICinquiry@nationalboard.org*

b) Response
The Secretary of the NBIC Committee shall acknowledge receipt of each properly prepared inquiry and shall provide a written response to the inquirer upon completion of the requested action by the NBIC Committee.

PART 2, SECTION 9
INSPECTION — GLOSSARY OF TERMS

9.1 DEFINITIONS

For the purpose of applying the rules of the NBIC, the following terms and definitions shall be used herein as applicable to each part:

Additional terms and definitions specific to DOT Transport Tanks are defined in NBIC Part 2, Supplement 6.

Accumulator — A vessel in which the test medium is stored or accumulated prior to its use for testing.

Alteration — A change in the item described on the original Manufacturer's Data Report which affects the pressure containing capability of the pressure-retaining item. (See NBIC Part 3, 3.4.3, *Examples of Alteration*) Nonphysical changes such as an increase in the maximum allowable working pressure (internal or external), increase in design temperature, or a reduction in minimum temperature of a pressure-retaining item shall be considered an alteration.

ANSI — The American National Standards Institute.

Appliance — A piece of equipment that includes all controls, safety devices, piping, fittings, and vessel(s) within a common frame or enclosure that is listed and labeled by a nationally recognized testing agency for its intended use.

ASME — The American Society of Mechanical Engineers.

ASME Code — The American Society of Mechanical Engineers Boiler and Pressure Vessel Code published by that Society, including addenda and Code Cases, approved by the associated ASME Board.

Assembler — An organization who purchases or receives from a manufacturer the necessary component parts of valves and assembles, adjusts, tests, seals, and ships safety or safety relief valves at a geographical location, and using facilities other than those used by the manufacturer.

Authorized Inspection Agency (AIA)

Inservice: An Authorized Inspection Agency is either:

a) a jurisdictional authority as defined in the National Board Constitution; or

b) an entity that is accredited by the National Board meeting NB-369, *Accreditation of Authorized Inspection Agencies Performing Inservice Inspection Activities*; NB-371, *Accreditation of Owner-User Inspection Organizations (OUIO);* or NB-390, *Qualifications and duties for Federal Inspection Agencies (FIAs) Performing Inservice Inspection Activities*.

New Construction: An Authorized Inspection Agency is one that is accredited by the National Board meeting the qualification and duties of NB-360, *Criteria for Acceptance of Authorized Inspection Agencies for New Construction*.

Biomass — Fuels which result from biological sources requiring a relatively short time for replenishment: Wood and bagasse are typical examples.

Biomass Fired Boiler — A boiler which fires biomass as its primary fuel. (15)

Capacity Certification — The verification by the National Board that a particular valve design or model has successfully completed all capacity testing as required by the ASME Code.

Boiler — A boiler is a closed vessel in which water or other liquid is heated, steam or vapor generated, steam or vapor is superheated, or any combination thereof, under pressure for use external to itself, by the direct application of energy from the combustion of fuels or from electricity or solar energy. The term boiler also shall include the apparatus used to generate heat and all controls and safety devices associated with such apparatus or the closed vessel.

High-Temperature Water Boiler — A power boiler in which water is heated and operates at a pressure in excess of 160 psig (1.1 MPa) and/or temperature in excess of 250°F (121°C).

Hot-Water Heating Boiler — A hot water boiler installed to operate at pressures not exceeding 160 psig (1,100 kPa) and/or temperatures not exceeding 250°F (121°C), at or near the boiler outlet.

Hot-Water Supply Boiler — A boiler that furnishes hot water to be used externally to itself at a pressure less than or equal to 160 psig (1,100 kPa gage) or a temperature less than or equal to 250°F (120°C) at or near the boiler outlet

Power Boiler — A boiler in which steam or other vapor is generated at a pressure in excess of 15 psig (100 kPa) for use external to itself. The term power boiler includes fired units for vaporizing liquids other than water, but does not include fired process heaters and systems. (See also High-Temperature Water Boiler).

Steam Heating Boiler — A steam boiler installed to operate at pressures not exceeding 15 psig (100 kPa).

Carbons Recycle — See Flyash Recycle.

Chimney or Stack — A device or means for providing the venting or escape of combustion gases from the operating unit.

Confined Space — Work locations considered “confined” because their configurations hinder the activities of employees who must enter, work in and exit them. A confined space has limited or restricted means for entry or exit, and it is not designed for continuous employee occupancy. Confined spaces include, but are not limited to, underground vaults, tanks, storage bins, manholes, pits, silos, process vessels, and pipelines. Regulatory Organizations often use the term “permit-required confined space” (permit space) to describe a confined space that has one or more of the following characteristics: contains or has the potential to contain a hazardous atmosphere; contains a material that has the potential to engulf an entrant; has walls that converge inward or floors that slope downward and taper into a smaller area which could trap or asphyxiate an entrant; or contains any other recognized safety or health hazard, such as unguarded machinery, exposed live wires, or heat stress. Confined space entry requirements may differ in many locations and the Inspector is cautioned of the need to comply with local or site- specific confined space entry requirements.

Conversion

Pressure Relief Devices — The change of a pressure relief valve from one capacity-certified configuration to another by use of manufacturer’s instructions.

Units of Measure — Changing the numeric value of a parameter from one system of units to another.

(15) **Conveyor System(s)** — A fuel transport system utilized on biomass boilers that drops fuel onto a moving belt, bucket elevator, drag link conveyor, or a screw or auger mechanism. (The speed of the conveyor may be varied to meet fuel demand.)

Demonstration — A program of making evident by illustration, explanation, and completion of tasks documenting evaluation of an applicant’s ability to perform code activities, including the adequacy of the applicant’s quality program, and by a review of the implementation of that program at the address of record and/or work location.

Dense Phase Pneumatic System(s) — A batch feed transport system used on solid fuel fired boilers for both fuel delivery and/or ash removal. In this system the material to be transported is dropped through a valve in a pressure vessel. When the vessel is filled the valve closes and air at a pressure from 30 to 100 psig (200 to 700 kPa) is admitted and the material leaves the vessel in the form of a “slug”. The sequence then repeats. (15)

Dutchman — Generally limited to tube or pipe cross-section replacement. The work necessary to remove a compromised section of material and replace the section with material meeting the service requirements and installation procedures acceptable to the Inspector. Also recognized as piecing.

Emissions — The discharge of various Federal or State defined air pollutants into the surrounding atmosphere during a given time period.

Emissions Control System — An arrangement of devices, usually in series, used to capture various air pollutants and thereby reduce the amount of these materials, or gases, being admitted to the surrounding atmosphere, below Federal or State defined standards.

Examination — In process work denoting the act of performing or completing a task of interrogation of compliance. Visual observations, radiography, liquid penetrant, magnetic particle, and ultrasonic methods are recognized examples of examination techniques.

Exit — A doorway, hallway, or similar passage that will allow free, normally upright unencumbered egress from an area.

Field — A temporary location, under the control of the Certificate Holder, that is used for repairs and/or alterations to pressure-retaining items at an address different from that shown on the Certificate Holder’s *Certificate of Authorization*

Fluidized Bed — A process in which a bed of granulated particles are maintained in a mobile suspension by an upward flow of air or gas.

Fluidized Bed (Bubbling) — A fluidized bed in which the fluidizing velocity is less than the terminal velocity of individual bed particles where part of the fluidizing gas passes through as bubbles.

Fluidized Bed (Circulating) — A fluidized bed in which the fluidizing velocities exceed the terminal velocity of the individual bed particles.

Flyash — Suspended ash particles carried in the flue gas.

Flyash Collector — A device designed to remove flyash in the dry form from the flue gas.

Flyash Recycle — The reintroduction of flyash/unburned carbon from the flyash collector into the combustion zone, in order to complete the combustion of unburned fuel, thereby improving efficiency.

Forced-Flow Steam Generator — A steam generator with no fixed steamline and waterline.

Fuel Transport Fan — A fan which generates airflow capable of moving fuel particles, in suspension, from a metering device to the combustion zone.

Grate — The surface on which fuel is supported and burned and through which air is passed for combustion.

Hydrostatic Test — A liquid pressure test which is conducted using water as the test medium.

Inspection — A process of review to ensure engineering design, materials, assembly, examination, and testing requirements have been met and are compliant with the code.

Induced Draft Fan — A fan exhausting hot gases from the heat absorbing equipment.

Inspector — See National Board Commissioned Inspector and National Board Owner-User Commissioned Inspector.

Intervening — Coming between or inserted between, as between the test vessel and the valve being tested.

Jurisdiction — A governmental entity with the power, right, or authority to interpret and enforce law, rules, or ordinances pertaining to boilers, pressure vessels, or other pressure-retaining items. It includes National Board member jurisdictions defined as "jurisdictional authorities."

Jurisdictional Authority — A member of the National Board, as defined in the *National Board Constitution*.

(15) **Lean Phase Pneumatic System(s)** — A fuel transport system utilized on biomass boilers that drops fuel into a moving airstream, mixes with the air, and travels through a pipe at a velocity in the region of 5,000 ft/min (1,525 m/min). Air pressures are in the region of 25 inches (635 mm) water column.

Lift Assist Device — A device used to apply an auxiliary load to a pressure relief valve stem or spindle, used to determine the valve set pressure as an alternative to a full pressure test.

Liquid Pressure Test — A pressure test using water or other incompressible fluid as a test medium.

Manufacturer's Documentation — The documentation that includes technical information and certification required by the original code of construction.

Mechanical Assembly — The work necessary to establish or restore a pressure retaining boundary, under supplementary materials, whereby pressure-retaining capability is established through a mechanical, chemical, or physical interface, as defined under the rules of the NBIC.

Mechanical Repair Method — A method of repair, which restores a pressure retaining boundary to a safe and satisfactory operating condition, where the pressure retaining boundary is established by a method other than welding or brazing, as defined under the rules of the NBIC.

Metering Device — A method of controlling the amount of fuel, or air, flowing into the combustion zone.

"NR" Certificate Holder — An organization in possession of a valid "NR" *Certificate of Authorization* issued by the National Board.

National Board — The National Board of Boiler and Pressure Vessel Inspectors.

National Board Commissioned Inspector — An individual who holds a valid and current National Board Commission.

NBIC — The *National Board Inspection Code* published by The National Board of Boiler and Pressure Vessel Inspectors.

Nuclear Items — Items constructed in accordance with recognized standards to be used in nuclear power plants or fuel processing facilities.

Original Code of Construction — Documents promulgated by recognized national standards writing bodies that contain technical requirements for construction of pressure-retaining items or equivalent to which the pressure-retaining item was certified by the original manufacturer.

Overfire Air — Air admitted to the furnace above the grate surface /fuel bed. Used to complete the combustion of fine particles, in suspension. Also aids in reducing NOx formation.

Owner or User — As referenced in lower case letters means any person, firm, or corporation legally responsible for the safe operation of any pressure-retaining item.

Owner-User Inspection Organization — An owner or user of pressure-retaining items that maintains an established inspection program, whose organization and inspection procedures meet the requirements of the National Board rules and are acceptable to the jurisdiction or jurisdictional authority wherein the owner or user is located.

Owner-User Inspector — An individual who holds a valid and current National Board Owner-User Commission.

Piecing — A repair method used to remove and replace a portion of piping or tubing material with a suitable material and installation procedure.

Pneumatic Test — A pressure test which uses air or another compressible gas as the test medium.

Potable Water Heaters — A corrosion resistant appliance that includes the controls and safety devices to supply potable hot water at pressure not exceeding 160 psig (1,100 kPa) and temperature not in excess of 210°F (99°C).

Fired Storage Water Heater — A potable water heater in which water is heated by electricity, the combustion of solid, liquid, or gaseous fuels and stores water within the same appliance.

Indirect Fired Water Heater — A potable water heater in which water is heated by an internal coil or heat exchanger that receives its heat from an external source. Indirect fired water heaters provide water directly to the system or store water within the same appliance.

Circulating Water Heater — A potable water heater which furnishes water directly to the system or to a separate storage tank. Circulating water heaters may be either natural or forced flow.

Pressure-Retaining Items (PRI) — Any boiler, pressure vessel, piping, or material used for the containment of pressure, either internal or external. The pressure may be obtained from an external source, or by the application of heat from a direct source, or any combination thereof.

Pressure Test — A test that is conducted using a fluid (liquid or gas) contained inside a pressure-retaining item.

Pressure Vessel — A pressure vessel is a container other than a boiler or piping used for the containment of pressure.

"R" Certificate Holder — An organization in possession of a valid "R" *Certificate of Authorization* issued by the National Board.

Re-ending — A method used to join original code of construction piping or tubing with replacement piping or tubing material for the purpose of restoring a required dimension, configuration or pressure-retaining capacity.

Repair — The work necessary to restore pressure-retaining items to a safe and satisfactory operating condition.

Re-rating — See alteration.

Safe Point of Discharge — A location that will not cause property damage, equipment damage, or create a health or safety threat to personnel in the event of discharge.

Safety Relief Valves — A safety relief valve is a pressure relief valve characterized by rapid opening or pop action, or by opening in proportion to the increase in pressure over the opening pressure, depending on application.

Seal Weld — Any weld designed primarily to provide a specific degree of tightness against leakage. A seal weld is not intended to provide structural integrity to a pressure retaining item. (15)

Settings — Those components and accessories required to provide support for the component during operation and during any related maintenance activity.

Shop — A permanent location, the address that is shown on the *Certificate of Authorization*, from which a Certificate Holder controls the repair and/or alteration of pressure-retaining items.

Suspension Burner — A combustion system in which the fuel is in the form of relatively small particles, Their buoyancy is maintained in the transport airstream and the fuel/air mixture flow stream, until combustion is completed.

Testing Laboratory — National Board accepted laboratory that performs functional and capacity tests of pressure relief devices.

Thermal Fluid Heater — A thermal fluid heater is a closed vessel in which a fluid other than water is heated by the direct application of heat from a thermal energy source. Depending on the process heating requirements, the fluid may be vaporized with normal circulation but, more often, the fluid is heated and circulated by a pump.

Transient — An occurrence that is maintained only for a short interval as opposed to a steady state condition.

Underfire Air — A method of introducing air beneath the grate surface/fuel bed.

"VR" Certificate Holder — An organization in possession of a valid "VR" *Certificate of Authorization* issued by the National Board.

Velocity Distortion — The pressure decrease that occurs when fluid flows past the opening of a pressure sensing line. This is a distortion of the pressure that would be measured under the same conditions for a non or slowly moving fluid.

Water Head — The pressure adjustment that must be taken into account due to the weight of test media (in this case, water) that is 0.433 psi/ft (10 kPa/m) added (subtracted) from the gage pressure for each foot the gage is below (above) the point at which the pressure is to be measured.

PART 2, SECTION 10
INSPECTION — NBIC APPROVED INTERPRETATIONS

10.1 SCOPE

a) This section provides a list of all approved interpretations for previous editions and addenda of the NBIC. A complete list of interpretations including approved interpretations for this edition is provided on the National Board website.

b) Each interpretation references the edition and addenda applicable to the committee response and approval. Use of interpretations, for other than the approved edition and addenda, may not be appropriate for reference.

c) Technical inquiries (also known as "request for interpretation") may be submitted to the NBIC committee to clarify the meaning or intent of existing rules to the NBIC. The requirements for submitting technical inquiries are described in NBIC Parts 1, 2, and 3 (Section 8), Preparation of Technical Inquiries to the NBIC Committee.

2013 INTERPRETATIONS

Interpretation	Edition	Part	Section	Subject
13-04	2013	3	3.3.2 e)	Seal Welding of Inspection Opening Covers
13-03	2011	3	3.3.2 d) 1)	Standard Threaded Fitting Welded through ASME VIII, Div. 1 Vessel
13-02	2011	3	5.7.5	Stamping Requirements for Alterations
13-01	2013	3	1.8.5 q)	Personnel Qualified IAW ANSI/ASME N45.2.23

2011 INTERPRETATIONS

Interpretation	Edition	Part	Section	Subject
11-06	2011	3	3.2.5	Calculations / Start of Work
11-05	2011	2	5.2.2 – 5.2.3	Replacement of Stamped Data on Corrugator Rolls
11-04	2011	3	1.7	Application of "VR" Stamp
11-03	2011	2	2.5.8	Test Frequencies
11-02	2011	3	4.4.2 a)	Liquid Pressure Test Requirements
11-01	2011	3	3.3.2	Routine Repair Considerations

2007 INTERPRETATIONS

Interpretation	Edition	Addenda	Part	Section	Subject
07-16	2007		3	3.3.5.2	Requirement for Repair / Alteration Plan
07-15	2007	2008	2	S2.10.6	Average Pitch
07-14	2007	2009	3	3.3.3	Replacement of Pressure Retaining Parts
07-13	2007	2009	All		The Original Code of Construction
07-12	2007	2009	3	3.4.3	Replacement of Heads with Different Types

2007 INTERPRETATIONS

Interpretation	Edition	Addenda	Part	Section	Subject
07-11	2007	2010	3	3.2.2 a)	Replacement Parts
07-10	2007	2009	3	3.3.2–3.3.3	Routine Repairs
07-09	2007	2008	2	S2.9 b) & S2.11 b) 7) b)	Schedule 80 Pipe in External Piping
07-08	2007	2009	3	3.4.3 c)	Handhole Replacement with Flush Patch
07-07	2007	2009	3	3.3.4.3 e) & 3.3.2 d) 3)	Weld Buildup of Wasted Area / Routine Repair
07-06	2007		3		Replacement Parts for Repairs and Alterations
07-05	2007	2008	1	2.9.5.1 c)	Change-Over Valve Permitted in ASME Code Case-2254 Use
07-04	2007		1	4.5.1 a)	Installation of New Rupture Disc in an Existing Holder
07-03	2007		3	2.5.3	Use of Alternative Welding Method 2 on P-No 4 and P-No 5A Base Material
07-02	2007		3	1.6.2, 1.7.5.4, & 1.8.2	NBIC Manual Requirements for “R”, “VR”, and “NR” Stamp Holders
07-01	2004	2006		RB-8400 & RB-8410	“Try Testing” of Pressure Relief Valves

2004 INTERPRETATIONS

Interpretation	Edition	Addenda	Section	Subject
04-23	2004	2005	RC-1110, RC-2050(c), RC-3030(c), & RC-3031(e)	Jurisdictional Acceptance of NDE
04-22	2004		RC-1130	Inspector Verification of NDE Performed
04-21	2004	2005	RC-1130	Inspector Involvement in NDE in Lieu of Pressure Test
04-20	2004	2005	RC-2051(d) & RC-3031(b)	Pneumatic Test in Lieu of Liquid Pressure Test
04-19	2004	2005	RD-2020	Repair of Threaded Bolt Holes
04-18	2004	2005	RD-3010	Re-rating Using a Later Edition/Addenda of The Original Code of Construction
04-17	2001	2003	RD-2020(c)	Procedures for Repairing Cracks and Crack Classification
04-16	2004		RA-2370	“NR” Certificate Interface with Owner’s Repair/Replacement Program
04-15	2004		RD-2060	Utilizing a Flush Patch to Gain Access Window in Pressure Retaining Items
04-14	2004		RC-1000 & RC-3000	Replacement Safety Valves with Different Capacities and Set Pressures than Boiler Data Report

2004 INTERPRETATIONS

Interpretation	Edition	Addenda	Section	Subject
04-13	2004		RC-1020, RC-1030, Appendix 4, & RC-3022	Replacement of a Cast Iron Section
04-12	2001	2003	RD-1030, RC-1050(c)	Post Weld Heat Treatment of Parts
04-11	2001	2003	RC-1050(c), RC-2050, & RC-2051	Requirements for Testing Replacement Parts
04-10	2004		RC-2031	Flush Patches in Pipes and Tubes NPS 5 or less
04-09	2004		RC-2031	Routine Repairs
04-08	2004		RE-1050	Fabricated Replacement Critical Parts
04-07	2004		RE-1050	Source for Critical Parts
04-06	2004		RC-1050(c), RC-2050, RC-2051, & RC-1110	Written Procedure Requirements for Non-Destructive Examinations
04-05	2001	2003	RC-1050(c) & RC-2050	"R" Stamp Holder Installation of Code Manufacturer Supplied Parts
04-04	2004		RC-3022(b) & (d)	Re-rating of Pressure-Retaining Items for Lethal Service/Removal of Insulation
04-03	2004		RC-3022(b) & (d)	Re-rating of Pressure-Retaining Items/Removal of Insulation
04-02	2004		RA-2213	"VR" Certificate Holder Verification of Manufacturer's Nameplate Capacity
04-01	2004		RD	Use of Welded Encapsulation Box in Lieu of Weld Build Up or Flush Patch

2001 INTERPRETATIONS

Interpretation	Edition	Addenda	Section	Subject
01-41	2001	2003	Appendix 2 & 5	Alteration Increasing Boiler Heating Surface & Stamping
01-40	2001	2003	RC-2051(e), RC-3031(c), RC-2050, & RC-3030(c)	Use of VT when Pressure Test Is Not Practicable
01-39	2001	2003	RC-3051	Inspector Responsibilities for Form R-2 after Witnessing Pressure Test
01-38	2001	2003	RD-3022(d)	Design Only "R" Stamp Holders Pressure Testing and Form R-2
01-37	2001	2003	RC-1140 & RC-3040	Construction Phase & Stamping when Re-rating without Physical Changes
01-36	2001	2002	RC-1020(b)	Application of "R" Stamp on Non-Code Pressure Retaining Items
01-35	2001	2002	RC-1040	Is Pre-Assembly of a Part Considered Fabrication
01-34	2001	2002	RD-1060(h)(2)	Butter Layers Using the SMAW Process
01-34	2001	2002	RD-1040(i)(6)	Shielding Gas Dewpoint Temperature

2001 INTERPRETATIONS

Interpretation	Edition	Addenda	Section	Subject
01-33	2001	2002	UG-45	Evaluation of Inservice Pressure Vessels and Requirement of UG-45
01-32	2001	2002	Introduction	Are Reference Codes and Standards Acceptable
01-31	2001	2002	RB-3238	Determination of Remaining Life Applicable to Boilers and Pressure Vessels
01-30	2001	2002	RC-1050(c)	Fabrication and Installation by “R” Stamp Holder
01-29	2001	2002	RC-2070	Installation of Replacement Parts
01-28	2001	2002	RC-1040	Use of Material That Has Been Previously Inservice
01-27	2001	2002	RC-1090	Welding Using Welders Who Are Not Employed by the “R” Stamp Holder
01-26	2001	2002	RB-3238(f)	Criteria for Determining Actual Thickness and Maximum Deterioration
01-25	2001		RC-3050	Documenting Alterations Performed by Two “R” Stamp Organizations
01-24	2001		RC-1110(a)	NDE of Tack Welds by Welders and Welder Operators
01-23	2001		RC-2031(a)(1)	Routine Repairs
01-22	2001		RC-2031	Routine Repairs
01-21	2001		Appendix 6, Part B	Alternative Welding Methods in Lieu of Post Weld Heat Treatment
01-20	2001		RC-2031(a)(1)	Routine Repairs
01-19	2001		RC-2031(a)(1)	Routine Repairs
01-18	2001		8-5000(b)	Repairs
01-17	2001		RC-3021	Calculations
01-16	2001		RC-3000	Alterations to ASME Section VIII, Div. 2 Vessels
01-15	2001		RC-2051	Pressure Test Repairs and Alterations by Isolating the Repaired Portion of a Pressure Retaining Item
01-14	2001		RC-2082(b)	Repair Plan (Sec. VIII, Div. 2) AIA Acceptance
01-13	2001		RB-4010	Replacement of Stamped Data
01-12	2001		RA-2274	Use of Owner/User Personnel during Repairs of Pressure Relief Valves
01-11	2001		RC-3022	Re-rating Based on Joint Efficiency
01-10	1998	2000	RD-1000	Alternative Postweld Heat Treatment Methods
01-09	1998	2000	RC-2031(a)(1)	Routine Repairs

2001 INTERPRETATIONS

Interpretation	Edition	Addenda	Section	Subject
01-08	1998	2000	RB-3853	Manually Operated Locking Devices
01-07	1998	2000	RA-2030(a)	Owner-User Inspection Organizations
01-06	1998	2000	RA-2010	Accreditation of Repair Organizations
01-05	1998	2000	RA-2330(n)	"NR" Program Audits
01-04	1998	2000	RC-2050, RC-3030, RA-2151(m)	Calibration of Pressure Gages
01-03	1998	2000	Appendix 4	Pressure Retaining Items
01-02	1998	1999	RC-2031(a)(3)	Weld Metal Build-Up
01-01	1998	1999	RA-2330(g)	Demonstration for an "NR" Certificate of Authorization

1998 INTERPRETATIONS

Interpretation	Edition	Addenda	Section	Subject
98-44	1995	1997	RC-1093	Welder Performance Qualification Using SWPS
98-43	1998	1999	Forward, Appendix 4 & Appendix 5	Alterations
98-42	1998	1999	RC-2031, RD-2030(d)	Weld Buildup of Wasted Area of Boiler Tubes
98-41	1998		RA-2330(g)	Compliance with Part RA-2330(g)
98-40	1998		RD-2070	Replacement of Threaded Stays with Welded Stays
98-39	1998	1999	R-1 & R-2 Forms	Inspector Requirements
98-38	1998	1999	RC-3031(c)	NDE in Lieu of Pressure Test
98-37	1998	1999	RC-1050(a)	Material Requirements
98-36	1998	1999	RD-2050	Original Code of Construction
98-35	1998	1999	RB-4000	Restamping or Replacement of Nameplate
98-34	1995	1996	RC-3030	Examination and Testing
98-33	1998		RC-2051	Liquid Pressure Test of Repairs
98-32	1998		RC-3022	Re-rating Using Higher Joint Efficiency
98-31	1998		RC-2031	Replacement of a Nozzle as Routine Repair
98-30	1998		Appendix 6C	Example of Alteration Due to Grinding or Machining
98-29	1998		Appendix 6	Tube Placement
98-28	1998		RC-1050(c)	Replacement Parts Fabricated by an "R" Certificate Holder
98-28	1998		Appendix 6	Pressure Retaining Replacement Items
98-28	1998		RC-1050	Definition of New Replacement Parts
98-27	1995	1996	RC-2050(b)	Pressure Test
98-27	1995	1996	RC-1050	Replacement Parts

1998 INTERPRETATIONS

Interpretation	Edition	Addenda	Section	Subject
98-26	1998		RA-2262(b)(1)	Resetting of PRV Springs per ASME Section 1, PG-72.3 or Section VIII, Div. 1, UG-126(c)
98-25	1998		RA-2262(b)(3)	Stamping on Repair Nameplate
98-24	1998		RA-2242(c)	"VR" Certificate Holders and Code Case 1923 & 1945
98-23	1995		Appendix 6, B-7	Head and Shell Thickness Limitations when Installing Nozzles
98-22	1998		RC-1010	Scope
98-21	1998		RA-2130(f)	Requirements for Applicants for "R" Certificate of Authorization
98-20	1998		RC-3022	Re-rating
98-19	1998		RB-3237	Inspection Interval
98-18	1998		RC-2031(a)(1)	Routine Repairs
98-17	1998		RA-2281	Testing Medium and Testing Equipment
98-16	1998		RA-3020	Prerequisites for Accreditation
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98-05	1995	1996	Forward	Determination of Repairs Must be Made
98-04	1995	1996	RC-2031	Routine Repairs
98-03	1995		RB-3238(f)	Interrupted Service
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95-56	1995	1996	RA-2231(b)(1)	Acceptance of Code Cases 1923 & 1945
95-55	1995	1996	RB-3550	Operational Inspection
95-54	1995	1996	RC-2050	Pressure Testing
95-53	1995		RD-2031	Routine Repairs
95-52	1995	1996	RD-2060	Patches, Figure 8
95-51	1995	1996	RC-1090	Weld Procedures/Qualified Welders
95-50	1995	1996	RC-2072 & RC-3052	R-3, R-4, & Manufacturer's Partial Data Report
95-49	1995		Appendix 6, B-17	P Numbers
95-48	1995		RC-1020, RB-1050(a) & Appendix 6, B-6	R-1 Forms
95-47	1995		RB-4020	Replacement Name Plates & National Board Numbers
95-46	1995		Appendix 6, B-7	Examples of Repairs
95-45	1995		Appendix 4	Repairs and Alterations
95-44	1995		Appendix 6, C-5	Alterations
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95-41	1995		RC-1110	Indications in Excess of that Allowed by the Original Code of Construction
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95-39	1995		RC-2050	Pressure Testing of Routine Repairs
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95-33	1995		RC-2031(a)(2)	Non-Load Bearing Attachments
95-32	1995		RC-2050	Pressure Testing
95-31	1995		RC-2031	Waiving the Inprocess Involvement of the Inspector
95-30	1995		Data Report Forms	API-510 Reporting and Inspector Involvement
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95-28	1995		RC-2031	R-1 Forms Inspector Involvement for Routine Repairs
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95-27	1995		RC-2060	Application of the "R" Symbol Stamp
95-27	1995		RC-2072	Responsibility for Performing Pressure Test
95-26	1995		RA-2262	Valve Nameplate Contents
95-25	1995		Appendix 5	Inspectors Requirements for Form R-1 on Routine Repairs
95-24	1995		Appendix 2	Nameplate Stamping and Layout
95-23	1995		RC-1010	Documentation of Repairs to Non-Symbol Stamped Cargo Vessels
95-22	1995		RC-3020 & RC-3021	Reclassification of Pressure Retaining Items
95-21	1995		Appendix 4	Repairs to PWHT Vessels Without Subsequent PWHT
95-20	1995		Foreword	Use of Earlier Edition and Addenda
95-19	1995		RC-1000	Original Code of Construction/Edition/Addenda
95-18	1992	1994	Appendix C-NR & NR-1000	Scope and Applicability
95-17	1992	1994	R-404	Documenting Repairs/Responsibility for Work Performed by Others
95-16	1992	1994	R-302.1	Owner/User Supplied Weld Procedures
95-15	1992	1994	R-307	Use of Replacement Parts/Assemblies from Other Inservice Vessels
95-14	1992	1994	R-202	Repairs to PWHT Vessels without Subsequent PWHT
95-13	1992	1994	U-106	Maximum Period between Inspection Intervals
95-12	1992	1994	U-107	Inspection of Corrosion and Other Deterioration
95-11	1992	1994	R-503	Re-rating of Complete Boilers or Pressure Vessels
95-10	1992	1994	R-301.2.2	Owner User Acceptance Inspection of Repairs and Alterations
95-09	1992	1994	Chapter III, Supplement 3	Welding Methods as an Alternative to Postweld Heat Treatment
95-08	1992	1994	Appendix C-R	Guide for Completing Form R-1
95-07	1992	1994	Appendix C-R, 3.0	Renewal of "R" Certificate of Authorization
95-06	1992	1993	R-401.2.2	Access Openings
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95-02	1992	1993	R-307	Use of R-Form When Replacing Parts with Different Materials without Welding
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94-1	1989		Chapter III	Repair of Valves Covered by B31.1
93-6	1992		Chapter III	Re-rating by Performing Radiography & Recalculating Joint Efficiency
93-5	1992		Chapter III, R-503(d)	Requirement for Pressure Test when Re-rating a Vessel
93-4	1992		Chapter III, R-301.2	Owner User Acceptance Inspection of Alterations
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93-1	1992			Requirements when More than One Inspector is Involved in a Repair
92-7	1992			Alterations with Different Certificate Holders Performing Design Calculations and Physical Work
92-6	1992			Out of State Organizations Performing Repairs
92-5	1992			Alternative Requirements of NBIC when There is No Jurisdiction
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